

# Test results of sorption-based helium-3 pump for a closed-cycle dilution refrigerator

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(2)



(3)



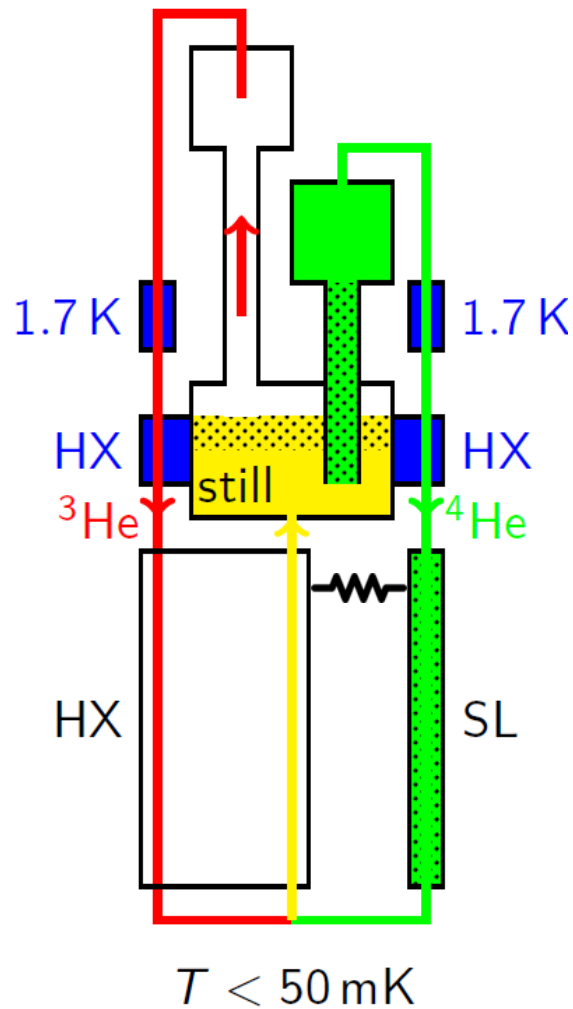
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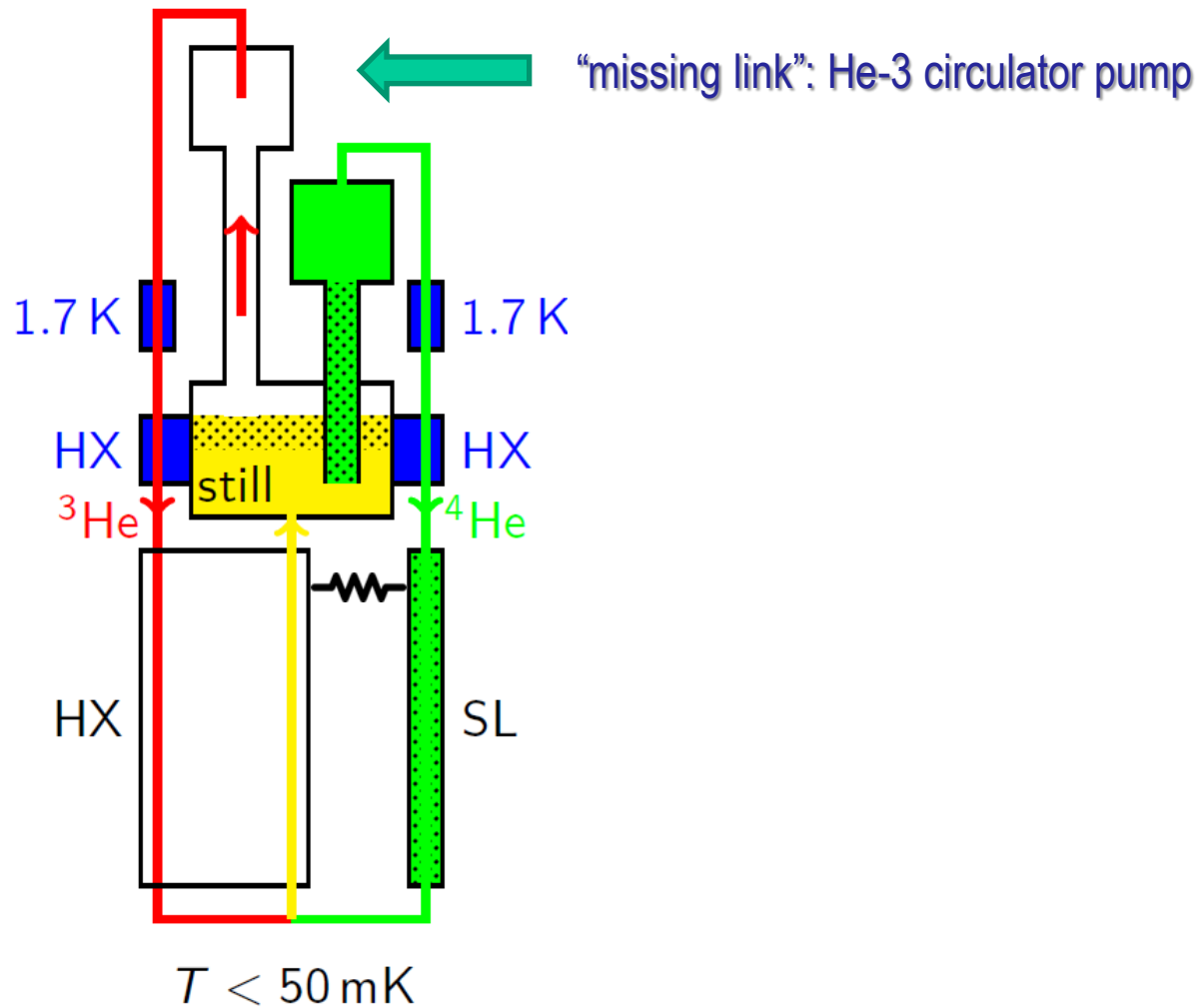
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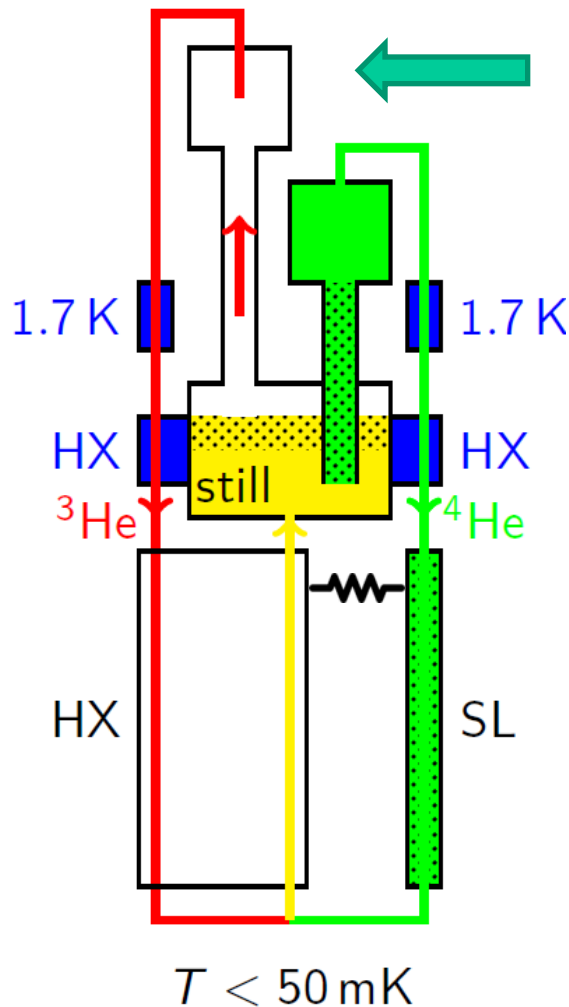
(1)



