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Helium Cryostats for Superconducting Devices

Vittorio Parma CERN – SY/RF Group

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- Helium cryostats for SC devices, functions and requirements
- Examples of cryostats
- Mechanical design and construction of cryostats:
	- Materials for cryostats and their properties
	- Pressure/vacuum vessels, codes, and norms
	- Supporting systems
- Heat transfer mechanisms at cryogenic temperatures:
	- Thermal radiation and thermal design solutions (thermal shielding, MLI)
	- Thermal conduction and thermal design solutions (feedthroughs, heat intercepts)
- Notions of cryogenic safety
- Calculation tool: *Cryostat Toolbox v.1.1*

1 h

1 h

1 h

Mechanical design and construction of cryostats

Materials in cryostats

- Helium tank (for SC device, ph.separator, etc.):
	- ✓ austenitic st.steels (Fe-Cr-Ni): 304L(1.4307), 316L(1.4404), 316LN
	- ✓ titanium alloys (Grade 7, Grade-5 (Ti-6Al-4V)) in SRF
- Internal (cold) supporting system
	- \checkmark Composites (e.g. GFRE, CFRP, ULTEM)
	- \checkmark St. steel, titanium alloys (tie rods)
- Thermal shielding:
	- \checkmark aluminum alloys (series 5xxx, 6xxx, 7xxx)
	- \checkmark Copper (Cu OF, Cu OFE)
- Vacuum vessel:
	- \checkmark Low carbon steels (e.g. DIN GS-21 Mn5)
	- \checkmark st. steels (304L)
- Cryogenic piping and expansion joints (bellows):
	- \checkmark st. steel (304L)
	- \checkmark Cu (HX tubes)
- RF Couplers/HOM (for SRF):
	- \checkmark St. steel Cu plated, Nb, ceramics, etc.
- Current leads (for SC magnets)
	- \checkmark Cu, HTS, st. steel, elect. insulating (Kapton), thermal insulating (G10), etc.
- Magnetic shielding (for SRF, as needed)
	- ✓ μ-metal, Cryoperm®, etc.

Useful material standards for cryostats

Relevant mechanical failure mechanisms in cryostats

• Helium tanks:

- \checkmark Rupture (rare!) or permanent deformation due to excessive mechanical stress (pressure loads)
- \checkmark Helium leaks in welds or material micro-crack
- Cryogenic lines/expansion joints:
	- \checkmark Buckling of expansions joints with or without rupture/leaks
	- \checkmark Helium leaks in welds or material micro-crack
- Vacuum vessels:
	- \checkmark Buckling under external pressure
	- \checkmark Permanent deformations due to excessive stress concentrations

• Internal supporting systems:

- \checkmark Failure due to excessive mechanical stress
- \checkmark Failure due to thermo-mechanical stress
- \checkmark Buckling under compressive load
- Thermal shields:
	- \checkmark Permanent deformation due to thermo-mechanical stress (CD/WU transients)
- Alignment jacks:
	- \checkmark Break of floor/fixations due to excessive load

Tensile test material properties

Ductile vs. brittle

Low temperature effect of tensile properties

- Ductile materials tend to become brittle (fragile) at cryogenic temperatures
- Increase of the yield and ultimate strength
- Young modulus also (marginally) increases.

Mechanical Properties at cryogenic temperatures

- Yield, ultimate strength
	- ✓ Yield and ultimate strengths increase at low temperature

Mechanical Properties at cryogenic temperatures (cont.d)

• Young modulus

• Fracture toughness

From: Technique de l'Ingénieur

Thin shells under external pressure

Buckling:

- Non-linear phenomenon. Actual critical pressure depends on initial imperfections: Safety factor needed!
- Buckling critical pressure for a thin tube of infinite length

$$
p_{cr} = \frac{E}{4(1 - v^2)} \left(\frac{t}{r}\right)^3
$$

• A conservative rule of thumb for stainless steel tubes under vacuum:

$$
\frac{t}{r} \ge \sqrt[3]{\frac{0.1MPa \times 4 \times (1 - 0.3^2)}{200 \times 10^3 MPa}} = 0.012
$$

• If we use a safety factor of 3:

$$
\frac{t}{r} \geq 3.7\%
$$

Example:

- $r = 500$ mm
- t > 18.5 mm
- Alternatively, we need to add reinforcements (e.g LHC vessels, t=12 mm)

Thin shells under internal pressure

For preliminary calculation *For detailed calculation see EN 13458-2 Cryogenic vessels – static vacuum insulated vessels*

valid for $r \geq 10t$

Example: cyl.helium tank

- $r = 400$ mm
- $-p = 4 \text{ barg } (0.4 \text{ MPa})$
- σ_a = 160 MPa (304L, Rp_{0.2}= 240 MPa, SF=1.5)
- t ≥ 1 mm

(Note: under vacuum (previous calculation) \rightarrow t \ge 15 mm !)

Pressure vessel codes regulations

- Pressure European Directive 2014/68/EC (PED) is a legal obligation in the EU since 2002
	- Applies to internal pressure **≥ 0.5 bar gauge**
	- Vessels must be designed, fabricated and tested according to the requirements defined
	- Establishes the conformity assessment procedure depending on the vessel category, which depends on the stored energy, expressed as Pressure x Volume in bar.l

For vessels with non-dangerous gases (cryogenic liquids are treated as gas)

Harmonised codes and standards

-
- Harmonised standards give presumption of conformity with the PED, within their scope. Useful codes for cryostat design and fabrication, including safety devices:

Very useful guidelines and design rules

Final lathe machining

ess relieving

LHC dipole Vacuum Vessels

Main features:

- Pipeline standard size: **36-inch OD (1013 mm)**, **12-mm thick**, low carbon steel (DIN GS-21 Mn5) tubes
- St. steel extremity flanges
- Material resilience: > 28 J/cm2 at -70°C
- Forged cradles, welded rings reinforcements
- Dimensional stability:
	- Stress relieving
	- Final machining to achieve tolerances at interface

Production:

- 1250 units
- 2 firms
- 4 yrs of production

LHC thermal shields

Aluminium alloy 6063 extrusions and 1100 top sheets

Thermo-mechanical considerations

Thermal expansion of some materials

Thermal stress in composite material assemblies: 3 cases

$$
\sigma 1 = \frac{E1 \, E2 \, A2}{E1 \, A1 + E2 \, A2} (\alpha 2 \, \Delta T2 - \alpha 1 \, \Delta T1) \qquad \sigma 2 = \frac{E1 \, E2 \, A1}{E1 \, A1 + E2 \, A2} (\alpha 2 \, \Delta T2 - \alpha 1 \, \Delta T1)
$$

LHC cryostats: longitudinal thermal contractions

-
- Cold mass, thermal shield, support posts and vacuum vessel must be free with each other to cope with longitudinal thermal contractions
- One fixed point per each component
- Leave plays to cope with all extreme T cases (ex. Cold mass cold, thermal shield warm)
- Guided sliding of cold mass onto vacuum vessel \rightarrow slot/key
- Flexible thermalisation anchors

Supporting systems

LHC Cryomodule, 400 MHz cavities (Nb on Cu) at 4.5 K

LHC Cryomodule Supporting System

LHC magnet Cryostats

- **4-mm thickness**, glass-fiber epoxy
- Manufactured by **Resin Transfer Moulding (RTM):**
	- Suited to a large-scale industrial production (4'700 units)
	- High reproducibility in thermo-mechanical properties

LHC Supporting system

The design is a trade-off between 2 conflicting requirements:

- High flexural stiffness (for mechanical stability) \rightarrow thick and bulky structure
- Low heat in-leaks \rightarrow thin and slender structure and low conductivity material

(F is mainly the result of interconnect forces and gravity component) F = 5 kN x = 0.1 mm θ = 1 mrad

 \rightarrow Flexural stiffness/conductivity as figure of merit in the choice of the material

Resin Transfer Moulding

Lay-up, calculated safety factors, material properties

Triaxial braid and % fiber volumes layup

4 layers of triaxial braid

6 layers

of biaxia hraid

Bending cantilever 40 kN. (vacuum barrier load)

