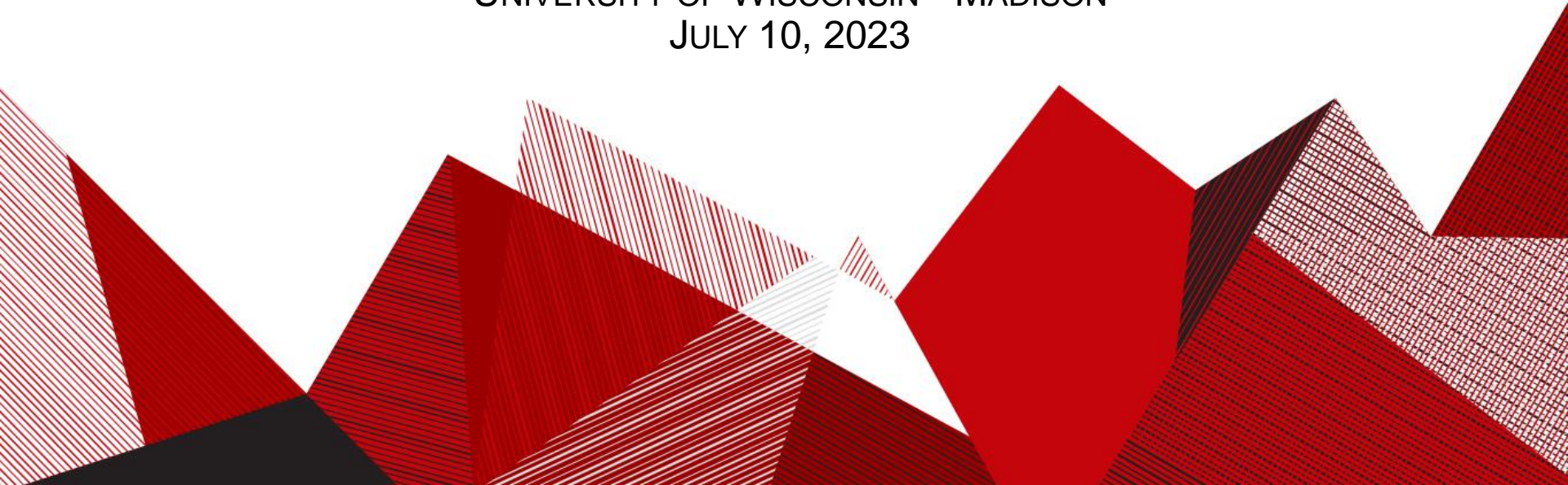





# FURTHER EXPERIMENTAL WORK IN MIXED-GAS JOULE-THOMSON CRYOCOOLING

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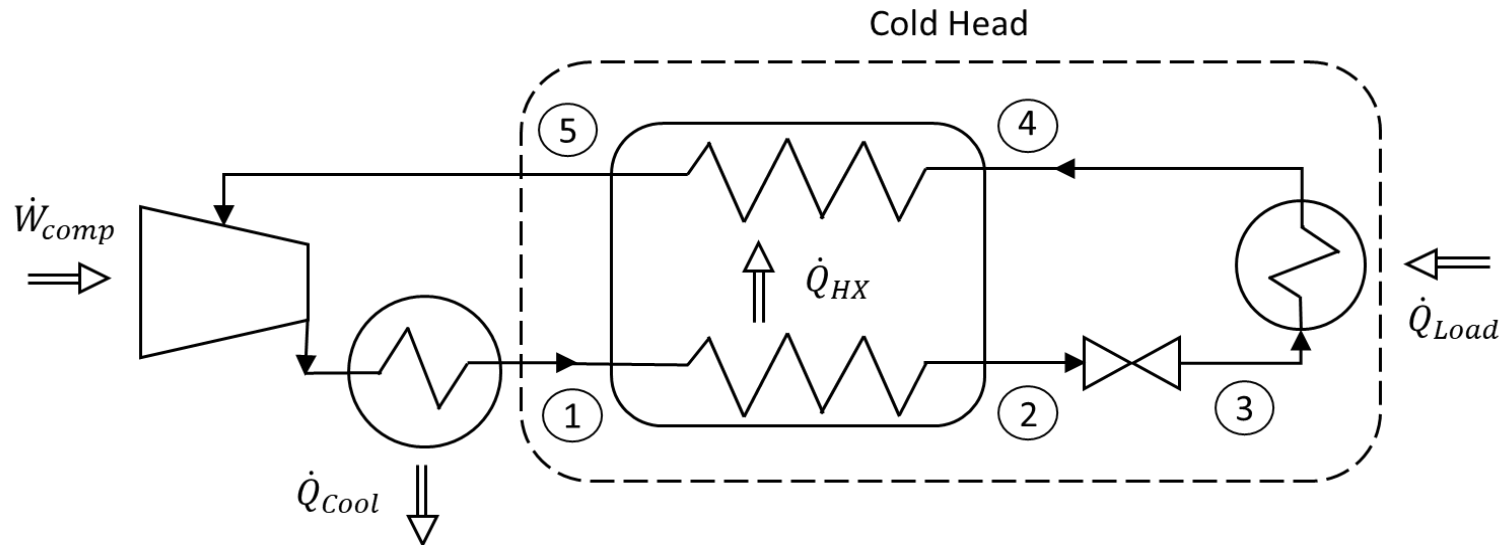


