

Helium Cryostats for Superconducting Devices

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- Helium cryostats for SC devices, functions and requirements
- Examples of cryostats
- Mechanical design and construction of cryostats:
 - Materials for cryostats and their properties
 - Pressure/vacuum vessels, codes, and norms
 - Supporting systems
- Heat transfer mechanisms at cryogenic temperatures:
 - Thermal radiation and thermal design solutions (thermal shielding, MLI)
 - Thermal conduction and thermal design solutions (feedthroughs, heat intercepts)
- Notions of cryogenic safety
- Calculation tool: Cryostat Toolbox v.1.1



1 h

1 h

1 h



Mechanical design and construction of cryostats

Materials in cryostats

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- Helium tank (for SC device, ph.separator, etc.):
 - ✓ austenitic st.steels (Fe-Cr-Ni): 304L(1.4307), 316L(1.4404), 316LN
 - ✓ titanium alloys (Grade 7, Grade-5 (Ti-6AI-4V)) in SRF
- Internal (cold) supporting system
 - ✓ Composites (e.g. GFRE, CFRP, ULTEM)
 - ✓ St.steel, titanium alloys (tie rods)
- Thermal shielding:
 - ✓ aluminum alloys (series 5xxx, 6xxx, 7xxx)
 - ✓ Copper (Cu OF, Cu OFE)
- Vacuum vessel:
 - ✓ Low carbon steels (e.g. DIN GS-21 Mn5)
 - ✓ st.steels (304L)
- Cryogenic piping and expansion joints (bellows):
 - ✓ st.steel (304L)
 - ✓ Cu (HX tubes)
- RF Couplers/HOM (for SRF):
 - ✓ St.steel Cu plated, Nb, ceramics, etc.
- Current leads (for SC magnets)
 - ✓ Cu, HTS, st.steel, elect. insulating (Kapton), thermal insulating (G10),etc.
- Magnetic shielding (for SRF, as needed)
 - ✓ µ-metal, Cryoperm®, etc.

Useful material standards for cryostats



Plates and sheets	•	EN 10028-1:2007+A1:2009 Flat products made of steels for pressure purposes - Part 1: General requirements		
	•	EN 10028-3:2009 Flat products made of steels for pressure purposes - Part 3: Weldable fine grain steels, normalized		
	•	EN 10028-7:2007 Flat products made of steels for pressure purposes - Part 7: Stainless steels		
Tubes	•	EN 10216-5:2004 Seamless steel tubes for pressure purposes - Technical delivery conditions - Part 5: Stainless steel tubes		
	•	EN 10217-7:2005 Welded steel tubes for pressure purposes - Technical delivery conditions - Part 7: Stainless steel tubes		
Forged blanks	•	EN 10222-1:1998 Steel forgings for pressure purposes - Part 1: General requirements for open die forgings		
	•	EN 10222-5:1999 Steel forgings for pressure purposes - Part 5: Martensitic, austenitic and austenitic-ferritic stainless steels		
Castings	•	EN 10213:2007 Steel castings for pressure purposes		
Pipe fittings	•	EN 10253-4:2008 Butt-welding pipe fittings - Part 4: Wrought austenitic and austenitic-ferritic (duplex) stainless steels with specific inspection requirement		
Bars	•	EN 10272:2007 Stainless steel bars for pressure purposes		
Aluminium	•	EN 12392:2000 Aluminium and aluminium alloys - Wrought products - Special requirements for products intended for the production of pressure equipment (choose materials included in the list given in EN 13445-8 section 5.6)		

Relevant mechanical failure mechanisms in cryostats



• Helium tanks:

- ✓ Rupture (rare!) or permanent deformation due to excessive mechanical stress (pressure loads)
- ✓ Helium leaks in welds or material micro-crack
- Cryogenic lines/expansion joints:
 - ✓ Buckling of expansions joints with or without rupture/leaks
 - ✓ Helium leaks in welds or material micro-crack
- Vacuum vessels:
 - ✓ Buckling under external pressure
 - ✓ Permanent deformations due to excessive stress concentrations

• Internal supporting systems:

- ✓ Failure due to excessive mechanical stress
- $\checkmark\,$ Failure due to thermo-mechanical stress
- \checkmark Buckling under compressive load
- Thermal shields:
 - ✓ Permanent deformation due to thermo-mechanical stress (CD/WU transients)
- Alignment jacks:
 - ✓ Break of floor/fixations due to excessive load

Tensile test material properties



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Ductile vs. brittle





Low temperature effect of tensile properties





- Ductile materials tend to become brittle (fragile) at cryogenic temperatures
- Increase of the yield and ultimate strength
- Young modulus also (marginally) increases.

Mechanical Properties at cryogenic temperatures

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- Yield, ultimate strength
 - ✓ Yield and ultimate strengths increase at low temperature





Mechanical Properties at cryogenic temperatures (cont.d)



Young modulus

• Fracture toughness



From: Technique de l'Ingénieur

Thin shells under external pressure

Buckling:

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- Non-linear phenomenon. Actual critical pressure depends on initial imperfections: Safety factor needed!
- Buckling critical pressure for a thin tube of infinite length

$$p_{cr} = \frac{E}{4(1-v^2)} \left(\frac{t}{r}\right)^3$$

Alternatively, we need to add reinforcements (e.g LHC vessels, t=12 mm)

• A conservative rule of thumb for stainless steel tubes under vacuum:

$$\frac{t}{r} \ge \sqrt[3]{\frac{0.1MPa \times 4 \times (1 - 0.3^2)}{200 \times 10^3 MPa}} = 0.012$$

• If we use a safety factor of 3:

$$\frac{t}{r} \ge 3.7\%$$

Example:

- r = 500 mm
- t > 18.5 mm



Thin shells under internal pressure

For preliminary calculation For detailed calculation see EN 13458-2 Cryogenic vessels – static vacuum insulated vessels

valid for $r \ge 10t$



Example: cyl.helium tank

- r = 400 mm
- p = 4 barg (0.4 MPa)
- σ_a= 160 MPa (304L, Rp_{0.2}= 240 MPa, SF=1.5)
- t ≥ 1 mm

(Note: under vacuum (previous calculation) \rightarrow t \geq 15 mm !)

Pressure vessel codes regulations

- Pressure European Directive 2014/68/EC (PED) is a legal obligation in the EU since 2002
 - Applies to internal pressure ≥ 0.5 bar gauge
 - Vessels must be designed, fabricated and tested according to the requirements defined
 - Establishes the conformity assessment procedure depending on the vessel category, which depends on the stored energy, expressed as Pressure x Volume in bar.l



For vessels with non-dangerous gases (cryogenic liquids are treated as gas)

Category	Conf. assessment module	Comment
SEP	None	The equipment must be designed and manufactured in accordance with sound engineering practice. No CE marking and no involvement of notified body.
I	А	CE marking with no notified body involvement, self-certifying.
II	A1	The notified body will perform unexpected visits and monitor final assessment.
III	B1+F	The notified body is required to approve the design, examine and test the vessel.
IV	G	Even further involvement of the notified body.





Harmonised codes and standards

 Harmonised standards give presumption of conformity with the PED, within their scope. Useful codes for cryostat design and fabrication, including safety devices:

Standard	Title
EN 764-5	Pressure equipment – Part 5: compliance and inspection documentation of materials
EN 764-7	Pressure equipment – Part 7: safety systems for unfired pressure vessels
EN 1251	Cryogenic vessels – Transportable vacuum insulated vessels of not more than 1000 litres volume
EN 1252	Cryogenic vessels – Materials
EN 1626	Cryogenic vessels – Valves for cryogenic service
EN 1797	Cryogenic vessels – Gas/material compatibility
EN 12213	Cryogenic vessels – Methods for performance evaluation of thermal insulation
EN 12300	Cryogenic vessels – Cleanliness for cryogenic service
EN 12434	Cryogenic vessels – Cryogenic flexible hoses
EN 13371	Cryogenic vessels – Couplings for cryogenic service
EN 13445	Unfired pressure vessels
EN 13458	Cryogenic vessels – Static vacuum insulated vessels
EN 13480	Metallic industrial piping
EN 13530	Cryogenic vessels – Large transportable vacuum insulated vessels
EN 13648	Cryogenic vessels – Safety devices for protection against excessive pressure
EN 14197	Cryogenic vessels – Static non-vacuum insulated vessels
EN 14398	Cryogenic vessels – Large transportable non-vacuum insulated vessels
EN 14917	Metal bellows expansion joints for pressure applications
EN ISO 4126	Safety devices for protection against excessive pressure

Very useful guidelines and design rules



Final lathe machining

ess relieving

LHC dipole Vacuum Vessels

Main features:

- Pipeline standard size: **36-inch OD (1013 mm)**, **12-mm thick**, low carbon steel (DIN GS-21 Mn5) tubes
- St. steel extremity flanges
- Material resilience: > 28 J/cm2 at -70°C
- Forged cradles, welded rings reinforcements
- Dimensional stability:
 - Stress relieving
 - Final machining to achieve tolerances at interface



