



PARAMETRIC STUDY FOR THE COOLING OF SUPERCONDUCTOR CURRENT LEADS (HTS CLs)

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Outline



- CLs key features
- Model
 - Cooling options
 - Design parameters of the analyzed current lead
 - Basic assumptions
 - HTS part
 - HEX part
 - Method of solution
 - Input parameters range
 - Cooling power requirements
- Results
- Conclusions



HTS CLs key features



PRO:

- No Joule heating in HTS part
 - lower heat leak at cold end
 - significant reduction of cooling power (by a factor 3)

CON:

- Higher investment costs



RT end

Cu heat exchanger (HEX)

HTS module (T < 80 K)

Cold end (T ~ 4.5 K)

70 kA HTS CL [1]

[1] Heller R, Darweshsad MS, Dittrich G, Fietz WH, Fink S, Herz W, Hurd F, Kienzler A, Lingor A, Meyer I, Noether G, Suesser M, Tanna VL, Vostner A, Wesche R, Wuechner F, Zahn G. *Experimental results of a 70 kA high temperature superconductor current lead demonstrator for the ITER magnet system*, IEEE Trans Appl Supercond 15, 1496 (2005)

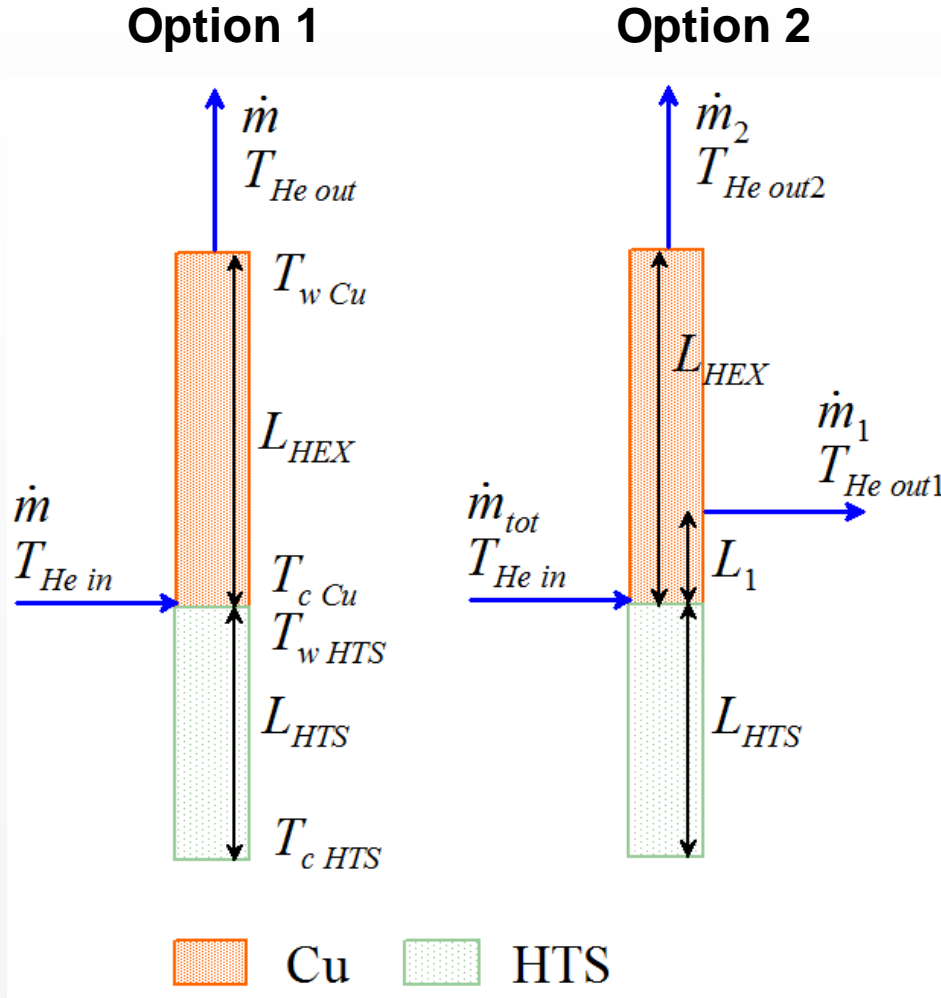


Cooling options



Forced –flow cooled.
Helium is warmed up to the RT.

Conduction Cooled.



Forced –flow cooled.
At length L_1 part of the helium mass flow is diverted. The remaining helium is warmed up to the RT.

Conduction Cooled.

Copper contact region is not taken into consideration $\rightarrow T_w \equiv T_w HTS \approx T_c Cu$



Design parameters of the current lead



Analysis based on the outline design of the 18 kA HTS CL for EDIPO [2], adjusted to operating current of 20 kA.