Closed-Cycle Dilution Refrigerator  
Presented by Gerard Vermeulen



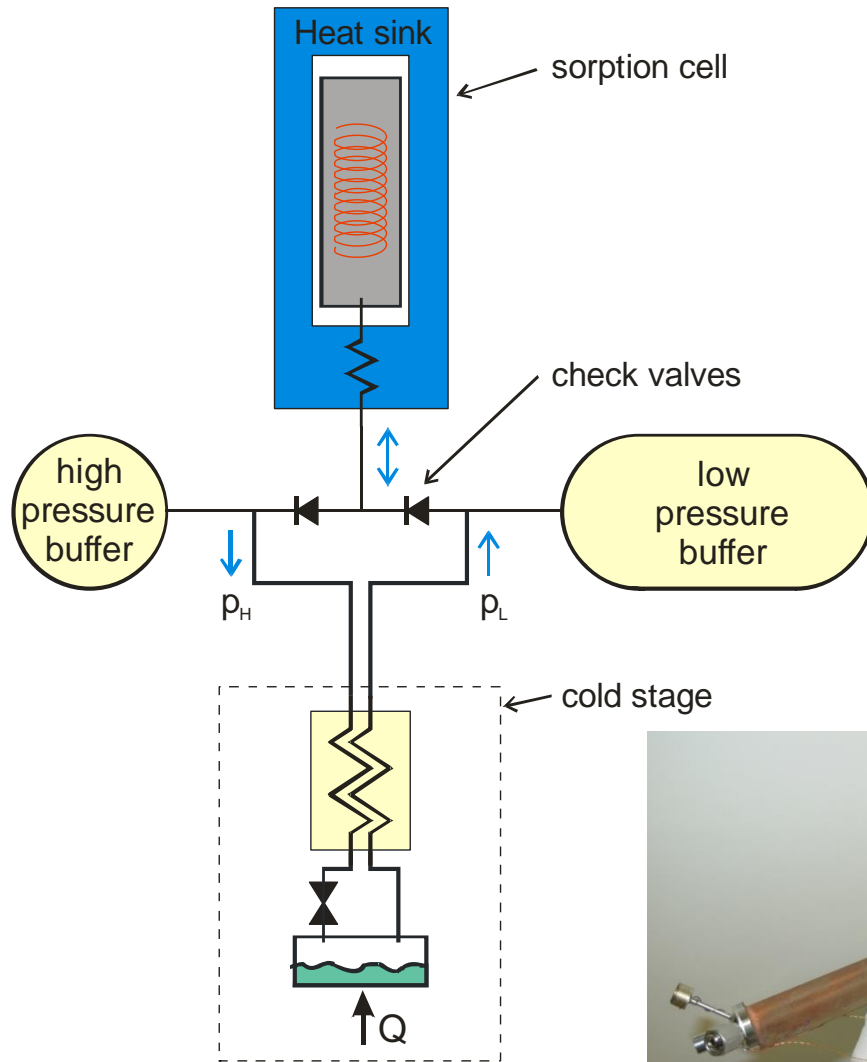
Closed-Cycle Dilution Refrigerator  
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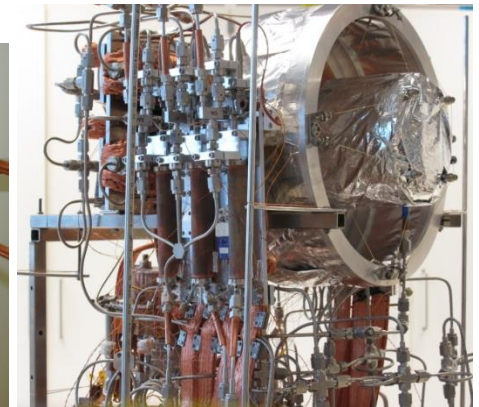
### He-3 pump requirements

Circulation rate:	10 – 30 $\mu\text{mol/s}$ (20 $\mu\text{mol/s}$ assumed in study)
Suction pressure:	5 mbar
Outlet pressure:	200 mbar
Lifetime:	5 – 10 years
Mass (incl. electronics) :	< 3 kg
Heat sink available:	100 mW at 15 K + 2 – 5 mW at 1.7 K
Max. pressure at 300 K:	20 bar
Vibration levels:	20 g
1 <sup>st</sup> resonance freq.:	> 100 Hz
Input power:	< 30 W