- 1250 units
- 2 firms
- 4 yrs of production





LHC thermal shields





Aluminium alloy 6063 extrusions and 1100 top sheets





Thermo-mechanical considerations

Thermal expansion of some materials







Thermal stress in composite material assemblies: 3 cases





$$\sigma 1 = \frac{E1 E2 A2}{E1 A1 + E2 A2} (\alpha 2 \Delta T2 - \alpha 1 \Delta T1) \qquad \sigma 2 = \frac{E1 E2 A1}{E1 A1 + E2 A2} (\alpha 2 \Delta T2 - \alpha 1 \Delta T1)$$

LHC cryostats: longitudinal thermal contractions

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- Cold mass, thermal shield, support posts and vacuum vessel must be free with each other to cope with longitudinal thermal contractions
- One fixed point per each component
- Leave plays to cope with all extreme T cases (ex. Cold mass cold, thermal shield warm)
- Guided sliding of cold mass onto vacuum vessel \rightarrow slot/key
- Flexible thermalisation anchors







Supporting systems

LHC Cryomodule, 400 MHz cavities (Nb on Cu) at 4.5 K





LHC Cryomodule Supporting System





LHC magnet Cryostats





- 4-mm thickness, glass-fiber epoxy
- Manufactured by **Resin Transfer Moulding (RTM)**:
 - Suited to a large-scale industrial production (4'700 units)
 - High reproducibility in thermo-mechanical properties



LHC Supporting system

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The design is a trade-off between 2 conflicting requirements:

- High flexural stiffness (for mechanical stability) \rightarrow thick and bulky structure
- Low heat in-leaks \rightarrow thin and slender structure and low conductivity material

(F is mainly the result of interconnect forces and gravity component) F = 5 kNx = 0.1 mm $\theta = 1 mrad$



→ Flexural stiffness/conductivity as figure of merit in the choice of the material

Resin Transfer Moulding





Lay-up, calculated safety factors, material properties





Triaxial braid and % fiber volumes



of biaxia braid

Tensile testing on 5 longitudinal samples, at 293 K, 77 K, and 4.2 K.									
Test at	Rm	Test at	Rm	Test at	Rm				
293K	(MPa)	77K	(MPa)	4.2K	(MPa)				
Average	4593	Average	570.4	Amrogo	406 7				
menage	-57.5	Average	370.4	Average	420./				
Min.	436.6	Min.	535	Min.	490.7				





MAG NIN:-2.64E-01 MAX: 4.26E-01 VALUE OPTION:ACTUA PLY NO: 4.26D-01 E1. 180 3.57D-0 2.860-0 2.190-01 1.50**D**-0 8.12D-0 1.22D-0 -S.88D-0 -1.26D-01 -1.96D-0 -2.84D-01

Bending cantilever 40 kN. (vacuum barrier load)

Tsai-Wu ply failure: Safety Factor = 2.7

SC magnet supporting systems from other machines





Hera dipole



Tevatron





SCC

Supporting system of Tesla/TTF/ILC Cryomodule





Supporting system of SNS and ESS high β Cryomodules





Supporting system of PIP II Cryomodule





SPL cryomodule: RF Coupler as support







Vertical loading of cavities string







Heat transfer mechanisms and thermal design

Heat transfer mechanisms

- Thermal radiation
- Thermal conduction
- Heat intercepts



Inspired by P. Duschene and JP. Thermeau



Thermal Radiation
Thermal Radiation



Stefan-Boltzmann's law

$$Q = \sigma A T^4$$
 black body

 $Q = \varepsilon \sigma A T^4 \qquad \text{gray bod} y,$

 $\sigma = 5.67 \ 10^{-8} \ W \ m^{-2} \ K^{-4}$ Stefan-Boltzmann's constant

 $\varepsilon < 1$

A, T area and temperature of the body, ε emissivity

exchange between **black bodies**

$$Q_{1-2} = F_{12}A_1 \sigma \left(T_1^4 - T_2^4\right) = F_{21}A_2 \sigma \left(T_1^4 - T_2^4\right)$$

exchange between **gray bodies**

$$Q_{1-2} = E_{12} \sigma A_1 (T_1^4 - T_2^4) = E_{21} \sigma A_2 (T_1^4 - T_2^4)$$

Figures source: "Heat Transfer", A.Bejan, John Wilney & Sons, Inc.

- F, geometrical view factors F_{1-2} (<1) between A_1 and A_2 (or F_{2-1} between A_2 and A_1), with A_1E_{12} = A_2E_{21} .
- E, effective emissivity, a function of view factors and emissivity ε_1 and ε_2 of the bodies

Black body radiation

 Hemispherical monochromatic emissive power [W/m·m2] (energy per unit time, wavelength, and surface area)

$$E_{b,\lambda} = \frac{C_1 \lambda^{-5}}{e^{(\frac{C_2}{\lambda T})} - 1}$$
 Planck's law

 $C_1 = 2 \pi h c^2 = 3.742 \ 10^{-16} W m^2$ $C_2 = \frac{h c}{k} = 1.439 \ 10^{-2} \ K m$

• Total emissive power (integrating over λ):

(k, Boltzmann constant, h, Planck constant, c, speed of light)

In practice: Blackbody emits ~ 420 W/m² at 293 K, and only ~2 W/m² at 77 K (200 times less!)

hemispherical emissive power (monochromatic)



Figures source: "Heat Transfer", A.Bejan, John Wilney & Sons, Inc.

Black and diffuse-gray model

Black model

 $\alpha \rightarrow \text{absorptivity}$ $\rho \rightarrow \text{reflectivity}$ $\tau \rightarrow \text{transmissivity}$ $\alpha + \rho + \tau = 1$

 $\alpha + \rho = 1 \quad (opaque, \tau = 0)$ $\alpha = 1 \quad (black, \rho = 0, \tau = 0)$



Black surface: $\alpha = 1$



Blackbody limit, $\epsilon_1 = \epsilon = 1$

Practical application in cryostats: every gap in shields is a black surface $(1 \text{ cm}^2 \text{ gap exposed to } 293 \text{ K}, \epsilon = 0.2 \rightarrow \sim 10 \text{ mW})$

Diffuse-gray model



Figures source: "Heat Transfer", A.Bejan, John Wilney & Sons, Inc.





Diffuse-gray model (good approximation for real surfaces in engineering):

- Gray: $\varepsilon_{\lambda}(\lambda, T) \approx \varepsilon(T)$
- Diffuse emitter/absorber (not directional)
- Opaque ($\tau = 0$)
- $\alpha(T) = \varepsilon(T)$

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Emissivity

- ε depends on wave-length and direction (neglected in gray-diffuse model). In metals emissivity rises sharply and up to more than 40% above 50 deg. incidence from the surface normal
- Clean, well-polished metallic surfaces have smaller ε , non-metallic materials have higher ε
- Metals: ε decreases with decreasing temperature, almost linearly at cryo temperatures
- Non-metals: ε may decrease or increase with decreasing temperature (increases for organic materials)
- Engineering approach. Due to uncertainties on real ε values, take conservatively high values for preliminary design. Measurement validation may be necessary

Temperature [K]	4	20	80	300
Copper mechanically polished	0.02		0.06	0.1
Copper black oxidized				0.8
Gold			0.01	0.02
Silver	0.005		0.01	0.02
Aluminium electropolished	0.04		0.08	0.15
Aluminium mechanically polished	0.06		0.1	0.2
Aluminium with 7µm oxide				0.75
Magnesium				0.07
Chromium			0.08	0.08
Nickel			0.022	0.04
Rhodium			0.08	
Lead	0.012		0.036	0.05
Tin	0.012		0.013	0.05
Zinc			0.026	0.05
Brass, polished	0.018		0.029	0.035
St.steel 18-8	0.2		0.12	0.2
Glass				0.94
Ice				0.96
Oil paints any color				0.92-0.96
Silver plate on copper		0.013	0.017	
Aluminium film 400A on Mylar			0.009	0.025
Aluminium film 200A on Mylar			0.015	0.035
Nickel coating on copper		0.027	0.033	

Métal	T (K)	ε _n	
Or	300 80	0,02 0,01	
Argent	300 80 4	0,02 0,01 0,005	
Aluminium commercial brut	nissivité totale r lques métaux. T (K) 300 80 300 80 4 300 80 80 4 300 80 80 4 300 80 80 4 300 80 80 4 4 300 80 80 80 4 4 300 80 80 80 80 4 300 80 80 80 80 4 300 80 80 80 80 4 4 300 80 80 80 4 4 300 80 80 4 4 300 80 80 4 4 300 80 80 4 4 300 80 80 4 4 300 80 80 4 4 300 80 80 4 4 300 80 80 80 4 4 300 80 80 4 4 300 80 80 4 4 300 80 80 4 4 300 80 80 4 4 300 80 80 80 80 80 80 80 80 80	0,25 0,12 0,07	
Aluminium poli mécanique	300 80 4	0,20 0,10 0,06	
Aluminium poli électrolytique	300 80 4	0,15 0,08 0,04	
Chrome	300	0,08	
Cuivre poli mécanique	300 80 4	0,10 0,06 0,02	
Étain	300 80 4	0,050 0,012 0,013	
Nickel	300 80	0,05 0,02	
Laiton poli	300 80 4	0,03 0,03 0,02	
Acier inoxydable 18-8	300 80 4	0,20 0,12 0,10	



