

Beam Pipes for Gravitational Wave Telescopes
23-27 March 2023, Geneva.

Leak Detection: component production to system installation

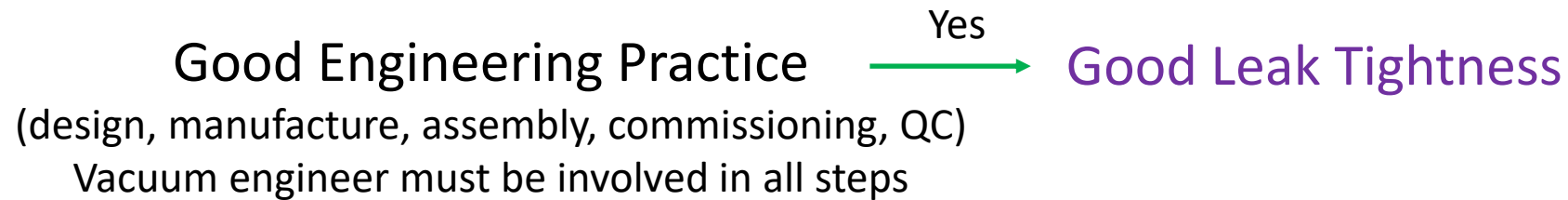
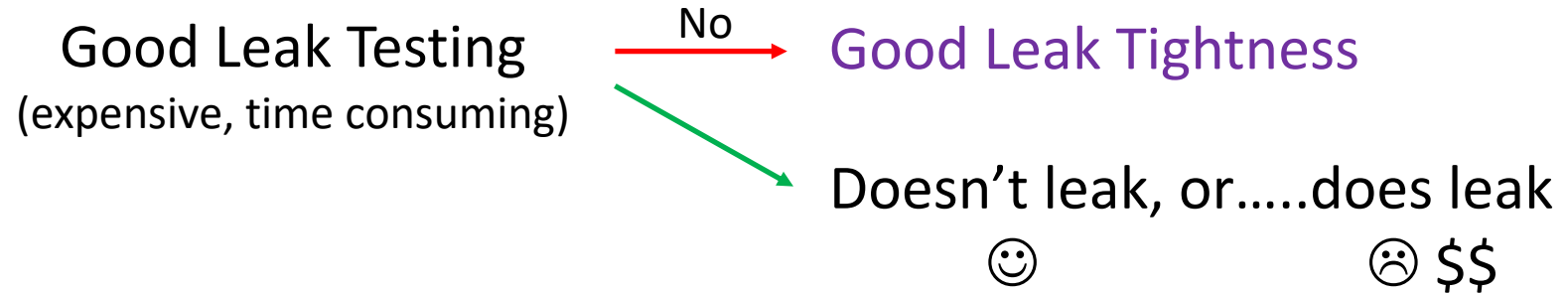
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with inputs from P. Chiggiato, A. Grimaud, W. Maan, J. Perez Espinos, C. Scarcia, J. Somoza Ferreira

Outline

- Introduction
- Testing considerations & strategies
- Testing without flanges
- Cost (gu)estimates
- Summary

Opening Remarks....



Gravitation Wave Telescopes are a new adventure for us so please guide us as much as possible !

LHC Insulation Vacuum

- A few numbers.....

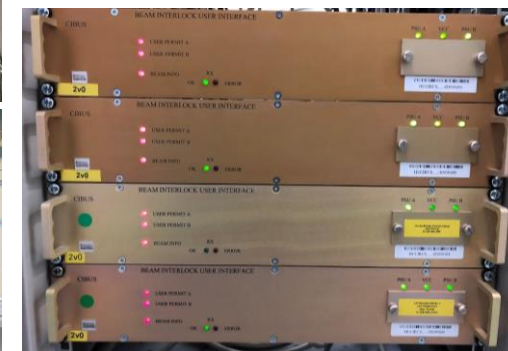
Characteristic	Quantity for LHC machine & distribution line (QRL)
Insulation vacuum system length	22,4 km & 25 km
Welds	~ 200 000 (> 60 000 in-situ)
Weld length	~ 100 000 m
Elastomer joints	~ 18000
Elastomer joint length	~ 22 000 m
Multi-layer insulation	~ 9 000 000 m ² or 200 m ² /m of cryostat
Vacuum subsectors	234
Vacuum subsector length	214 m (machine) & 428 m (QRL)
Vacuum subsector volume	~ 80 m ³
Fixed turbo pumps	178
Nominal turbo pumping speed	0,25 l/s/m of cryostat
Fixed vacuum gauges	974
Mobile turbo pumping groups	36
Mobile primary pumping groups	36



Machine	Type	Year	Energy	Bakeout	Pressure [mbar]	Length
Linacs, Booster, ISOLDE, PS, n-TOF and Antimater						2.6 Km
Linac 4	linac	2018	160 MeV	ion pumps	10^{-7}	40 m
ISOLDE	electrostatic	1992	60 keV	—	10^{-6}	150 m
REX-HIE ISOLDE	linac	2001-2016	5.5 MeV/u	partly	10^{-7} - 10^{-12}	50 m
MEDICIS		2017	—	—	10^{-6}	10 m
Linac 3	linac	1994	4.2 MeV/u	ion pumps	10^{-8}	30 m
LEIR	accumulator	1982/2005	72 MeV/u	complete	10^{-12}	78 m
PSB	synchrotron	1972-2020	1-2 MeV	ion pumps	10^{-9}	157 m
PS	synchrotron	1959	26 GeV	ion pumps	10^{-9} - 10^{-10}	628 m
AD	decelerator	1999	100 MeV	complete	10^{-10}	182 m
ELENA	decelerator	2016		complete	10^{-12}	31 m
PS to SPS TL	transfer lines	1976	26 GeV	—	10^{-8}	1.3 km
SPS complex						15.7 Km
SPS	synchrotron	1976	450 GeV	extractions	10^{-9}	7 km
SPS North Area	transfer line	1976		—	10^{-3} - 10^{-8}	1.2 km
SPS HiRadMat		2011		—	10^{-8}	1.4 km
SPS to LHC TL		2004/06		—	10^{-8}	2 x 2.7 km
AWAKE		wakefield acc		2017	—	10^{-8}
LHC						109 Km
LHC Arcs (Beam vacuum)	collider	2007	2 x 7 TeV	complete	$<10^{-8}$	50 km
LHC Arcs (insulation vacuum)						50 Km
LSS RT separated beams						2 x 3.2 km
LSS RT recombination						570 m
Rxperimental areas						180 m
Beam dump lines TD62/68	transfer lines	2006	7 TeV	—	10^{-8}	2 x 720 m
				High Vacuum		≈ 12
				UHV-XHV		≈ 65
				Insulation vacuum		≈ 50
						≈ 127 km



Vacuum of CERN's accelerators



Typical ET Build Sequence

Arm Vacuum - System Total length (m)	120000
Arm Vacuum - System length (m)	10000
Arm Vacuum - Vacuum Sector length (m)	5000
Arm Vacuum - Pipe String length (m)	312.5

- Components: Manufacture ‘Pipes’ & ‘Pumping Modules’
 - Inspect, clean, condition?, **helium leak test**, vacuum characterisation?, wrap?,
- Assemblies: Weld Pipes into x00 m ‘Strings’
 - Inspect, clean?, pump, **helium leak test new welds**,
- ‘Vacuum Sector’: Weld ‘Pumping Modules’ between ‘Strings’
 - Inspect, clean?, instrument, pump, **helium leak test new welds & CF instr flanges**, bake, global tests.