# Outline:

1. Background and Motivation
  2. Primary Objective of Research
  3. Design Considerations for the Test Section
  4. Fabrication of the Test Section
  5. Experimental Measurements and Discussion
  6. Conclusions and Future Work
- 

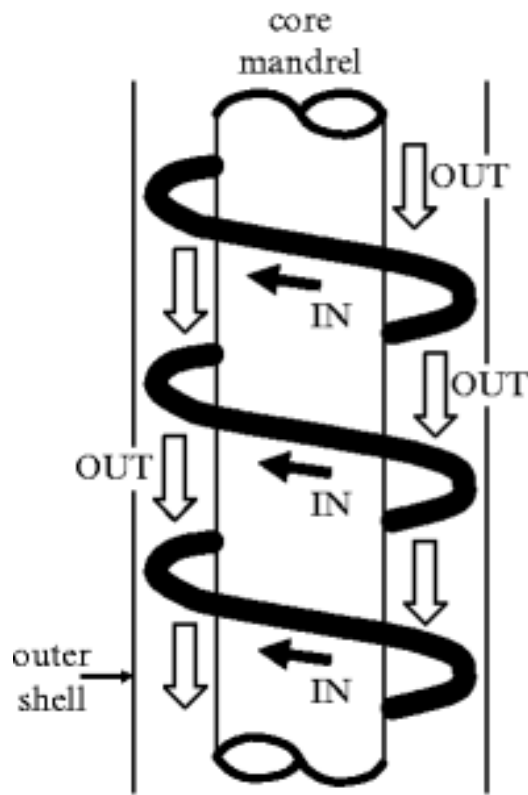
# Background and Motivation:

- Recent advances increased interest in Joule-Thomson (JT) cryocoolers with cooling potential from 125 to 150 K
- To achieve high efficiency and use a low-cost compressor, must provide cooling at low pressure ratios and values of operating pressures
- Under these conditions research has shown using a suitable mixed gas can provide greater cooling capacity than pure fluid

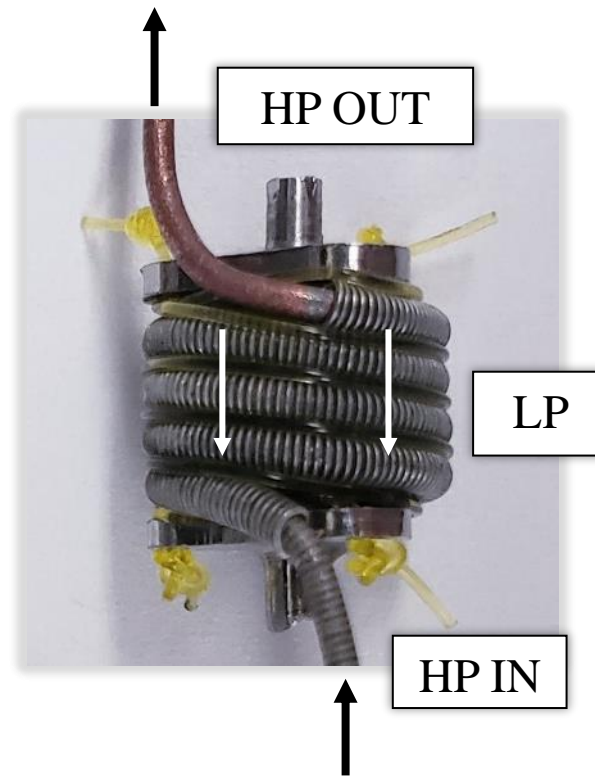


# Background and Motivation:

- Coiled Finned-tube heat exchangers are most widely used hx for miniature JT cryocoolers (also known as Giauque-Hampson hx)