Ref. https://neutrium.net/heat-transfer/emissivity/

Ref. R.B.Scott, Cryogenic Engineering, (Van Nostrand, New York, 1959; Y.S. Touloukian, Thermophysical Properties of Matter, (Plenum Press, New York, 1995))

Ref. Cryogenie, ses applications en supraconductivite. Techniques de l'ingenieur, Ed. 1995



normal

Radiation between 2 diffuse-gray enclosures

- Radiation balance between A1 and A2 surfaces: $q_{1-2} = \frac{\sigma(T_{1}^{4} - T_{2}^{4})}{\frac{1-\varepsilon_{1}}{\varepsilon_{1}A_{1}} + \frac{1}{A_{1}F_{12}} + \frac{1-\varepsilon_{2}}{\varepsilon_{2}A_{2}}}$
- For **2 enclosed cylinders** or **spheres** (not necessarily concentric!), *F*₁₂=1 :

 $q_{1_{-2}} = \frac{\sigma A_1 (T_1^4 - T_2^4)}{\frac{1}{\epsilon_1} + \frac{A_1}{A_2} (\frac{1}{\epsilon_2} - 1)}$

- Limit size of A₁ (SC device vessel)
- Reduce A₂ (vac.vessel as small as possible)
- **Small emissivities**: ε_1 reduced by low T; ε_2 at RT & moderated by A₁/A₂

*Figures source: "*Heat Transfer", A.Bejan, John Wilney & Sons, Inc.

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(see numerical application in Annex)





Radiation between 2 diffuse-gray flat plates

• Radiation balance between A1 and A2 (A1=A2=A), F_{12} =1 :







Radiation with an intermediate floating shield







 \rightarrow Can be generalized to N shields



• Radiation balance between A1 and A2:



• For flat surfaces approximation, and same ε :

$$q_{1-s} = \frac{\sigma A \left(T_1^4 - T_s^4\right)}{\binom{2}{\varepsilon} - 1} = \frac{\sigma A \left(T_s^4 - T_2^4\right)}{\binom{2}{\varepsilon} - 1} = q_{s-2} \qquad \Rightarrow \mathsf{T_s}^4 = \frac{T_1^4 + T_2^4}{2}$$

 $q_{1-2} = \frac{\sigma A (T_1^4 - T_2^4)}{2\ell_{\mathcal{E}}^2 - 1}$

 \rightarrow with 1 shield $\frac{1}{2}$ of the rate without shield

$$q_{1-2} = \frac{\sigma A (T_1^4 - T_2^4)}{(N+1)(\frac{2}{\varepsilon} - 1)}$$

 \rightarrow with N shield <u>1/(N+1)</u> of the rate without shield

N shields \rightarrow Multi Layer Insulation (MLI)

Working principles:

- Low emissivity of aluminium layer
- Multi-layer to enhance radiation protection:
 - N+1 radiation shielding
- Minimal thermal conduction between reflective layers → interposing of isolating layers (e.g polyester net):
- Enhanced performance at low T \rightarrow use actively cooled shield:
 - Lower emissivity of reflective material layers at low T
 - Reduce radiation from inner-most layers, cooled at T of shield
 - Extract heat at higher thermal shield T → thermodynamic efficiency



MLI material



LHC MLI:

- **Reflecting film**: 6 µm thick polyethylene teraphthalate (PET) film coated with 400 Å minimum aluminium on each side (Physical Vapor Deposition process) •
- **Spacer**: polyester net of very low weight (< 5 g/m2) •
- 10 or 15 layer **pre-assembled blankets** (outermost layer reinforced with a polyester net) •
- Blanket overall thickness: > 2 (3) mm for 10 (15) layers •
- Perforated layers for outgassing: 0.05-0.15 % surface •





LHC MLI blankets

Features:

1 blanket (10 reflective layers) on cold masses (1.9 K) 2 blankets (15 reflective layers each) on Thermal Shields (50-65 K) Reflective layer: double aluminized polyester film (2 km²) Spacer: polyester net

Stitched Velcro™ fasteners for rapid mounting and quality closing



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MLI: How many reflective layers (N)?

Arbitrary units

- No straightforward answer ! Not just a matter of N !
- Complex system to model, with parameters needing experimental qualification
- Radiation vs. conduction
 - ✓ Radiation reduces as 1/N
 - Conduction proportional to packing density (N/mm)
- Residual helium gas conduction
 - ✓ Negligeable at res. pressure $p < 10^{-4}$ Pa (10⁻⁶ mbar)
 - ✓ Sizeable contribution at res. pressure 10⁻⁴ Pa -3</sup> Pa (10⁻⁵ mbar)
 - ✓ Dominates at res. pressure $p > 10^{-2}$ Pa (10⁻⁴ mbar)
- Packing density should be limited → typically 20-25 N/cm
 - > Avoid "compressed" blankets (do not put as much MLI as you can fit!)
 - Reserve space allocation for MLI blankets
 - Consider differential thermal contractions wrt support (Al shields, cold mass...): blankets must remain quite loose at cold
- Overall performance depends very much on:
 - ✓ Application design solutions
 - ✓ Craftsmanship quality



MLI application: important tips





Handle MLI with gloves (fingerprints are a black body!)

Velcr	о тм	Reflective laye	r
T _{hot}			and a
T _{cold}			



Some tapes are resin coated = black body ! Check conductivity





loose at RT (MLI contracts more than metal support)



Not tool much MLI (risk of thermal shorts)



Thermal path warm to cold layers





(images: courtesy of Meyer Tool & MFG.)

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Performance measurements on MLI samples

- 300 K 77 K, abundant literature (see a few ref. [1], [2])
- 77 K 4 K, fewer results. CERN experimental work (see a few ref.[3],[4],[5])
- Some values, in good vacuum (<10⁻⁴ Pa) [3]:



[1] T.Nast, Multilayer Insulation Systems, in Handbook of Cryogenic Engineering, ed. J.G.Weisend II, Taylor & Francis, Philadelphia (1998),

[2] M. G. Kaganer, Thermal Insulation in Cryogenic Engineering, Jerusalem, Israel Program for Scientific Translation, (1969),

[3] L.Mazzone et al., Measurements of Multi-Layer Insulation at high boundary temperature, using a simple non-Calorimetric method. Proceedings ICEC 19, 2002, Grenoble, France.

[4] Ph.Lebrun et al., Investigation and qualification of thermal insulation systems between 80 K and 4.2 K, Proceedings ICEC/ICMC, 1992, Kiev, Ukraine

[5] V.Venturi, Thermodynamic and technological optimization of complex insulation systems. PhD thesis, 2019, WUST University, Poland.

Practical MLI performance values



- MLI samples measured performance is considerably degraded in applications due to the engineered solutions and installation procedures:
 - > pre-assembled blankets vs. rolled MLI
 - complex (non developable) geometries
 - ➤ junctions, stitches, VelcroTM fasteners, etc.
 - higher than ideal packing density (e.g. self-weight compaction)
 - thermal shorts between cold and warm layers (e.g. overlapped blanket closure)
 - quality of assembly (lab vs. industrial scale)
- Engineering values: what values should one use for HL first estimates?
 ➤ Take generous margins. Rule of thumb → x 2 sample measurements
- LHC cryostat (+) (a thermally well optimized large-scale application), average measure on 2.7 km length sector :
 - \geq 293 K to 50 K thermal shield with 30 MLI layers: \rightarrow ~1 W/m²
 - > 50 K to 2 K magnet with 10 MLI layers: \rightarrow ~ 54 mW/m²

Summary of radiation HL exercises (for details see spare slides)





Thermal Conduction

Thermal Conduction

- When a T gradient exists in a body, there is a heat transfer from the high T region to the low T region (Fourier Law):
- For one-dimensional problems (ex. a bar or tube):
- k is the thermal conductivity (W m⁻¹ K⁻¹), normally a function of P,T, material structure, non-homogeneity, anisotropy (ex. Composite materials).
- k is strongly T-dependent and non-linear at low T
- "good conductors" vs. "poor conductors" → k range ~ 5-6 orders of magnitude



0.1



Thermal conductivity of various materials





- Metals: mainly free electron contribution
- Resistivity from electron scatter with phonons (lattice vibrations) α T² and with impurities α 1/T
- Increasing effect of impurities in less pure metals and dominates in alloys
- Maximum of conductivity reduces and shifts towards higher T with increasing impurities
- Al and st.steel alloys: conductivity α T
- Non cristalline materials and insulators dominated by phonon contribution