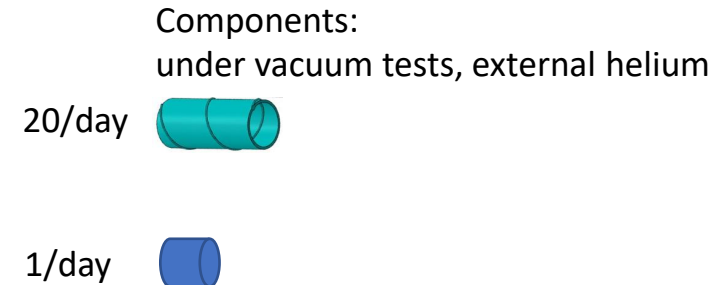
What leak test delivery rates to achieve ? I’ve assumed a 2 yr build period, ~ 400 working days.

Vacuum System Item	Qty	Leak tests/day	
		Factory	On-site
Arm Pipe (15m unit length, Ø 1.2 m)	8000	20/day	
Arm Pumping Module (1m unit /312.5m)	385	~ 1/day	
Arm Pipe String (312.5m lengths)	384		~ 1/day
Arm Vacuum Sectors (5000 m length)	24		~1/month

Leak Testing: What could leak ?

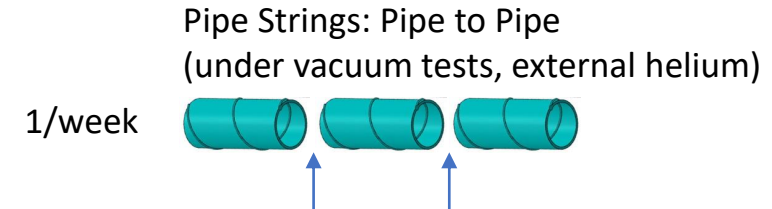
- Ex-situ (components)

- 15m Pipe
 - longitudinal weld (spiral or straight)
 - circumferential welds (if any)
 - material through-wall defects (porosity, inclusions, damage, weld arc errors, ..)
- 1 m Pumping Module
 - welds, material defects, flange NC,...



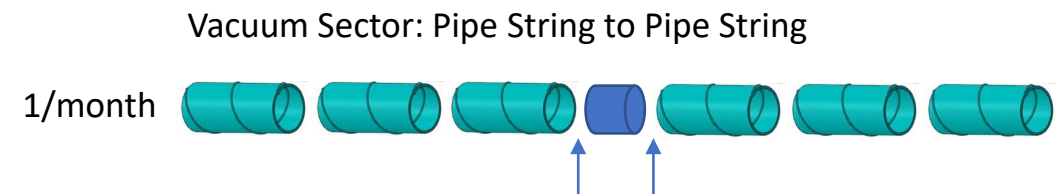
- In-situ (x00 m Pipe Strings)

- Pipe to Pipe circumferential welds
- Degradation of validated components (transport, corrosion, etc)



- In-situ (5 km Vacuum Sector)

- Pipe to Pumping Module circumferential welds
- Vacuum Instrumentation CF flange connections



Leak Testing Considerations

- ⇒ Assume manufacture/installation in 400 working days.
- ⇒ Use COTS vacuum equipment – mobile pumping groups, MSLD, etc.

Big infrastructure cost
& space needs

$$\tau = \frac{V(\text{liters})}{S_{\text{eff}}(\text{liters / s})}$$

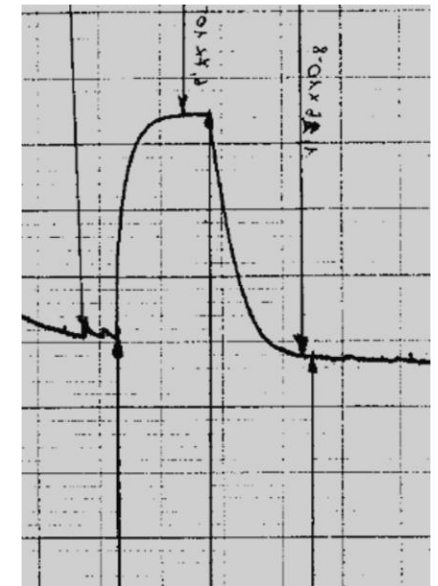
Vacuum System Item	Qty	Leak tests/day		Volume (m3)	Time constant (s) (with Seff 1000 l/s)
		Factory	On-site		
Arm Pipe (15m unit length, Ø 1.2 m)	8000	20/day		~ 15	~ 15
Arm Pumping Module (1m unit /312.5m)	385	~ 1/day		~ 1	~ 1
Arm Pipe String (312.5m lengths)	384		~ 1/day	~ 312	~ 312
Arm Vacuum Sectors (5000 m length)	24		~1/month	~ 5000	~ 5000

S_{eff} needs to be in
~ 10000 l/s range

Assume target tightness: 10^{-10} mbarl/s per component (yes?)

Signal rise time
(& recovery time)
needs to be considered

$$P_{\text{He}} = \frac{q}{S_{\text{eff}, \text{He}}} \left(1 - e^{-\frac{t}{(V / S_{\text{eff}, \text{He}})}}\right)$$



$$P_{\text{He}} = \frac{q}{S_{\text{eff}, \text{He}}} \left(e^{-\frac{t}{(V / S_{\text{eff}, \text{He}})}}\right)$$

Leak Testing: Strategy Options

Leak Test Strategy	Fixed Costs (std tests)	Variable Costs (leaks)
'Max' Testing Strategy (classic, preventive approach)	Ex-situ: 100 % Component leak test (\$\$\$), In-situ: 100 % Subsector leak test(\$\$), In-situ: Vacuum Sector leak test (\$),	NC localisation, repairs & retest (\$) NC localisation, repairs & retest (\$) NC localisation, repairs & retest (\$)
'Mid' Testing Strategy	In-situ: 100 % Subsector leak test(\$\$), In-situ: Vacuum Sector leak test (\$),	NC localisation, repairs & retest (\$\$) NC localisation, repairs & retest (\$)
'Min' Strategy (corrective approach)	In-situ: Vacuum Sector test (\$)	NC localisation, repairs & retest (\$\$\$)

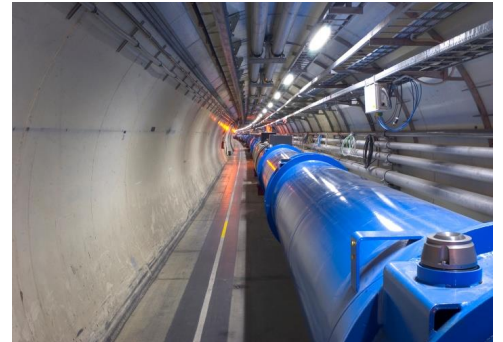
Max, Mid or Min approach ?

Leak Test Strategy will depend on:

- ⇒ How many leak we expect to get (past experience from similar projects),
- ⇒ Fixed cost of 100% component test vs Variable costs of leak repairs in-situ
- ⇒ Solutions for in-situ leak localization
- ⇒ Solutions for in-situ leak repairs
- ⇒ Other constraints eg all 8000 Pipes need individual insulation/bakeout/vacuum characterized before installation ?
- ⇒ Approach can be changed/tailored during execution.....

How many leaks ?

