

Sectorisation, pumping system, commissioning and operation of ET beampipes

Carlo Scarcia on behalf of CERN TE/VSC

28/03/2023

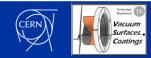
Summary

- Assumptions
- Sectorization
- Commissioning:
 - Rough pumping
 - HV pumping
 - UHV pumping at RT
- Bake-out: insulation and operational aspects
- Pressure monitoring:
 - Air leak: impact on total pressure
- Vacuum system cost assessment (hardware only)
- Final considerations

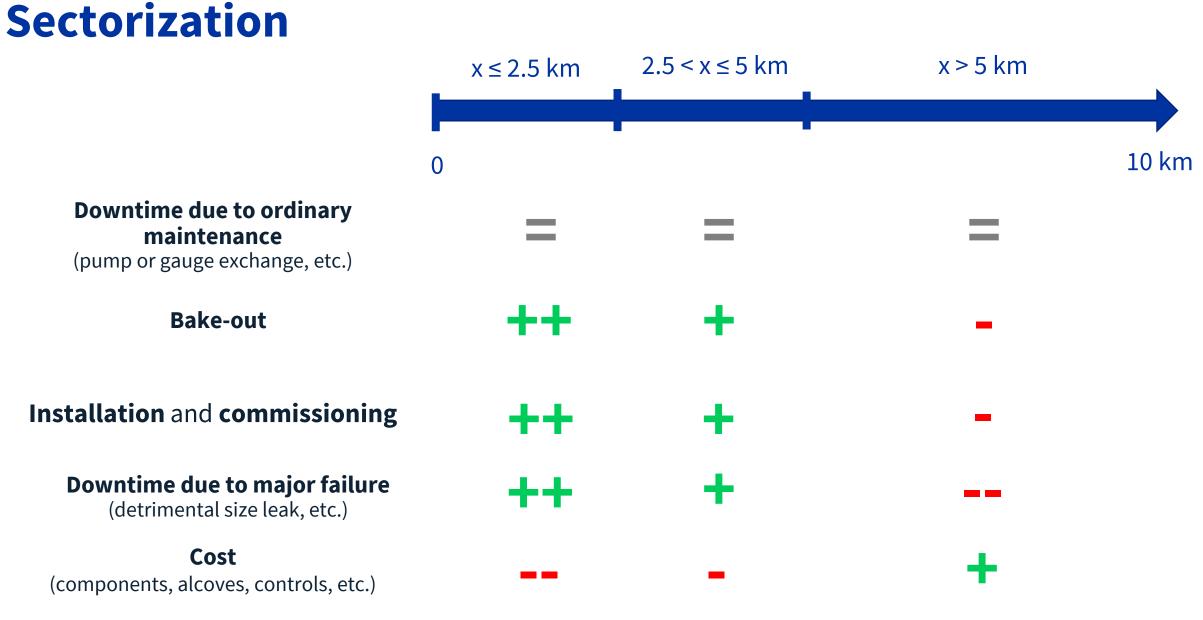


Assumptions

- The **beampipe internal diameter** is here assumed to be of **1.2 m**.
- Material properties (vacuum outgassing, electrical and thermal): Mild steel.
- Water outgassing rate simulation done using a quasi-equilibrium (1D) models (Kanazawa hyp.) based on Temkin isotherm.
- Compact and evenly distributed pumping groups.
- Gate valves to separate the tube from the pumping group.
- **Pumping speeds** used are **nominal** (**no conductance limited by the gate valve**).
- UHV pumping only with capture pumps (no noise, low power needed).



Sectorization

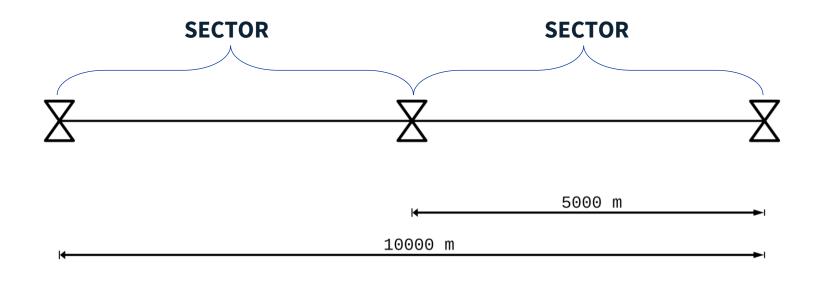




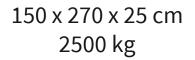


For this scenario, we chose to have a balanced option between cost and system flexibility. Therefore, we foreseen the use of one **sector gate valve (DN1250) every 5 km**.

Note: to be checked the possibility of reduced aperture for the middle sector valve









Commissioning

Commissioning of the vacuum system

- Rough pumping (from atmospheric pressure to 10⁻¹ mbar)
- HV pumping (from HV to UHV range)
- UHV pumping at RT



Rough pumping (from atmospheric pressure to 10⁻¹ mbar)

Rough pumping: pump-down curve

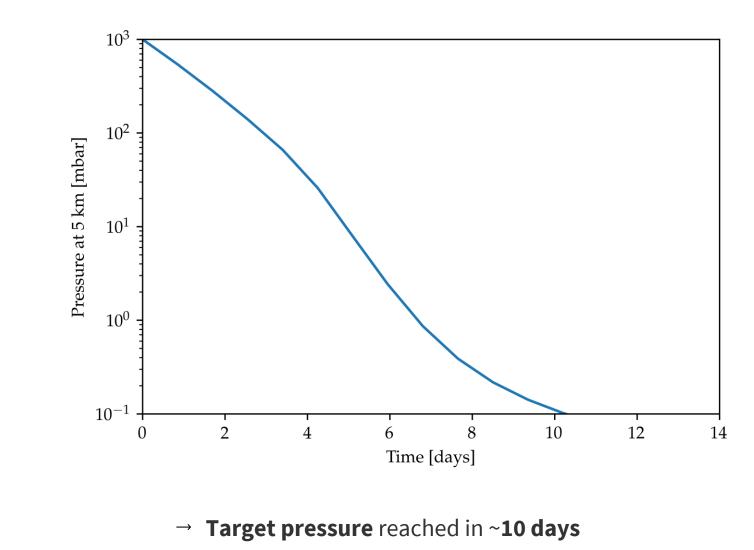
Ρ

Instrumented rough pumping group:

- Nominal pumping speed = **1000 m³ h⁻¹**
 - Ultimate pressure = **1×10⁻² mbar**
- Target pressure = 1×10⁻¹ mbar
 - x 10 higher to reduce any back streaming of gas

5000 m

• Low enough for TMPs starting

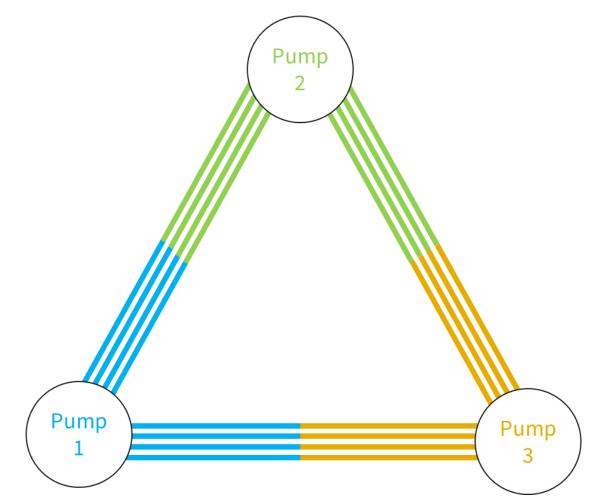




Rough pumping: optimization

In view of their weight (>350 kg), these pumping groups cannot be easily transported along the arm length.