Thermal conductivity in epoxy-based composite materials



- Low conduction (little electron conduction), essentially phonon driven
- Anisotropic structure, (fibers/matrix) with constituentsspecific thermal conductivity properties
- Conductivity highly depends on:
 - Material (fiber) orientation
 - Ratio between fibre and matrix (Vf)
- Glass-fiber is the "conductive" fraction and also the "structural" constituent
- Epoxy is the "isolating" fraction material and is the "less structural" constituent
- Conductivity (W/m.K) 1.000 0.800 0.600 0.400 0.400 0.200 0.000 100.00 200.00 300.00 400.00 Temperature (K)

(Data from Schwartzberg F.H., Cryogenic Material Data Handbook, Martin Marietta Corrp, Denvers, Co, 1970)



Longitudinal and transversal conductivity laminate studies for LHC supports, (based on data from Schwartzberg F.H.), collaboration CERN-ESIGEC (Univ.Savoie), 1997

- Vf typically around 40-70%
- Cryogenic grade G10-CR and G11 are widely used standard laminates in various forms (plates, tubes, rods). Properties data can be found in: <u>https://trc.nist.gov/cryogenics/index.html</u>



Glass-fiber dry fabric





LHC supports



Support posts measurements

49 ± 10% mW @ 1.9K 450 ± 10% mW @ 4.5-10K 7.1 ± 5% W @ 50-65K



0.2

The conduction equation (unidirectional case)





No heat deposition and steady-state



Thermal conductivity integrals (conductance) for some materials [W/m]







Highest T (Lowest T =4.2 K)	20 K	80 K	290 K
OFHC Copper	11000	60600	152000
DHP Copper	395	5890	46100
Aluminium 1100	2740	23300	72100
Aluminium 2024	160	2420	22900
Stainless steel AISI 304	16,3	349	3060
Typical Glass-fiber/Epoxy Composite G-10	2	18	153

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...more conductivity integrals

Tableau E. – Valeurs de l'intégrale $\int_{4,2}^{T} k(T) dT$ pour quelques matériaux.								
T (K) Matériau	6	8	10	15	20	60	80	300
Conducteurs (en W/cm)								
Cuivre extra-pur	166	382	636	1270	1790	2960	3090	4000
Cuivre électroécroui	8,0	19,1	33,2	80,2	140	587	707	1620
Argent	320	670	990	1610	1980	2570	2670	3570
Aluminium extra-pur	73	168	280	600	907	1740	1840	2390
Aluminium du commerce	1,38	3,42	6,07	15,2	27,6	170	232	728
Or	41	93	149	274	364	612	682	1370
Laiton	0,0531	0,129	0,229	0,594	1,12	10,4	17,7	172
Plomb (normal)	27,0	37,3	42,4	49,0	52,5	73,8	81,3	160
Titane	0,115	0,277	0,488	1,21	2,20	15,5	22,6	99,6
Monel	0,0235	0,0605	0,112	0,315	0,618	5,23	8,24	52,5
Acier inoxydable	0,0063	0,0159	0,0293	0,0816	0,163	1,98	3,49	30,6
Isolants (en mW/cm)								
Verre	2,11	4,43	6,81	13,1	20,0	115	194	1990
Téflon	1,13	2,62	4,4	9,85	16,4	93,6	139	702
Plexiglas	1,18	2,38	3,59	6,69	10,1	68,3	110	630
Nylon	0,321	0,807	1,48	4,10	8,23	85,9	142	895

Electrical network analogy

• The inverse of the *thermal conductance* \rightarrow *thermal resistance:*

For variable k, define an average value k_{AV} :

$$k_{AV} = \frac{\int_{T_0}^{T_L} k(T) dT}{(T_L - T_0)} \qquad \Longrightarrow \qquad R_t = \frac{L}{k_{AV}A}$$

$$\dot{q} = -\frac{A}{L} \int_{T_0}^{T_L} k(T) dT = \frac{T_0 - T_L}{R_t}$$

• Analogy with the electrical resistance (replace q with I, T with V):

$$I = \frac{V_0 - V_L}{R}$$

• We can therefore model a complex thermal conductivity problem by elementary *thermal resistances Ri*, and solve the network by using *Kirckhoff's laws*.

$$\sum_{i=1}^{n} q_{i} = 0 \quad (at \ knots)$$
$$\sum_{i=1}^{m} (T_{i} - T_{i-1}) = 0 \quad (in \ loops)$$



Thermal conduction with uniform heat deposition q_x q_x

- Beam of length L, thickness t, width w (= 1m);
- beam *thermalized* on one side at To
- uniform heat deposition from one side, q (W/m²)
- considering k constant with T
- Boundary conditions: a) for x= 0 T=To (heat sink); b) q=0 for x=L (isolated tip)
- Integrating and imposing the 2 boundary conditions:

$$T(x) = To - \frac{q}{2kt}x^{2} + \frac{qL}{kt}x$$

$$\Delta T_{\text{max}} = TL - To = \frac{qL^{2}}{2kt}$$

$$T_{0}$$

-

practical interest:

calculate minimum thickness to limit ΔT_{max}



Thermal diffusivity

• For small variations of k with x:

Solid bar cooled at one tip

- Conduction equation (no heat generation)
- $\frac{\partial}{\partial x} \left(k \frac{\partial T}{\partial x} \right) = \rho c \frac{\partial T}{\partial t}$ $\frac{\partial^2 T}{\partial t} = 1 \frac{\partial T}{\partial t}$

 $\frac{1}{\partial x^2} = \frac{1}{\alpha} \frac{1}{\partial t}$

with
$$\alpha = \frac{k}{\rho c}$$

- T perturbation δ travels towards warm end:
- t_c , critical time for T perturb. to reach warm tip:







Heat capacity

- Specific heats: $c_{\rm P} = \left(\frac{\partial Q}{{\rm m}\,{\rm d}{\rm T}}\right)_P = \left(\frac{1}{{\rm m}}\frac{\partial {\rm H}}{\partial {\rm T}}\right)_P \qquad c_{\rm V} = \left(\frac{\partial Q}{{\rm m}\,{\rm d}{\rm T}}\right)_V = \left(\frac{1}{{\rm m}}\frac{\partial U}{\partial {\rm T}}\right)_V$
- For (incompressible) substances: Cp(T) = Cv(T) = C(T)
- Change of internal energy U (or enthalpy):

 $\blacktriangleright \Delta \mathbf{U} = Q = m \int_{T_1}^{T_2} c(T) dT$

- Cooling (or heating) power: $P(T) = m c(T) \frac{dT}{dt}$
- Specific heats/unit vol. sometimes preferred
- Below 10 K enthalpy of helium overtakes all solids









Measuring Thermal Performance of Cryostats

Measure of Heat Loads to liquid helium tanks

SC level gauge Isothermal cooling (2-phase helium tanks) vapor liquid volume replaced He boil-off along saturation line m by fraction of boil-off 20 \checkmark Latent Heat (L_v) of vaporisation h_{fe} (kJ/kg) vapor (no filling) ✓ Isothermal cooling (T constant if P constant) 10 \checkmark Measure p, and m. ✓ Liquid/gas volumetric corrective factor 15 2 T (K) Latent heat of vaporization \boldsymbol{q} $q = m \cdot Lv \cdot$ Example: 150 ✓ Mass flow measurement: 7 g/s ✓ P measured: 1.78 bar LIQUID ✓ (T on saturation line (phase diagram): 4.8 K) 100 \checkmark L_v = 14'116 (J/kg) (tables, or state equations) kg/m³) from diagrams measure \checkmark $v_q = 3.0 \ 10{\text{-}2} \ (\text{m3/kg}); v_1 = 9.3 \ 10{\text{-}3} \ (\text{m3/kg});$ (phase diagrams) 50 → $\dot{q} = 7.0 \ 10 - 3 \cdot 14116 \cdot \left(\frac{3.0 \ 10 - 2}{3.0 \ 10 - 2}\right) = 143 \ \text{W}$ VAPOR 1.45! T(K)

Density of saturated liquid helium

- He boil-off liquid level measurement:
 - Measure level I with SC level gauge •
 - Boil-off mass flow measure through reservoir geometrical correlation between level and volume: f(I), and knowledge of density ρ and L,

$$\dot{q} = f(\Delta l) \cdot \rho \cdot Lv$$

Measure of Heat Loads to liquid helium tanks (cont.d)

Non-isothermal cooling

- Calorimetry in superfluid helium (LHeII):
 - LHe II very high thermal conductivity \rightarrow isothermal bath
 - Measure internal energy change (closed system) in time Δt
 - Needs precise measure of helium content
 - and sub-mK resolution measurement of T at T< 2.17 K

$$\dot{q} = \frac{\Delta U(t)}{\Delta t} = \frac{m \cdot \Delta u(t)}{\Delta t}$$