Closed-Cycle Dilution Refrigerator  
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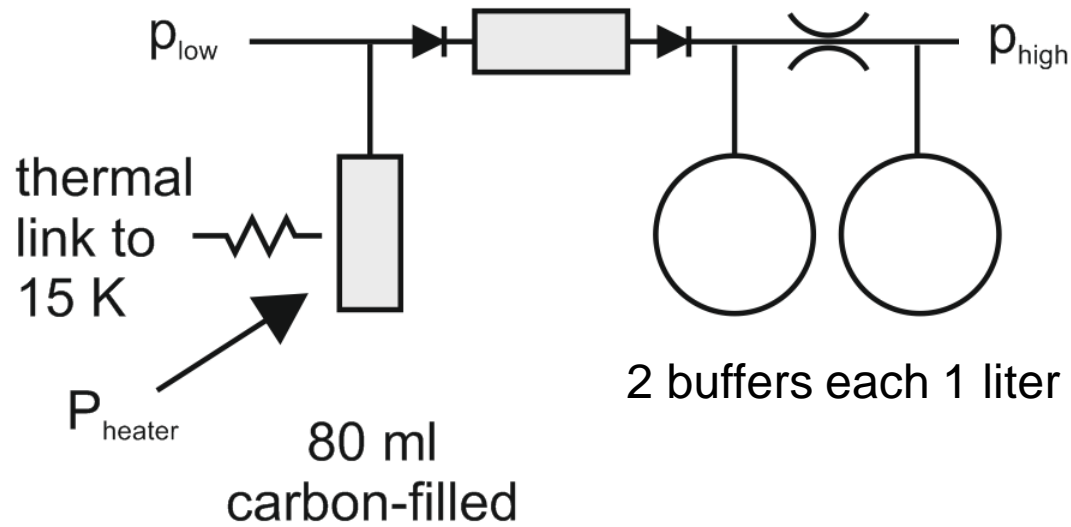