Can be deployed to all 8 - 5km long sector sharing the same vertex.

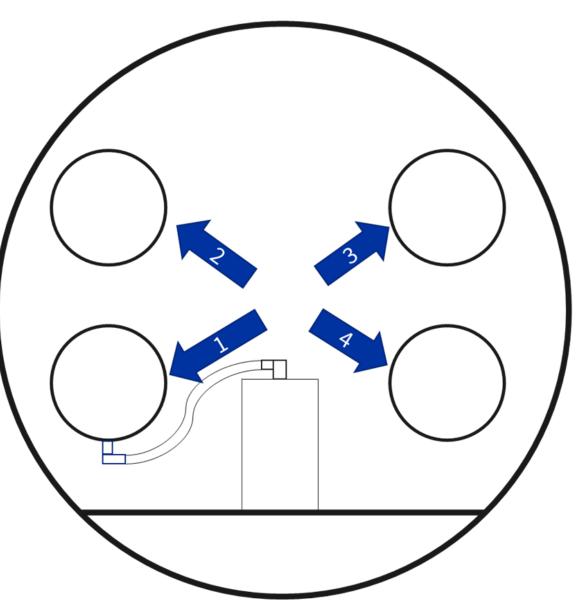




Rough pumping: optimization

In view of their weight (>350 kg), these pumping groups cannot be easily transported along the arm length.

Can be deployed to all 8 - 5km long sector sharing the same vertex.





HV pumping (from HV to UHV range)

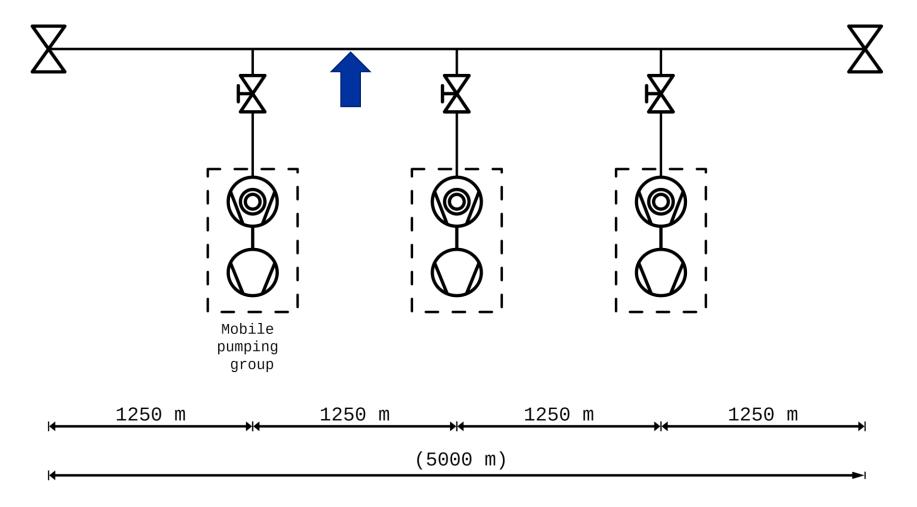
HV pumping: vacuum layout

- Assumption: Mobile pumping groups (Turbomolecular pump + primary pump).
 - → At UHV range, they will be substituted with capture pumps.
 - Gate valves to separate the tube from the mobile pumping group.
 (preferably electropneumatic).
 - Pumps evenly distributed.



HV pumping: vacuum layout

After a set of iterations, an optimal solution could be:





HV pumping: optimal turbomolecular pumps

What is the impact of the TMP pumping speed on the pump-down time?

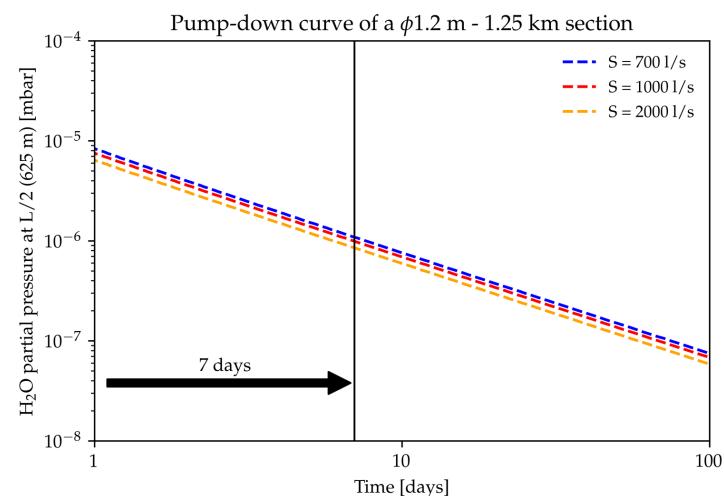
TMP pumping before bake-out starts: 7 days

No clear advantage shown for going > 700 l s⁻¹. At most the gain in pressure is of ~25% (for S = 2000 l s⁻¹)

 \rightarrow 700 l s⁻¹ pump represent the optimal solution

700 l s⁻¹ TMPs:

- Off the shelf product
- Air cooled
- Compact solution (with fittings)





From HV to UHV pumping: bake-out

Bake-out strategy must take in account several constraints on:

- ventilation system
- power consumption
- increase of temperature in the tunnel

Assumptions:

Bake-out temperature :Less than 100°CBake-out duration:max 30 days

NEG pumps

Bake-out performance can be enhanced by increasing the local pumping speed



Parameters:

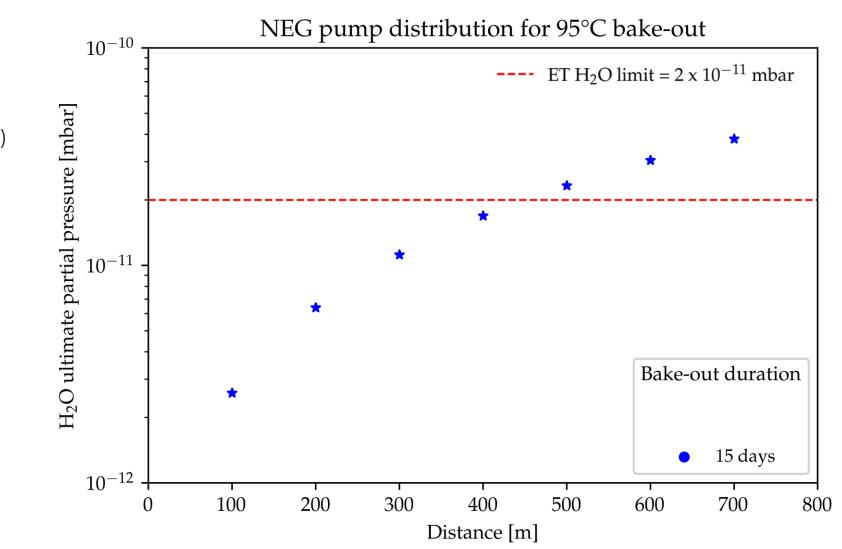
D = 1.2 m

L = 1250 m (distance between two turbos)

TMP pump-down duration: 7 days

S_{TURBO} = 700 ls⁻¹

 $S_{NEG} = 1500 \text{ ls}^{-1} (\text{H}_2\text{O})$





Parameters:

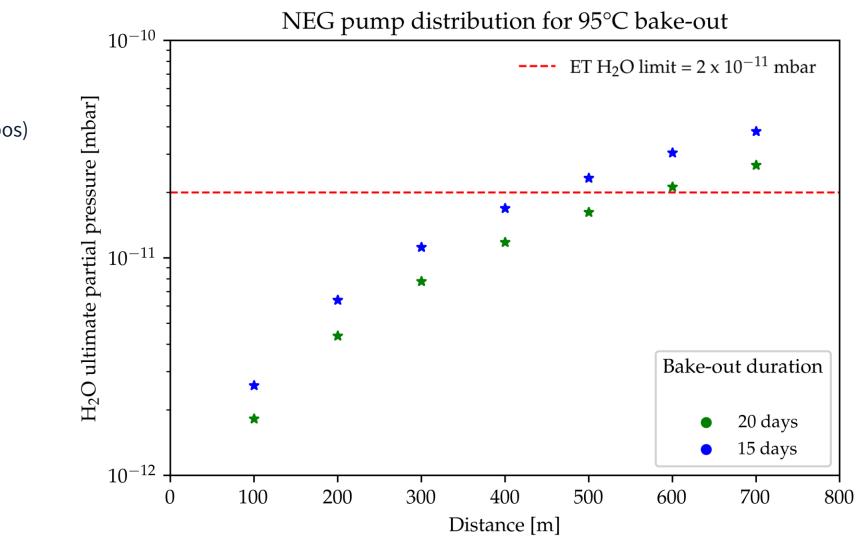
D = 1.2 m

L = 1250 m (distance between two turbos)

TMP pump-down duration: 7 days

S_{TURBO} = 700 ls⁻¹

 $S_{NEG} = 1500 ls^{-1} (H_2O)$





Parameters:

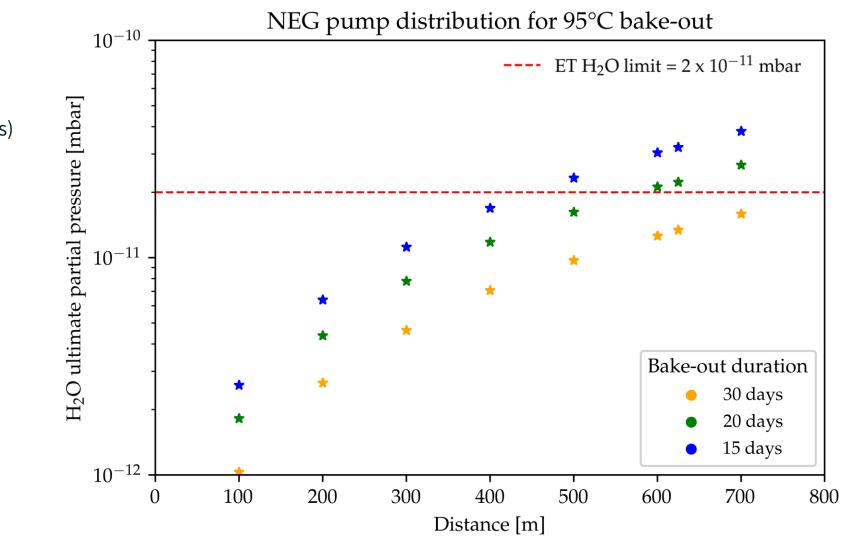
D = 1.2 m

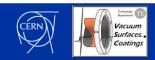
L = 1250 m (distance between two turbos)

TMP pump-down duration: 7 days

S_{TURBO} = 700 ls⁻¹

 $S_{NEG} = 1500 \text{ ls}^{-1} (H_2 \text{O})$





Parameters:

D = 1.2 m

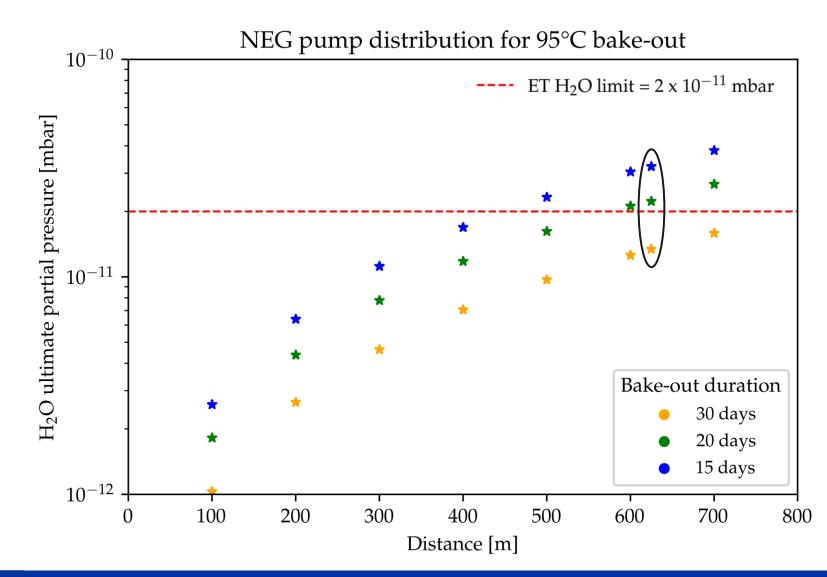
L = 1250 m (distance between two turbos)

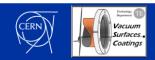
TMP pump-down duration: 7 days

S_{TURBO} = 700 ls⁻¹

 $S_{NEG} = 1500 \text{ ls}^{-1} (H_2 \text{O})$

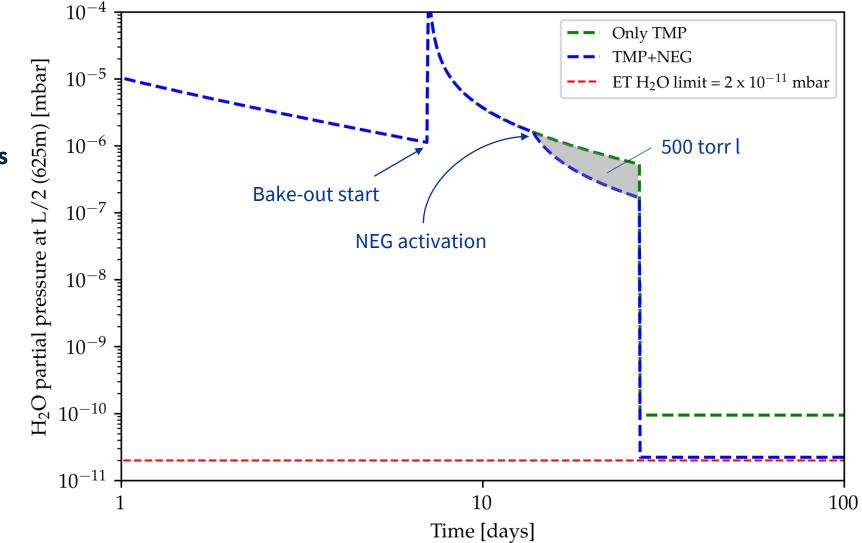
One NEG pump every 625 m to assist the bake-out cycle