Measure of Heat Loads to Thermal Shields

Non-isothermal cooling

- Forced internal (conduit) convection of single-phase fluid:
 - Non-isothermal cooling: enthalpy change of fluid (here c_p assumed constant)
 - Needs the measure of mass flow, and T at entry and exit of conduit



$$\dot{q} = \Delta H = \dot{m} \cdot cp \cdot (\mathsf{T}_{\mathsf{out}} - \mathsf{T}_{\mathsf{in}})$$



Forced Convection heat transfer in conduits



- Forced flow of coolant fluid in round tube cooling lines
- Considering hydro-dynamically and thermally fully developed flow
- Uniform wall heat flux (linear T profiles)
- Convection heat transfer from wall to fluid:
- Enthalpy balance along the line L:
- Reynolds No.:
- Nusselt No.:
- ✓ For laminar flow: constant
- ✓ For turbulent flow, NuD=f(ReD, Pr): (Dittus and Boelter formula)

$$\stackrel{\bullet}{q} = h \cdot D\pi L \cdot (T_w - T_m)$$

$$q = m \cdot c_p \cdot (T_{out} - T_{in})$$

$$\operatorname{Re}_{D} = \frac{UD}{v}$$
$$NuD = \frac{h \cdot D}{k}$$

$$Nu_D = \frac{h \cdot D}{k} = 4.364$$
 $\frac{dT_m}{dx} =$

$$Nu_D = 0.023 \cdot \text{Re}_D^{4/5} \text{Pr}^{2/5}$$

ts

$$\int_{AT_{in}} T_{out} \int_{T_{u}(x)} \int_{AT_{out}} \int_{T_{u}(x)} \int_{AT_{out}} \int_{AT_{out}} \int_{T_{in}} \int_{T_{in}} \int_{T_{in}} \int_{T_{in}} \int_{AT_{out}} \int_{C_{in}} \int_{C$$

 $2500 \le \text{Rep} \le 1.2410 + 5$

CERN

 $\alpha = thermal diffusivity$

Frictional pressure drop in a tube



Pressure drop along tube

 Experimental plots or semiempirical formulations (ex. Colebrook formulation)



f = Fanning friction factorU = Mean velocity



Ref. "Heat Transfer", A.Bejan, John Wilney & Sons, Inc.



Feedthroughs and heat intercepts

Feedthroughs in cryostats





- Supporting systems
- **Current leads**
- RF main coupler ٠
- Instrumentation feed-throughs ٠
- Beam tubes Cold-to-Warm (CWT) transitions
- Necks (vertical cryostats) ٠



Neck



LHC instrumentation capillary at assembly




Heat intercepts (heat sinking) at intermediate temperatures







$$\dot{\mathbf{Q}} = \frac{A}{L} \int_{\mathrm{Tc}}^{\mathrm{Tw}} k(T) dT$$

• 1 heat intercept at optimal distance

$$\min\{f(L_1) = C1 \cdot \frac{A}{L_1} \int_{T_W}^{SOK} k(T) dT + C2 \cdot \frac{A}{L - L_1} \int_{SOK}^{T_C} k(T) dT\}$$

$$\rightarrow L_1$$

• 2 heat intercepts at optimal distance

$$8\mathsf{K}$$

$$\min\{f(L_1, L_2) = C1 \times \frac{A}{L_1} \bigcup_{\mathrm{Tw}}^{\mathrm{SOK}} k(T) dT + C2 \times \frac{A}{L_2 - L_1} \bigcup_{\mathrm{SOK}}^{\mathrm{SK}} k(T) dT + C3 \times \frac{A}{L - L_2} \bigcup_{\mathrm{SK}}^{\mathrm{Tc}} k(T) dT\}$$

$$\rightarrow \mathsf{L}_1, \mathsf{L}_2$$
73





LHC supports





	$Q_{1.8K}$	Q_{5K}	Q_{75K}	Qelec.
	[W]	[W]	[W]	[W]
1	2.79	-	-	2790
2	0.541	-	6.44	638
3	0.047	0.42	7.1	252

Heat loads comparison for GFRE with & without heat intercepts

- 4-mm thickness, glass-fiber epoxy
- Manufactured by **Resin Transfer Moulding (RTM)**:
 - Suited to a large-scale industrial production (4'700 units)
 - High reproducibility in thermo-mechanical properties

Vapour cooling in solid conduction



- Vapor cooled wall
- Assuming perfect exchange $(T_{vapor} = T_{wall})$

$$k(T) \cdot A \cdot \frac{dT}{dx} = \dot{Q} + \dot{m} \cdot Cp \cdot (T - Tl)$$

• If Q, which is the residual heat to the bath, is equivalent to the evaporation (i.e. self-sustained):

$$\rightarrow Q = m \cdot Lv$$
 Lv, latent heat of evap.



Large enthalpy in He vapours (1550 kJ/kg from 4.2K to 300K) \rightarrow usable cooling capacity

		-
	Thermal conductivity integral	Effective thermal conductivity
	$[W \text{ cm}^{-1}]$	integral [W cm ⁻¹]
ETP copper	1620	128
OFHC copper	1520	110
Aluminium 1100	728	39.9
AISI 300 st.steel	30.6	0.92

Reduced heat conduction in self-sustained helium cooling for selected technical materials

(ref. G. Vandoni, Heat Transfer, CAS, Erice 2003)

SPL cryomodule: actively cooled RF main couplers



Vapor cooled RF coupler (double-walled tube). Effective cooling with gas regulation:

- Conduction heat loads (RF off)
- Conduction + RF EM resistive heating (RF on)

Double-walled tube:

- ~Φ 100 mm
- Inner wall: st.steel, 1.5-mm thick
- External wall: st.steel, 2-mm thick







Notions of Cryogenic Safety

Cryostats and safety





- Cryostats include inventory of cryogenic fluids, potentially unstable stored energy, and sometimes large electromagnetic stored energy in superconducting devices
- Managing safety in cryostat covers multiple aspects: safety of personnel and equipment
 - Risk assessment: cryostat as part of a cryogenic system in an environment
 - Safety hazard from relief of cryogens to the environment: ODH, burns, escape paths, safety training, use of personnel protection equipment, risk to adjacent equipment, etc.

→ Understanding pressure hazards and making the correct choice of the pressure relief devices to protect from overpressure of the cryostat envelopes

Liquid helium (and nitrogen) stored energies



Property	Unit	⁴He	N ₂
T _{boil.} (at 1'013 mbar)	[K]	4.2	77.3
Liquid density (at T _{boil.})	[kg/m³]	125	804
Density ratio $\rho_{\text{liquid}} / \rho_{\text{gas}}$ (gas at boiling temperature and 1'013 mbar)	-	7.4	175
Gas/liquid volume ratio (gas at 273 K, 1'013 mbar)	-	702	652
Latent heat of evaporation (at T _{boil.,} and 1'013 mbar)	[kJ/kg]	21	199
Latent heat of evaporation per unit vol. (at T _{boil.,} 1'013 mbar)	[kJ/l]	2.6	160
Enthalpy change from $T_{\text{boil.}}$ to 300 K per unit vol. (at 1'013 mbar)	[kJ/l]	194	189
Total liquefaction energy in 1 liter of liquid	[kJ/l]	196.6	349
Expansion work (isobar at 1'013 mbar, reversible) for 1 liter of liquid	[kJ/l]	71	66

One LHC dipole:

- Magnetic stored energy: ~7 MJ
- Helium content: 375 liters
- Total stored energy (in liquid): 74 MJ (x10 times stored magnetic energy!)
- Total magnet cold surface: ~4 m²
- Latent heat per unit volume: He x60 lower than $N_2 \rightarrow$ (roughly) venting a cryostat with ~6 liter air (~N₂) boils off He in 1 dipole
- Air condensation power on cold surface with MLI: 6 kW/m² (40 kW/m² on bare surface !)
- Vacuum insulation breach: peak power deposition: $24 \text{ kW} \rightarrow -40 \text{ s}$ to boil-off liquid, -50 min. to deplete liquid stored energy,

→ Large volumetric inventories and energies released in reduced time ! → pressure relief devices !