[2] Wesche R, Bagnasco M, Bruzzone P, Felder R, Guetg M, Hostenstein M, Jenni M, March S, Roth F, Vogel M. *Test results of the 18 kA EDIPO HTS current leads*. Fusion Eng Des (2011) in press

Main input parameters:

| Parameter [Unit] | Value |
|---|------------|
| HTS part | |
| I/O diameter of the cylinder [mm] | 59.8/45.8 |
| Cylinder length [mm] | 405 |
| Number of AgMg/Ag/Bi-2233 stacks | 22 |
| Stack width [mm] | 4.2 |
| Stack height [mm] | $1.9n_t/8$ |
| Averaged value of the perpendicular magnetic field [mT] | 70 |
| HEX part | |
| Copper RRR | 50 |
| Number of strands | 118440 |
| Strand diameter [mm] | 0.1 |
| Inner diameter of the embedding tube [mm] | 84.9 |
| Helium pressure [MPa] | 1 |
| Warm end copper temperature [K] | 300 |



HTS module – Basic assumptions



Number of AgMg/Ag/Bi-2233 tapes in each stack:

$$n_t(T_w) \approx \frac{I}{22 f_s I_c(70 \text{ mT}, T_w)} \quad f_s = 0.65 - \text{ safety factor}$$

Critical current for a single tape:

$$I_c(70 \text{ mT}, T) = 0.5 [I_c(60 \text{ mT}, T) + I_c(80 \text{ mT}, T)]$$

$$I_c(B, T) = 0.9 I_c(B, 0) \left[1 - \frac{T}{T_c(B)} \right]^\alpha$$

| Parameter [Unit] | Value |
|--|-------|
| $T_c(60 \text{ mT})$ [K] | 95.45 |
| $T_c(80 \text{ mT})$ [K] | 94.56 |
| $I_c(60 \text{ mT}, 0)/I_c(\text{sf}, 77 \text{ K})$ | 6.705 |
| $I_c(80 \text{ mT}, 0)/I_c(\text{sf}, 77 \text{ K})$ | 6.31 |
| $I_c(\text{sf}, 77 \text{ K})$ [A] | 110 |
| α | 1.5 |

Bruker HTS GmbH. Data sheet BHTS current lead application tape. <http://www.bruker-est.com/>

Heat leak at the cold end of the CL:

$$\left| \dot{Q}_0(T_w) \right| = \frac{A_{steel}}{L_{HTS}} \int_{4.5K}^{T_w} k_{steel}(T) dT + \frac{A_{HTS}}{L_{HTS}} \int_{4.5K}^{T_w} k_{HTS}(T) dT$$



HEX part – governing equations



Steady state energy balance equations:

$$\frac{d}{dx} \left[k_{Cu} (T_{Cu}) \frac{dT_{Cu}}{dx} \right] + \frac{I^2 \rho_{Cu} (T_{Cu})}{A^2} - \frac{H_{eff} P_{w,eff}}{A} (T_{Cu} - T_{He}) = 0$$

$$\dot{m}_{He} C_{p,He} (T_{He}) \frac{dT_{He}}{dx} = H_{eff} P_{w,eff} (T_{Cu} - T_{He})$$

x – coordinate directed along a strand, m

I – operating current, A

ρ_{Cu} – copper electric resistivity, Ω m

k_{Cu} – copper thermal conductivity, W/(m K)

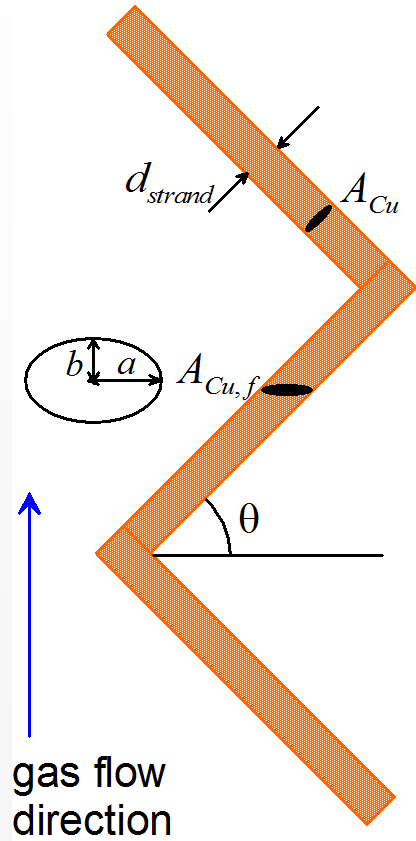
$A = N_{str} A_{Cu}$ – cross section strands in a direction perpendicular to x , m²

A_{Cu} – cross section of a single strand in a direction perpendicular to x , m²

\dot{m}_{He} – helium mass flow rate, g/s

$C_{p,He}$ – helium specific heat at constant pressure, J/(kg K)

HEX part – Heat transfer [3]



$$L_{HEX} = L_{str} \sin \theta = \frac{L_{str}}{\Psi} \quad \text{length of HEX}$$

$$A_f = A_{tube} - N_{str} A_{Cu,f} \quad \text{flow area}$$

$$A_{Cu,f} = \Psi \pi d_{str}^2 / 4 = \Psi A_{Cu}$$

$$p_{w,f} = N_{str} p_{Cu,f} = \left[\frac{3(1 + \Psi)}{4} - \frac{\sqrt{\Psi}}{2} \right] N_{str} \pi d \approx 1.21 N_{str} \pi d$$

$$p_{w,eff} = N_{str} \pi d \quad \text{wetted perimeter}$$

$$Nu = (0.4 Re^{1/2} + 0.2 Re^{2/3}) Pr^{0.4} \quad \text{correlation for the laminar flow in a packed bed [4]}$$

$$H(\dot{m}_{He}, T_{He}) = Nu k_{He} / D_h$$

Effective heat transfer coefficient:

$$H p_{w,f} L_{HEX} = H_{eff} p_{w,eff} L_{str} \Rightarrow H_{eff} \approx 0.86 H$$

[3] Anghel A., *Heat transfer from fluid to a wire bundle*, PSI Technical Physics internal report (1992)

[4] Gamson B.W., Thodos G.E., Hougen O.A., *Heat Mass and Momentum Transfer in the Flow of Gases Through Granular Solids*. Trans. AIChE **39**, 1 (1943)