Tsai-Wu ply failure: Safety Factor = **2.7**

SC magnet supporting systems from other machines

Hera dipole

Tevatron

SCC

Supporting system of Tesla/TTF/ILC Cryomodule

Supporting system of SNS and ESS high β Cryomodules

Supporting system of PIP II Cryomodule

SPL cryomodule: RF Coupler as support

Heat transfer mechanisms and thermal design

Heat transfer mechanisms

- Thermal radiation
- Thermal conduction
- Heat intercepts

Inspired by P. Duschene and JP. Thermeau

Thermal Radiation
Thermal Radiation

Stefan-Boltzmann's law

$$
Q = \sigma A T^4
$$
 black body

 $Q = \varepsilon \sigma A T^4$ gray body, $\varepsilon < 1$

 $\sigma = 5.67 \ 10^{-8} \ W \ m^{-2} \ K^{-4}$ Stefan-Boltzmann's constant

A, T area and temperature of the body, ε emissivity

exchange between **black bodies**

$$
Q_{1-2} = F_{12}A_1 \sigma (T_1^4 - T_2^4) = F_{21}A_2 \sigma (T_1^4 - T_2^4)
$$

exchange between gray bodies

$$
Q_{1-2} = E_{12} \sigma A_1 (T_1^4 - T_2^4) = E_{21} \sigma A_2 (T_1^4 - T_2^4)
$$

*Figures source: "*Heat Transfer", A.Bejan, John Wilney & Sons, Inc.

- F, geometrical view factors F_{1-2} (<1) between A_1 and A_2 (or F_{2-1} between A_2 and A_1), with $A_1E_{12}=$ A_2E_{21} .
- E, effective emissivity, a function of view factors and emissivity ε_1 and ε_2 of the bodies

Black body radiation

• Hemispherical monochromatic emissive power [W/m∙m2] (energy per unit time, wavelength, and surface area)

$$
E_{b,\lambda} = \frac{c_1 \lambda^{-5}}{e^{(\frac{c_2}{\lambda T})} - 1}
$$
 Planck's law

 C_1 = 2 π h c^2 = 3.742 10⁻¹⁶ W m^2 $C_2=$ $h c$ $\frac{1}{k}$ = 1.439 10⁻² K m

• Total emissive power (integrating over λ):

$$
Eb(T) = \int_{0}^{\infty} E_{b,\lambda} d\lambda = \sigma \cdot T^{4} \quad (W/m^{2})
$$

with: $\sigma=$ $2\pi^5 k^4$ $\frac{2h}{15} h^3 c^2$ = 5.67 10−8 (W/m² ⋅ K⁴) Stefan–Boltzmann's constant

(k, Boltzmann constant, h, Planck constant, c, speed of light)

In practice: Blackbody emits ~ 420 W/m² at 293 K , and only ~2 W/m² at 77 K (200 times less!)

*Figures source: "*Heat Transfer", A.Bejan, John Wilney & Sons, Inc.

Black and diffuse-gray model

Black model

- $\alpha \rightarrow$ absorptivity $\rho \rightarrow$ reflectivity
- $\tau \rightarrow$ transmissivity

 $\alpha + \rho + \tau = 1$

 $|\alpha=1$ *(black, p = 0, τ = 0)* $\alpha + \rho = 1$ *(opaque,* $\tau = 0$ *)*

Black surface: *α* = 1

 λ

Practical application in cryostats: every gap in shields is a black surface (1 cm² gap exposed to 293 K, $\varepsilon = 0.2 \rightarrow \sim 10 \text{ mW}$)

Diffuse-gray model

*Figures source: "*Heat Transfer", A.Bejan, John Wilney & Sons, Inc.

 λ_{2}

Diffuse-gray model (good approximation for real surfaces in engineering):

- Gray: $ε_λ(λ, T) ≈ ε(T)$
- Diffuse emitter/absorber (not directional)
- Opaque $(\tau = 0)$
- $\alpha(T) = \varepsilon(T)$

40

normal

Emissivity

• ε depends on wave-length and direction (neglected in gray-diffuse model). In metals emissivity rises sharply and up to more than 40% above 50 deg. incidence from the surface normal

Métal

- Clean, well-polished metallic surfaces have smaller ε , non-metallic materials have higher ε
- Metals: ε decreases with decreasing temperature, almost linearly at cryo temperatures
- Non-metals: ε may decrease or increase with decreasing temperature (increases for organic materials)
- Engineering approach. Due to uncertainties on real ε values, take conservatively high values for preliminary design. Measurement validation may be necessary

300 $0,02$ Or 0.01 80 300 $0,02$ Argent 80 0.01 $\overline{4}$ $0,005$ 300 0.25 Aluminium commercial brut 80 $0, 12$ \overline{A} $0,07$ 300 $0,20$ 0.10 Aluminium poli mécanique 80 0.06 $\overline{4}$ 300 0.15 Aluminium poli électrolytique 80 0.08 $\overline{4}$ 0.04 Chrome 300 $0,08$ 300 0.10 Cuivre poli mécanique 80 0.06 \overline{A} $0,02$ 300 0,050 Étain 80 0.012 \overline{A} 0,013 300 0.05 Nickel 80 $0,02$ 300 0.03 Laiton poli 80 0.03 \overline{A} $0,02$ 300 $0,20$ 80 Acier inoxydable 18-8 $0,12$ $0,10$

Tableau G. - Émissivité totale normale de quelques métaux

 $T(K)$

 ε_n

Ref. https://neutrium.net/heat-transfer/emissivity/

Ref. R.B.Scott, Cryogenic Engineering, (Van Nostrand, New York, 1959; Y.S.Touloukian, Thermophysical Properties of Matter, (Plenum Press, New York, 1995))

Ref. Cryogenie, ses applications en supraconductivite.Techniques de l'ingenieur, Ed.1995

Radiation between 2 diffuse-gray enclosures

 σT_2^4 A_2 , T_2 , ϵ_2 $q_1 \longrightarrow {\mathop{\bigwedge \bigwedge^{}_{l=1}^{L_{b,1}}}}\limits_{\substack{1-\epsilon_1 \\ \epsilon_1 A_1}} \frac{J_1}{\frac{1}{A_1 F_{12}}}\quad \frac{J_2}{\frac{1-\epsilon_2}{\epsilon_2 A_2}} \longleftarrow q_2$ dA_1 (Fig. 10.22) 4 4 $\sigma (T_1^{\; +} - T_2^{\; +})$ 2 • Radiation balance between $q_{1-2} = \frac{1}{1-\varepsilon_1} \frac{1}{1}$ -2 $=$ $\mathcal E$ ${\cal E}$ 2 1 $-\frac{1}{\epsilon_1} + \frac{1}{\epsilon_2} +$ A1 and A2 surfaces: 1 A_1 A_1 F_{12} ε_2 A $\mathcal E$ $\mathcal E$ 2 A 2

 $\sigma A_1 (T_1^4 - T_2^4)$

1

 $\overline{\varepsilon_2}$

 $+\frac{A_1}{4}$ $\overline{A^{}_2}$

• For 2 enclosed cylinders or spheres (not necessarily concentric!), $F_{12}=1$:

1

 $\overline{\varepsilon_1}$

For cryostats, to **reduce heat load** to inner cold surface:

 \overline{q}

 1_{-2} =

- **Limit size of A₁** (SC device vessel)
- **Reduce A²** (vac.vessel as small as possible)
- **Small emissivities**: *ε¹* reduced by low T; *ε²* at RT & moderated by A1/A²

*Figures source: "*Heat Transfer", A.Bejan, John Wilney & Sons, Inc.