Pressure hazards in cryostats



- Potential pressure hazards:
 - Compressors connected to cryo lines
 - Heating of "trapped" volumes (typically in a circuit between valves) during warm-ups
 - Helium leak to insulation vacuum, with consequent increased conduction/convection heat loads to cryogenic liquid vessels
 - Cryo-condensed air leaks on cold surfaces and consequent pressure increase and increased conduct/convection heat loads during warm-ups
 - A) Heating/vaporization of cryogens from sudden release of stored energy in SC device (e.g. quench or arcing in a SC magnet circuit)
 - B) Accidental release of cryogenic fluid to higher T surfaces (thermal shield and vacuum vessel), and consequent pressure increase and increased of conduction/convection heat loads to cold surfaces
 - C) Accidental air venting of insulation vacuum with sudden condensation on cold surfaces, helium boil-off and pressure build-up







(Snowball effect A) + B) + C) \rightarrow LHC event of Sept.2008)

How things can go wrong...LHC 19th sept. 2008















General approach for sizing of safety devices

CERN

Risk analysis & mitigation:

- Make a thorough risk analysis and evaluate risk hazards
- Identify mitigation measures (e.g. protections of exposed bellows and flanged connections)
- Identify severity of consequences and appreciate probability of the event
- Define the maximum credible incident(s) (MCIs) and design the safety relief system accordingly
- The safety relief system must be designed to keep pressure rise within the limits of the Maximum Allowable Working Pressure (MAWP)

Design steps for the MCI:

- Estimate the heat flux to helium and its conversion to mass flow rates to be discharged
- Choose the type of safety device (burst disks, valves, plates) and size the safety device (orifice area and set pressure). Make use of standards and safety device manufacturers datasheet
- Check the sizing of piping (generally designed for normal operation) to the relief device and increase if necessary (pressure drop limited to a few % of total discharge Δp)

$$\dot{Q} \rightarrow \dot{M}$$

Heat flux (W) \rightarrow Relieving mass flow rate (kg/s)





 $\rho_{\textit{th}} \textit{v}_{\textit{th}_{,}}$ density and velocity giving the \dot{m} in the throat

→ Methodology explained in a new standard EN 17527 just issued devoted to Helium cryostats - Protection against excessive pressure

EN 17527 Helium cryostats - Protection against excessive pressure

Publication of EN 17527



Scope includes:

✓ SC magnet cryostats

✓ SRF cavity cryomodules

- ✓ Ultra-low T refrigerator systems
- ✓ Coldboxes of helium refrigerators and liquefiers
- Helium distribution systems including valve boxes

Overall concept:

- ✓ Standardization of the approach
- ✓ Specification of procedures and minimum requirements
- ✓ Risk assessment, definition of scenarios
- Protection concepts (single-stage, multistage)
- ✓ Dimensioning rules of pressure relief devices (HEM Model)

A few suppliers Herose, Rembe, Ramseyer, Leser...

Safety devices

- 1. Safety valves
- 2. Burst discs
- 3. Pressure relief plate

2.





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EN Standards for Safety Relief Devices

EN 764-7:2002 Pressure equipment. Part 7: Safety systems for unfired pressure equipment

EN ISO 4126-1:2013 / Safety devices for protection against excessive pressure - Part 1: Safety valves (ISO 4126-1:2013) 12/08/2016

EN ISO 4126-2:2013 / Safety devices for protection against excessive pressure - Part 2: Bursting disc safety devices

EN ISO 4126-3:2006 / Safety devices for protection against excessive pressure - Part 3: Safety valves and bursting disc safety devices in combination (ISO 4126-3:2006) 12/08/2016

EN ISO 4126-4:2013 / Safety devices for protection against excessive pressure - Part 4: Pilot-operated safety valves (ISO 4126-4:2013) 12/08/2016

EN ISO 4126-5:2013 / Safety devices for protection against excessive pressure - Part 5: Controlled safety pressure relief systems (CSPRS) (ISO 4126-5:2013) 12/08/2016

EN ISO 4126-7:2013 / Safety devices for protection against excessive pressure - Part 7: Common data (ISO 4126-7:2013) 12/08/2016

EN 13648-1:2008 / Cryogenic vessels - Safety devices for protection against excessive pressure - Part 1: Safety valves for cryogenic service 12/08/2016

EN 13648-2:2002 / Cryogenic vessels - Safety devices for protection against excessive pressure - Part 2: Bursting disc safety devices for cryogenic service 12/08/2016

ISO 21013-3:2016 Cryogenic vessels -- Pressure-relief accessories for cryogenic service -- Part 3: Sizing and capacity determination

EN ISO 4126-6:2013 / Safety devices for protection against excessive pressure - Part 6: Application, selection and installation of bursting disc safety devices

EN ISO 4126-10:2013 / Safety devices for protection against excessive pressure - Part 10: Sizing of safety valves for gas/liquid two-phase flow

EN 13648-3:2002 Cryogenic vessels. Safety devices for protection against excessive pressure. Determination of required discharge. Capacity and sizing

ISO 21013-1:2008 Cryogenic vessels -- Pressure-relief accessories for cryogenic service -- Part 1: Reclosable pressure-relief valves

(ISO/AWI 21013-1 Cryogenic vessels -- Pressure-relief accessories for cryogenic service -- Part 1: Reclosable pressure-relief valves [Under development])

ISO 21013-2:2007 Cryogenic vessels -- Pressure-relief accessories for cryogenic service -- Part 2: Non-reclosable pressure-relief devices + ISO 21013-2:2007/Amd 1:2018

ISO 21013-4:2012 Cryogenic vessels -- Pilot operated pressure relief devices -- Part 4: Pressure-relief accessories for cryogenic service + ISO 21013-4:2012/Amd 1:2019





Thank you for your attention

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The content of the training includes contributions from many colleagues from CERN and from external institutes. I wish to thanks them for their precious contributions.



Annex: numerical calculations exercises

Exercise: calculate a thermal shield thickness in an LHC-type (



- Symmetry: point opposite of cooling line is an isolated tip
- Take $\frac{1}{2}$ shield: $L = \frac{1}{2} \frac{A_s}{1 m} = \frac{1}{2} 2.35 m = 1.17 m$
- Uniform heat deposition: $q = \frac{q_{shield}}{A_s} = \frac{2.55 W}{2.35 m^2} = 1.08 W/m^2$
- Let's set the maximum $\Delta T_{\text{max}} = 5 \text{ K}$
- Take k aluminium (Al6061) at ~80 K: 85 W/(K m)

 \rightarrow t = 1.7 mm



Exercise: calculate helium heat transfer in a thermal shield in an LHC-type cryostat $T \uparrow Wall, T(x) \to T$

- Non-isothermal cooling along an L=3 km long thermal shielding line
- Cooling line: D=80 mm, roughness aluminium drawn tube (ϵ = 0.05 mm)
- $T_{in} = 60 \text{ K}, T_{out} < 75 \text{ K}$
- p_{in} = 5 bar
- Calculate mass flow, heat exchange parameters, and pressure drop
- Assumptions: $T_m(x) = \frac{1}{2}(T_{out}+T_{in}) = \text{const.}$; $\Delta T_{in} = \Delta T_{out}$ (wall with uniform heat flux \dot{q})
- Take $T_{out} = 75 \text{ K}$
- $T_m = \frac{1}{2} (75 \text{ K} + 60 \text{ K}) = 67.5 \text{ K}$
- $\dot{q} = q_{shield} \cdot L = 2.55 \text{ W/m} \cdot 3000 \text{ m} = 7'650 \text{ W}$ (see previous calculation of thermal shield heat load)
- From enthalpy balance (with $T_{in} = 60$ K, $T_{out} = 75$ K, and $C_p(67.5 \text{ K}) = 5300 \text{ J/kg/K}) \rightarrow \dot{m} = \frac{\dot{q}}{C_n (Tout Tin)} = 0.096 \text{ kg/s}$
- Calculate flow properties and thermal convection heat exchange (use Cryostat Toolbox):
 - Re = 1.9 10+5 , turbulent OK !
 - V = 5.4 m/s
 - Pr = 7.03
 - Nu = 345
 - h = 247 (W/m²/K)
 - $\Delta T_{in} = \Delta T_{out} = 0.04 \text{ K} (T_w \approx T_m)$
- Calculate pressure drop (use Cryostat Toolbox):
 - Δp = 380 mbar (~8%)





Radiation calculation exercises for an LHC-like cryostat

Exercise: Radiation in LHC-like cryostat

- Thermal radiation HL for a 1-m cryostat unit length
- Vacuum vessel diameter: $1m (A_2 = \pi x 1 = 3.14 m^2)$
- Cold mass diameter: $0.5 \text{ m} (A_1 = \pi \times 0.5 = 1.57 \text{ m}^2)$
- T₁ cold mass: 2 K
- T₂ vac.vessel: 293 K
- $\mathcal{E}_1 = 0.12$ (st.steel, mec.polished, 2 K)
- $\mathcal{E}_2 = 0.2$ (low carbon.steel, mec.polished, 293 K)

 \rightarrow q₁₋₂ = 63.5 W (41.6 W/m²)

- Sensitivity wrt & uncertainties:
 - ➢ E₁ = 0.18 (+50%), E₂ = 0.20
 - \succ €1 = 0.12, ε_2 = 0.30 (+50%)
 - \succ $\epsilon_1 = 0.18 (+50\%), \epsilon_2 = 0.30 (+50\%)$
 - Note: assuming black bodies ($\mathcal{E}_1 = \mathcal{E}_2 = 1$) → $q_{1-2} = 656$ W ! (x10!)