Problem to be solved

$$\frac{d}{dx} \left[k_{Cu}(T_{Cu}) \frac{dT_{Cu}}{dx} \right] + \frac{I^2 \rho_{Cu}(T_{Cu})}{A^2} - \frac{H_{eff} p_{w,eff}}{A} (T_{Cu} - T_{He}) = 0$$

$$\dot{m}_{He} C_{p,He}(T_{He}) \frac{dT_{He}}{dx} = H_{eff} p_{w,eff} (T_{Cu} - T_{He})$$

Boundary conditions:

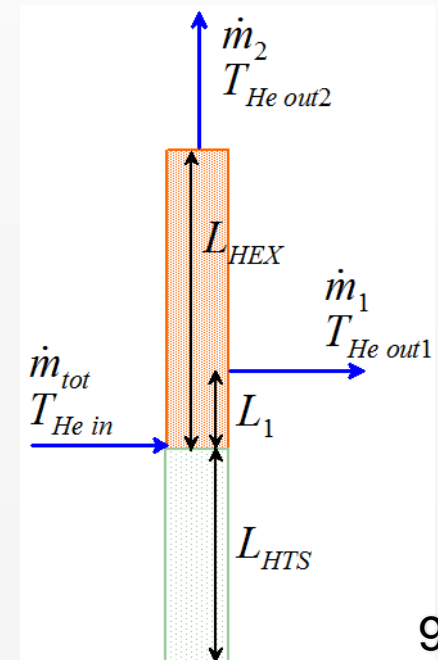
$$T_{Cu}(0) = T_w$$

$$\frac{dT_{Cu}}{dx}(0) = \frac{|\dot{Q}_0(T_w)|}{k_{Cu}(T_w)A}$$

$$T_{He}(0) = T_{He,in}$$

Additional conditions for the Option 2:

- continuity of the temperature and heat flux at $x = \Psi L_1$
- $\dot{m}_{He} = \dot{m}_{tot}$ for $x < \Psi L_1$ and $\dot{m}_{He} = \dot{m}_2$ for $x > \Psi L_1$



Solution method [5]

The HEX part of a CL is divided into many short segments of length Δx .

Neglecting the variation of $\Delta T = T_{Cu} - T_{He}$ and the temperature dependence of the material properties (k_{Cu} , ρ_{Cu} , $C_{p,He}$) within a single segment we get the recurrence solution equations:

$$T_{Cu_{i+1}} = -\frac{1}{2k_{Cu}(T_{Cu_i})A} \left[\frac{I^2 \rho_{Cu}(T_{Cu_i})}{A} - H_{eff} p_{w,eff} \Delta T_i \right] \Delta x^2 - \frac{\dot{Q}_i}{k_{Cu}(T_{Cu_i})A} \Delta x + T_{Cu_i}$$

$$\dot{Q}_{i+1} = \dot{Q}_i + H_{eff} p_{w,eff} \Delta T_i \Delta x - \frac{I^2 \rho_{Cu}(T_{Cu_i}) \Delta x}{A}$$

$$T_{He_{i+1}} = T_{He_{i+1}} + \frac{H_{eff} p_{w,eff} \Delta T_i}{\dot{m}_{He} C_{p,He}} \Delta x$$

- Integration procedure repeated for various mass flow rates until $T_{Cu} = 300$ K and $\dot{Q} = 0$ W is reached at the warm end of HEX
 → optimum mass flow rate and optimum HEX length
- Solution independent of the segment length for $\Delta x = 10^{-5}$ m (or smaller)



Range of input parameters



- **Option 1**

$$T_w = 40 \text{ to } 75 \text{ K}$$

$$T_{He,in} = 5 \text{ K to } (T_w - 5 \text{ K})$$

- **Option 2**

$$T_w = 47 \text{ to } 73 \text{ K}$$

$$T_{He,in} = (T_w - 8 \text{ K}) \text{ to } (T_w - 2 \text{ K})$$

$$L_1 = 3, 4 \text{ and } 5 \text{ cm}$$

$$\dot{m}_2 / \dot{m}_{tot} = 0.05 \text{ to } 1$$



Cooling power requirements



Ideal refrigerator input power required to cool the whole binary HTS CL

- for the cooling option 1:

$$P_{ideal,1} = \frac{T_{max} - T_0}{T_0} |\dot{Q}_0| + \dot{m} \left\{ T_{max} [s(T_{max}) - s(T_{He,in})] - [h(T_{max}) - h(T_{He,in})] \right\}$$

- for the cooling option 2:

$$P_{ideal,2} = \frac{T_{max} - T_0}{T_0} |\dot{Q}_0| + \dot{m}_1 \left\{ T_{max} [s(T_{He,out1}) - s(T_{He,in})] - [h(T_{He,out1}) - h(T_{He,in})] \right\} + \dot{m}_2 \left\{ T_{max} [s(T_{max}) - s(T_{He,in})] - [h(T_{max}) - h(T_{He,in})] \right\}$$