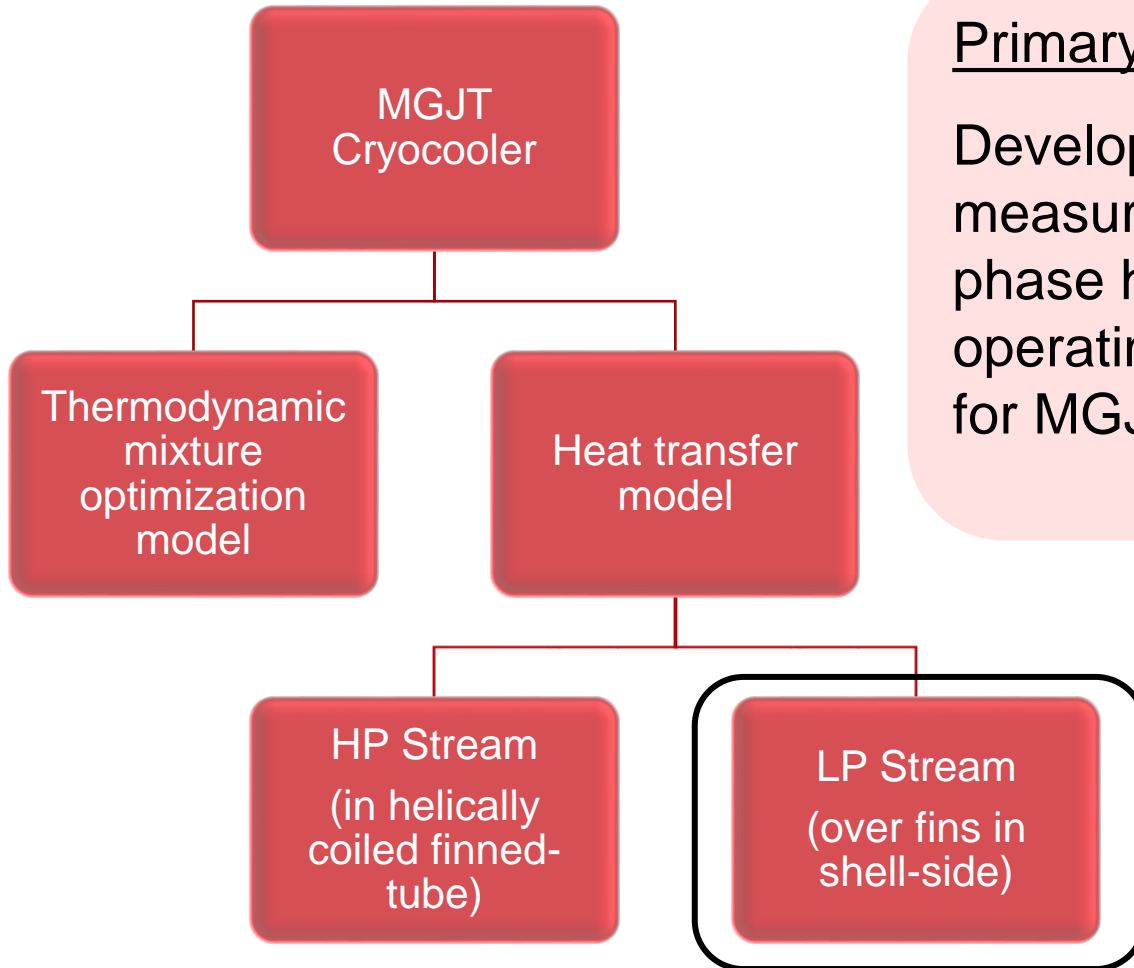


Illustration



Photo

# Background and Motivation:



## Primary research objective:

Develop test facility capable of measuring the shell-side two-phase htc for GH hx at operating conditions of interest for MGJT cryocooling