- LIGO experience on 20 m Pipes (report P990023-00-B)
 - Auto welding \Rightarrow visual inspection (plus x-ray or US ?) \Rightarrow manual weld repairs \Rightarrow leak test.
 - **No leaks on ~ 1000 tube/components.** Statistics on in-situ leaks to be gathered
- VIRGO experience
 - Statistics on component & in-situ leaks to be gathered
- LHC experience on insulation vacuum
 - Zero leaks on spiral weld of dipole cryostats (~ 1350 units)
 - Leaks of 1-5 %o welds in overall project $\sim 200k$ welds (auto & manual)
 - 2d inclusions, Cu contamination, poor manual/auto execution, damage, etc.
 - Some leaks only appear during or after cold thermal cycle
- Applying LHC experience to ET Arm Vacuum (120 km)
 - ~ 10000 ex-situ welds \Rightarrow **qty of leaks: 10 – 50 range** ($< 1\%$ of Pipes may leak)
 - ~ 10000 in-situ welds \Rightarrow **qty of leaks: 10 - 50 range** (< 1 leak / km)



Ex-situ Component welds:

8000 Pipes

400 Pump Modules



In-situ Assembly welds:

8000 Pipe-Pipe

800 Pipe-Pump Modules

400 CF flanges

Vacuum Vessel Testing: With/without flanges

ARIA Cryostats without flanges

LHC Cryostats with flanges



Leak Testing without flanges - ARIA experience

(300m tall Ar distillation column)

28 cryogenic pipe elements



29 bellows elements

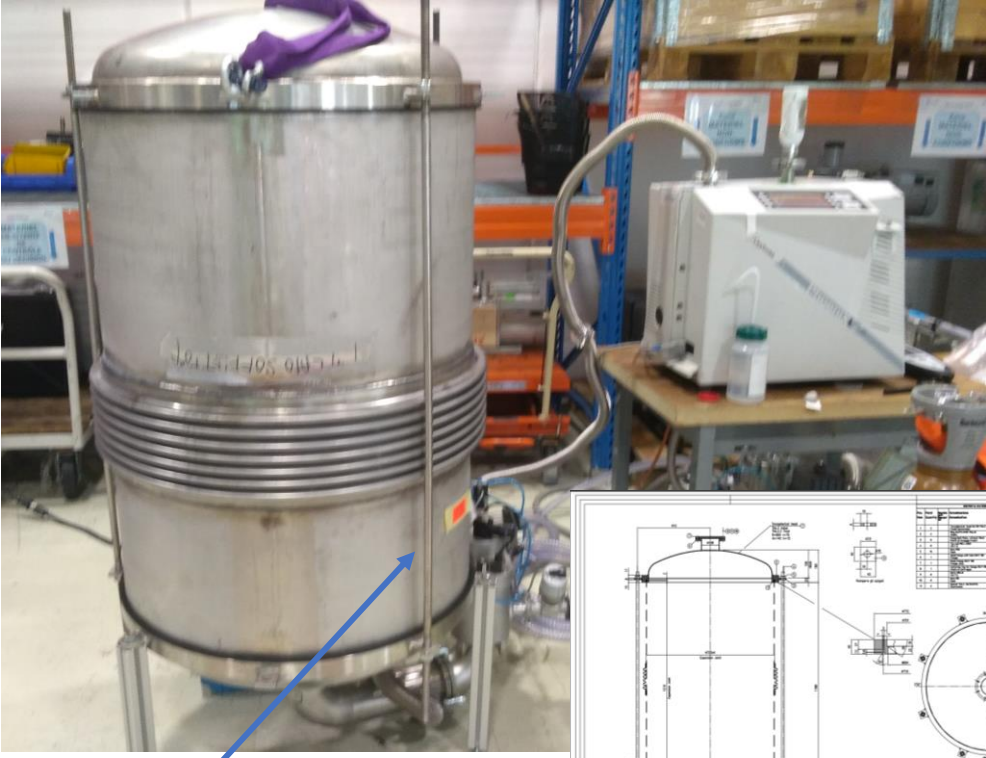


End Sealing without flanges

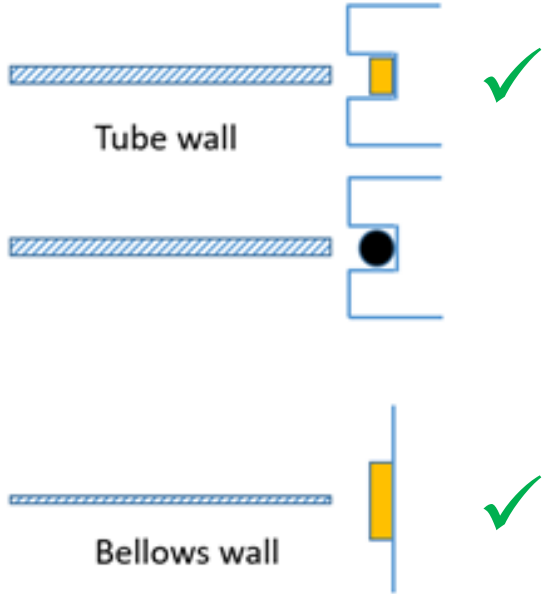
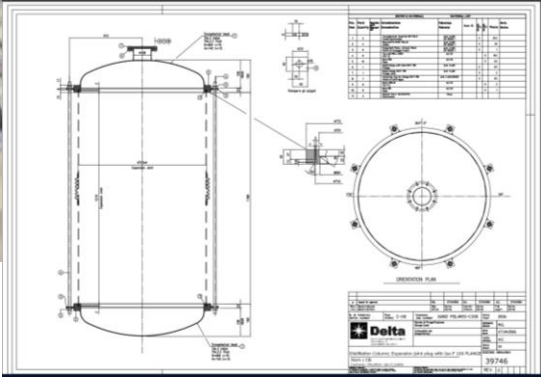
DCM bellow – end flanges