Radiation between 2 diffuse-gray flat plates

• Radiation balance between A1 and A2 (A1=A2=A), $F_{12}=1$:

Radiation with an intermediate floating shield

 \rightarrow Can be generalized to N shields

• Radiation balance between A1 and A2:

• For flat surfaces approximation, and same ε :

$$
q_{1-s} = \frac{\sigma A (T_1^4 - T_s^4)}{(\frac{2}{\varepsilon} - 1)} = \frac{\sigma A (T_s^4 - T_2^4)}{(\frac{2}{\varepsilon} - 1)} = q_{s-2} \qquad \Rightarrow T_s^4 = \frac{T_1^4 + T_2^4}{2}
$$

 $q_{1-2} =$ $\sigma A (T_1^4 - T_2^4)$ 2(2 $\overline{\varepsilon}$ − 1)

 \rightarrow with 1 shield $\frac{1}{2}$ of the rate without shield

$$
q_{1-2} = \frac{\sigma A (T_1^4 - T_2^4)}{(N+1)(\frac{2}{\varepsilon} - 1)}
$$

 \rightarrow with N shield $1/(N+1)$ of the rate without shield

N shields \rightarrow Multi Layer Insulation (MLI)

Working principles:

- Low emissivity of aluminium layer
- Multi-layer to enhance radiation protection:
	- N+1 radiation shielding
- Minimal thermal conduction between reflective layers \rightarrow interposing of isolating layers (e.g polyester net):
- Enhanced performance at low $T \rightarrow \alpha$ use actively cooled shield:
	- Lower emissivity of reflective material layers at low T
	- Reduce radiation from inner-most layers, cooled at T of shield
	- Extract heat at higher thermal shield $T \rightarrow$ thermodynamic efficiency

MLI material

LHC MLI:

- **Reflecting film**: 6 µm thick polyethylene teraphthalate (PET) film coated with 400 Å minimum aluminium on each side (Physićal Vapor Deposition process)
- **Spacer**: polyester net of very low weight (< 5 g/m2)
- 10 or 15 layer **pre-assembled blankets** (outermost layer reinforced with a polyester net)
- Blanket overall **thickness**: > 2 (3) mm for 10 (15) layers
- **Perforated layers** for outgassing: 0.05-0.15 % surface

LHC MLI blankets **Features:**

1 blanket (10 reflective layers) on cold masses (1.9 K) 2 blankets (15 reflective layers each) on Thermal Shields (50-65 K) Reflective layer: double aluminized polyester film (2 km^2) Spacer: polyester net

Stitched Velcro™ fasteners for rapid mounting and quality closing

MLI: How many reflective layers (N)?

Arbitrary units

- No straightforward answer ! Not just a matter of N !
- Complex system to model, with parameters needing experimental qualification
- Radiation vs. conduction
	- \checkmark Radiation reduces as 1/N
	- \checkmark Conduction proportional to packing density (N/mm)
- Residual helium gas conduction
	- \checkmark Negligeable at res. pressure $p < 10^{-4}$ Pa (10⁻⁶ mbar)
	- \checkmark Sizeable contribution at res. pressure 10^{-4} Pa $\lt p \lt 10^{-3}$ Pa (10⁻⁵ mbar)
	- ◯ Dominates at res. pressure $p > 10^{-2}$ Pa (10⁻⁴ mbar)
- Packing density should be limited \rightarrow typically 20-25 N/cm
	- ➢ Avoid "compressed" blankets (do not put as much MLI as you can fit!)
	- ➢ Reserve space allocation for MLI blankets
	- Consider differential thermal contractions wrt support (AI shields, cold mass...): blankets must remain quite loose at cold
- Overall performance depends very much on:
	- \checkmark Application design solutions
	- \checkmark Craftsmanship quality

MLI application: important tips

Handle MLI with gloves (fingerprints are a black body!)

Some tapes are resin coated = black body ! Check conductivity

loose at RT (MLI contracts more than metal support)

Not tool much MLI (risk of thermal shorts)

Thermal path warm to cold layers

(images: courtesy of Meyer Tool & MFG.)

Performance measurements on MLI samples

- 300 K 77 K, abundant literature *(see a few ref. [1], [2])*
- 77 K 4 K, fewer results. CERN experimental work *(see a few ref.[3],[4],[5])*
- Some values, in good vacuum (<10-4 Pa) [3]:

[1] T.Nast, Multilayer Insulation Systems, in Handbook of Cryogenic Engineering, ed. J.G.Weisend II, Taylor & Francis, Philadelphia (1998),

[2] M. G. Kaganer, Thermal Insulation in Cryogenic Engineering, Jerusalem, Israel Program for Scientific Translation, (1969),

[3] L.Mazzone et al., Measurements of Multi-Layer Insulation at high boundary temperature, using a simple non-Calorimetric method. Proceedings ICEC 19, 2002, Grenoble, France.

[4] Ph.Lebrun et al., Investigation and qualification of thermal insulation systems between 80 K and 4.2 K, Proceedings ICEC/ICMC, 1992, Kiev, Ukraine

[5] V.Venturi, Thermodynamic and technological optimization of complex insulation systems. PhD thesis, 2019, WUST University, Poland.

Practical MLI performance values

- MLI samples measured performance is considerably degraded in applications due to the engineered solutions and installation procedures:
	- ➢ pre-assembled blankets vs. rolled MLI
	- \triangleright complex (non developable) geometries
	- \triangleright junctions, stitches, VelcroTM fasteners, etc.
	- \triangleright higher than ideal packing density (e.g. self-weight compaction)
	- ➢ thermal shorts between cold and warm layers (e.g. overlapped blanket closure)
	- \triangleright quality of assembly (lab vs. industrial scale)
- Engineering values: what values should one use for HL first estimates? \triangleright Take generous margins. Rule of thumb \rightarrow x 2 sample measurements
- LHC cryostat (+) (a thermally well optimized large-scale application), average measure on 2.7 km length sector :
	- \geq 293 K to 50 K thermal shield with 30 MLI layers: \rightarrow ~1 W/m²
	- \geq 50 K to 2 K magnet with 10 MLI layers: \rightarrow ~ 54 mW/m²

Summary of radiation HL exercises (for details see spare slides)

Thermal Conduction

Thermal Conduction

- When a T gradient exists in a body, there is a heat transfer from the high T region to the low T region (Fourier Law):
- For one-dimensional problems (ex. a bar or tube):
- k is the thermal conductivity $(W m^{-1} K^{-1})$, normally a function of P,T, material structure, non-homogeneity, anisotropy (ex. Composite materials).
- k is strongly T-dependent and non-linear at low T
- "good conductors" vs. "poor conductors" \rightarrow k range \sim 5-6 orders of magnitude

 0.1

Thermal conductivity of various materials

- Metals: mainly free electron contribution
- Resistivity from electron scatter with phonons (lattice vibrations) α T² and with impurities α 1/T
- Increasing effect of impurities in less pure metals and dominates in alloys
- Maximum of conductivity reduces and shifts towards higher T with increasing impurities
- Al and st.steel alloys: conductivity α T
- Non cristalline materials and insulators dominated by phonon contribution

Thermal conductivity in epoxy-based composite materials

- Low conduction (little electron conduction), essentially phonon driven
- Anisotropic structure, (fibers/matrix) with constituentsspecific thermal conductivity properties
- Conductivity highly depends on:
	- ➢ Material (fiber) orientation
	- \triangleright Ratio between fibre and matrix (Vf)
- Glass-fiber is the "conductive" fraction and also the "structural" constituent
- Epoxy is the "isolating" fraction material and is the "less structural" constituent

(Data from Schwartzberg F.H., Cryogenic Material Data Handbook, Martin Marietta Corrp, Denvers, Co, 1970)

Longitudinal and transversal conductivity laminate studies for LHC supports, (based on data from Schwartzberg F.H.), collaboration CERN-ESIGEC (Univ.Savoie), 1997

- Vf typically around 40-70%
- Cryogenic grade G10-CR and G11 are widely used standard laminates in various forms (plates, tubes, rods). Properties data can be found in: <https://trc.nist.gov/cryogenics/index.html>

LHC supports

Support posts measurements

49 ± 10% mW @ 1.9K 450 ± 10% mW @ 4.5-10K 7.1 ± 5% W @ 50-65K

0.2

The conduction equation (unidirectional case)

No heat deposition and steady-state

Thermal conductivity integrals (conductance) for some materials [W/m]

…more conductivity integrals

Electrical network analogy

• The inverse of the *thermal conductance* → *thermal resistance:*

For variable k, define an average value k_{AV} *:*

$$
k_{AV} = \frac{\int_{\text{To}}^{\text{TL}} k(T) dT}{(T_L - T_0)} \qquad R_t = \frac{L}{k_{AV}A}
$$

$$
\dot{q} = -\frac{A}{L}\int_{\text{To}}^{\text{TL}} k(T)dT = \frac{T_0 - T_L}{R_t}
$$

• Analogy with the electrical resistance (replace q with I, T with V):

$$
I=\frac{V_0-V_L}{R}
$$

• We can therefore model a complex thermal conductivity problem by elementary *thermal resistances Ri*, and solve the network by using *Kirckhoff's laws*.