h - helium specific enthalpy, J/kg

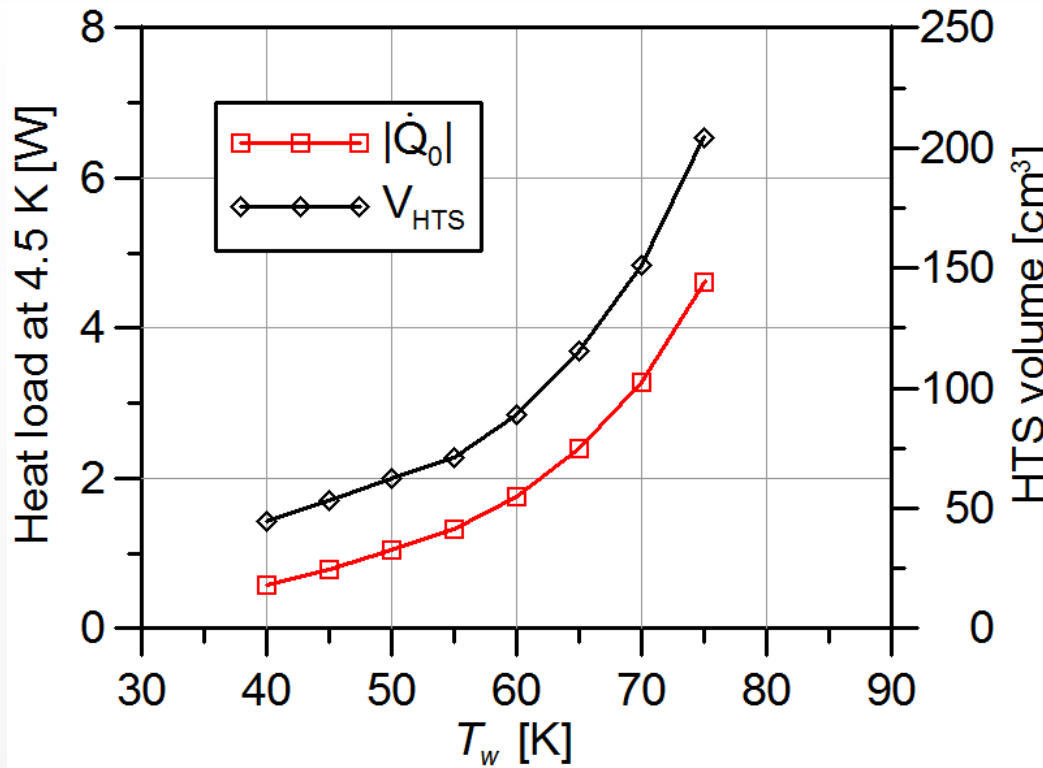
s - helium specific entropy, J/(kg K)

$T_0 = 4.5$ K

$T_{max} = 300$ K

Results (I)

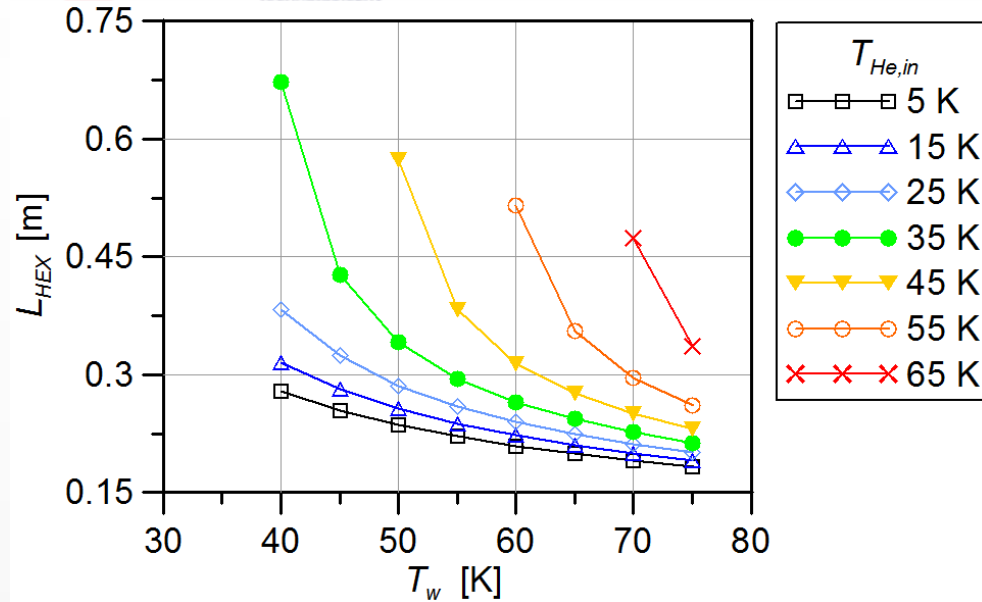
Heat leak at the cold end



Heat load at the cold end of the HTS CL and the required volume of 0.405 m long HTS tapes as a function of the temperature at the warm end of the HTS part.

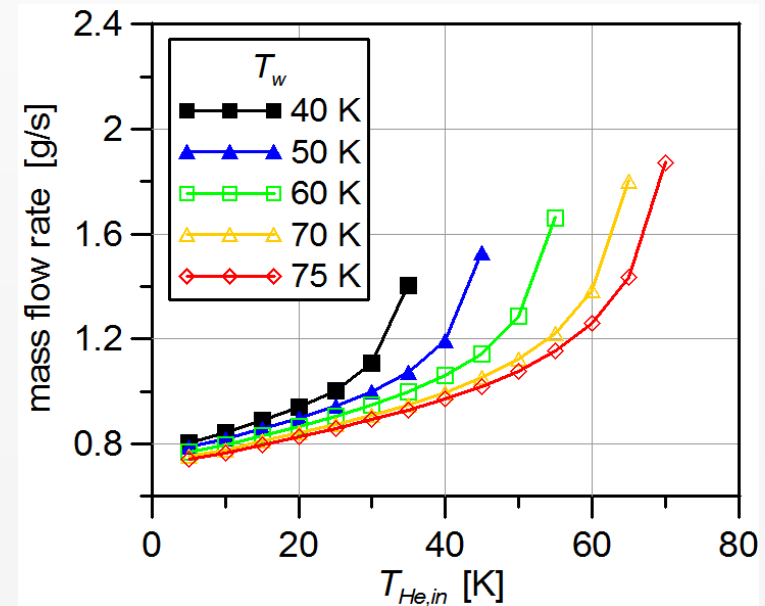
Results (II)