4.5 K helium cooler (CEC 2007)

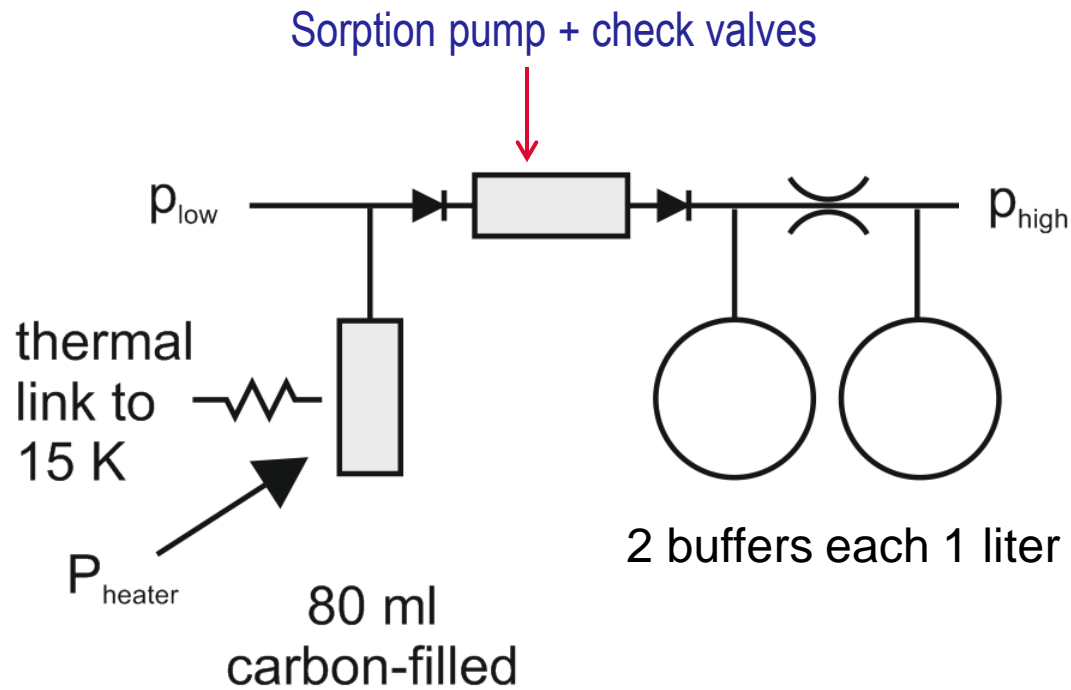


14.5 K hydrogen cooler (CEC 2013)

# Sorption-based He3 pump conceptual design

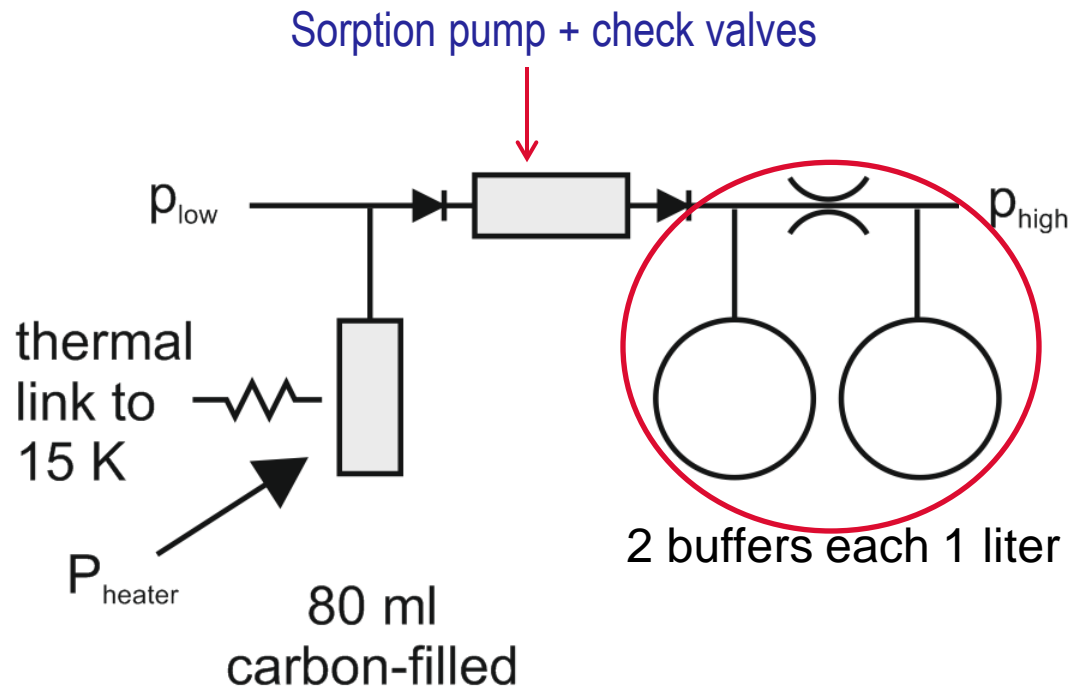


# Sorption-based He3 pump conceptual design





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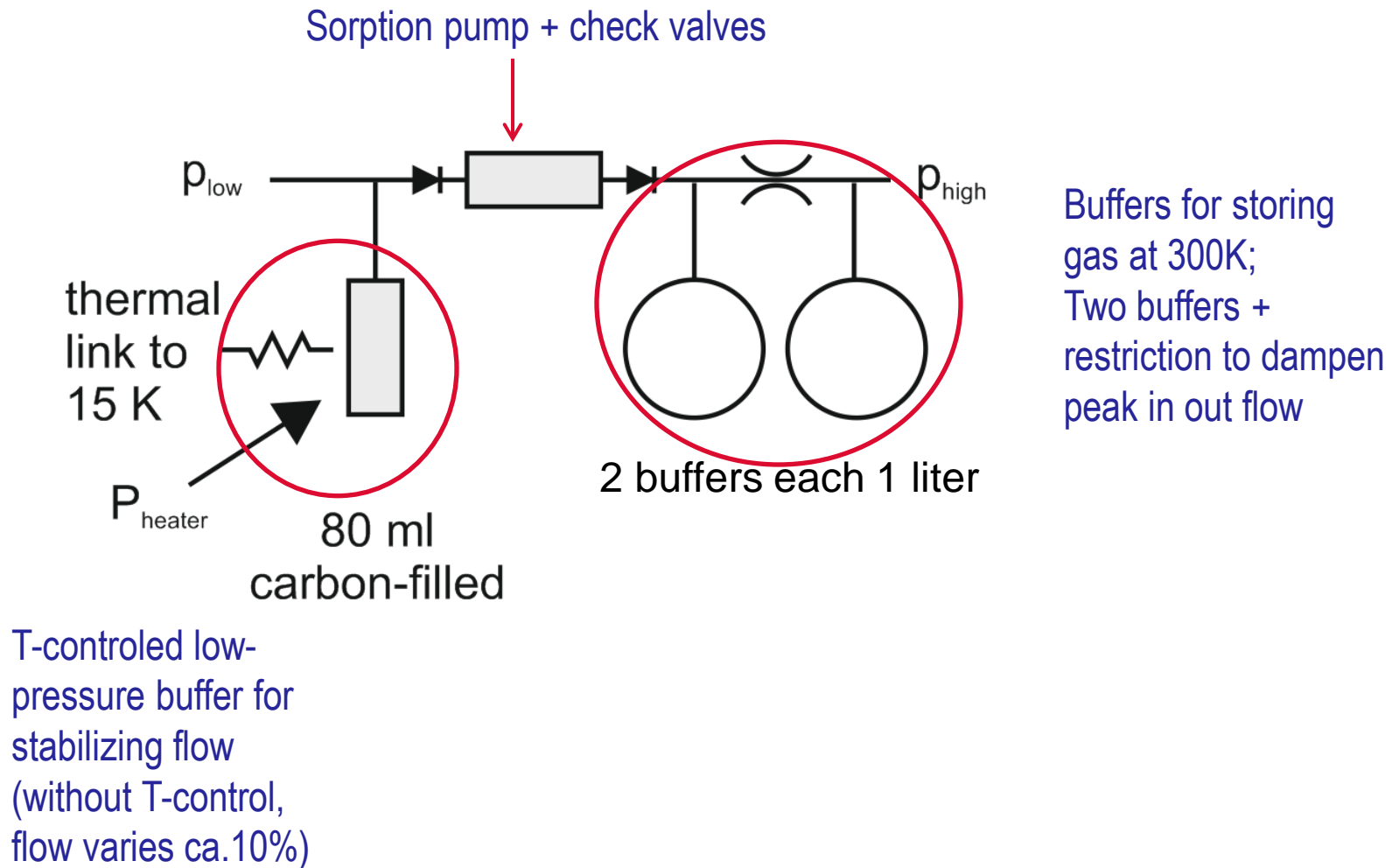


Buffers for storing gas at 300K;  
Two buffers + restriction to dampen peak in out flow