$$
\sum_{i=1}^{n} \dot{q_i} = 0 \quad (at \, knots)
$$

$$
\sum_{i=1}^{m} (\text{T}_i - \text{T}_{i-1}) = 0 \quad (in \, loops)
$$

Thermal conduction with uniform heat deposition $\int + \frac{4}{t} = 0$ $\bigg)$ $\overline{}$ \setminus $\left(k \cdot \frac{dT}{dx}\right) + \frac{q}{t}$ *q dx* $k\cdot\frac{dT}{dT}$ *dx d q q^x* $To \nightharpoonup x$ t

- Beam of length L, thickness t, width $w (= 1m)$;
- beam *thermalized* on one side at To
- uniform heat deposition from one side, $q (W/m^2)$
- considering k constant with T
- Boundary conditions: a) for $x=0$ T=To (heat sink); b) $q=0$ for $x=L$ (isolated tip)
- Integrating and imposing the 2 boundary conditions:

$$
T(x) = To - \frac{q}{2kt}x^{2} + \frac{qL}{kt}x
$$

\n
$$
\Delta T_{\text{max}} = T_{L} - To = \frac{qL^{2}}{2kt}
$$

\n
$$
t = \frac{q \cdot L^{2}}{2 \cdot k \cdot \Delta T_{\text{max}}}
$$

\n
$$
q_{x}(T) = -kwt \frac{dT}{dx} = qwx - qwL
$$

 $\mathbf{\tau}$

practical interest:

calculate minimum thickness to limit ΔTmax

Thermal diffusivity

• For small variations of k with x:

• Solid bar cooled at one tip

- Conduction equation (no heat generation)
- ∂ $\frac{\partial}{\partial x}\left(k\right)$ ∂T ∂x $= \rho c$ ∂T ∂t $\partial^2 T$ 1 ∂T

α

=

 ∂x^2

with
$$
\alpha = \frac{k}{\rho c}
$$

- T perturbation δ travels towards warm end:
- \bullet t_c, critical time for T perturb. to reach warm tip:

Heat capacity

- Specific heats: *P* $\binom{m}{P}$ $c_{\rm p} = \left| \frac{\partial Q}{\partial r} \right| = \left| \frac{1}{r} \frac{\partial T}{\partial r} \right|$ \int \backslash I \setminus $\bigg($ д $\begin{pmatrix} 1 & \partial \\ -\frac{\partial}{\partial x} & \partial \end{pmatrix}$ \int \setminus I \setminus $=\left(\frac{\delta Q}{m dT}\right)_P = \left(\frac{1}{m} \frac{\partial H}{\partial T}\right)$ H $m dL$ m $\lfloor m \rfloor$ Q p δ O) (1 *V U V* $c_v = \left| \frac{\partial Q}{\partial r} \right| = \left| \frac{1}{r} \frac{\partial C}{\partial r} \right|$ \int \backslash I \setminus $\bigg($ д $\begin{pmatrix} 1 & \partial \\ -\end{pmatrix}$ \int \backslash I \setminus $=\left(\frac{\delta Q}{m dT}\right)_V = \left(\frac{1}{m} \frac{\partial U}{\partial T}\right)_V$ ${\rm Q}$ v δ O) (1
- For (incompressible) substances: $Cp(T) = Cv(T) = C(T)$
- Change of internal energy U (or enthalpy):

 $\sum \Delta U = Q = m \int_{T_1}^{T_2} c(T) dT$

- Cooling (or heating) power: \triangleright P(T) = m c(T) $\frac{dT}{dt}$ dt
- Specific heats/unit vol. sometimes preferred
- Below 10 K enthalpy of helium overtakes all solids

Measuring Thermal Performance of Cryostats

Measure of Heat Loads to liquid helium tanks

SC level gauge Isothermal cooling (2-phase helium tanks) vapor liquid volume replaced • He boil-off along saturation line *m* by fraction of boil-off 20 \checkmark Latent Heat (L_v) of vaporisation $h_{\rm fg}$ (kJ/kg) vapor (no filling) \checkmark Isothermal cooling (T constant if P constant) • \checkmark Measure p, and m \checkmark Liquid/gas volumetric corrective factor $\sqrt{5}$ $\overline{v_g}$ • $\mathbf{2}$ $T(K)$ • Latent heat of vaporization *q* $=$ m \cdot $Lv \cdot ($ $\frac{y}{v_g - v l}$ • Example: 150 \checkmark Mass flow measurement: 7 g/s \checkmark P measured: 1.78 bar LIQUID \checkmark (T on saturation line (phase diagram): 4.8 K) 100 \checkmark L_v = 14'116 (J/kg) (tables, or state equations) $kg/m₃$ measure from diagrams \mathcal{V} v_g = 3.0 10-2 (m3/kg); v_l = 9.3 10-3 (m3/kg); (phase diagrams) 50 $\rightarrow \dot{q} = 7.0 \, 10 - 3 \cdot 14116 \cdot (\frac{3.0 \, 10 - 2}{3.0 \, 10 \cdot 3.0 \, 3.$ $\frac{3.0 \, 10^{-2}}{3.0 \, 10^{-2} - 9.3 \, 10^{-3}} = 143 \, W$ • He boil-off liquid level measurement: **VAPOR 1.45 !** • Measure level l with SC level gauge • Boil-off mass flow measure through reservoir geometrical correlation $T(K)$ between level and volume: $f(1)$, and knowledge of density ρ and L_{v} Density of saturated liquid helium

$$
\dot{q} = f(\Delta l) \cdot \rho \cdot Lv
$$

 \overline{q} •

66

Measure of Heat Loads to liquid helium tanks (cont.d)

Non-isothermal cooling

- Calorimetry in superfluid helium (LHell):
	- LHe II very high thermal conductivity \rightarrow isothermal bath
	- Measure internal energy change (closed system) in time Δt
	- Needs precise measure of helium content
	- and sub-mK resolution measurement of T at T< 2.17 K

$$
\hat{q} = \frac{\Delta U(t)}{\Delta t} = \frac{m \cdot \Delta u(t)}{\Delta t}
$$

Measure of Heat Loads to Thermal Shields

Non-isothermal cooling

- Forced internal (conduit) convection of single-phase fluid:
	- Non-isothermal cooling: enthalpy change of fluid (here c_p assumed constant)
	- Needs the measure of mass flow, and T at entry and exit of conduit

$$
\hat{q} = \Delta H = \hat{m} \cdot cp \cdot (T_{\text{out}} - T_{\text{in}})
$$

Forced Convection heat transfer in conduits

•

- Considering *hydro-dynamically* and *thermally* **fully developed flow**
- **Uniform** wall heat flux (linear T profiles)
- **Convection heat transfer** from wall to fluid:
- **Enthalpy balance** along the line L:
- **Reynolds No.:**
- **Nusselt No.:**
- ✓ For **laminar flow**: constant
- \checkmark For **turbulent flow**, Nu_D=f(ReD, Pr): (Dittus and Boelter formula)

$$
\begin{vmatrix} \bullet & \cdot \\ \mathbf{q} = h \cdot D \pi L \cdot (T_w - T_m) \end{vmatrix}
$$

$$
q = m \cdot c_p \cdot (T_{out} - T_{in})
$$

$$
\text{Re } D = \frac{UD}{V}
$$

$$
N u D = \frac{h \cdot D}{k}
$$

$$
Nu_D = \frac{h \cdot D}{k} = 4.364 \qquad \frac{dT}{dx}
$$

m

=. — · 4

 $2500 \leq$ Rep $\leq 1.2410 + 5$

 $0.7 \le Pr \le 120$

for heated fluid;

$$
Nu_D = 0.023 \cdot \text{Re}_D^{4/5} \text{Pr}^{2/5}
$$

T mean temperature T wall temperature m w ⁼ =Re *^D* ⁼ = *k*inematic viscosit y (/) = therm. conductivity *^c U dx D q p* • Pr ⁼ReD>2000 → turbulent flow, ReD<2000 → laminar flow *T fluid entrance temperature T fluid exit temperature ^m mass flow[kg/s] in out* ⁼ ==•

 α = *thermal diffusivity*

 α

Frictional pressure drop in a tube

• **Pressure drop** along tube

• Experimental plots or semi empirical formulations (ex. Colebrook formulation)