ARIA bellow – Ø723 mm, no flanges, 4 mm wall

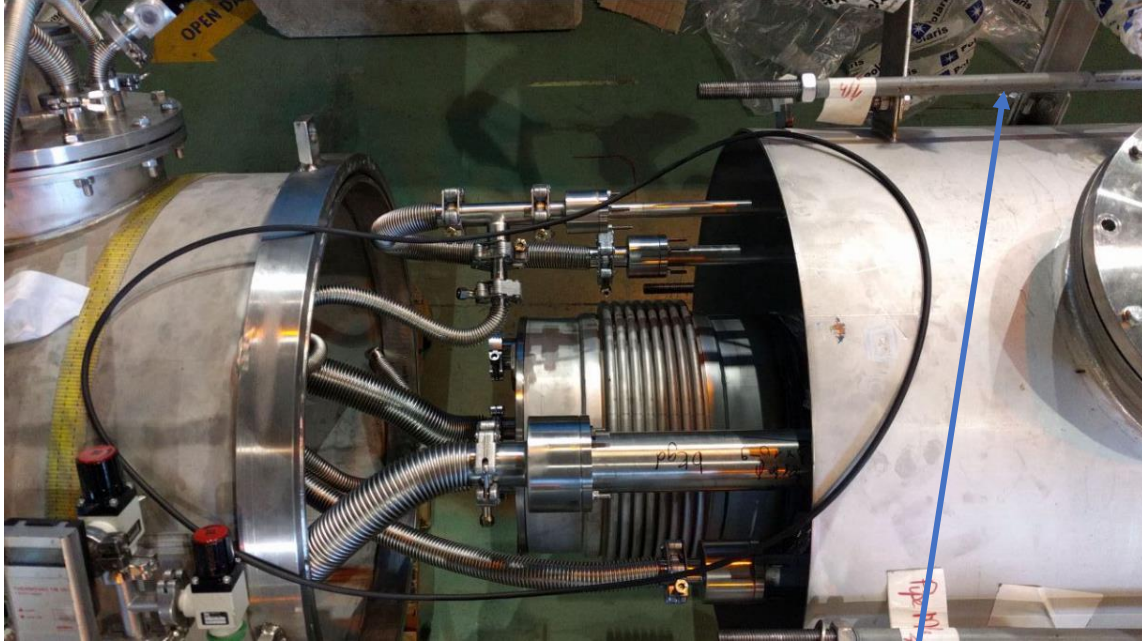


Tie rods

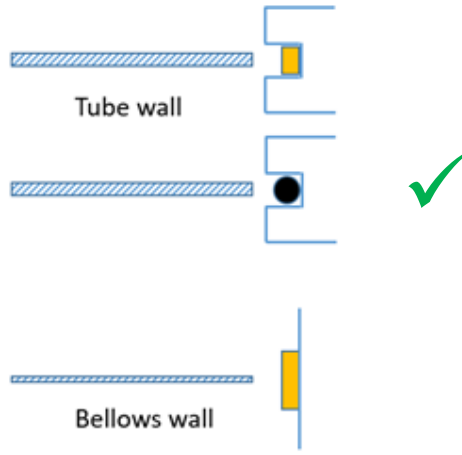


End sealing without flanges

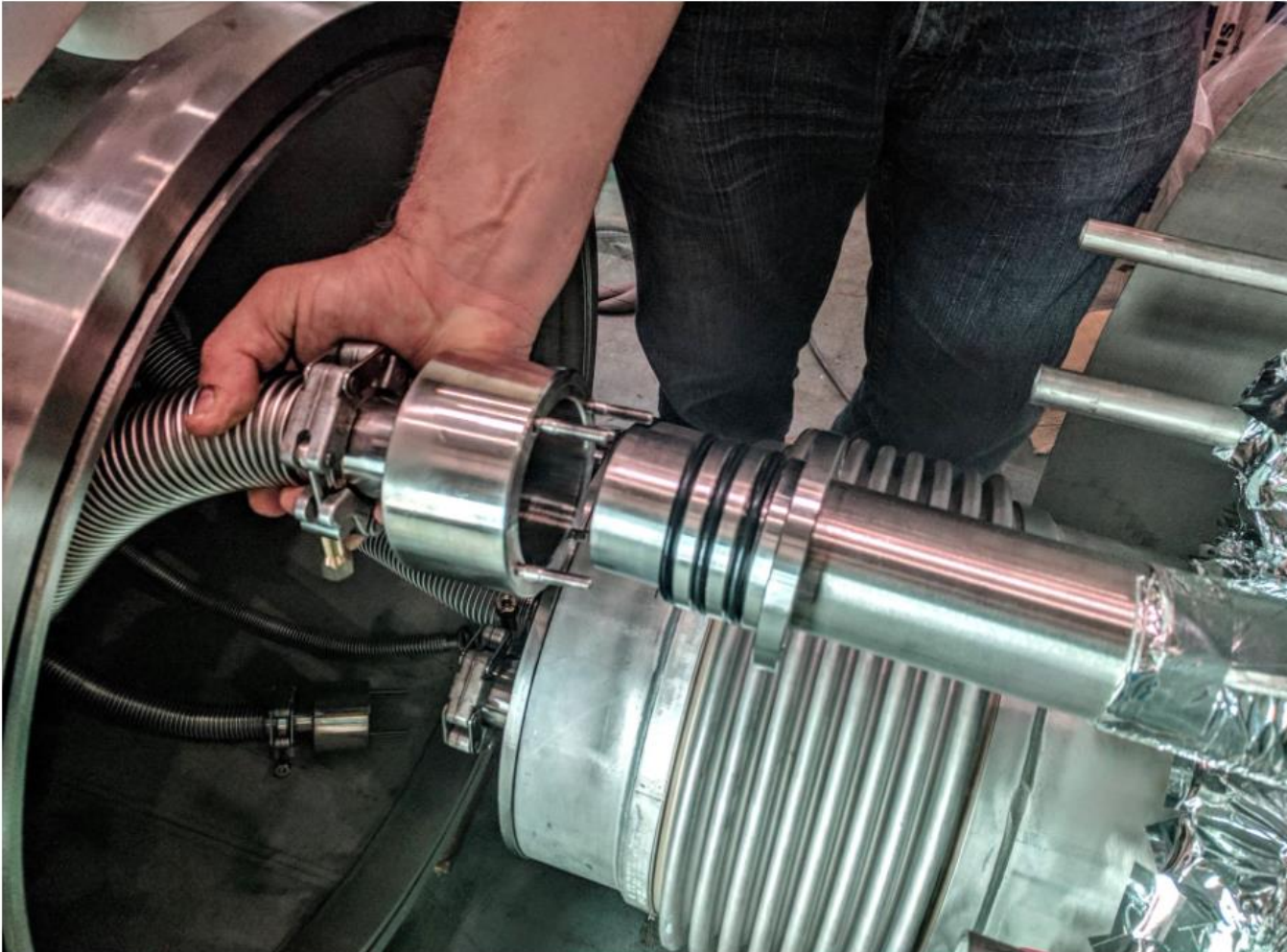
4 mm wall



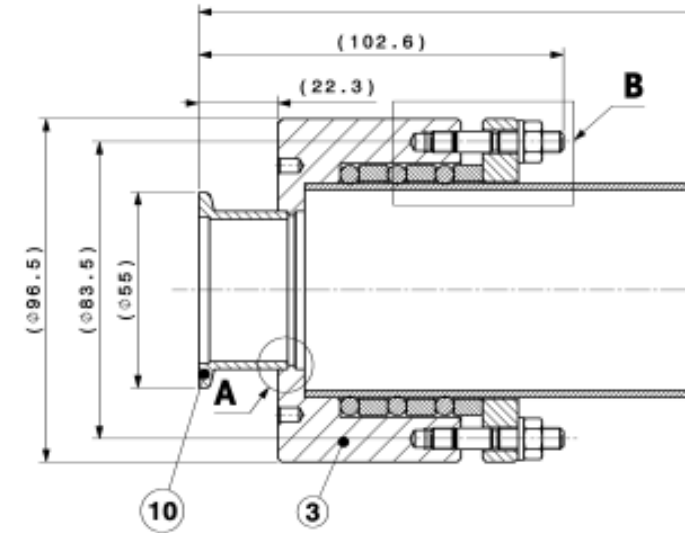
Tie rods



End Sealing – no flanges



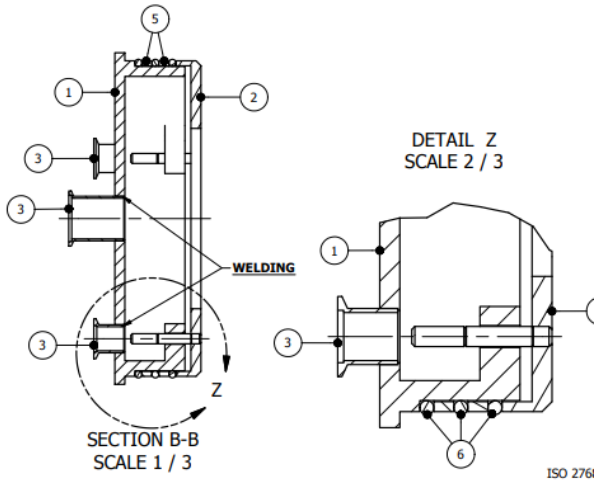
Triplet o-rings to prevent helium permeation