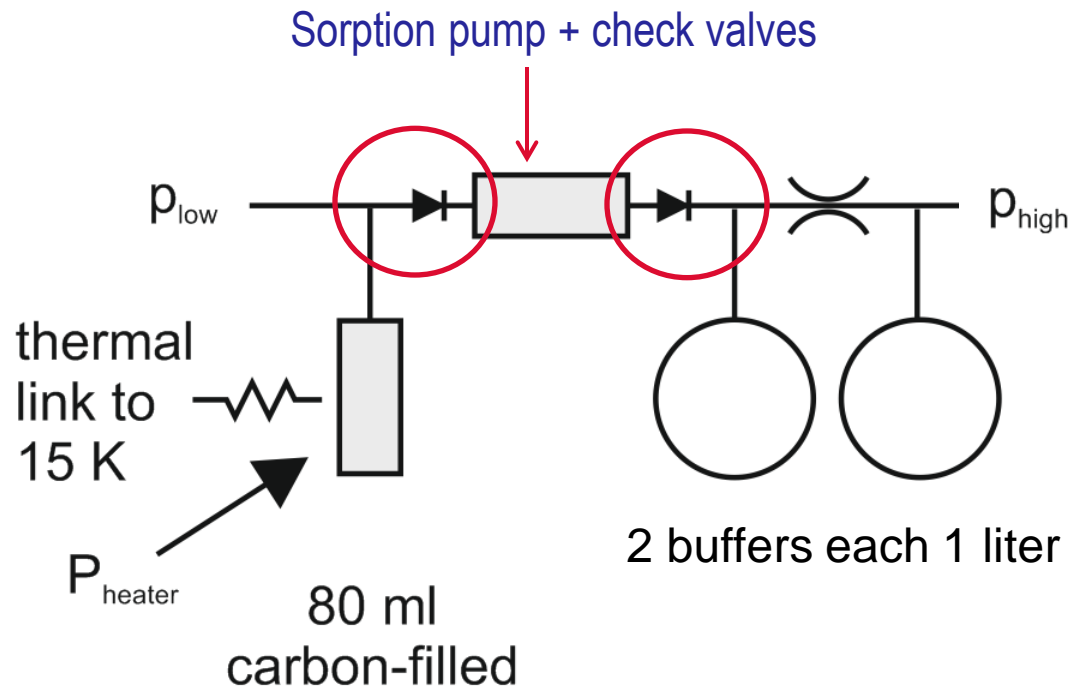
2 buffers each 1 liter



# Sorption-based He3 pump conceptual design



## Check valves: requirements



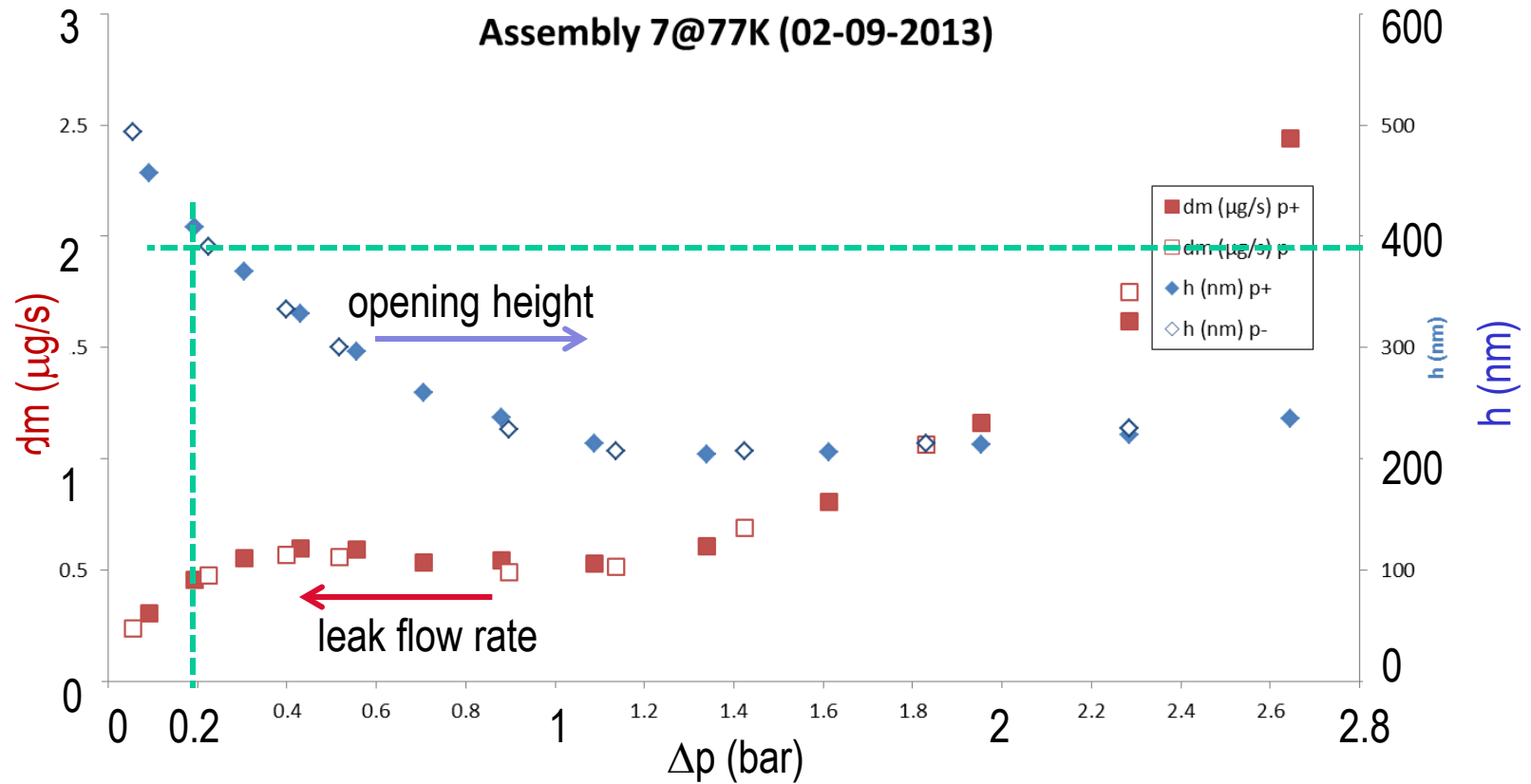
Check valves:

Forward pressure drop:  $< 0.5$  mbar (in 5 mbar suction valve)