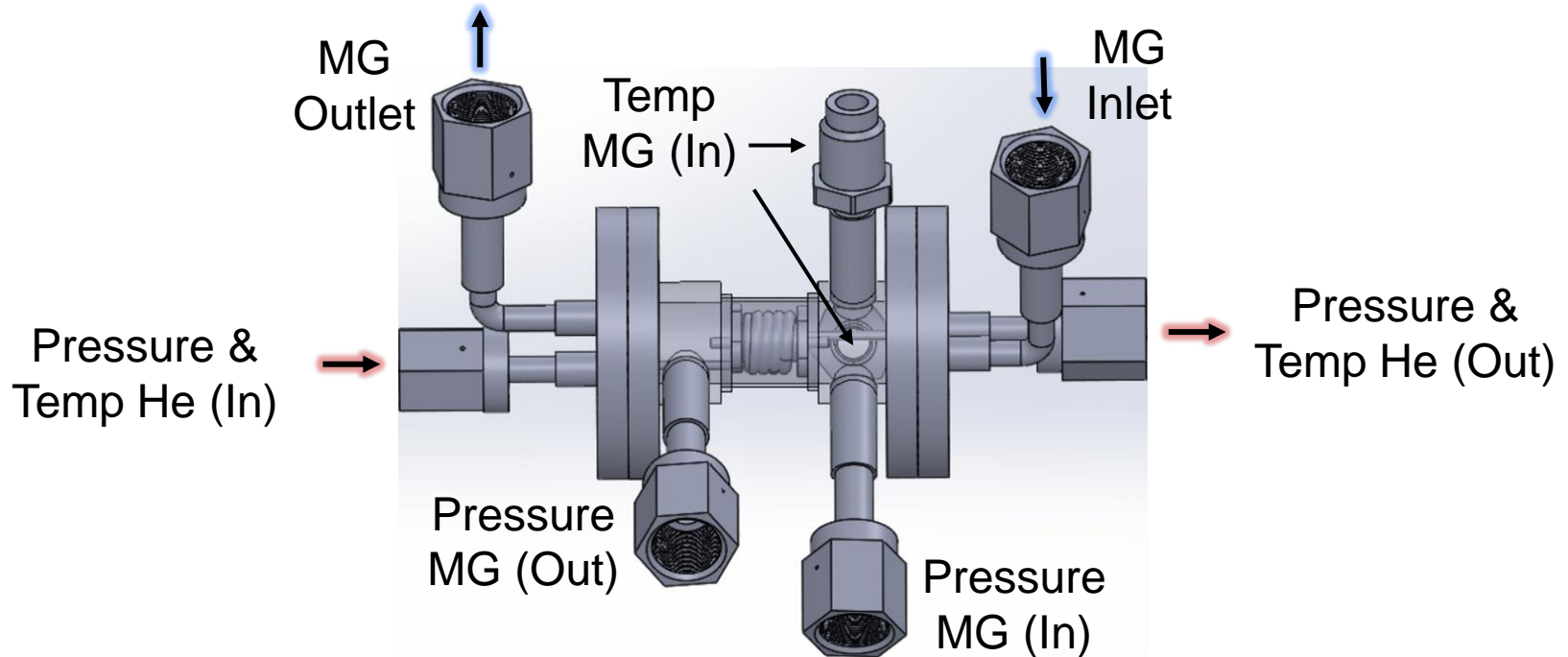
# Primary Objective of Research

- Develop test facility capable of measuring shell-side  $h_{m,g}$  of GH hx at operating conditions of interest for MGJT cryocooling

Operating Parameter	Value
Inlet temperature of MG ( $T_{in,mg}$ )	110-300 K
Mass flow rate of MG ( $\dot{m}_{mg}$ )	0.05-0.15 g/s
Inlet pressure of MG ( $P_{in,mg}$ )	345-862 kPa (50-125 psi)
Inlet pressure of He ( $P_{in,he}$ )	862 kPa (125 psia)
Operating fluid	Range of gas mixtures composed of Ar, butane, ethane, methane, R14, R23, R32 and N <sub>2</sub>

- Geometry - helically coiled finned-tube
  - 70/30 CuNi tube with  $D_i$ ,  $D_o$  and  $D_f$  of 0.49, 0.97, and 1.46 mm (0.019", 0.038" and 0.057")
  - Fin density of 3.94 fins per millimeter (100 fins per inch)

# Design Considerations for Test Section



- Heat load is applied to gas mixture via interaction with helium in coiled finned-tube
- From measurements of flow rates and inlet and outlet conditions, conductance of hx is determined
- $\bar{h}_{he}$  is well-known and  $R_{he}$  is small from experimental set-up. Therefore  $h_{mg}$  is determined from total resistance.



# Design Considerations for Test Section

## Length of Finned High-Pressure Tube

- Analysis required to understand tradeoff between the uncertainty of  $h_{mg}$  and change in quality of the mixed gas
- No correlation available to predict even the magnitude of the  $htc$  for two-phase multi-component mixture

Evaluate  $htc$  of pure fluid on shell-side in current design using Gupta et al.

Evaluate  $htc$  of pure fluid in horizontal tube with same dimensions and operating conditions as Barraza et al.

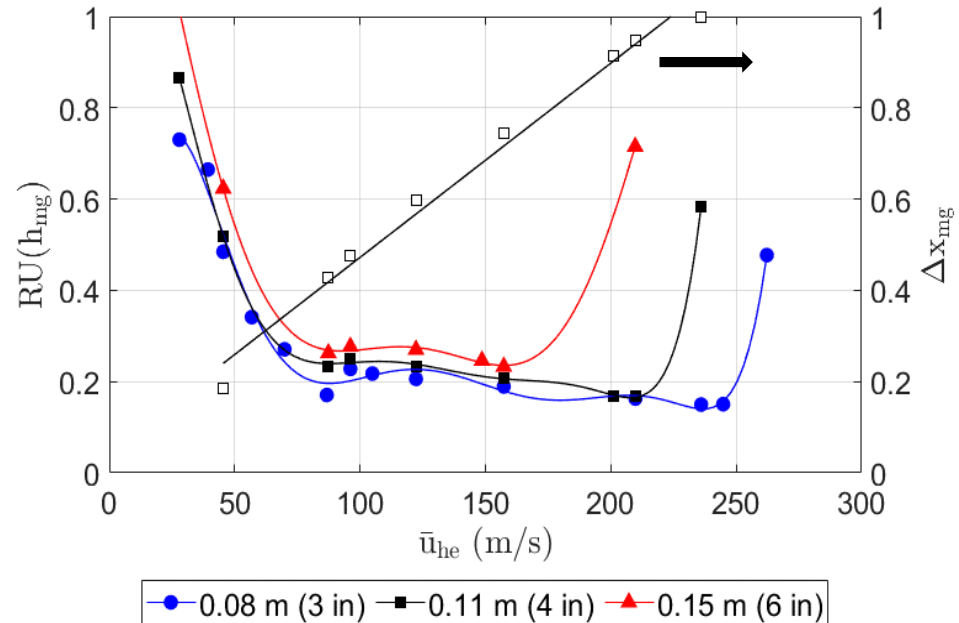
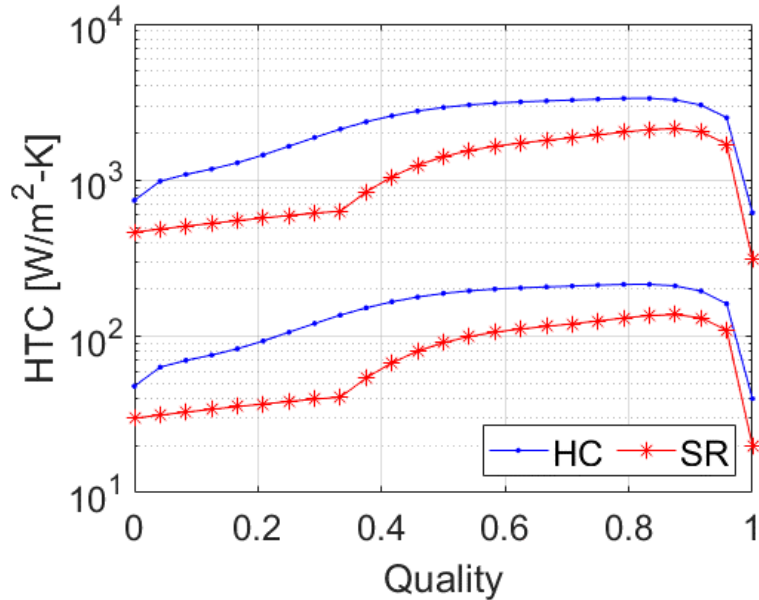
$$SF = htc_{shell} / htc_{straight\ pipe}$$