Sealing – no flanges



End plug sealing on internal tube surface



Smoothing of the longitudinal weld seam

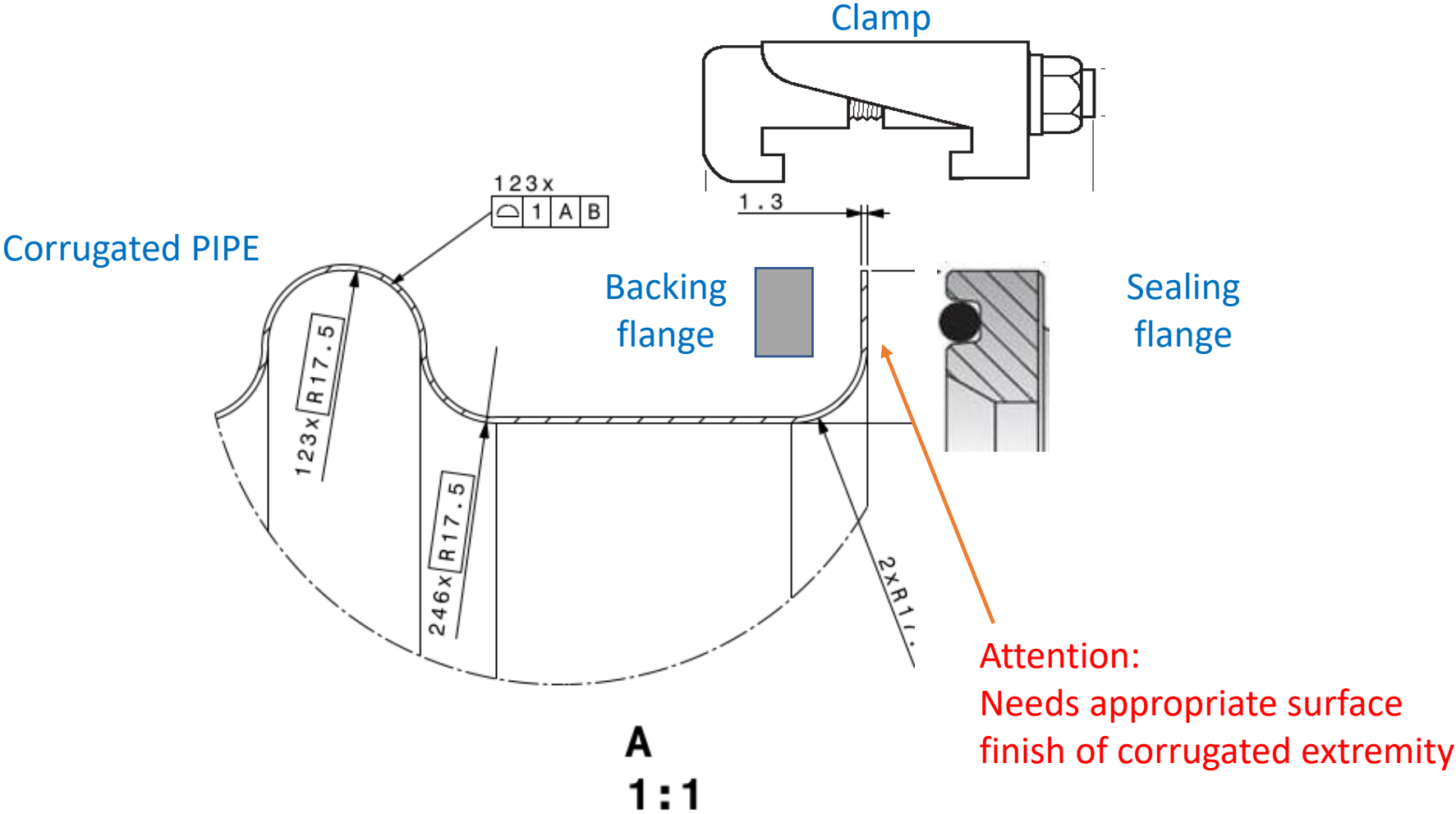


End Sealing – no flanges



Inflatable plug
solution

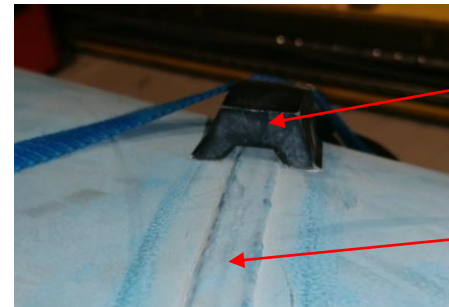
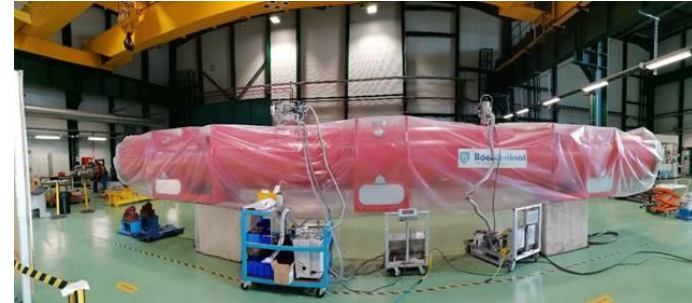
End Sealing – no flanges



Helium delivery during 'under vacuum' testing ?

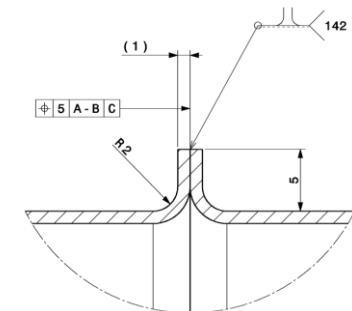
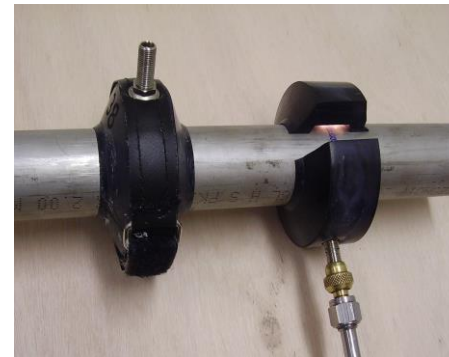
He delivery options:

- ⇒ Jet (not ideal for global test on large volumes)
- ⇒ Total immersion (ext pocket, ext secondary chamber)
 - ⇒ Large helium cost
 - ⇒ Rise in helium background in air
 - ⇒ Complex tooling to recovery helium
- ⇒ Local channel at weld to deliver external helium:
 - ⇒ At longitudinal weld (spiral or straight)
 - ⇒ At circumferential weld
- ⇒ External vacuum clamshell, internal helium
 - ⇒ At Pumping Module circumferential welds
 - ⇒ Helium (jet) delivery thro pumping port