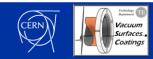




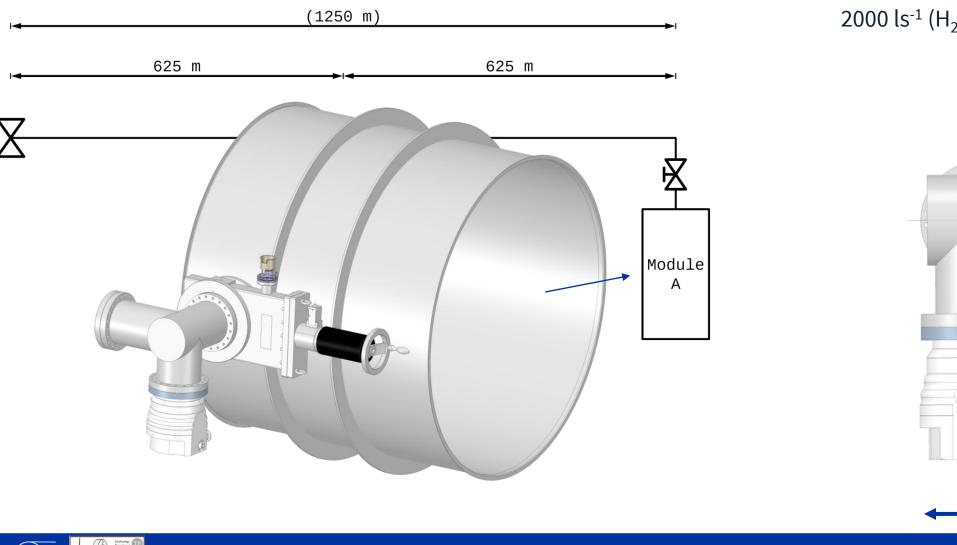
HV pumping: ultimate pressure after bake-out

- Isotherm: Temkin
- TMP pump-down duration: 7 days
- Bake-out = 95°C, 20 days
- Neg activation: after 1/3 of bake-out duration
- → H_2O ultimate $P \approx 2 \times 10^{-11}$ mbar



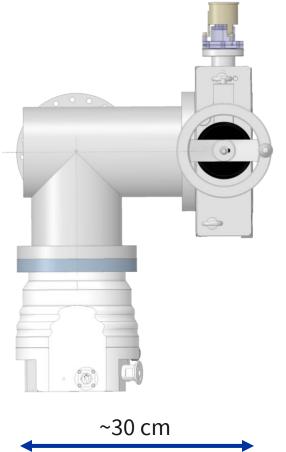


HV pumping: vacuum layout



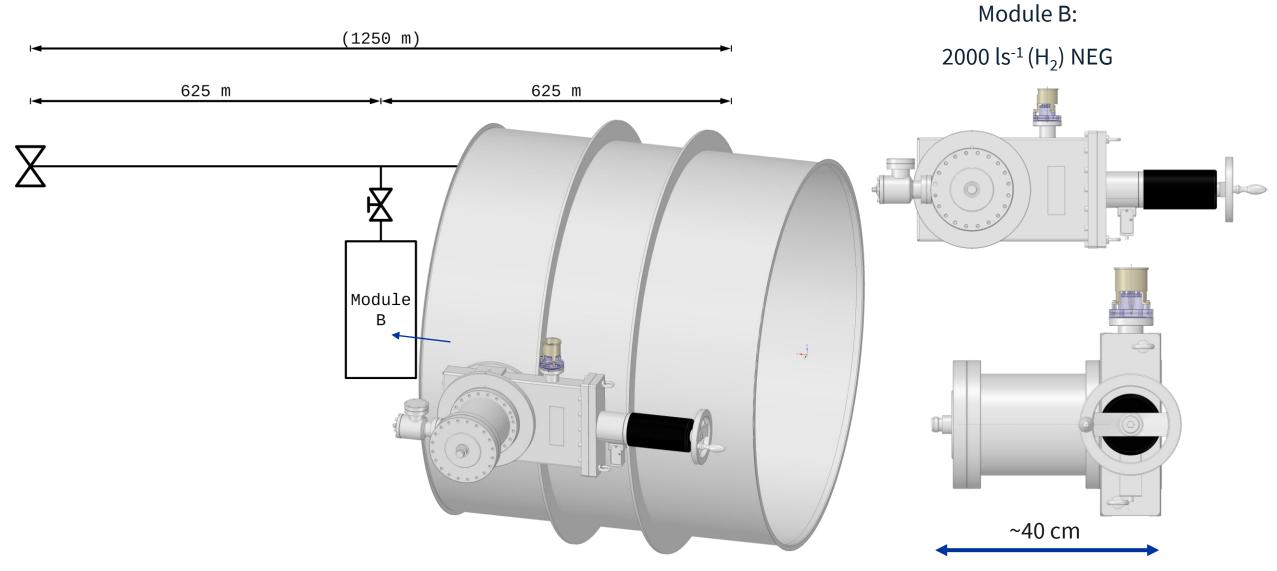
Module A (mobile):

2000 ls⁻¹ (H₂) NEG + 700 ls⁻¹ TMP



Surface

HV pumping: vacuum layout





UHV pumping at RT $(H_{2}, CH_{4}, CO and CO_{2})$

UHV pumping at RT: pressure requirements

Very strong pressure requirements from physics (both for LF and HF line):

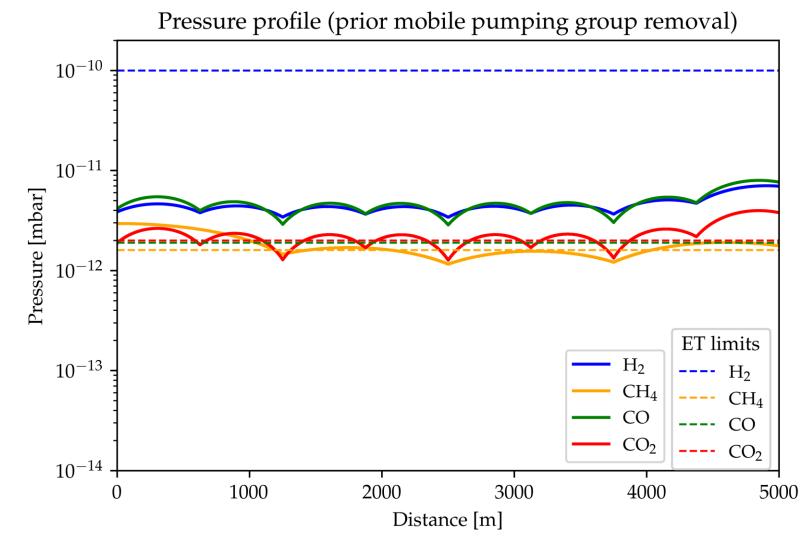
Gas	Goal P _{ET} [mbar]
H ₂	1 x 10 ⁻¹⁰
CH ₄	1.6 x 10 ⁻¹²
СО	1.9 x 10 ⁻¹²
CO ₂	2 x 10 ⁻¹²



UHV pumping at RT: pressure profile post bake-out

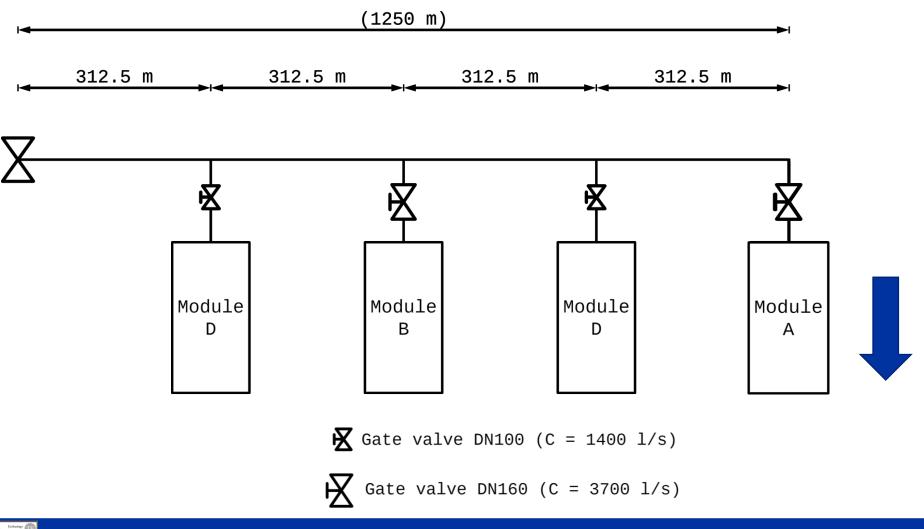
If we rely only on the pumps from HV pumping layout, we cannot meet the requirement.