 \rightarrow q₁₋₂ = 87 W (+37%)

 \rightarrow q₁₋₂ = 69 W (+9%)

 \rightarrow q₁₋₂ = 98 W (+54%)

 $\boldsymbol{\zeta}$

 $\underline{\sigma A_1(T_1^{\ 4} - T_2^{\ 4})}$

 $q_{1_{2}} = \frac{1}{\frac{1}{\varepsilon_{1}} + \frac{A_{1}}{A_{2}} \left(\frac{1}{\varepsilon_{2}}\right)}$



0.1

0.01



0.2

εssi

0.3

0.4

Exercise: Radiation in LHC-like cryostat (cont.d)

0.8





• Sensitivity with vac.vessel diam. (D_e): ~12 W/m

• Sensitivity with inner vessel diam. (D_i): ~ 100 W/m



 $(D_i=0.5m, D_e=1m)$ 65 q1-2 (W) Q1(De) 60 $\frac{dq_{1-2}(De)}{dD_{e}} = 12.3$ W/m 55 50 50 0.8 1.2 1.4 0.6 1 0.5 De (m) 1.5 Sensitivity with Di (De=1m) 100 80 (D_i=0.5m, D_e=1m) q1-2 (W) 6(Q1(Di) $dq_{1-2}(Di)$ = 102 W/mdDi 20 10 0.2 0.4 0.6 0.8

Di (m)

Sensitivity with De (Di=0.5m)

70

0.2

Exercise: Radiation in LHC-like cryostat (cont.d)

• Floating AI shield



Floating Al shield:

- Thermal shield diameter: $0.75 \text{ m} (A_s = \pi \times 0.75 = 2.35 \text{ m}^2)$
- F_{1s}= 1; F_{2s}= 1
- $T_s = 80 \text{ K} \text{ (first guess)}$
- $\mathcal{E}_{s,1} = \mathcal{E}_{s,2} = 0.1$ (Aluminum, mec.polished, 80 K)
- \rightarrow q₁₋₂ = q_{1-s} = q_{s-2} = 28.5 W
- Calculate Ts by *trial and error* to obtain power balance $q_{1-s} = q_{s-2}$
- → $T_s = 260 \text{ K}$ → increase $\mathcal{E}_{s,1} = \mathcal{E}_{s,2}$ (0.15?) and recalculate
- \rightarrow q₁₋₂ = q_{1-s} = q_{s-2} = 35.4 W (to be compared to 63.5 W without shield)
- → $q_{1-s} = 35.4 \text{ W} (22.5 \text{ W/m}^2), q_{s-2} = 35.4 \text{ W} (15 \text{ W/m}^2)$

\rightarrow 1 floating thermal shield reduces to <u>almost ½ the radiation</u> to the low T (close to flat plates approximation for this geometry)





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Exercise: Radiation in LHC-like cryostat (cont.d)

 $q_{s-e} = \frac{\sigma Aav(Ts^4 - Te^4)}{(N+1)(\frac{2}{\varepsilon} - 1)}$

- MLI with N reflectors, <u>floating shields</u>
- Radiation between shield and vac.vessel (flat plat approximation):

- $T_s = 80 \text{ K} \text{ (first guess)}$
- $\mathcal{E}_{e} = 0.2$ (low carbon.steel, mec.polished, 293 K)
- $\varepsilon_s = 0.08$ (Aluminium reflector, electrolytical deposition, 80 K)
- $\mathcal{E}_{av} = \frac{1}{2} (\mathcal{E}_s + \mathcal{E}_e)$ (average emissivity)
- $A_{av} = \frac{1}{2} (A_s + A_e)$ (average area)
- \rightarrow $\rm q_{s\text{-}e}$ = 2.7 W (0.14 W/m^2) $\,$ (with $\rm T_{s}$ = 80 K)
- Radiation between shield (80 K) and helium vessel (formula between enclosed cylinders):
- \rightarrow q_{i-s} = 0.23 W (0.012 W/m²) (with T_s = 80 K)
- Calculate T_s by trial and error (and tune \mathcal{E}_s) to obtain power balance $q_{s-e} = q_{i-s}$ (floating shield condition)
- \rightarrow T_s = 143 K, \rightarrow E_s= 0.1

 $q_{s-e} = q_{i-s}$ → $q_{s-e} = 2.6 \text{ W} (1.65 \text{ W/m}^2)$ → $q_{i-s} = 2.6 \text{ W} (0.96 \text{ W/m}^2)$

\rightarrow MLI (30 layers) reduce the HL to the thermal shield (and cold surface) by a factor x25 wrt no shield





Exercise: Radiation in LHC-like cryostat (cont.d)

 $q_{s-e} = \frac{\sigma Aav (Ts^4 - Te^4)}{(N+1)(\frac{2}{\varepsilon} - 1)}$

- MLI with N reflectors, actively cooled shield
- Radiation between shield and vac.vessel (flat plat approximation):
 - N = 30
 - $T_s = 80 \text{ K}$ (now an input)
 - $\mathcal{E}_s = 0.08$ (Aluminium reflector, electrolytical deposition, 80 K)
 - $\mathcal{E}_{av} = \frac{1}{2} (\mathcal{E}_s + \mathcal{E}_e)$ (average emissivity)
 - $A_{av} = \frac{1}{2} (A_s + A_e)$ (average area)

 \rightarrow q_{s-e} = 2.78 W (1.0 W/m²)

• Radiation between shield (80 K) and helium vessel (2 K) (formula between enclosed cylinders):

 $\rightarrow q_{i-s}^* = 0.23 \text{ W} (0.14 \text{ W/m}^2) (x10 \text{ times less than with floating shield })$

• Radiation heat extraction from thermal shield (not to be forgotten!):

 \rightarrow q_{shield} = q_{s-e} - q_{i-s} = 2.55 W

→<u>Actively cooled shield with MLI</u> dramatically reduces radiation to the low T: this <u>is a</u> standard practice in cryostats!



CERN

Exercise: Residual gas conduction in LHC-like cryostat

- Typical dimension (space between surfaces): d = 0.25 m
- Good insulation vacuum:
 - <u>p = 10⁻⁶ mbar (10⁻⁴ Pa) ("standard" good vacuum in cryostats)

 </u>
- Calculate λ_{molecule} (between shield and inner vessel):
 ✓ λ_{molecule} = 20 m (~ x100 d) → molecular regime
- Calculate residual gas conduction with Kennard's law:
 ✓ Q_{res} = 0.034 W (0.02 W/m²)
- Negligeable additional contribution wrt previously computed radiation:

 q_{i-s} = 0.23 W (0.14 W/m²)
- Degraded insulation vacuum:

 $\sqrt{p} = 10^{-5} \text{ mbar} (10^{-3} \text{ Pa}) (degraded vacuum from helium leak in cryostats)$

• Calculate $\lambda_{\text{molecule}}$ (between shield and inner vessel):

✓ $\lambda_{\text{molecule}} = 2 \text{ m} (\sim x10 \text{ d}) \rightarrow \text{still molecular regime}$

• Calculate residual gas conduction with Kennard's law:

 $\sqrt{Q_{res}} = 0.34 \text{ W} (0.22 \text{ W/m}^2)$

→ gas conduction contribution ($Q_{res} = 0.22 \text{ W/m}^2$) now higher than radiation ($q_{i-s} = 0.14 \text{ W/m}^2$). Total HL to cold surface: 0.34 W/m²



Summary of radiation HL exercises





Spare slides

Material mechanical properties at cryogenic temperatures





1. PROPRIÉTÉS MÉCANIQUES DES MATÉRIAUX

100

0

200

300



Limite de rupture (MPa)







300

T (K)

Fig. G. - Module d'élasticité, limite élastique, limite de rupture, allongement à la rupture, énergie de rupture mesurée au mouton de Charpy, limite de fatigue après 10⁶ cycles pour quelques matériaux [Baron].

Source: Techniques de l'ingenieur

Material mechanical properties at cryogenic temperatures





PROPRIÉTÉS MÉCANIQUES

Les lettres qui suivent les désignations indiquent les traitements thermiques ou les traitements mécaniques (écrouissage).