Temporary channel
at the weld bead

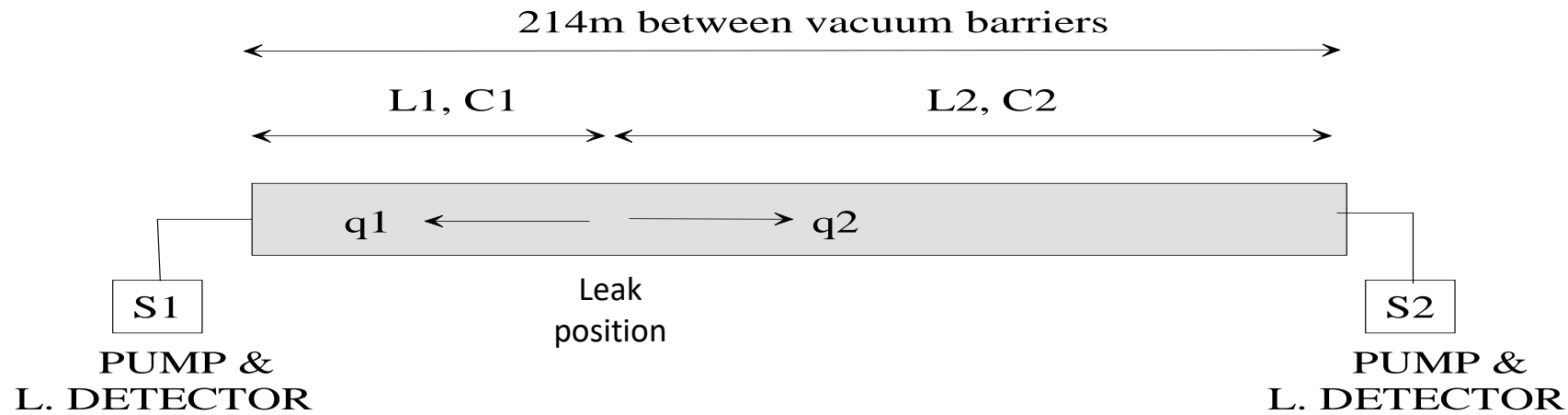
Spiral
weld



Leak localization in Pipe Strings



Method was used for leak localization in LHC internal helium circuits



‘Under vacuum’ leak test in molecular flow conditions:

- 2 identical turbo pumps at each extremity, plus leak detectors
- Helium as tracer gas.
- Measurements are made with system in equilibrium conditions.

Linear conductance of vacuum system, so $C \propto 1/L$

For $S \gg C1$ or $C2$: $q1/q2 \propto C1/C2 \propto L2/L1$

Ratio of He signal arriving at each detector is inversely proportional to its distance from the leak

Leak Testing Costs - Pipes



- Pipes (15m components)

- **Equipment** costs for 2 leak test benches

- 2 benches 60k, 2 pumping systems 100k, 2 leak detectors 40k = **200 kCHF**
- Dedicated facility of 150 m² @ 2 kCHF/m² = **300 kCHF**
(not including land purchase, in/out storage areas, handling, transport logistics, etc)

- **Manpower**

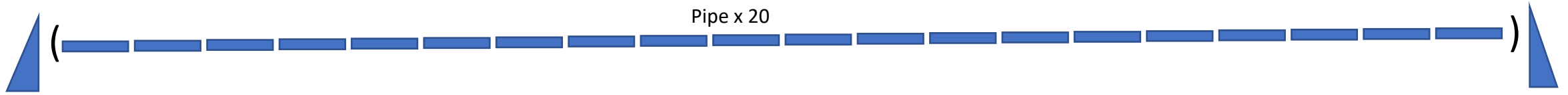
- 2 vacuum technicians producing 2 leak tests/day = **0.5 kCHF/test**
- 2 vacuum technicians localizing 1 leak, repair and retest = **1 kCHF/NC repair & retest**

⇒ 8000 Pipes in 4000 days (2 benches): **500 kCHF & 4000 kCHF (+ NC repair & retest)**

⇒ 8000 Pipes in 400 days (20 benches x 0.5): **2500 kCHF & 2000 kCHF (+ NC repair & retest)**

Effect of scaling & synergies

Leak Testing Costs: Pipe Strings



- Pipes Strings (312 m)

- **Equipment** costs for 1 leak test setup:

- 2 mobile end caps (20k) , 2 mobile fixed points (20k) = 40 kCHF
 - 1 mobile roughing (60k), 2 mobile 700 l/s turbos* (60k), 2 leak detectors (40k) = 160 kCHF



- **Manpower**

- 2 technicians producing 1 leak test/week = 5 kCHF/test
 - 4 technicians localizing 1 leak, repair & retest = 10 kCHF/NC repair & retest

⇒ 400 Pipes Strings, 400 wks:

200 kCHF & 2000 kCHF (+ NC repair & retests)

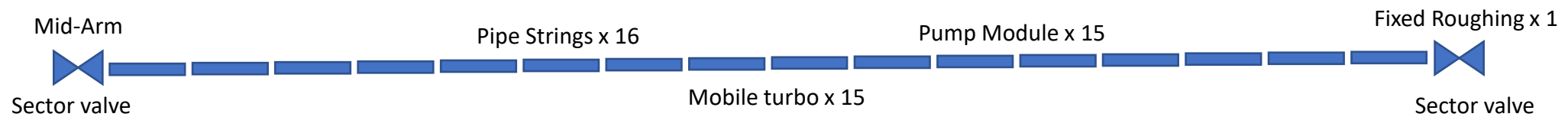
⇒ 400 Pipes Strings, 80 wks (5 setups x 0.5):

500 kCHF & 1000 kCHF (+ NC repair & retests)

Effect of scaling & synergies

*check any double counting

Leak Testing Costs – 5 km Vacuum Sectors



- Pipe Strings (312 m)

- Equipment costs for 1 leak test setup

- 1 fixed roughing unit (0 CHF)
 - 15 mobile 700 l/s turbos* (450 kCHF), 5 leak detectors (100 kCHF)

- Manpower

- 2 technicians producing 1 leak test/month = 20 kCHF/test
 - 4 technicians localizing 1 leak, repair & retest = 40 kCHF/NC repair & retest



⇒ 24 Vacuum Sectors in 24 months: 550 kCHF & 480 kCHF (+ NC repair & retests)

Leak Test Cost v Strategy v Leak Occurrence

To test	Leak test type	Qty	Fixed Cost		Test Strategy			Cost 1 leak (kCHF)	Variable Costs			
			Equipment (kCHF)	Manpower (kCHF)	Max Pipe,String,Sector (kCHF)	Mid String,Sector (kCHF)	Min Sector (kCHF)		1 ‰ leak		10 ‰ leak	
		weld						Qty	Cost (kCHF)	Qty	Cost (kCHF)	
8000 Pipes	Ex-situ Pipe weld	8000	2500	2000	4500			1	8	8	80	80
400 Strings	In-situ Pipe weld	8000	0	1000		1000		10	8	80	80	800
400 Strings	In-situ Pipe-Pipe weld	8000	500	1000	1500	1500		10	8	80	80	800
24 Sectors	In-situ String-String & CF	1200	550	240	790	790		40	1.2	48	12	480
24 Sectors	In-situ Pipe weld	8000	550	480			1030	40	8	320	80	3200
24 Sectors	In-situ Pipe-Pipe weld & CF	8400	550	480			1030	40	8.4	336	84	3360
Total fixed costs (no leaks)					6790	3290	2060					
Variable cost 1 ‰ leak					136	208	656					
Fixed + Variable 1 ‰ leak					6926	3498	2716					
Variable cost 10 ‰ leak					1360	2080	6560					
Fixed + Variable 10 ‰ leak					8150	5370	8620					