U Mean velocity = *f Fanning friction factor* =

Feedthroughs and heat intercepts

Feedthroughs in cryostats

Solid conduction paths:

- Supporting systems
- Current leads
- RF main coupler
- Instrumentation feed-throughs
- Beam tubes Cold-to-Warm (CWT) transitions
- Necks (vertical cryostats)

CWT SPL cryomodule

LHC instrumentation capillary at assembly

Heat intercepts (heat sinking) at intermediate temperatures

 \mathbb{L}

 $\overline{}$

$$
\dot{\mathbf{Q}} = \frac{A}{L} \int_{\text{Tc}}^{\text{Tw}} k(T) dT
$$

• 1 heat intercept at optimal distance

$$
\min\{f(L_{1})=C1\cdot\frac{A}{L_{1}}\int_{\text{Tw}}^{\text{30K}}k(T)dT+C2\cdot\frac{A}{L-L_{1}}\int_{\text{30K}}^{\text{Te}}k(T)dT\}
$$

Q @ 8K • 2 heat intercepts at optimal distance $\min\{f(L_1,L_2) = C_1 \times \}$ *A L*¹ *k*(*T*)*dT* Tw 80K $\int k(T) dT + C2 \times \frac{1}{2}$ *A L*² - *L*¹ *k*(*T*)*dT* 80K 8K $\int k(T) dT + C3$ *-*A L* - *L*² *k*(*T*)*dT* 8K Tr $\hat{g} k(T)dT$ \rightarrow L₁, L₂ $\frac{1}{73}$

 $\overrightarrow{A} \longrightarrow Q$ @ 80K

LHC supports

- **4-mm thickness**, glass-fiber epoxy
- Manufactured by **Resin Transfer Moulding (RTM):**
	- Suited to a large-scale industrial production (4'700 units)
	- High reproducibility in thermo-mechanical properties

Heat loads comparison for GFRE with & without heat intercepts

Vapour cooling in solid conduction

• Vapor cooled wall

•

Assuming perfect exchange $(T_{vapor} = T_{wall})$

$$
k(T) \cdot A \cdot \frac{dT}{dx} = Q + m \cdot Cp \cdot (T - Tl)
$$

• If Q , which is the residual heat to the bath, is equivalent to the evaporation (i.e. self-sustained):

$$
\rightarrow Q = m \cdot Lv
$$
 Lv, latent heat of evap.

Large enthalpy in He vapours (1550 kJ/kg from 4.2K to 300K) \rightarrow usable cooling capacity

	Thermal conductivity integral $[W \text{ cm}^{-1}]$	Effective thermal conductivity integral $[W \text{ cm}^{-1}]$
ETP copper	1620	128
OFHC copper	1520	110
Aluminium 1100	728	39.9
AISI 300 st.steel	30.6	0.92

Reduced heat conduction in self-sustained helium cooling for selected technical materials

(ref. G. Vandoni, Heat Transfer, CAS, Erice 2003) 75

SPL cryomodule: actively cooled RF main couplers

Vapor cooled RF coupler (double-walled tube). Effective cooling with gas regulation:

- Conduction heat loads (RF off)
- Conduction + RF EM resistive heating (RF on)

Double-walled tube:

- $~\sim$ Φ 100 mm
- Inner wall: st.steel, 1.5-mm thick
- External wall: st.steel, 2-mm thick

Notions of Cryogenic Safety

Cryostats and safety

- Cryostats include inventory of cryogenic fluids, *potentially* unstable stored energy, and sometimes large electromagnetic stored energy in superconducting devices
- Managing safety in cryostat covers multiple aspects: safety of personnel and equipment
	- Risk assessment: cryostat as part of a cryogenic system in an environment
	- Safety hazard from relief of cryogens to the environment: ODH, burns, escape paths, safety training, use of personnel protection equipment, risk to adjacent equipment, etc.

→ *Understanding pressure hazards and making the correct choice of the pressure relief devices to protect from overpressure of the cryostat envelopes*

Liquid helium (and nitrogen) stored energies

One LHC dipole:

- Magnetic stored energy: ~7 MJ
- Helium content: 375 liters
- Total stored energy (in liquid): 74 MJ (x10 times stored magnetic energy!)
- Total magnet cold surface: \sim 4 m²
- Latent heat per unit volume: He x60 lower than $N_2 \to (roughly)$ venting a cryostat with \sim 6 liter air $(\sim N_2)$ boils off He in 1 dipole
- Air condensation power on cold surface with MLI: $6 \frac{\text{kW}}{m^2}$ (40 kW/m² on bare surface!)
- Vacuum insulation breach: peak power deposition: 24 kW \rightarrow ~40 s to boil-off liquid, ~50 min. to deplete liquid stored energy,

→ **Large volumetric inventories** and energies **released in reduced time** ! → **pressure relief devices !**

Pressure hazards in cryostats

• Potential pressure hazards:

• …

- Compressors connected to cryo lines
- Heating of "trapped" volumes (typically in a circuit between valves) during warm-ups
- Helium leak to insulation vacuum, with consequent increased conduction/convection heat loads to cryogenic liquid vessels
- Cryo-condensed air leaks on cold surfaces and consequent pressure increase and increased conduct/convection heat loads during warm-ups
- A) Heating/vaporization of cryogens from sudden release of stored energy in SC device (e.g. quench or arcing in a SC magnet circuit)
- B) Accidental release of cryogenic fluid to higher T surfaces (thermal shield and vacuum vessel), and consequent pressure increase and increased of conduction/convection heat loads to cold surfaces
- C) Accidental air venting of insulation vacuum with sudden condensation on cold surfaces, helium boil-off and pressure build-up

 $(Snowball effect A) + B) + C) \rightarrow LHC$ event of Sept.2008)

How things can go wrong...LHC 19th sept. 2008

General approach for sizing of safety devices

Risk analysis & mitigation:

- Make a thorough risk analysis and evaluate risk hazards
- Identify mitigation measures (e.g. protections of exposed bellows and flanged connections)
- Identify severity of consequences and appreciate probability of the event
- Define the maximum credible incident(s) (MCIs) and design the safety relief system accordingly
- The safety relief system must be designed to keep pressure rise within the limits of the Maximum Allowable Working Pressure (MAWP)

Design steps for the MCI:

- Estimate the heat flux to helium and its conversion to mass flow rates to be discharged
- Choose the type of safety device (burst disks, valves, plates) and size the safety device (orifice area and set pressure). Make use of standards and safety device manufacturers datasheet
- Check the sizing of piping (generally designed for normal operation) to the relief device and increase if necessary (pressure drop limited to a few % of total discharge Δp)

$$
\dot{Q} \to \dot{M}
$$

Heat flux (W) \rightarrow Relieving mass flow rate (kg/s)

 $\rho_{th} v_{th}$ density and velocity giving the *m* in the throat

→ Methodology explained in a **new standard EN 17527 just issued** devoted to *Helium cryostats - Protection against excessive pressure*

EN 17527 Helium cryostats - Protection against excessive pressure

Publication of EN 17527

Scope includes:

- \checkmark SC magnet cryostats
- \checkmark SRF cavity cryomodules
- ✓Ultra-low T refrigerator systems
- ✓Coldboxes of helium refrigerators and liquefiers
- \checkmark Helium distribution systems including valve boxes

Overall concept:

- \checkmark Standardization of the approach
- \checkmark Specification of procedures and minimum requirements
- ✓ Risk assessment, definition of scenarios
- ✓ Protection concepts (single-stage, multistage)
- ✓ Dimensioning rules of pressure relief devices (HEM Model)

A few suppliers Herose, Rembe, Ramseyer, Leser…

- Safety devices
	- 1. Safety valves
	- 2. Burst discs
	- 3. Pressure relief plate

EN Standards for Safety Relief Devices

EN 764-7:2002 Pressure equipment. Part 7: Safety systems for unfired pressure equipment

EN ISO 4126-1:2013 / Safety devices for protection against excessive pressure - Part 1: Safety valves (ISO 4126-1:2013) 12/08/2016

EN ISO 4126-2:2013 / Safety devices for protection against excessive pressure - Part 2: Bursting disc safety devices

EN ISO 4126-3:2006 / Safety devices for protection against excessive pressure - Part 3: Safety valves and bursting disc safety devices in combination (ISO 4126-3:2006) 12/08/2016