Estimate  $h_{mg}$  in shell-side of GH hx by applying SF



# Design Considerations for Test Section

## Length of Finned High-Pressure Tube



- Using SF,  $h_{mg}$  is predicted to fall between the very large range of 20 to 3000  $W/m^2-K$

- RU analyzed using greatest predicted  $h_{mg}$
- Target helium flow rate of 85  $m/s$  and length of 0.11 m (4 inch)

# Fabrication of the Test Section



Mandrel Plugs & Mandrel

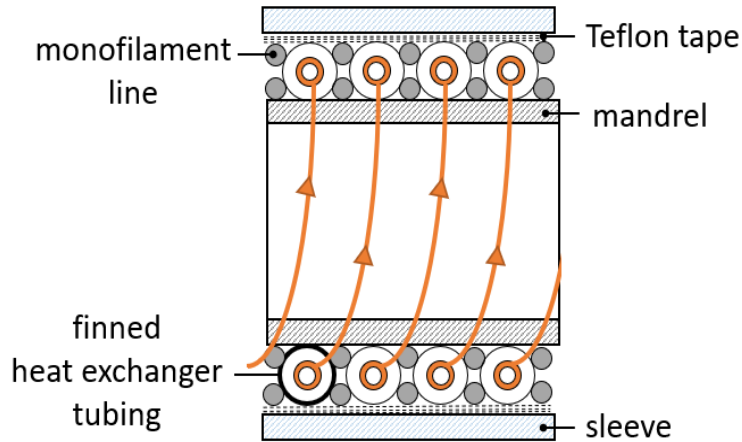


Illustration - HX Test Section

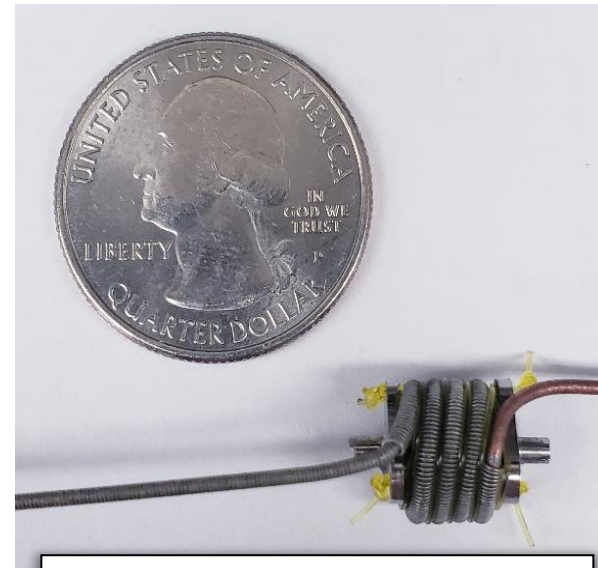
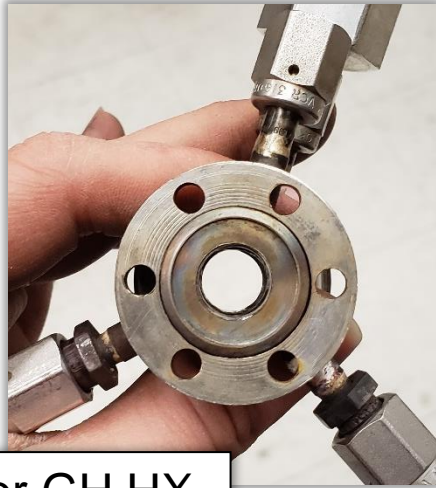