Moreover, when mobile pumping groups are removed, we need to pump CH₄ and to lower CO and CO₂ pressures.



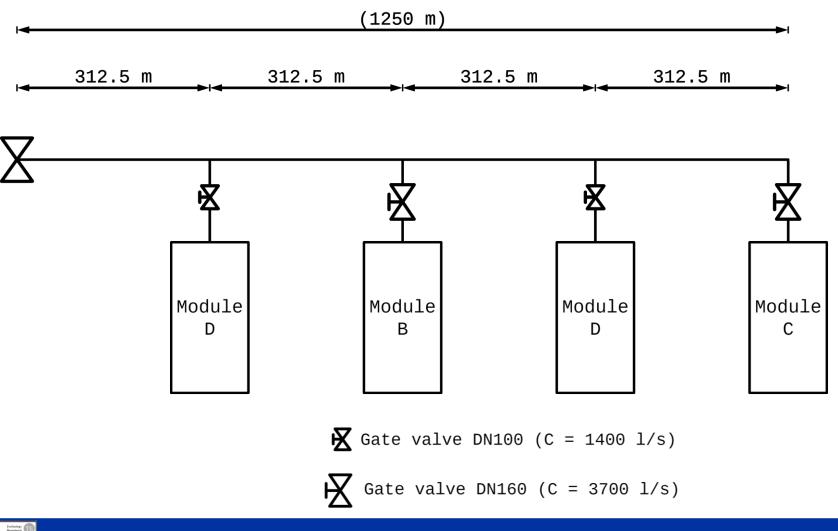


Keeping symmetry:

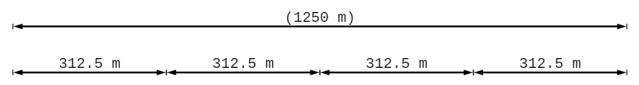




Keeping symmetry:

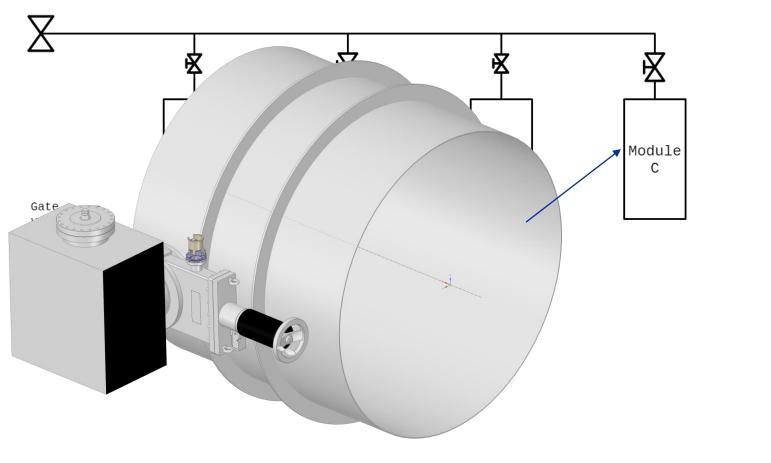


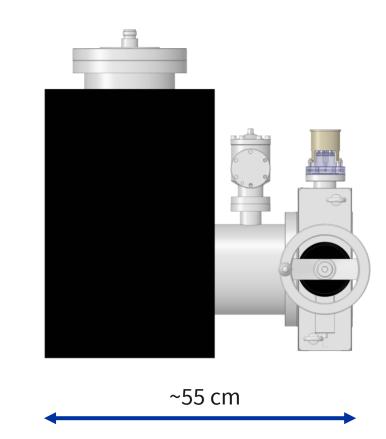




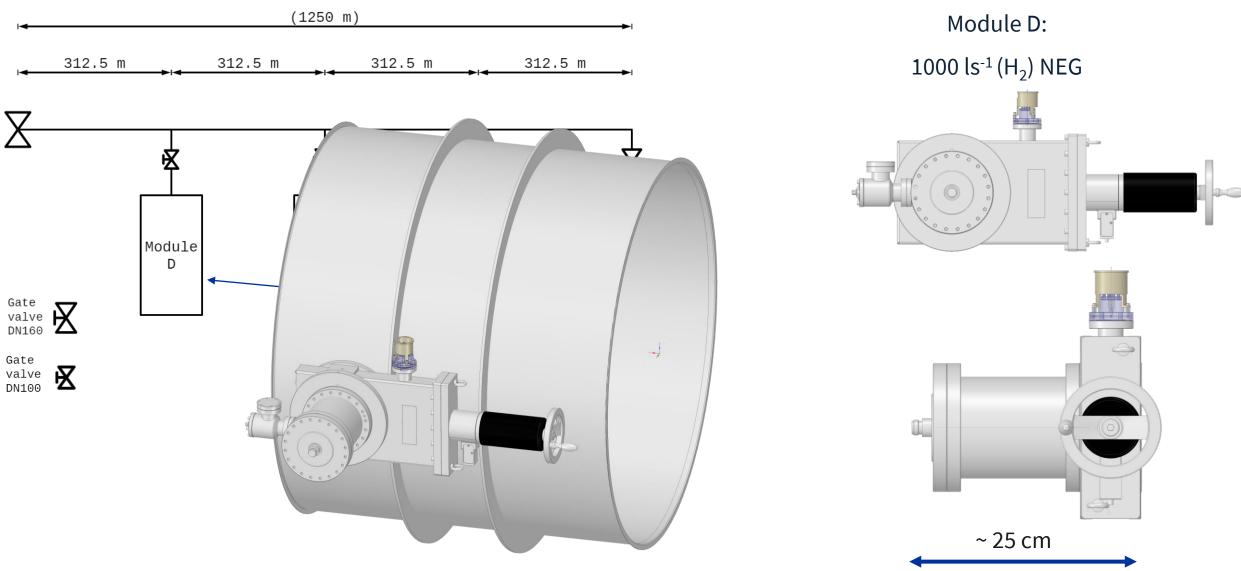
Module C:

2000 ls⁻¹ (H₂) NEG + 500 ls⁻¹ IP

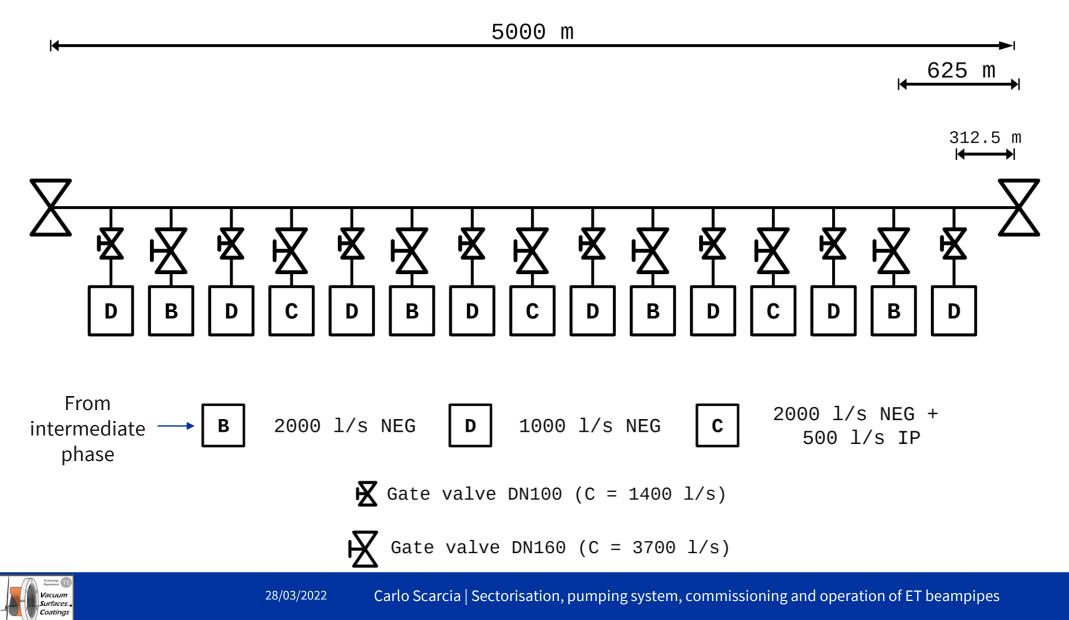










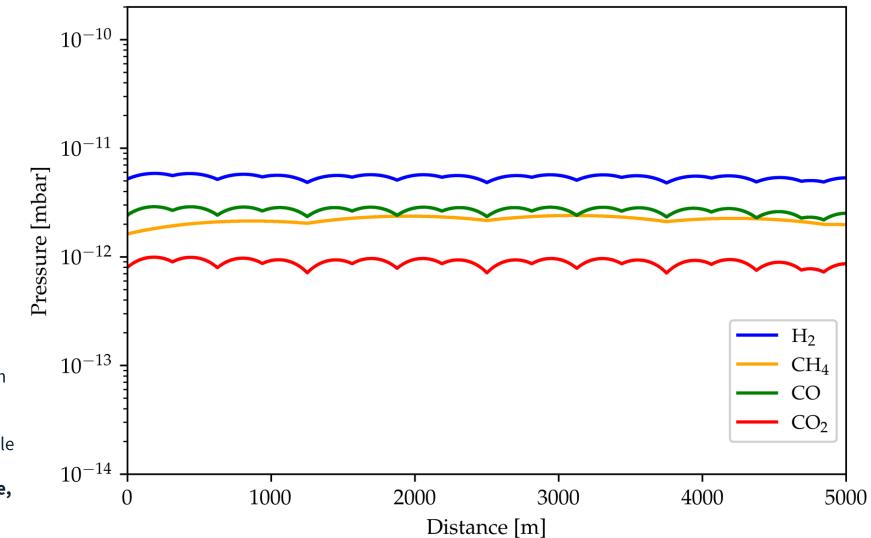


UHV pumping at RT: ultimate pressures

Gas	Pressure from sim. [mbar]
H ₂	6 x 10 ⁻¹²
CH ₄	2.5 x 10 ^{-12 *}
со	3 x 10 ^{-12 *}
CO ₂	1 x 10 ^{-12 *}

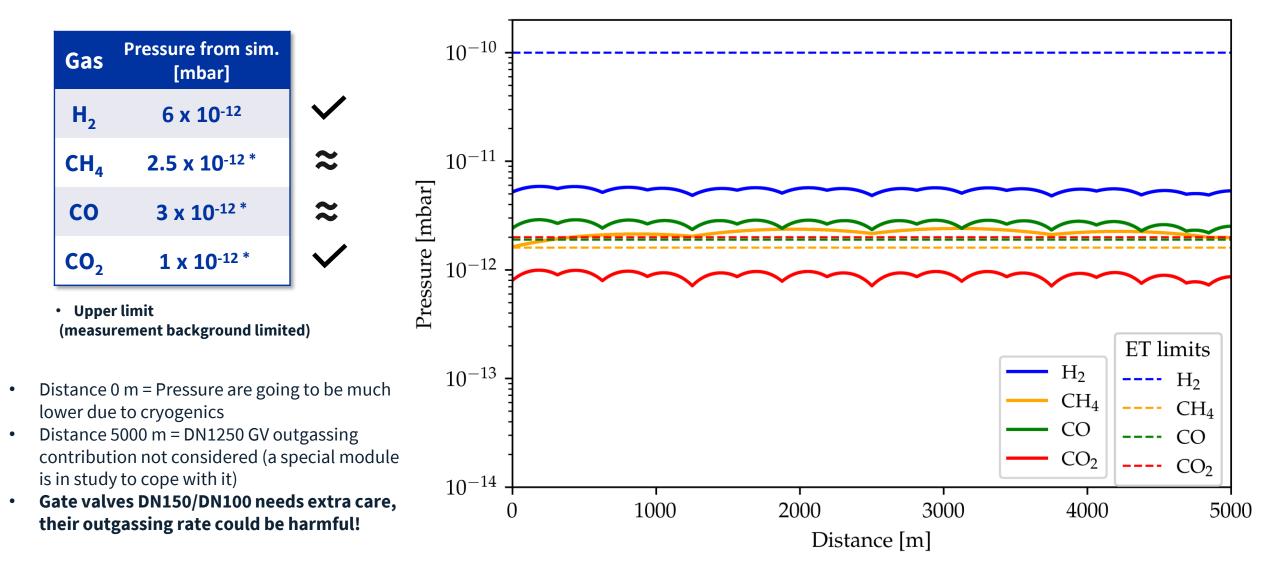
 Upper limit (measurement background limited)

- Distance 0 m = Pressure are going to be much lower due to cryogenics
- Distance 5000 m = DN1250 GV outgassing contribution not considered (a special module is in study to cope with it)
- Gate valves DN150/DN100 needs extra care, their outgassing rate could be harmful!