EN ISO 4126-4:2013 / Safety devices for protection against excessive pressure - Part 4: Pilot-operated safety valves (ISO 4126-4:2013) 12/08/2016

EN ISO 4126-5:2013 / Safety devices for protection against excessive pressure - Part 5: Controlled safety pressure relief systems (CSPRS) (ISO 4126-5:2013) 12/08/2016

EN ISO 4126-7:2013 / Safety devices for protection against excessive pressure - Part 7: Common data (ISO 4126-7:2013) 12/08/2016

EN 13648-1:2008 / Cryogenic vessels - Safety devices for protection against excessive pressure - Part 1: Safety valves for cryogenic service 12/08/2016

EN 13648-2:2002 / Cryogenic vessels - Safety devices for protection against excessive pressure - Part 2: Bursting disc safety devices for cryogenic service 12/08/2016

ISO 21013-3:2016 Cryogenic vessels -- Pressure-relief accessories for cryogenic service -- Part 3: Sizing and capacity determination

EN ISO 4126-6:2013 / Safety devices for protection against excessive pressure - Part 6: Application, selection and installation of bursting disc safety devices

EN ISO 4126-10:2013 / Safety devices for protection against excessive pressure - Part 10: Sizing of safety valves for gas/liquid two-phase flow

EN 13648-3:2002 Cryogenic vessels. Safety devices for protection against excessive pressure. Determination of required discharge. Capacity and sizing

ISO 21013-1:2008 Cryogenic vessels -- Pressure-relief accessories for cryogenic service -- Part 1: Reclosable pressure-relief valves

(ISO/AWI 21013-1 Cryogenic vessels -- Pressure-relief accessories for cryogenic service -- Part 1: Reclosable pressure-relief valves [Under development])

ISO 21013-2:2007 Cryogenic vessels -- Pressure-relief accessories for cryogenic service -- Part 2: Non-reclosable pressure-relief devices + ISO 21013-2:2007/Amd 1:2018

ISO 21013-4:2012 Cryogenic vessels -- Pilot operated pressure relief devices -- Part 4: Pressure-relief accessories for cryogenic service + ISO 21013-4:2012/Amd 1:2019

Thank you for your attention

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Annex: numerical calculations exercises

Exercise: calculate a thermal shield thickness in an LHC-type cryostat

- Symmetry: point opposite of cooling line is an isolated tip
- Take $\frac{1}{2}$ shield: $L = \frac{1}{2}$ $A_{\overline{s}}$ $1 m$ $=$ ½ 2.35 m = 1.17 m
- Uniform heat deposition: $q = \frac{q_{\text{shield}}}{4}$ A_{s} $=\frac{2.55 W}{3.35 m^2}$ $2.35 m²$ $= 1.08 W/m^2$
- Let's set the maximum $\Delta T_{\text{max}} = 5 \text{ K}$
- Take k aluminium (Al6061) at \sim 80 K: 85 W/(K m)

 \rightarrow t = 1.7 mm

Exercise: calculate helium heat transfer in a thermal shield in an LHC-type cryostat TΛ Wall,

- Non-isothermal cooling along an L=3 km long thermal shielding line
- Cooling line: D=80 mm, roughness aluminium drawn tube (ε = 0.05 mm)
- T_{in} = 60 K, T_{out} < 75 K
- $p_{in} = 5$ bar
- Calculate mass flow, heat exchange parameters, and pressure drop
- Assumptions: $T_m(x) = \frac{1}{2}(T_{out} + T_{in}) = \text{const.}$; $\Delta T_{in} = \Delta T_{out}$ (wall with uniform heat flux \dot{q})
- Take $T_{\text{out}} = 75 \text{ K}$
- $T_m = \frac{1}{2} (75 K + 60 K) = 67.5 K$
- $\dot{q} = q_{\text{shield}} \cdot L = 2.55 \text{ W/m} \cdot 3000 \text{ m} = 7.650 \text{ W}$ (see previous calculation of thermal shield heat load)
- From enthalpy balance (with T_{in} = 60 K, T_{out} = 75 K, and C_p(67.5 K) = 5300 J/kg/K) \rightarrow $\dot{m} = \frac{\dot{q}}{C(T_0)u}$ $\frac{q}{c_p \left(Tout-Tin\right)}$ = 0.096 kg/s
- Calculate flow properties and thermal convection heat exchange (use *Cryostat Toolbox*):
	- $Re = 1.9 10+5$, turbulent OK !
	- $V = 5.4$ m/s
	- $Pr = 7.03$
	- $Nu = 345$
	- $h = 247$ (W/m²/K)
	- $\Delta T_{in} = \Delta T_{out} = 0.04 \text{ K } (T_w \approx T_m)$
- Calculate pressure drop (use *Cryostat Toolbox*):
	- $Δp = 380$ mbar $(-8%)$

Radiation calculation exercises for an LHC-like cryostat

Exercise: Radiation in LHC-like cryostat

 \overline{q} 1° =

1

 $\overline{\varepsilon_1}$

 $+$

 $\sigma A_1 (T_1^4 - T_2^4)$

1

 $\overline{\varepsilon_2}$

− 1

 A_1 $\overline{A^{}_2}$

- Thermal radiation HL for a 1-m cryostat unit length
- Vacuum vessel diameter: $1m (A₂= \pi \times 1=3.14 m²)$
- Cold mass diameter: 0.5 m (A₁ = π x 0.5 = 1.57 m²)
- T_1 cold mass: 2 K
- T_2 vac.vessel: 293 K
- $\epsilon_1 = 0.12$ (st. steel, mec. polished, 2 K)
- $\epsilon_2 = 0.2$ (low carbon.steel, mec.polished, 293 K)

 \rightarrow q₁₋₂ = 63.5 W (41.6 W/m²)

- Sensitivity wrt & uncertainties:
	- ≥ 0.18 (+50%), $\&2 = 0.20$ \rightarrow $q_{1.2} = 87$ W (+37%)
	- $\geq C_1 = 0.12, \, C_2 = 0.30 \, (+50\%)$ \Rightarrow $q_{1.2} = 69 \, W \, (+9\%)$
	- \triangleright $\varepsilon_1 = 0.18$ (+50%), $\varepsilon_2 = 0.30$ (+50%) \rightarrow $q_{1-2} = 98$ W (+54%)
	- \triangleright Note: assuming black bodies $(\mathcal{E}_1 = \mathcal{E}_2 = 1)$ \rightarrow $q_{1-2} = 656$ W ! (x10!)

\rightarrow Influence of \mathcal{E}_1 is 4 times more important than \mathcal{E}_2

$$
A1, \varepsilon_1
$$

 0.1 0.2 0.3

0

Exercise: Radiation in LHC-like cryostat (cont.d)

• Sensitivity with vac.vessel diam. (D_e) : ~12 W/m

• Sensitivity with inner vessel diam. $(D_i): ~ 100 \text{ W/m}$

Exercise: Radiation in LHC-like cryostat (cont.d)

• Floating Al shield

Floating Al shield:

- Thermal shield diameter: 0.75 m (A_s = π x 0.75 = 2.35 m²)
- $F_{1s} = 1$; $F_{2s} = 1$
- $T_s = 80$ K (first guess)
- $\mathcal{E}_{s,1} = \mathcal{E}_{s,2} = 0.1$ (Aluminum, mec.polished, 80 K)
- \rightarrow q₁₋₂ = q_{1-s} = q_{s-2} = 28.5 W
- Calculate Ts by *trial and error* to obtain power balance $q_{1-s} = q_{s-2}$
- \rightarrow T_s = 260 K \rightarrow increase $\mathcal{E}_{s,1} = \mathcal{E}_{s,2}$ (0.15?) and recalculate
- \rightarrow q_{1-2} = q_{1-5} = q_{5-2} = 35.4 W (to be compared to 63.5 W without shield)
- \rightarrow q_{1-s} = 35.4 W (22.5 W/m²), q_{s-2} = 35.4 W (15 W/m²)

\rightarrow 1 floating thermal shield reduces to almost $\frac{1}{2}$ the radiation to the low T (close to flat plates approximation for this geometry)

Exercise: Radiation in LHC-like cryostat (cont.d)

 $\sigma A a v (Ts^4 - Te^4)$

2

 $\frac{2}{\varepsilon_{av}}$ – 1)