Reverse leakage flow:  $< 1\%$  of forward flow

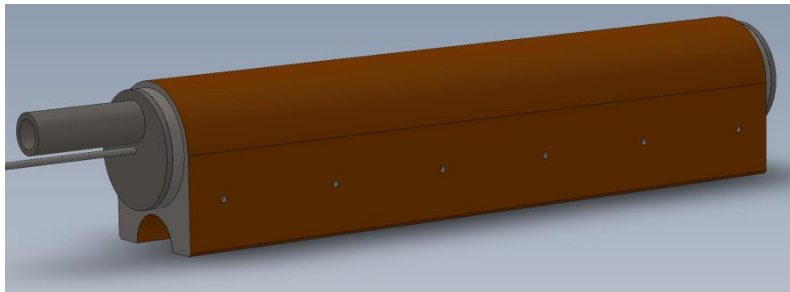
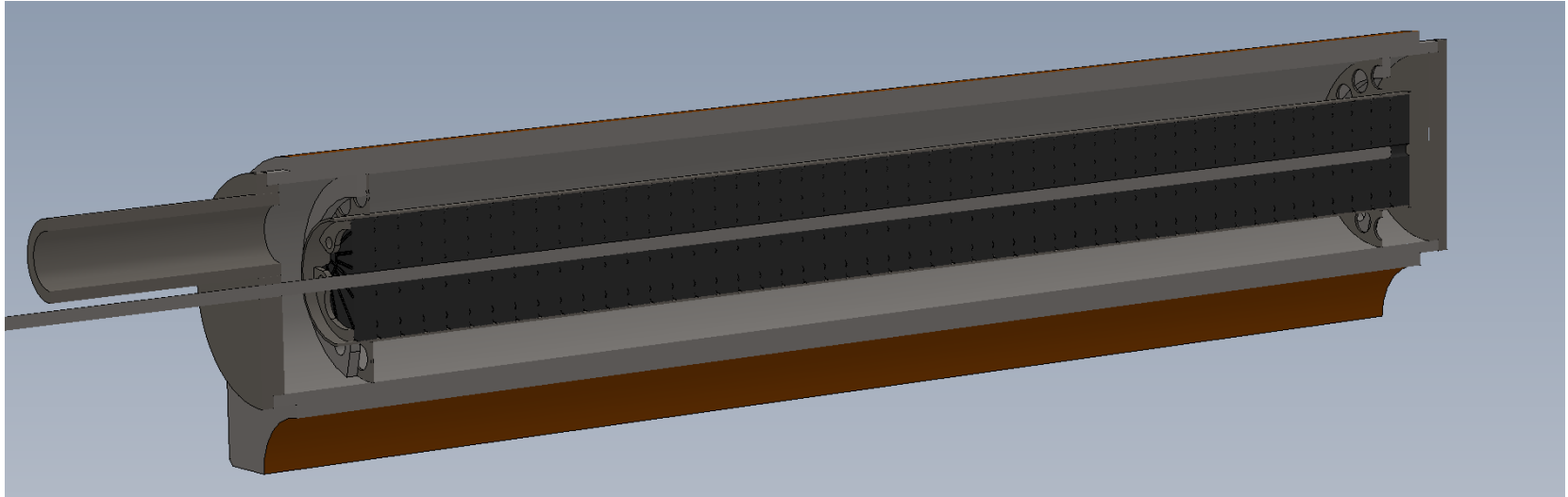


# Check valves: leak test at 77 K before (open symbols) and after shaking (closed)



Seat #	Flap #	gapheight (nm)			flowrate @ 15K (ug/s)			% forw flow (60 ug/s) @ 15K		
		min	nom	max	min	nom	max	min	nom	max
Assembly 7 @ 77K	7	204	<b>400</b>	494	0.1	<b>0.6</b>	1.1	0.2%	<b>1.0%</b>	1.8%
Assembly 9 @ 77K	8	302	<b>415</b>	445	0.3	<b>0.7</b>	0.8	0.5%	<b>1.1%</b>	1.4%
Assembly 4 @ 77K	3	293	<b>410</b>	656	0.3	<b>0.7</b>	2.5	0.4%	<b>1.1%</b>	4.1%

Carbon cell length 10 cm. Carbon pill diameter 9 mm, gap 2 mm (no gas-gap heat switch!)  
Pressure drop in cell and tubing ( $< 0.1$  mbar); spacing between carbon pills