Photo - HX Test Section

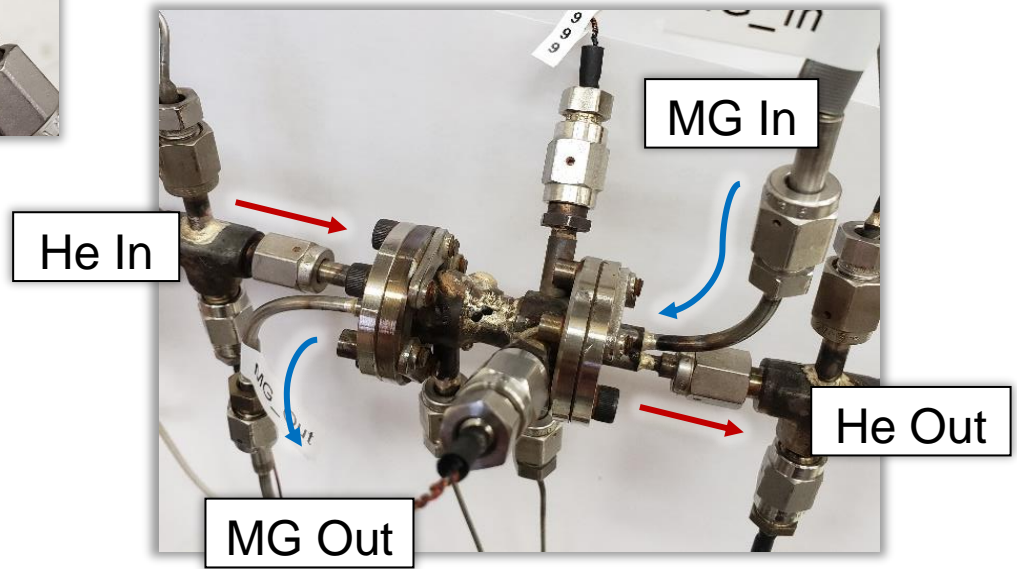
# Fabrication of the Test Section



Shell for GH HX



He Entrance/Exit



He In

MG In

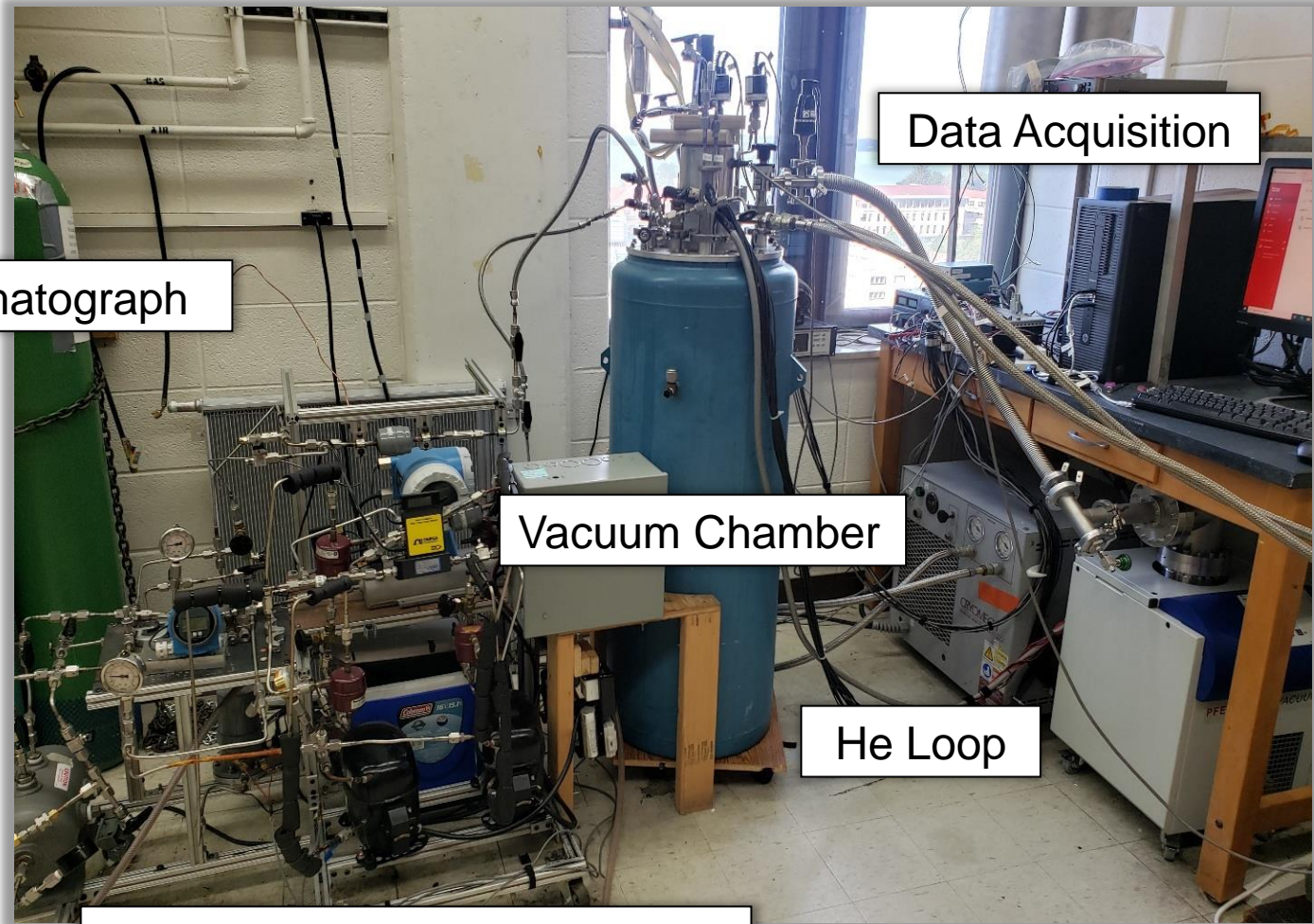
He Out

MG Out

Assembled Test Section



# Experimental Test Facility



Gas Chromatograph

Data Acquisition

Vacuum Chamber

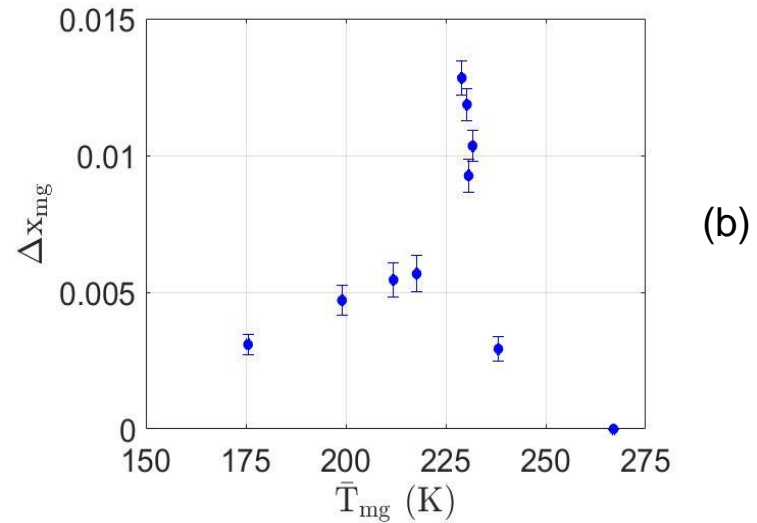
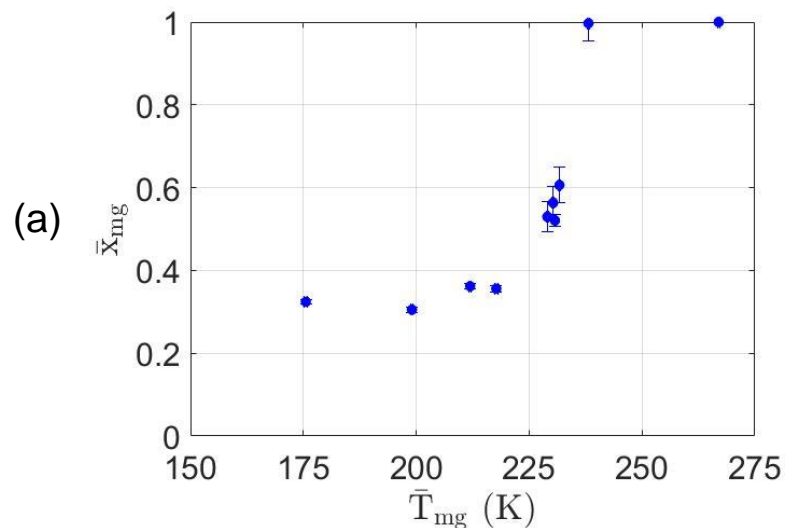
He Loop

Mixed Gas Compressor Station

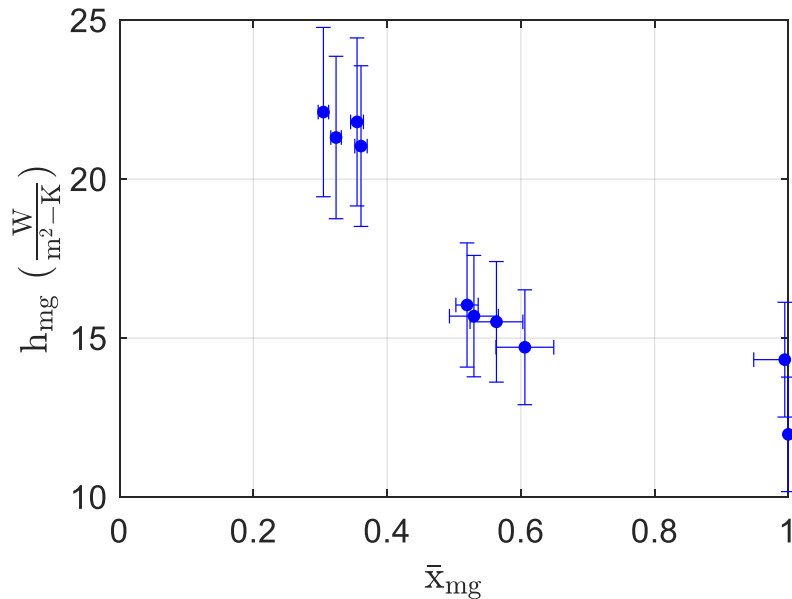
# Experimental Measurements and Discussion

## Operating Conditions -

	Parameter	Operating Range
Mixed Gas	Inlet Temperature, $T_{mg,in}$	174-267 K
	Inlet Pressure, $P_{mg,in}$	268-311 kPa (39-45 psi)
	Mass flow rate, $\dot{m}_{mg}$	0.15-0.16 g/s
	Molar fraction of R32	0.67-0.86
	Molar fraction of R14	0.33-0.14
Helium	Inlet Temperature, $T_{he,in}$	226-275 K
	Inlet Pressure, $P_{he,in}$	608-721 kPa (88-105 psi)
	Volumetric flow rate, $\dot{V}_{ref}$	0.19 L/min