Fig. H. – Limite d'élasticité et allongement à la rupture d'alliages d'aluminium, d'alliages spéciaux et de diverses nuances d'aciers inoxydables

Source: Techniques de l'ingenieur

Thermal conductivity in solids (& metals)

The conductivity is attributed to the movement of **conduction electrons** ("electron gas"), ke, and the effects of **phonon lattice vibrations**, kl :

$$k = k_e + k_l$$

 $k \approx k \gg k_{l}$

- In metals, the electron contribution dominates :
- The movement of conduction electrons is impeded by scatter: interactions with phonons, and interactions with impurities/imperfections. We can introduce *thermal resistivities*:
- $\frac{1}{k_e} = \frac{1}{k_p} + \frac{1}{k_i} \qquad \qquad \frac{1}{k_p} = a_p T^2 \quad \frac{1}{k_i} = \frac{a_i}{T}$ be expressed as: $k = \frac{1}{a_p T^2 + \frac{a_i}{T}}$ $k_{\text{max}} = \frac{3}{2^{\frac{2}{3}}} a_p^{\frac{1}{3}} a_i^{\frac{2}{3}} \text{ at } T = \left(\frac{a_i}{2a_i}\right)^{\frac{1}{3}}$ And has a **maximum**, which shifts at higher T with increasing impurity (see coppers) and vanishes for highly impure alloys (see steels), as impurity scatter dominates, and for which at T < RT:
- For metals, analogy between electron thermal and electrical diffusion \rightarrow Wiedemann-Franz law

Therefore for **metals**, the resistivity can be expressed as:

- Good agreement at T<< RT >> T
- Better agreement from T<< to T>> with increasing impurities

$$k = \frac{L_o}{\rho_e} T$$

 $k \cong \frac{T}{k}$

Lorentz constant

$$Lo = 2.45 \cdot 10^{-8} \left(\frac{V}{K} \right)^2$$
 (Constant for metals)
103



and $a_{p}a_{i}$ constants

Vacuum in cryostats







- 2-4.5 K surfaces have high pumping speed & capacity.
- Gas species have very low vapour pressure except helium.
- Without helium leaks, equilibrium pressures $\leq 10^{-6}$ mbar are obtained

He gas conduction



- **Viscous regime** ($\lambda_{\text{molecule}} \ll d$):
 - At "high" gas pressure: classical conduction (Fourier law-like)
 - independent of pressure
 - (*natural convection* should be added !)

Molecular regime ($\lambda_{\text{molecule}} >> d$):

- At "low" gas pressure
- Kennard's law
- Conduction is proportional to p
- A1 is the surface receiving the flow —
- $-\alpha(T) \rightarrow accommodation coefficient$ depending on gas species, T1, T2 and surface geometry (applicable for flat parallel surfaces, coaxial cylinders and spheres)

$$P_{\text{plecule}} = \text{mean free path}$$

$$= \frac{\eta}{p} \sqrt{\frac{\pi R T}{2 M}} \qquad \begin{array}{l} \eta = \text{gas viscosity in } [Pa. s] \\ p = \text{pressure in, } [Pa] \\ T = \text{temperature, K} \\ R = \text{gas constant } [J.K^{1}.\text{mol}^{-1}] \\ M = \text{molar mass } [\text{kg/mol}] \end{array} \qquad \begin{array}{l} T_{1} \\ T_{1} \\ A_{1} \\ \end{array} \qquad \begin{array}{l} T_{2} \\ A_{1} \\ A_{2} \end{array} \qquad \begin{array}{l} T_{2} \\ A_{2} \\ \end{array} \qquad \begin{array}{l} T_{2} \\ T_{2} \\ \end{array} \qquad \begin{array}{l} T_{2} \\ T_{2} \\ \end{array} \qquad \begin{array}{l} T_{2} \\ T_{2} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{2} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{2} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{2} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{2} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{3} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{3} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{3} \\ T_{3} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{3} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{3} \\ T_{3} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{3} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{3} \\ T_{3} \\ T_{3} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{3} \\ T_{3} \\ T_{3} \\ T_{3} \\ T_{3} \\ \end{array} \qquad \begin{array}{l} T_{3} \\ T_{3} \\$$

$$\begin{array}{l} \rho = \mbox{ gas density in } [kg/m^3] \\ R = ideal \mbox{ gas constant} \\ \lambda = mean \mbox{ free path } [m] \\ C_v = \mbox{ specific heat at constant pressure } [J.kg^{-1}K^{-1}] \end{array}$$

$$Q_{res} = A_1 \cdot \alpha \cdot \left(\frac{\gamma + 1}{\gamma - 1}\right) \cdot \left(\frac{R}{8\pi}\right)^{1/2} \cdot \frac{p}{\sqrt{MT}} \cdot (T_2 - T_1)$$

with
$$\gamma = C_p/C_v$$

with $k = \frac{1}{3} \rho \sqrt{\frac{8RT}{\pi M}} \lambda C_v$

Accommodation coefficient α

$$\alpha = \frac{\alpha_1 \alpha_2}{\alpha_2 + \alpha_1 (1 - \alpha_2) \frac{A_1}{A_2}}$$

econtinuou coefficient ai				
Temp. [K]	Helium			
300	0.3			
80	0.4			
20	0.6			
4	1			

Thermal conductivity in solids (& metals)

The conductivity is attributed to the movement of **conduction electrons** ("electron gas"), ke, and the effects of **phonon lattice vibrations**, kl :

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 (Constant for metals)
106



and $a_{p}a_{i}$ constants

2 main mechanisms of interest for cryostats



- Vaporisation in pool boiling (2-phase)
 - Latent Heat (Lv) of vaporisation
 - Isothermal cooling (T constant if P constant)



Vaporisation under 1 W heat load

Cryogen	Latent Heat (at 1tm) [kJ/kg]	[mg/s]	[l/h] (liquid)	[l/min] (gas NTP)
Helium	21	48	1.38	16.4
Nitrogen	199	5	0.02	0.24

- Forced internal (tube) convection of single-phase fluid:
 - Non-isothermal cooling: enthalpy change of fluid (c_p assumed constant)
 - Depends on thermo-hydraulics of the flow (see next slide)
 - Used in cooling of thermal shields (supercritical He)

For more cooling mechanisms see dedicated lectures

Helium as a coolant for SC devices



Property

(ref. S. Van Sciver, Helium Cryogenics)

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⁴He

 N_2

FRN

Units
Heat capacity

- Specific heats: $c_{\rm P} = \left(\frac{\partial Q}{{\rm m}\,{\rm d}{\rm T}}\right)_P = \left(\frac{1}{{\rm m}}\frac{\partial {\rm H}}{\partial {\rm T}}\right)_P \qquad c_{\rm V} = \left(\frac{\partial Q}{{\rm m}\,{\rm d}{\rm T}}\right)_V = \left(\frac{1}{{\rm m}}\frac{\partial U}{\partial {\rm T}}\right)_V$
- For (incompressible) substances: Cp(T) = Cv(T) = C(T)
- Change of internal energy U (or enthalpy):

 $\blacktriangleright \Delta \mathbf{U} = Q = m \int_{T_1}^{T_2} c(T) dT$

- Cooling (or heating) power: $P(T) = m c(T) \frac{dT}{dt}$
- Specific heats/unit vol. sometimes preferred
- Below 10 K enthalpy of helium overtakes all solids







Design stresses for some materials

- Design stresses for plates less than 12 mm thick applicable to membrane stress (safety factor 1.5 included) according to EN 13445-3
- For stainless steels:

For stainless steels:		$f = \frac{R_{p1.0}}{1.5}$		$f_{test} =$	$f_{test} = \frac{R_{p1.0}}{1.05}$	
	Material	R _{p1.0} (MPa)		f (MPa)	f _{test} (MPa)	
	1.4306 (304L)	240		160	228	
	1.4435/1.4404 (316L)	260		173	247	
	1.4406/1.4429 (316LN)	320		213	304	
	AW 5083-0/HIII			83		
For aluminium-magnesium alloys:		f	=	$\min(\frac{R_{p0.2}}{1.5}, \frac{R_m}{2.4})$	$f_{test} = \frac{R_{p0.2}}{1.05}$	
	Material	$R_{p1.0}/R_m$ (MPa)		f (MPa)	f _{test} (MPa)	
	AW 5083-O/HIII	125/270		83	119	



Best practices



- Using a coherent set of standards throughout the lifecycle of the cryostat is the simplest and safest approach. As an example when using only EN harmonised standards:
 - Error margins of pressure relief devices are taken into account in the design rules
 - The design rules are only applicable if the material has enough ductility
 - Materials certified for pressure vessels have measured minimum fracture toughness
 - Safety factors included in buckling formulae take into account shape imperfections up to the allowable tolerances layed out in the manufacturing section of the standards
 - The extent of welding inspection must be compatible with the joint coefficient used in thickness calculations
 - Coherence of test pressure and testing procedure with the design rules

Liquid helium pumping

- Pressure reduction by pumping above helium liquid at 4.2 K, with latent heat L(T) and specific heat c(T):
 - L(T) dm = m c(T) dT
- Neglecting external heat loads and vessel heat capacity
- Integrating over T and m, with m_0 initial helium mass:





(ref. R.R.Conte, Elements de Crogenie)



LHC dipole cryostat assembly





Towing through, sliding on vacuum vessel



Assembly bench

Expansion joints (bellows) for cryogenic lines

- Compensation of longitudinal thermal contractions
- Compensation of transversal and angular offsets (not twist!)

→Extensive use in cryo-magnet interconnections

- Beware of bellows stability issues in pressurised lines:
 - Stiff guiding
 - Limit transversal and angular off-sets





RHIC, BNL

LHC String 1, CERN