Cooling Option 1



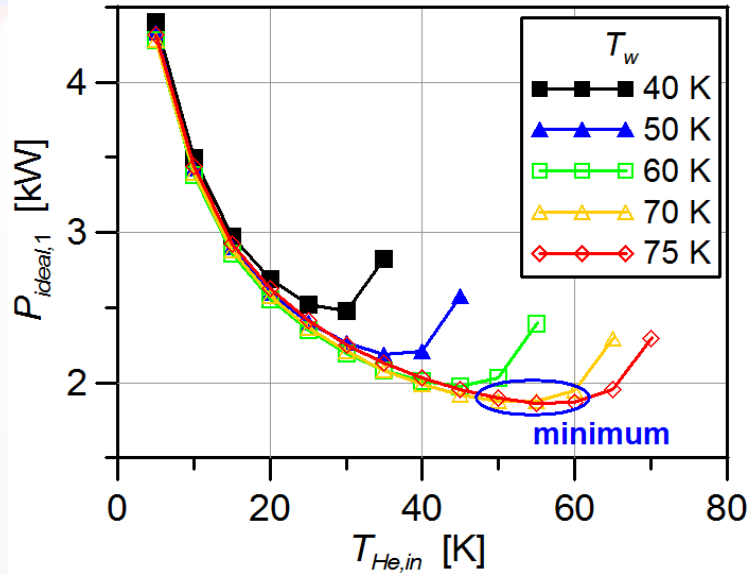
Optimum length of the HEX part

Optimum helium mass flow rate required to cool the HEX



Results (III)

Cooling Option 1 - summary



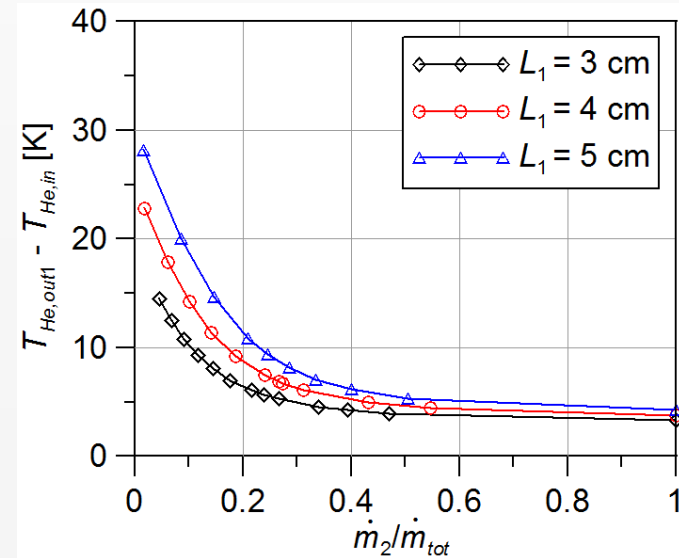
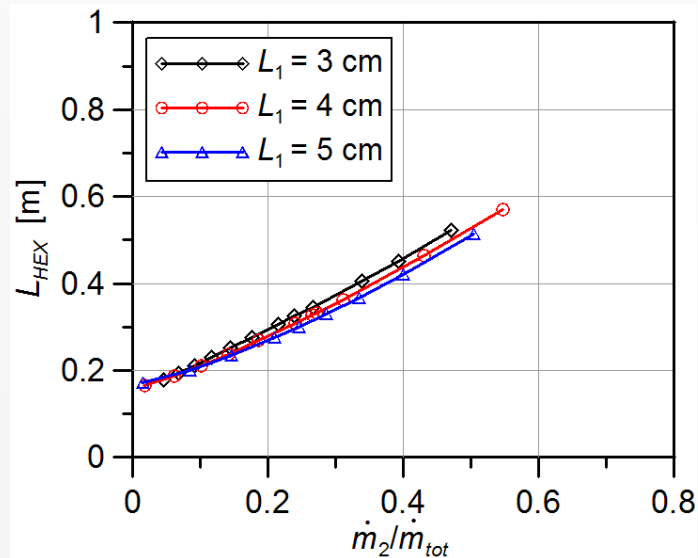
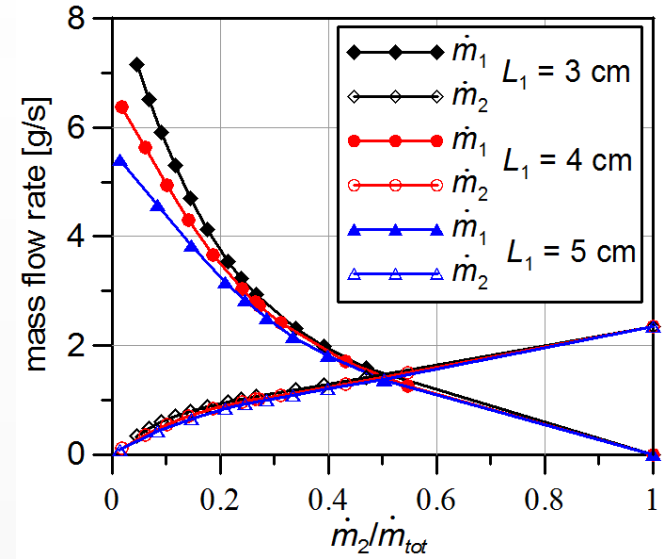
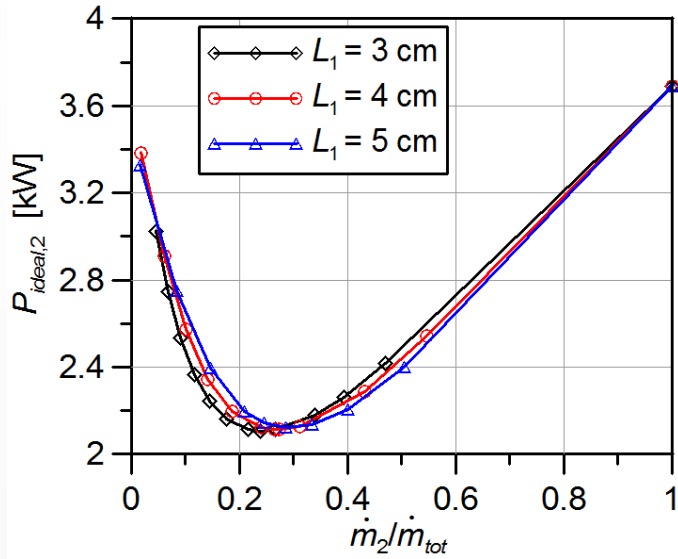
Ideal refrigerator input power necessary to cool the whole CL