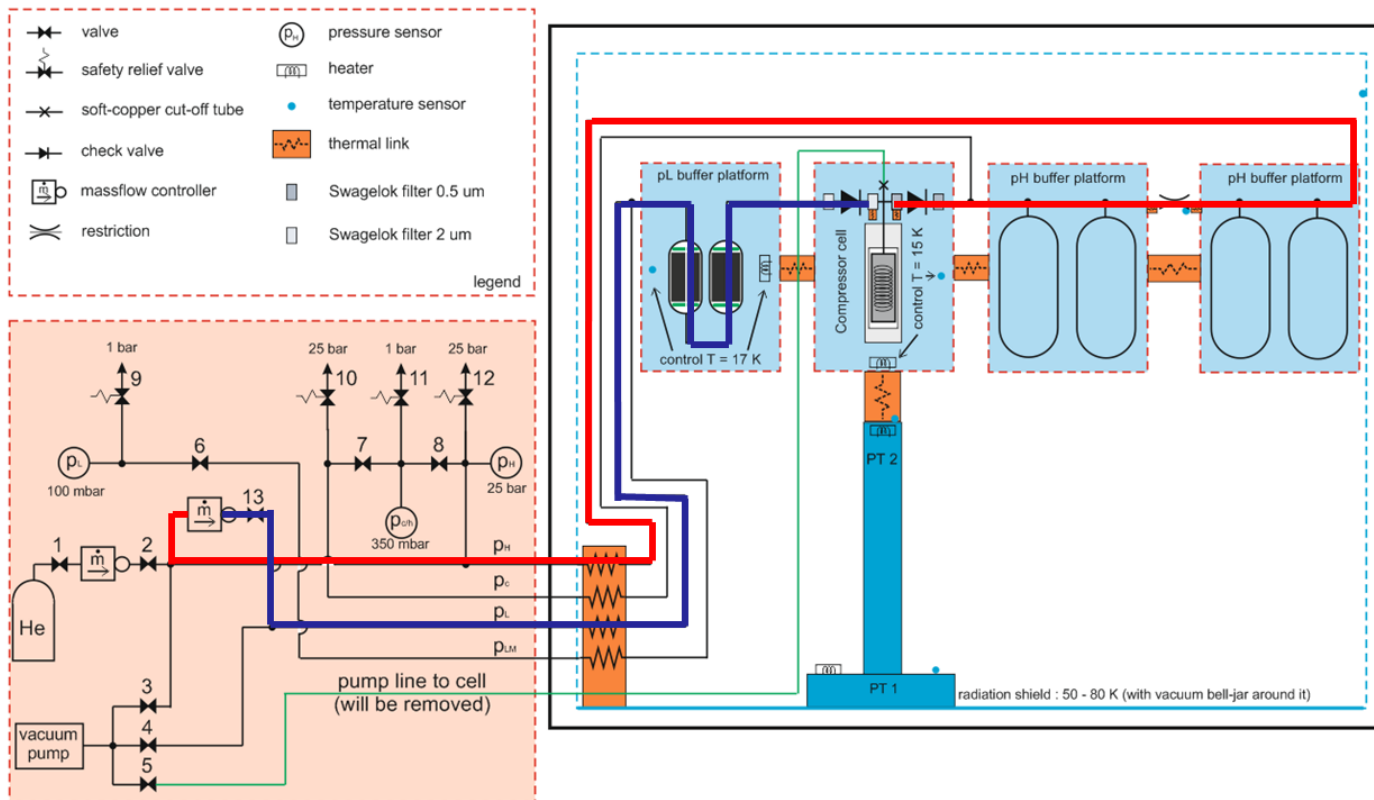
# Measurement setup

$$\dot{m} = c p_{high}$$

→ c is controlled so  $p_{high}=200\text{mBar}$  on average

Each cycle has a specific c

test experiments with He4  
(sorption characteristics  
similar to He3)



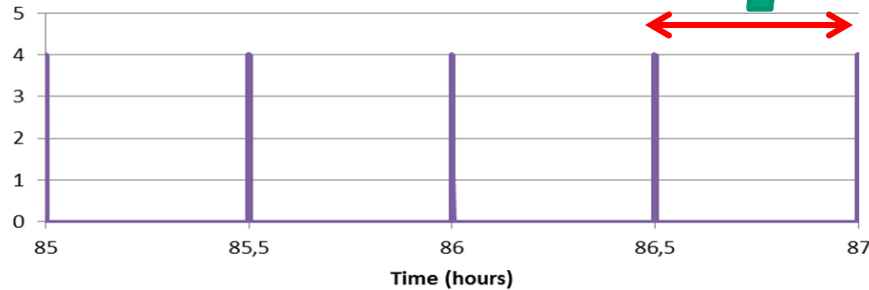
- Low pressure stabilization at 5 mbar (optional)
- Only output is mass flow
- FOM for performance is mass flow/input powers



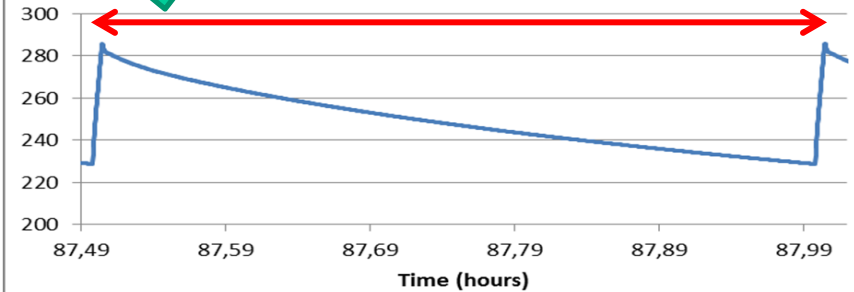
# Test results of sorption pump

## Nominal setting with control of $p_{low}$

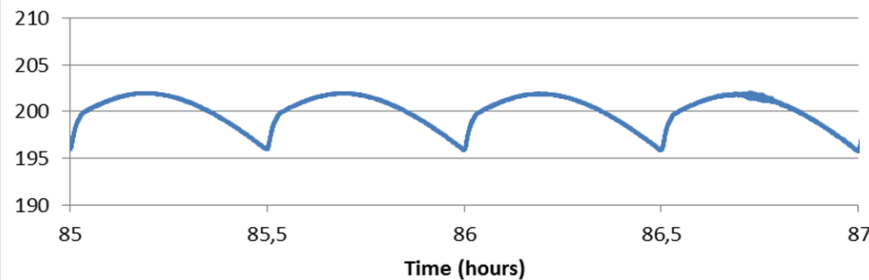
Power Compressor (W)



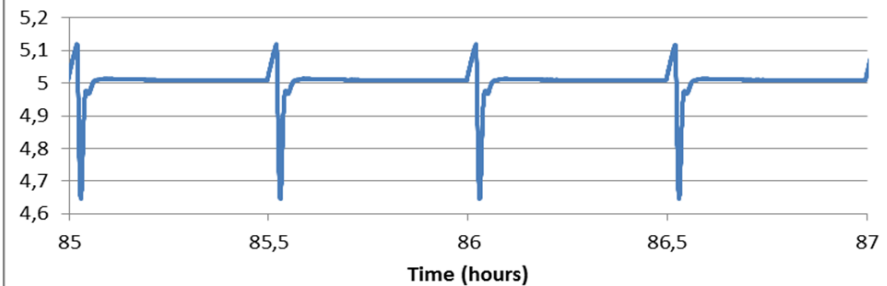
High pressure compressor side (mbar)



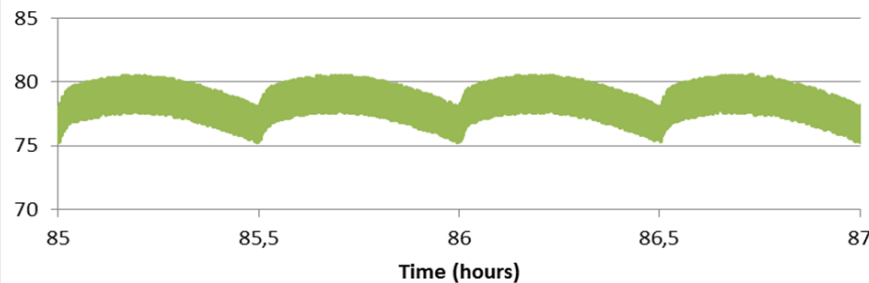
High pressure (mBar)



Low pressure (mBar)



Mass flow ( $\mu\text{g/s}$ )