Leak Test Cost v Strategy v Leak Occurrence

Max Strategy:

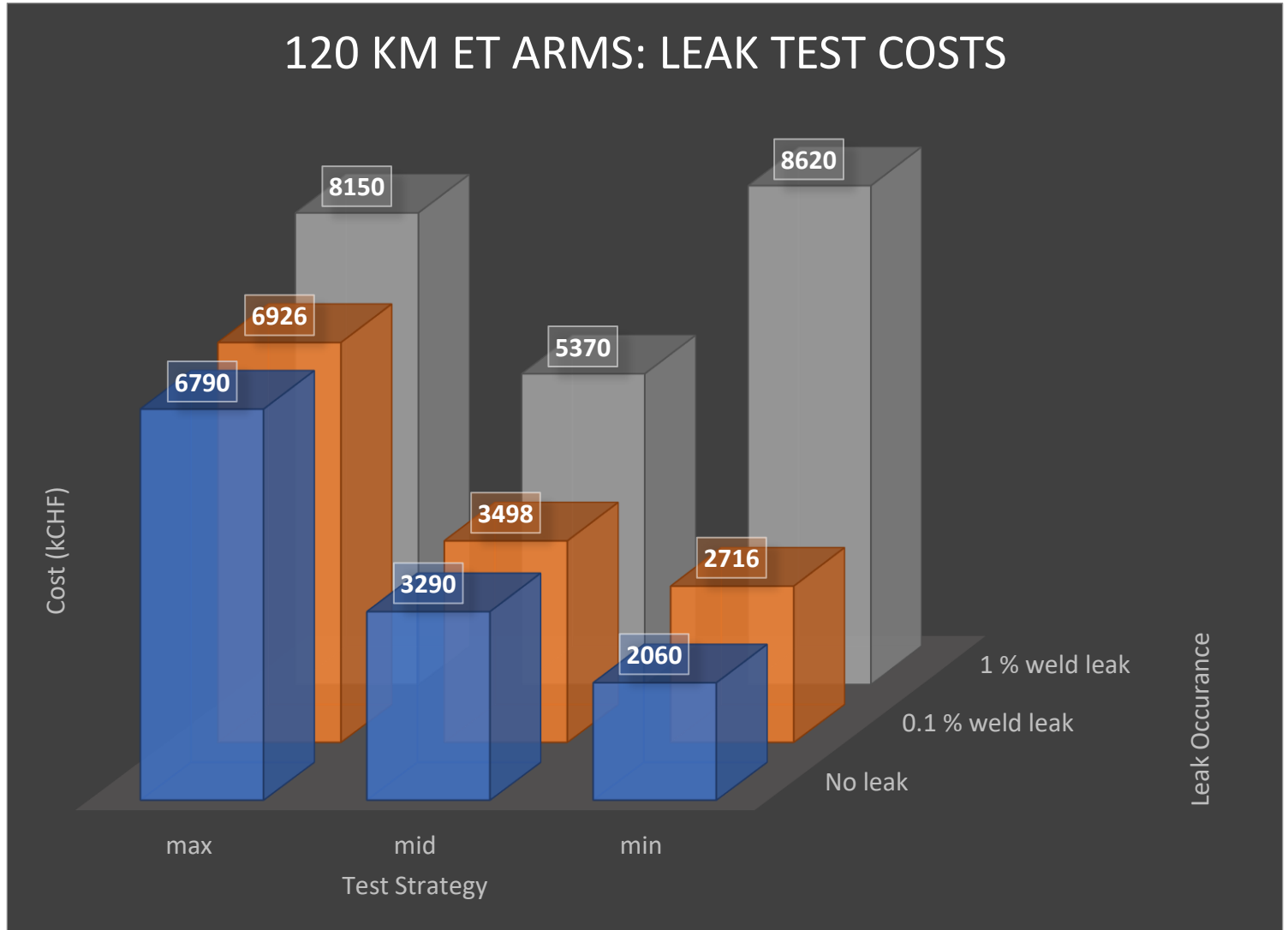
- Low risk
- Early warning of leak issues
- Dominated by component testing costs

Min Strategy:

- High risk (high confidence)
- Dependent on low leak occurrence
- Potential minimum cost

Mid Strategy

- Medium risk
- Higher leak occurrence can be tolerated wrt cost.
- Can review strategy dependent on field results.



ET Leak Test Strategy – brainstorming !

- ⇒ assume leaks in low ‰ range by stringent control on material & welding quality
- ⇒ adopt ‘Mid’ strategy, but with some targeted checking of Pipes as components

- Step 1 – Components, ex-situ

- Leak test first 100 Pipes (eliminate systematics)
- Leak test every 20th Pipe (avoid production deviations, cleanliness check, etc)
- Leak test every Pump Module

100 tests }
~ 400 tests } 6 % Pipes
~ 400 tests }

- Step 2a - 312 m Pipe Strings, in-situ

- Pump & leak test longitudinal & circumferential Pipe welds

~ 400 tests

- Step 2b - 5000 m Vacuum Sector, in-situ

- Clamshell test Pipe to Pumping Module welds
- Pump & leak test fully equipped Sector prior to bakeout