 $(N + 1)$ (

- MLI with N reflectors, floating shields
- Radiation between shield and vac.vessel (flat plat approximation):

$$
\bullet \quad N=30
$$

- $T_s = 80$ K (first guess)
- $\epsilon_e = 0.2$ (low carbon.steel, mec.polished, 293 K)
- $\epsilon_s = 0.08$ (Aluminium reflector, electrolytical deposition, 80 K)
- $\varepsilon_{av} = \frac{1}{2} (\varepsilon_s + \varepsilon_e)$ (average emissivity)
- $A_{av} = \frac{1}{2} (A_s + A_e)$ (average area)
- \rightarrow q_{s-e} = 2.7 W (0.14 W/m²) (with T_s = 80 K)
- Radiation between shield (80 K) and helium vessel (formula between enclosed cylinders):

 $q_{s-e} =$

- \rightarrow q_{i-s} = 0.23 W (0.012 W/m²) (with T_s = 80 K)
- Calculate T_s by *trial and error* (and tune \mathcal{E}_s) to obtain power balance $q_{s-e} = q_{i-s}$ (floating shield condition)
- \rightarrow T_s = 143 K, \rightarrow E_s= 0.1

 $q_{s-e} = q_{i-s}$ \rightarrow q_{s-e} = 2.6 W (1.65 W/m²) \rightarrow q_{i-s} = 2.6 W (0.96 W/m²)

\rightarrow MLI (30 layers) reduce the HL to the thermal shield (and cold surface) by a factor x25 wrt no shield

(*) can be further reduced to 0.18 W (0.11 W/m²) with ε i = 0.08 (for example 1 or more MLI layers on cold mass) 97

Exercise: Radiation in LHC-like cryostat (cont.d)

 $\sigma A a v (Ts^4 - Te^4)$

2

 $\frac{2}{\varepsilon_{av}}$ – 1)

 $(N + 1)$ (

- MLI with N reflectors, actively cooled shield
- Radiation between shield and vac.vessel (flat plat approximation):

 $q_{s-e} =$

- \cdot N = 30
- $T_s = 80$ K (now an input)
- ϵ_s = 0.08 (Aluminium reflector, electrolytical deposition, 80 K)
- $\varepsilon_{av} = \frac{1}{2} (\varepsilon_{s} + \varepsilon_{e})$ (average emissivity)
- $A_{av} = \frac{1}{2} (A_s + A_e)$ (average area)

 \rightarrow q_{s-e} = 2.78 W (1.0 W/m²)

• Radiation between shield (80 K) and helium vessel (2 K) (formula between enclosed cylinders):

 \rightarrow q_{i-s}^{*} = 0.23 W (0.14 W/m²) (x10 times less than with floating shield !)

- Radiation heat extraction from thermal shield (not to be forgotten!):
- \rightarrow $q_{\text{shield}} = q_{\text{s-e}} q_{\text{i-s}} = 2.55$ W

→ Actively cooled shield with MLI dramatically reduces radiation to the low T: this is a standard practice in cryostats!

Exercise: Residual gas conduction in LHC-like cryostat

- Typical dimension (space between surfaces): $d = 0.25$ m
- **Good insulation vacuum:**
	- $\sqrt{p} = 10^{-6}$ mbar (10⁻⁴ Pa) <u>("standard" good vacuum</u> in cryostats)
- Calculate $\lambda_{\text{molecule}}$ (between shield and inner vessel): \checkmark $\lambda_{\text{molecule}} = 20 \text{ m } (-x100 \text{ d}) \rightarrow \text{molecular regime}$
- Calculate residual gas conduction with Kennard's law: $\sqrt{Q_{res}} = 0.034 \text{ W} (0.02 \text{ W/m}^2)$
- Negligeable additional contribution wrt previously computed radiation: v $\mathsf{q}_{i-s} = 0.23 \, \text{W}$ (0.14 W/m²)
- **Degraded insulation vacuum:**

 $\sqrt{p} = 10^{-5}$ mbar (10⁻³ Pa) (degraded vacuum from helium leak in cryostats)

• Calculate $\lambda_{\text{molecule}}$ (between shield and inner vessel):

 \checkmark $\lambda_{\text{molecule}} = 2 \text{ m } (-x10 \text{ d}) \rightarrow \text{still molecular regime}$

• Calculate residual gas conduction with Kennard's law:

 $\sqrt{Q_{res}} = 0.34 \text{ W} (0.22 \text{ W/m}^2)$

 \rightarrow gas conduction contribution ($Q_{res} = 0.22$ W/m²) now higher than radiation $(q_{i-s} = 0.14 \text{ W/m}^2)$. Total HL to cold surface: 0.34 W/m²

Summary of radiation HL exercises

Spare slides

Material mechanical properties at cryogenic temperatures

1. PROPRIÉTÉS MÉCANIQUES DES MATÉRIAUX

100

 $\sqrt{2}$

200

300

 $T(K)$

 10

200

300

Fig. G. - Module d'élasticité, limite élastique, limite de rupture, allongement à la rupture, énergie de rupture mesurée au mouton de Charpy, limite de fatigue après 10⁶ cycles pour quelques matériaux [Baron].

 100

Source: Techniques de l'ingenieur

Material mechanical properties at cryogenic temperatures

PROPRIÉTÉS MÉCANIQUES

Les lettres qui suivent les désignations indiquent les traitements thermiques ou les traitements mécaniques (écrouissage)

Fig. H. - Limite d'élasticité et allonge ent à la rupture d'alliages d'alu snéciaux et de divers nuances d'aciers inoxydables

Source: Techniques de l'ingenieur

Thermal conductivity in solids (& metals)

• The conductivity is attributed to the movement of **conduction electrons** ("electron gas"), *k*e, and the effects of **phonon lattice vibrations**, *k*l :

$$
k = k + k
$$

 $k \approx k \gg k$

i

 $k \cong$

k

=

 a_i

L

 $\rho_{\scriptscriptstyle{\theta}}$

e

o

T

T

k

p

= $\frac{1}{2}$ $\frac{1}{2}$

In metals, the electron contribution dominates :

• Therefore for **metals**, the resistivity can be expressed as:

• The movement of conduction electrons is impeded by scatter: interactions with phonons, and interactions with **impurities/imperfections**. We can introduce *thermal resistivities:*

 k_e k_p k_i 1

1 1 1 $=$ $+$

- And has a **maximum**, which shifts at higher T with increasing impurity (see coppers) and vanishes for highly impure alloys (see steels), as impurity scatter dominates, and for which at $T < RT$:
- *T* $a_{\scriptscriptstyle\cal P} T^{\scriptscriptstyle 2}$ + $\overset{a}{-}$ *p* + $=$ $\frac{1}{T^2}$ $\frac{1}{3}$ $\frac{1}{3}$ $\frac{2}{3}$ $\frac{2}{3}$ $\frac{2}{3}$ $\frac{2}{3}$ $\frac{2}{3}$ at 2 $\mu_{\text{max}} = \frac{3}{2} a_p^{1/3} a_i^{2/3}$ at $T = \left(\frac{a_i}{a_i}\right)^2$ $\bigg)$ \backslash I \setminus $=\frac{3}{\sqrt{2}} a_{\nu}^{3/3} a_{i}^{2/3}$ at $T=\left(\frac{3}{\sqrt{2}}\right)$ *p i p i a* $k_{\text{max}} = \frac{3}{\sqrt{2}} a_{\text{max}}^{3/3} a_{\text{i}}^{2/3}$ at $T = \frac{a}{\sqrt{2}}$

k

• For **metals**, analogy between electron thermal and electrical diffusion → *Wiedemann-Franz law* :

- Good agreement at T<< RT >> T
- Better agreement from T<< to T>> with increasing impurities

$$
\overline{a}
$$

 a_pT

p

T

k

1

i

=

a

i

Lorentz constant

$$
L_o = 2.45 \cdot 10^{-8} \left(\frac{V}{K}\right)^2
$$
 (Constant for metals)

and *^ap*,*aⁱ* constants

Vacuum in cryostats

- 2-4.5 K surfaces have high pumping speed & capacity.
- Gas species have very low vapour pressure except helium.
- Without helium leaks, equilibrium pressures $\leq 10^{-6}$ mbar are obtained

He gas conduction

- **Viscous regime** $(\lambda_{\text{molecule}} << d)$:
	- At "high" gas pressure: classical conduction (Fourier law-like)
	- independent of pressure
	- (*natural convection* should be added !)