Optimum cooling conditions for different values of the temperature at the warm end of the HTS part

| T_w [K] | $T_{He,in}$ [K] | \dot{m} [g/s] | L_{HEX} [m] | $P_{ideal,1}$ [kW] |
|-----------|-----------------|-----------------|---------------|--------------------|
| 50 | 37 | 1.1116 | 0.3605 | 2.191 |
| 60 | 45 | 1.1442 | 0.3141 | 1.992 |
| 70 | 53 | 1.1759 | 0.2832 | 1.889 |
| 74 | 56 | 1.1834 | 0.2722 | 1.876 |
| 75 | 57 | 1.1896 | 0.2707 | 1.884 |

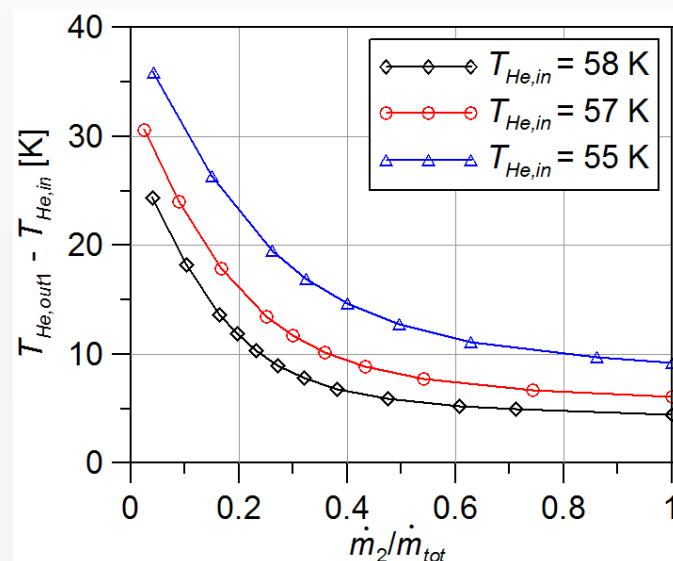
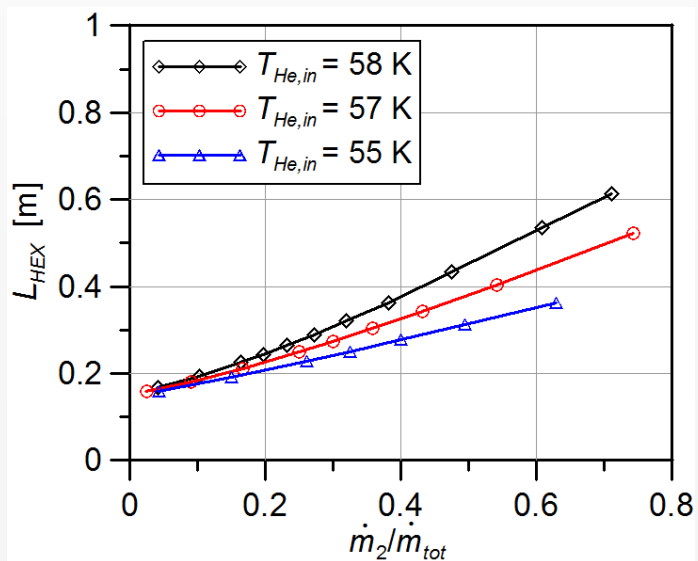
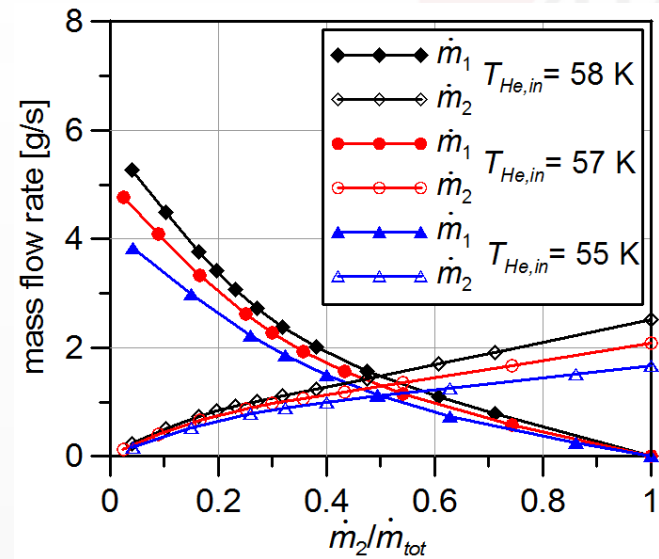
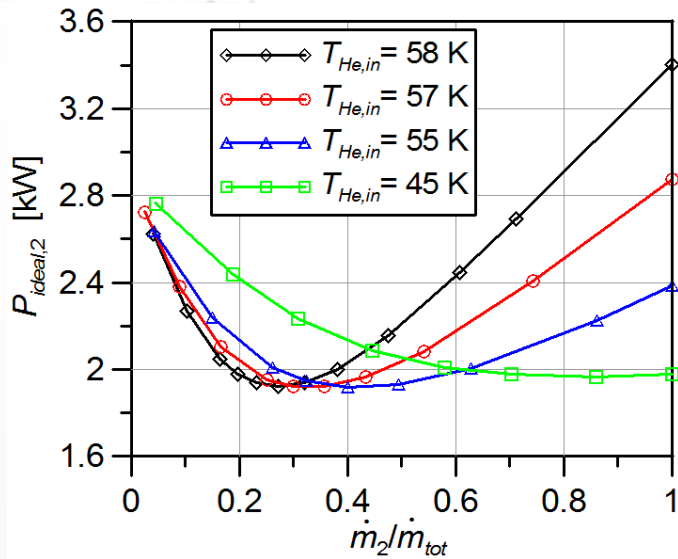
Results (IV) - Option 2