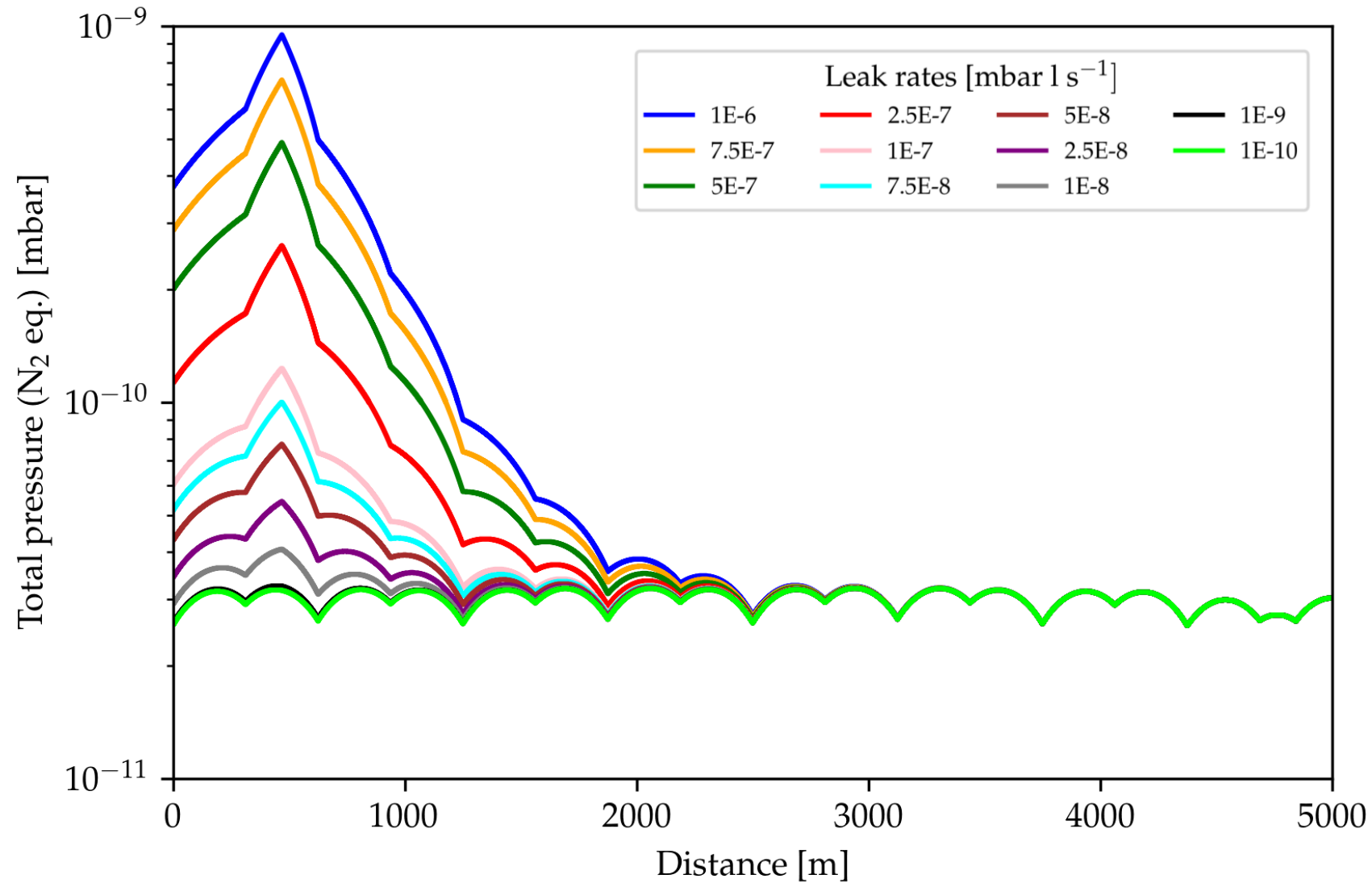
24 tests

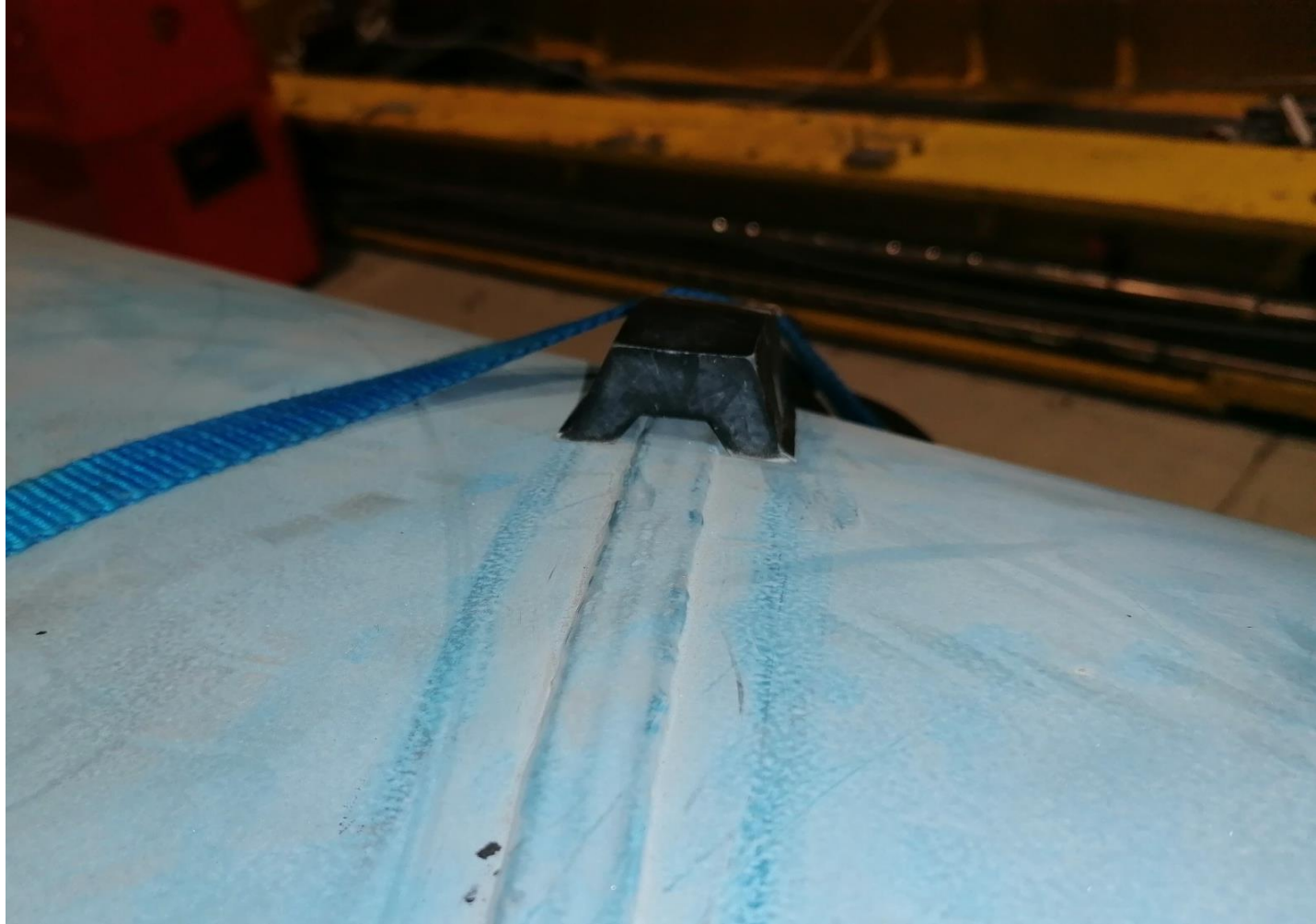
Summary

- Good engineering is better than good leak detection.
- We can build upon the leak testing experience (good & bad) from existing GWD and LHC type accelerators.
- Standard leak testing equipment and methods can be applied, but care must be taken with large volumes.
- Different leak testing strategies can be considered – each has its merits and drawbacks with respect to duration, cost, risk.....and we need to remain flexible based on return of experience.
- Testing strategy will strongly depend on the Pipe manufacturing & installation techniques, together with our confidence level wrt to leak occurrence
- Solutions exist to close vacuum vessels without flanges.
- Cost (gu) estimates should be considered as a starting point for discussions. Need to check double counting of vacuum equipment costs eg mobile pumping groups already included elsewhere.
- There are no showstoppers, so “[Let’s get to work.....](#)” on more brainstorming.

Thanks for your attention !

Air leak: impact on total pressure





Duration(days)	312 m String - leak test activities			
	1 installation temporary end caps, fixed points, mobile pumping systems			
	1 roughing (Saturday)			
	1 turbo (Sunday)			
	1 leak test (including system calibration)			
	1 leak test			
	1 margin, problem solving,			
	1 vent, removal fixed points, transport to next test zone			
	7			
Duration (days)	5 km Vacuum Sector - leak test activities			
	4 Clamshell test of each Pump Mod weld			
	6 Roughing (8 edays), moile pumping groups			
	3 Turbo pumping			
	5 Leak test (including system calibration)			
	1 Margin, problem solving,			
	2 Mobile equipment removal, transfer to next zone			
	21			

Leak Testing Cost Estimate – Pumping Modules

- Pumping Modules (1m components)
 - **Equipment** costs for leak test bench
 - 1 bench 40k, 1 pumping system 40k, 1 leak detector 20k = **100 kCHF**
 - **Manpower**
 - 1 vacuum technician producing 1 leak test/day = **0.5 kCHF/test**
- ⇒ 400 Pumping Modules in 400 days: **100 kCHF & 200 kCHF (+ 1% NC)**