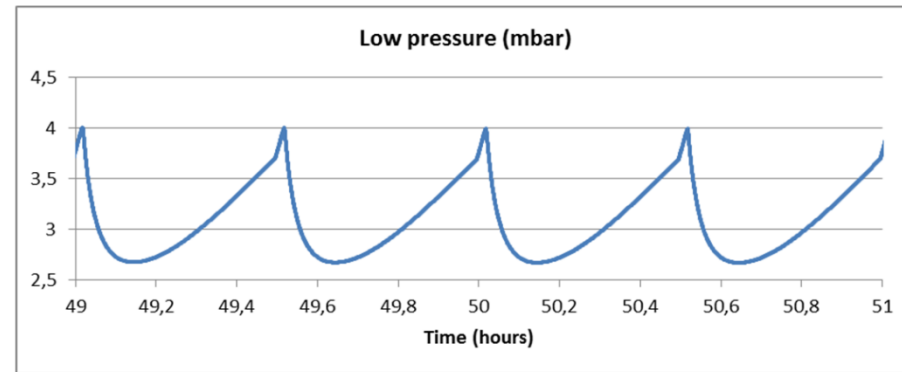
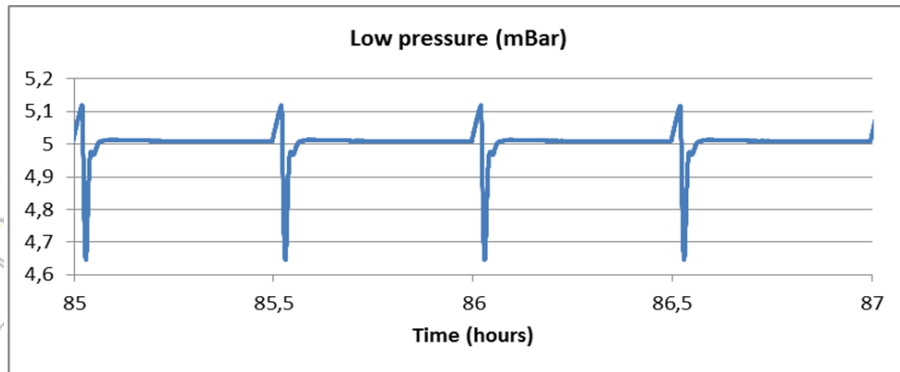


- Peak heating power = 4.0W
- Heating time = 28s
- Cycle time = 1800s
- $p_{low}$  = 5 mbar (controlled through temperature of low pressure buffer platform)
- $p_{high}$  = 200 mbar (controlled by mass flow)



# Test results of sorption pump

Yes or No....  $p_{low}$  control ??



With control:

$P_{low}$  varies 0.5 mbar

Power input doubles (60 to 120 mW)

Without control:

$P_{low}$  varies 1,3 mbar

Power input only for pump (60 mW)

	$t_{cycle}$ (s)	$t_{heat}$ (s)	$P_{w, comp}$ (W)	$p_{low}$ (mBar)	Avg mass flow ( $\mu g/s$ )	$p_{high}$ 1 (mBar)	Avg Pwr $p_{low}$ (W)	Avg Pwr total (W)	FOM tot ( $\mu g/s/W$ )	FOM comp ( $\mu g/s/W$ )	Ratio FOM tot (%)	Ratio FOM comp (%)
1. Nominal settings 1: reference	1800	28	4	5	78,4	229-286	0,059	0,121	647	1260	0%	0%
2. Nominal, no $p_{low}$ control	1800	28	4	2,7-4	72,6	238-292	0	0,062	1167	1167	+80%	-7%

What  $p_{low}$  variation is acceptable?

# Test results of sorption pump Verification matrix



ID	Requirement	Short description	Measured Value	Achieved
F1	Flow rate: 10-30 $\mu\text{mol/s}$	Measured by a Bronkhorst flow controller at room temperature using He-4.	19.6 $\mu\text{mol/s}$	✓
F2	Low pressure 5-10 mbar	Measured at room temperature by a MKS pressure transducers with a range of 100 mbar. Can be controlled to stable pressure by controlling the buffer temperature, accepting extra input power	Control at 5 mbar gives fluctuations of 4.6-5.1 mbar	✓
F3	High pressure: 200 mbar	Measured at room temperature by a UNIK 5000 pressure sensor with a range of 350 mbar and improved accuracy	200 mbar (controlled)	✓
F4	Flow stability +/- 10 %	Mass flow sensor at room temperature	75-81 $\mu\text{g/s}$ , is within 10%	✓
F5	External leak rate : $< 10^{-6}$ mbarL/s	Helium leak test	Tested and achieved	✓
F6	Outgassing: low	Design requirement		✓
S1	Life time: 5-10 years	No experiment, analysis only		✓
S2	Mass: < 3 kg	Mass measured on component level	5.9 kg mostly buffers	NA
T3a	Heat sink temperature: 15 K	Cryogenic temperature sensor in feedback loop, also higher temperatures possible.	15 K controlled	✓
T3b	Heat rejection at 15K: $\leq 100$ mW	Heater power to control low pressure buffer platform and the heater power to the compressor will be measured and added.	121 mW	close
T5	Non-operating temperature: 223-323K	Design requirement only		✓
M1	Pressure at 300 K: $\leq 20$ bar	Filling pressure will be around 12 bar and filled mass will be measured	9.0 bar	✓
M2	Vibration levels: 20g (Ariane 5 spectrum)	Design requirement, no measurements		✓
M4	Minimum pressure : 0 bar (abs)	Design requirement, intrinsically tested		✓
M5	First resonance frequency : > 100 Hz	Design requirement, no measurements		✓

### Conclusions

- Pump delivers 19.6  $\mu\text{mol/s}$  between 5 and 200 mbar
- Requirement on low-pressure stabilization is critically important
- Sensitivity analyses shows that only a higher low pressure increases pump performance (higher filling pressure)

### Future activities

- Interfacing with dilution refrigerator (requirement on  $p_{\text{low}}$ )
- Run with He-3
- Low-pressure buffer heater in the carbon (more direct control)
- Reduce peak heat load to heat-sink platform
- Analyze attainable reduction in size and mass