$T_w = 50 \text{ K}$, $T_{He,in} = 48 \text{ K}$



Results (V) - Option 2

$T_W = 60 \text{ K}$, $L_1 = 4 \text{ cm}$





Results (VI) Summary



Optimum cooling conditions for different values of the copper temperature at the cold end of HEX

OPTION 2

| T_w [K] | $T_{He,in}$ [K] | \dot{m}_{tot} [g/s] | \dot{m}_2 [g/s] | L_{HEX} [m] | $T_{He,out1}$ [K] | $P_{ideal,2}$ [kW] |
|-----------|-----------------|-----------------------|-------------------|---------------|-------------------|--------------------|
| 50 | 47 | 3.10 | 1.0119 | 0.3262 | 55.45 | 2.122 |
| 60 | 56 | 2.75 | 1.0111 | 0.2826 | 68.83 | 1.930 |
| 70 | 65 | 2.55 | 1.0106 | 0.2540 | 82.67 | 1.831 |

OPTION 1

| T_w [K] | $T_{He,in}$ [K] | \dot{m} [g/s] | L_{HEX} [m] | $P_{ideal,1}$ [kW] |
|-----------|-----------------|-----------------|---------------|--------------------|
| 50 | 37 | 1.1116 | 0.3605 | 2.191 |
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Results (VI) Summary



Optimum cooling conditions for different values of the copper temperature at the cold end of HEX

OPTION 2

| T_w [K] | $T_{He,in}$ [K] | \dot{m}_{tot} [g/s] | \dot{m}_2 [g/s] | L_{HEX} [m] | $T_{He,out1}$ [K] | $P_{ideal,2}$ [kW] |
|-----------|-----------------|-----------------------|-------------------|---------------|-------------------|--------------------|
| 50 | 47 | 3.10 | 1.0119 | 0.3262 | 55.45 | 2.122 |
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|-----------|-----------------|-----------------|---------------|--------------------|
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Results (VI) Summary



Optimum cooling conditions for different values of the copper temperature at the cold end of HEX