# Experimental Measurements and Discussion



- Measured  $h_{mg}$  ranges from 12-22  $\text{W/m}^2\text{-K}$  with uncertainties of 12-15%
- $h_{mg}$  in two-phase region (0.32-0.61 for data collected) is increased compared to quality of 1
- Reveals that the  $h_{mg}$  may be dominant thermal resistance in hx for these flow conditions

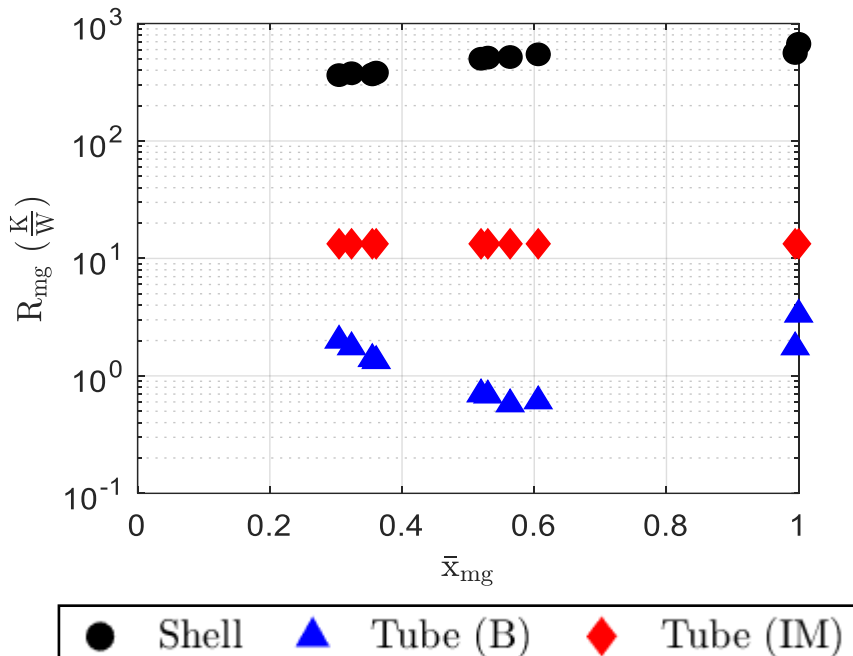
# Experimental Measurements and Discussion

Source	Correlations	Reynolds Number	Dimensions
Croft and Tebby	Single-phase pure fluid	Not reported	$D_o = 8.1 \text{ mm}$ (0.32") $h_f = 4.1 \text{ mm}$ (0.16")
Gupta et al.	Single-phase pure fluid	$500 < Re_f < 1900$	$D_o = 11 \text{ mm}$ (0.42") $h_f = 1.4 \text{ mm}$ (0.06") $D_c = 145 \text{ mm}$ (5.7")
Timmerhaus and Flynn	Single-phase pure fluid	$400 < Re_{D_h} < 10,000$	Annular-flow with helical fin from mandrel to shell
Howard et al.	Single-phase pure fluid	$100 < Re_{D_h} < 10,000$	$D_o = 10 \text{ mm}$ (0.38") $h_f = 6.4 \text{ mm}$ (0.25") $D_c = 143 \text{ mm}$ (5.7")
Test Section	Two-phase multi-component mixture	$10 < Re_{D_h} < 40$	$D_o = 1.5 \text{ mm}$ (0.04") $h_f = 0.5 \text{ mm}$ (0.01") $D_c = 7.9 \text{ mm}$ (0.31")

- Single-phase pure fluid correlations not suited for two-phase multi-component mixtures
- Reynolds number and test section dimensions are a magnitude lower



# Experimental Measurements and Discussion



- Tube (B) -  $R_{mg,t}$  estimated by SF from data of Barraza et al.  
 $h_{mg,t} \approx 2000 - 14,000 \text{ W/m}^2\text{-K}$
- Tube (IM) -  $R_{mg,t}$  estimated by 75% reduction of ideal mixture  
 $h_{mg,t} \approx 500 \text{ W/m}^2\text{-K}$

- $R_{mg,s}$  is over a magnitude larger than conservative estimate of  $R_{mg,t}$  and two magnitudes larger than estimate using Barraza et al.
- $R_{mg}$  in shell is significantly larger than in helically coiled tube

# Conclusions & Future Work

- Return stream in a GH hx is often neglected during JT cryocooler design
- Data collected clearly demonstrates the need for and importance of developing accurate correlations at these operating conditions
  - Offers magnitude of  $h_{mg}$
  - Demonstrates thermal resistance of LP stream is significant
  - Provides insight to flow characteristics – indicates low velocity gas flow
- Future work includes a large test matrix for multi-component mixtures with varying geometrical parameters at operating conditions associated with MGJT cryocoolers
- With the large data campaign proposed and enabled by the test facility developed in this work, correlations can be developed

Questions?  
Thank you!