Molecular regime $(\lambda_{\text{molecule}} >> d)$:

- At "low" gas pressure
- Kennard's law
- Conduction is proportional to p
- A1 is the surface receiving the flow
- α(T) → *accommodation coefficient* depending on gas species, T1, T2 and surface geometry *(applicable for flat parallel surfaces, coaxial cylinders and spheres)*

$$
\frac{(T_2 - T_1)}{d}
$$
\n
$$
\frac{(T_2 - T_1)}{d}
$$
\n
$$
\rho = \text{gas density in } [kg/m^3]
$$
\n
$$
\rho = \text{gas density in } [kg/m^3]
$$

 $R =$ *ideal gas constant* $\lambda =$ mean free path [m] $C_v = specific heat at constant pressure$ [J.kg⁻¹K⁻¹.]

$$
Q_{res} = A_1 \cdot \alpha \cdot \left(\frac{\gamma + 1}{\gamma - 1}\right) \cdot \left(\frac{R}{8 \pi}\right)^{1/2} \cdot \frac{p}{\sqrt{MT}} \cdot (T_2 - T_1)
$$

with
$$
\gamma = C_p/C_v
$$

 $Q_c = A_1 \cdot k \cdot$

 $rac{1}{3} \rho \sqrt{\frac{8RT}{\pi M}}$

 $\frac{\partial H}{\partial \pi M}$ λ C_v

with $k = \frac{1}{2}$

 $\alpha =$

Accommodation coefficient *αⁱ*

$$
\frac{\alpha_1\alpha_2}{\alpha_2+\alpha_1(1-\alpha_2)\frac{A_1}{A_2}}
$$

Thermal conductivity in solids (& metals)

• The conductivity is attributed to the movement of **conduction electrons** ("electron gas"), *k*e, and the effects of **phonon lattice vibrations**, *k*l :

$$
k=k_{e}+k_{l}
$$

 $k \approx k \gg k$

In metals, the electron contribution dominates :

• Therefore for **metals**, the resistivity can be expressed as:

• The movement of conduction electrons is impeded by scatter: interactions with phonons, and interactions with **impurities/imperfections**. We can introduce *thermal resistivities:*

 k_e k_p k_i 1

1 1 1 $=$ $+$

- And has a **maximum**, which shifts at higher T with increasing impurity (see coppers) and vanishes for highly impure alloys (see steels), as impurity scatter dominates, and for which at $T < RT$:
- *T* $a_{\scriptscriptstyle B} T^{\scriptscriptstyle 2}$ + $\overset{a_{\scriptscriptstyle i}}{-}$ *p* + 2 $\frac{1}{3}$ $\frac{1}{3}$ $\frac{2}{3}$ $\frac{2}{3}$ $\frac{2}{3}$ $\frac{2}{3}$ $\frac{2}{3}$ at 2 $\mu_{\text{max}} = \frac{3}{2} a_p^{1/3} a_i^{2/3}$ at $T = \left(\frac{a_i}{a_i}\right)^2$ $\bigg)$ \backslash I \setminus $=\frac{3}{\sqrt{2}} a_{\nu}^{3/3} a_{i}^{2/3}$ at $T=\left(\frac{3}{\sqrt{2}}\right)$ *p i p i a* $k_{\text{max}} = \frac{3}{\sqrt{2}} a_{\text{max}}^{3/3} a_{\text{i}}^{2/3}$ at $T = \frac{a}{\sqrt{2}}$

 $k =$

• For **metals**, analogy between electron thermal and electrical diffusion → *Wiedemann-Franz law* :

- Good agreement at T<< RT >> T
- Better agreement from T<< to T>> with increasing impurities

$$
k=\frac{L_o}{\rho_e}T
$$

 a_i

T

k

p

= $\frac{1}{2}$ $\frac{1}{2}$

 a_pT

p

T

k

1

i

=

a

i

 $k \cong$

Lorentz constant

$$
L_o = 2.45 \cdot 10^{-8} \left(\frac{V}{K}\right)^2
$$
 (Constant for metals)

and *^ap*,*aⁱ* constants

2 main mechanisms of interest for cryostats

- Vaporisation in pool boiling (2-phase)
	- Latent Heat (Lv) of vaporisation
	- Isothermal cooling (T constant if P constant)

 \overline{q} •

Vaporisation under 1 W heat load

- Forced internal (tube) convection of single-phase fluid:
	- Non-isothermal cooling: enthalpy change of fluid $(c_p$ assumed constant)
	- Depends on t*hermo-hydraulics* of the flow (see next slide)
	- Used in cooling of thermal shields (supercritical He)

$$
\mathcal{T}_{in} \xrightarrow{\begin{array}{c}\n\mathbf{i} & \mathbf{j} & \mathbf{k} & \mathbf{k
$$

For more cooling mechanisms see dedicated lectures

Helium as a coolant for SC devices **Property** Boiling T (at 1 atm)

 \bigcirc \bigcirc

(ref. S. Van Sciver, Helium Cryogenics)

FRN
Heat capacity

- Specific heats: *P* $\binom{m}{P}$ $c_{\rm p} = \left| \frac{\partial Q}{\partial r} \right| = \left| \frac{1}{r} \frac{\partial T}{\partial r} \right|$ \int \setminus I \setminus $\bigg($ д $\begin{pmatrix} 1 & \partial \\ -\frac{\partial}{\partial x} & \partial \end{pmatrix}$ \int \setminus I \setminus $=\left(\frac{\delta Q}{m dT}\right)_P = \left(\frac{1}{m} \frac{\partial H}{\partial T}\right)$ H $m dL$ m $\lfloor m \rfloor$ Q p δ O) (1 *V U V* $c_v = \left| \frac{\partial Q}{\partial r} \right| = \left| \frac{1}{r} \frac{\partial C}{\partial r} \right|$ \int \backslash I \setminus $\bigg($ д $\begin{pmatrix} 1 & \partial \\ -\end{pmatrix}$ \int \backslash I \setminus $=\left(\frac{\delta Q}{m dT}\right)_V = \left(\frac{1}{m} \frac{\partial U}{\partial T}\right)_V$ ${\rm Q}$ v δ O) (1
- For (incompressible) substances: $Cp(T) = Cv(T) = C(T)$
- Change of internal energy U (or enthalpy):

 $\sum \Delta U = Q = m \int_{T_1}^{T_2} c(T) dT$

- Cooling (or heating) power: \triangleright P(T) = m c(T) $\frac{dT}{dt}$ dt
- Specific heats/unit vol. sometimes preferred
- Below 10 K enthalpy of helium overtakes all solids

Design stresses for some materials

- Design stresses for plates less than 12 mm thick applicable to membrane stress (safety factor 1.5 included) according to EN 13445-3
- For stainless steels:

Best practices

- Using a coherent set of standards throughout the lifecycle of the cryostat is the simplest and safest approach. As an example when using only EN harmonised standards:
	- Error margins of pressure relief devices are taken into account in the design rules
	- The design rules are only applicable if the material has enough ductility
	- Materials certified for pressure vessels have measured minimum fracture toughness
	- Safety factors included in buckling formulae take into account shape imperfections up to the allowable tolerances layed out in the manufacturing section of the standards
	- The extent of welding inspection must be compatible with the joint coefficient used in thickness calculations
	- Coherence of test pressure and testing procedure with the design rules

Liquid helium pumping

- Pressure reduction by pumping above helium liquid at 4.2 K, with latent heat L(T) and specific heat $c(T)$:
	- $L(T) dm = m c(T) dT$

 dT

- Neglecting external heat loads and vessel heat capacity
- Integrating over T and m, with m_0 initial helium mass:

 $log\frac{m}{m}$

(ref. R.R.Conte, Elements de Crogenie)

LHC dipole cryostat assembly

Towing through, sliding on vacuum vessel

Assembly bench

Expansion joints (bellows) for cryogenic lines

- Compensation of longitudinal thermal contractions
- Compensation of transversal and angular offsets (not twist!)

→Extensive use in cryo-magnet interconnections

- Beware of bellows stability issues in pressurised lines:
	- Stiff guiding
	- Limit transversal and angular off-sets