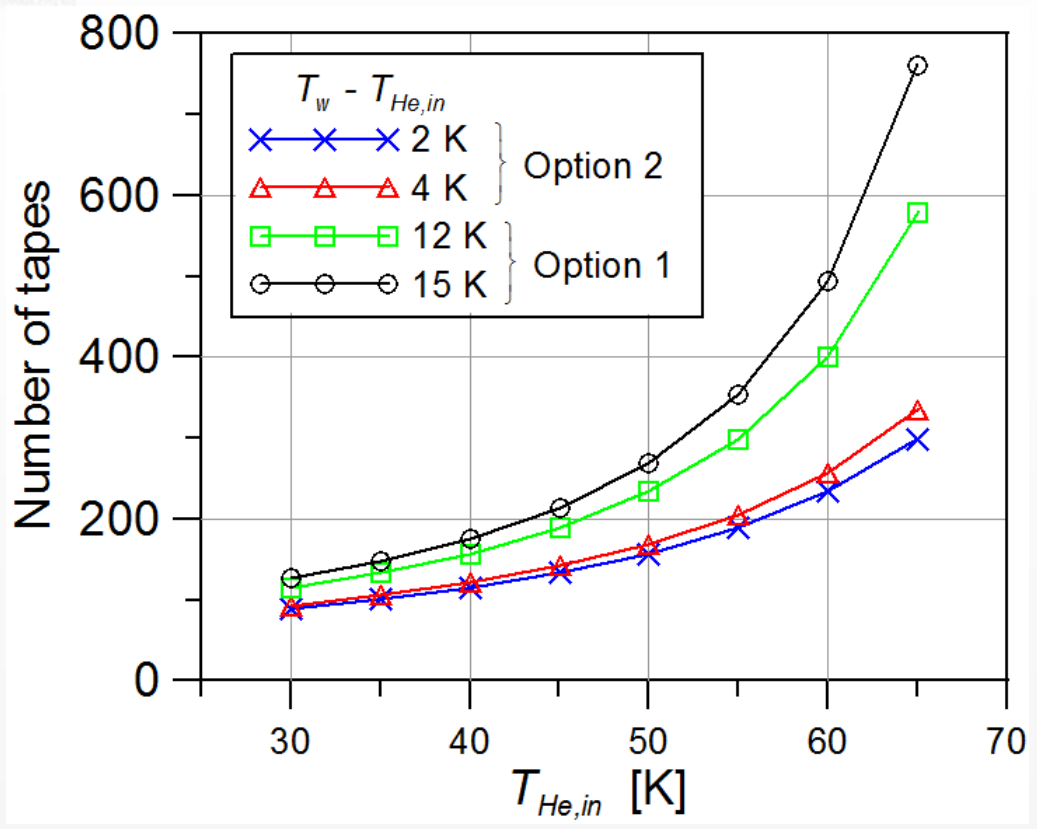
OPTION 2

| T_w [K] | $T_{He,in}$ [K] | \dot{m}_{tot} [g/s] | \dot{m}_2 [g/s] | L_{HEX} [m] | $T_{He,out1}$ [K] | $P_{ideal,2}$ [kW] |
|-----------|-----------------|-----------------------|-------------------|---------------|-------------------|--------------------|
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Results (VII)



The required number of HTS tapes as a function of the helium inlet temperature for various values of the temperature at the warm end of HTS part.



Summary and conclusions



- Comparative analysis of the two cooling options for the HEX part of the 20 kA HTS CL has been performed.
- **Option 1**
 - **PRO:** simple operating control
 - **CON:** T_w much higher than $T_{He,in}$
- **Option 2**
 - **PRO:** T_w only 2 – 4 K higher than $T_{He,in}$
 - possible reduction of T_w at a given $T_{He,in}$
 - possible reduction of the required number of HTS tapes
 - **CON:** complicated operating control
 - further more detailed investigation necessary



Thank you for your attention



Option 3 - model



$$\frac{d}{dx} \left[k_{steel}(T_s) \frac{dT_s}{dx} \right] - \frac{H(T_{He}) p_{w,s}}{A_s} (T_s - T_{He}) = 0$$

$$\frac{d}{dx} \left[k_c(T_c) \frac{dT_c}{dx} \right] - \frac{H(T_{He}) p_{w,c}}{A_c} (T_c - T_{He}) = 0$$

$$\dot{m}_1 C_{p,He}(T_{He}) \frac{dT_{He}}{dx} = H(T_{He}) p_{w,s} (T_s - T_{He}) + H(T_{He}) p_{w,c} (T_c - T_{He})$$

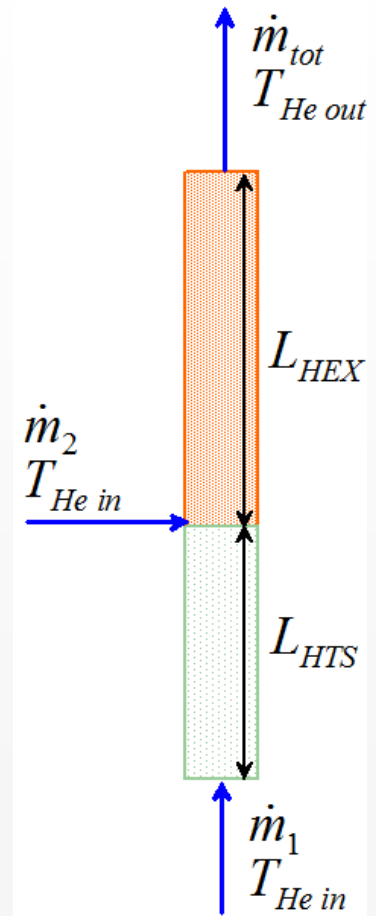
Indices *c* and *s* are related to the conductor (cylinder + HTS stacks) and steel tube, respectively.

Effective thermal conductivity of the conductor

$$k_c(T) = \frac{A_{steel} k_{steel}(T) + A_{HTS} k_{HTS}(T)}{A_{steel} + A_{HTS}}$$

Ideal refrigerator power required to cool the whole HTS CL

$$P_{ideal,3} = \frac{T_{max} - T_0}{T_0} (\dot{Q}_{s0} + \dot{Q}_{c0}) + \dot{m}_{tot} \left\{ T_{max} [s(T_{max}) - s(T_{He,in})] - [h(T_{max}) - h(T_{He,in})] \right\}$$





Option 3 - results

| Input parameters | T_w [K] | $P_{ideal,3}$ [kW] | $ \dot{Q}_0 $ [W] | $P_{ideal,1}$ [kW] |
|---|-----------|--------------------|-------------------|--------------------|
| $\dot{m}_1 = 0.002$ g/s $ \dot{Q}_{s0} = 0.039$ W $ \dot{Q}_{c0} = 0.934961209421591$ W | 54.83 | 4.365 | 1.350 | 4.375 |
| $\dot{m}_1 = 0.0072$ g/s $ \dot{Q}_{s0} = 0.0049$ W $ \dot{Q}_{c0} = 0.3143991062199854$ W | 54.78 | 4.326 | 1.348 | 4.375 |
| $\dot{m}_1 = 0.00852$ g/s $ \dot{Q}_{s0} = 0.0009$ W $ \dot{Q}_{c0} = 0.2139682329056472$ W | 54.85 | 4.318 | 1.351 | 4.375 |

- Cooling power consumption only about 1% lower than in the Option 1 for the same T_w and $T_{He,in} = 4.5$ K.
- Lower heat leak at the cold end
 - possible application in cases when a high heat load in HTS part, e.g. due to AC losses, is expected