UHV pumping at RT: ultimate pressures





Bake-out: insulation and operational aspects

Bake-out: Insulation

Low temperature bake-out, opens also to more options for insulation



Mineral wool



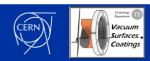


Phenolic/Polyurethane foam



Aerogel





Bake-out: Insulation thickness

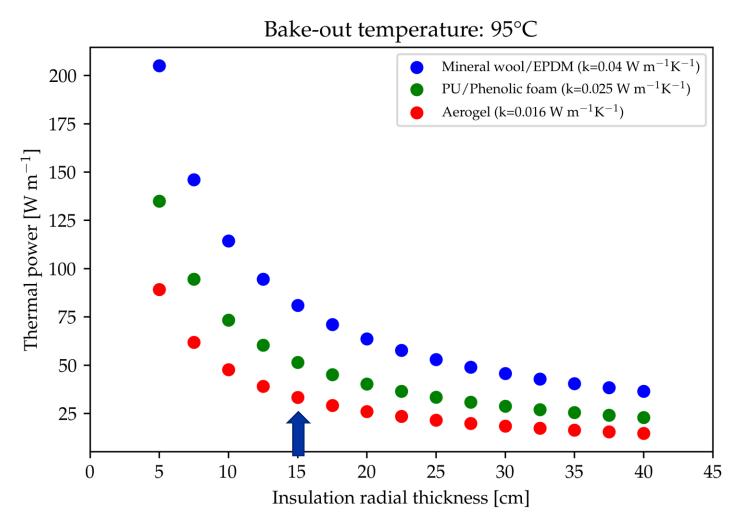
Assuming:

• $h_{air} = 5 W m^{-2} K^{-1}$ (calm air, free convection)

• t_{tube} = 3 mm

For 15 cm of insulation (2G like):

Q [W m⁻¹] \approx 81, 72, 35



*Only thermal power loss is considered **2.77×10⁻⁷ ohm m @ 95°C



Bake-out: Insulation thickness

Assuming:

• $h_{air} = 5 W m^{-2} K^{-1}$ (calm air, free convection)

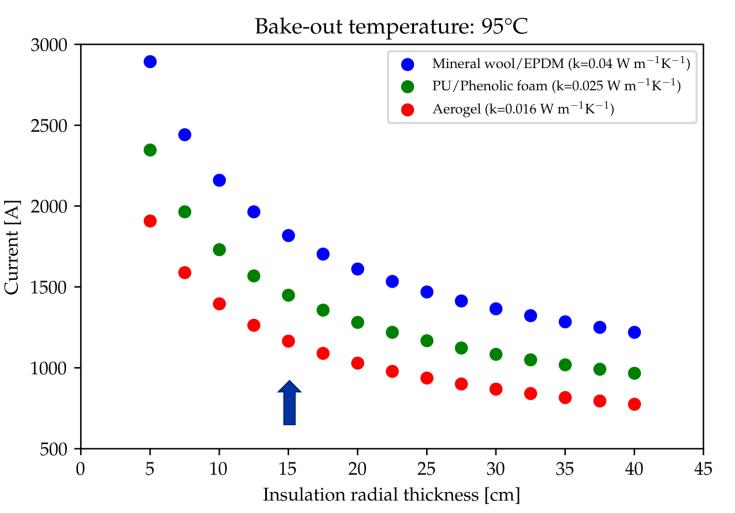
• t_{tube} = 3 mm

For 15 cm of insulation (2G like):

Q [W m⁻¹] \approx 81, 72, 35

Assuming mild steel electrical resistivity** to be ~30% of the SS one:

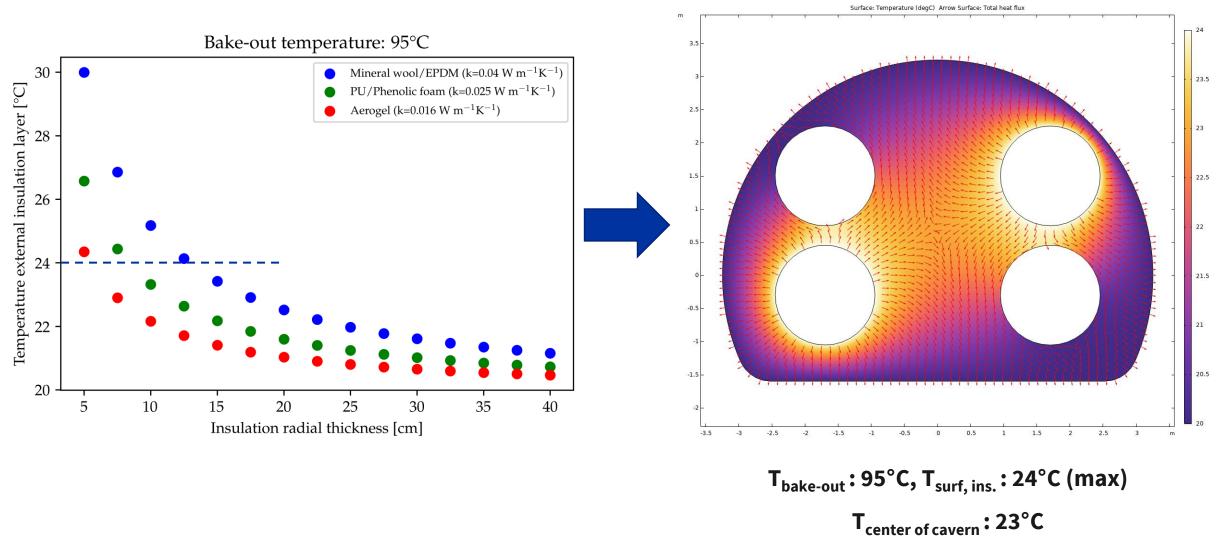
I^{*} [A] ≈ 1820, 1450, 1165



*Only thermal power loss is considered **2.77×10⁻⁷ ohm m @ 95°C



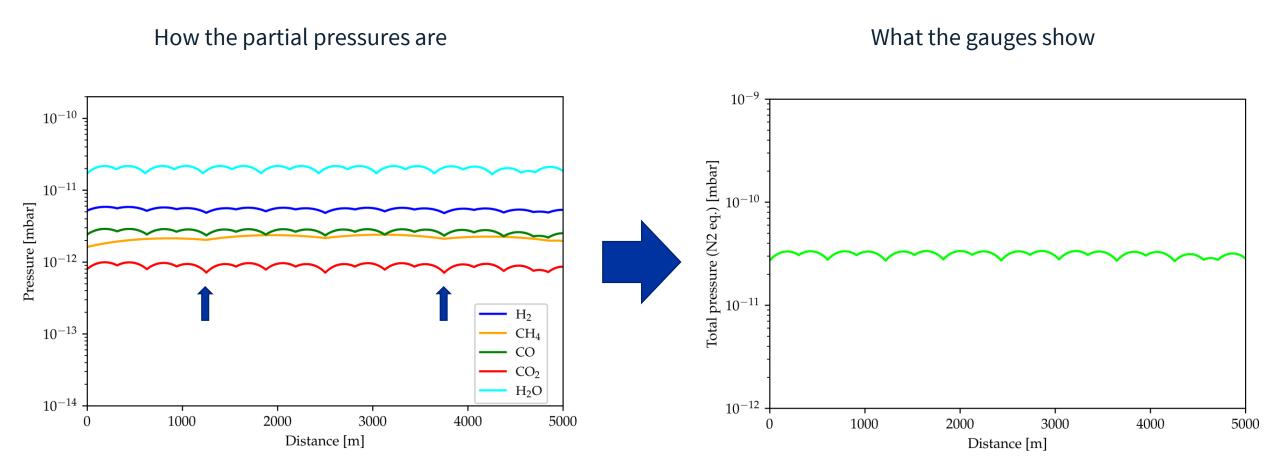
Bake-out: cavern temperature



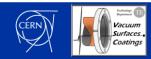


Pressure monitoring

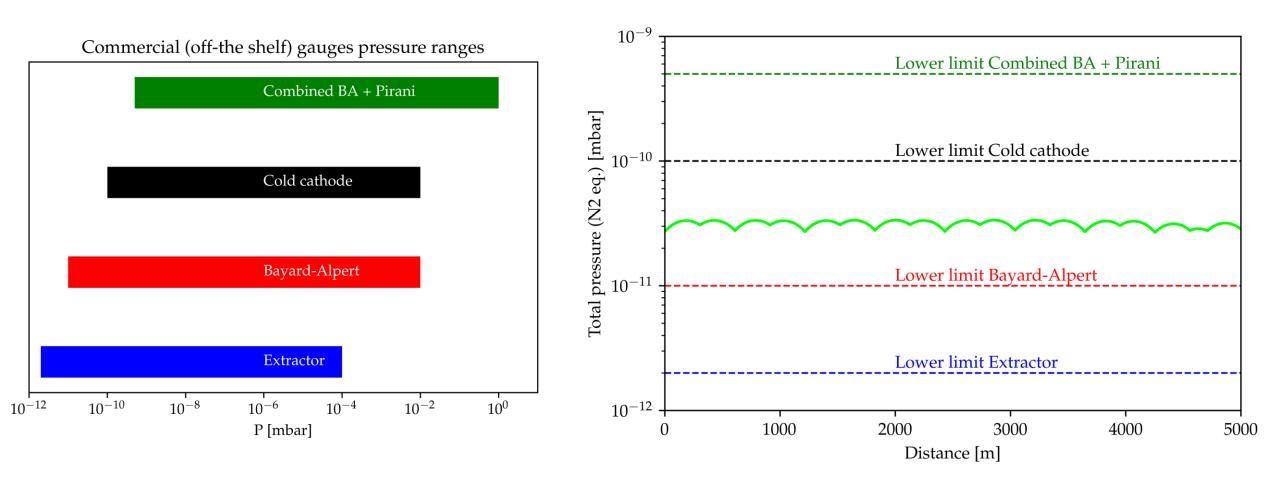
Pressure monitoring: total pressure profile

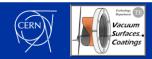


Possible RGAs position (min. 2 RGA/sector). Allocation strategy under evaluation.

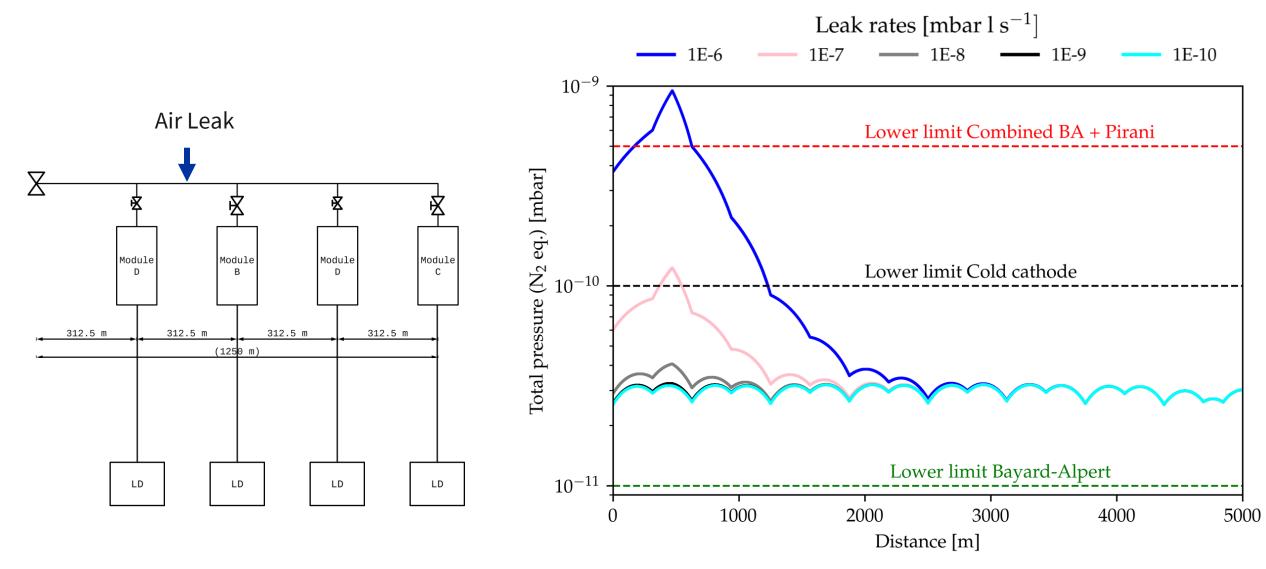


Pressure monitoring: total pressure profile vs. gauge limits





Air leak: impact on total pressure





Vacuum system cost assessment

Vacuum system cost assessment (hardware only)

Assuming market prices as of 2023, in absence of a specific contract:

Component	Quantity (+ spare)	Estimated cost [k€/unit]	Estimated ET total cost [k€]
Gate valve (DN1000 or) DN1250	36	200 - 250	7200 – 9000
Rough pumping group	3 (+3)	50	300
Mobile pumping group (TMP + PP, module A)	18 (+4)	50	1100
2000 ls ⁻¹ NEG (module A, B, C)	312 (+8)	15	4800
500 ls ⁻¹ lon pump (module C)	72 (+8)	6.5	520
1000 ls ⁻¹ NEG (module D)	192 (+8)	5.5	1100
Gate valve DN150 (Viton - all metal)	168 (+8)	10 - 25	1760 - 4400
Gate valve DN100 (Viton - all metal)	192 (+8)	5 - 15	1000 - 3000
Angle valve DN40	360 (+10)	1	370
RGA	48-72 (+4)	10	520 - 760
Gauges (Bayard-Alpert)	360 + (10)	0.7	260
Leak detector	18 (+6)	15	360
Miscellaneous (bolts, gaskets, flanges)	-	-	500



Vacuum system cost assessment (hardware only)

Assuming market prices as of 2023, in absence of a specific contract:

Component	Quantity (+ spare)	Estimated cost [k€/unit]	Estimated ET total cost [k€]
Gate valve (DN1000 or) DN1250	36	200 - 250	7200 – 9000
Rough pumping group	3 (+3)	50	300
Mobile pumping group (TMP + PP, module A)	18 (+4)	50	1100
2000 ls ⁻¹ NEG (module A, B, C)	312 (+8)	15	4800
500 ls ⁻¹ lon pump (module C)	72 (+8)	6.5	520
1000 ls ⁻¹ NEG (module D)	192 (+8)	5.5	1100
Gate valve DN150 (Viton - all metal)	168 (+8)	10 - 25	1760 - 4400
Gate valve DN100 (Viton - all metal)	192 (+8)	5 - 15	1000 - 3000
Angle valve DN40	360 (+10)	1	370
RGA	48-72 (+4)	10	520 - 760
Gauges (Bayard-Alpert)	360 + (10)	0.7	260
Leak detector	18 (+6)	15	360
Miscellaneous (bolts, gaskets, flanges)	-	Total cost: ~20 – 25 M€	



Considerations

- Sector can be pumped from **1013 mbar to 10⁻¹¹ mbar ≈ 6 weeks using compact products**.
- NEG assisted low temperature bake-out represents a viable solution and could have a positive impact on running and installation costs.
- Some insulation options (thin walled) could ease the installation and exploit the performances of the bake-out while keeping the cost under control.
- Pressure monitoring devices needs to be chosen carefully to balance the need of pressure reading, accidental phenomena, costs and controls.
- The costs of the vacuum system hardware could be reduced through further optimization of component selection and specific quotations/contracts.
- Any parameter change (material, bake-out temperature, etc.) can be easily applied since the model is parametric.





Thank you for your attention!

home.cern