Investigation and optimization of the continuous and discrete heat exchangers in the mK dilution refrigerator for cooling superconducting quantum chips Yujia Zhai^{1,3*}, Haizheng Dang^{1,2,3,4}

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Introduction

Superconducting quantum computing demand:

- \succ Ultra-low temperature: 10~100 mK \succ Low vibration \succ Low electromagnetic interference
- Dilution refrigerator (DR) has become an indispensable technology to provide cryogenic environment for the quantum chips.
- Two types of heat exchangers (HEXs) plays crucial role in the DR, including the continous heat exchanger (CHEX) and the discrete heat exchanger (DHEX).
- ✤ The flow and heat transfer characteristics is related to working conditions and dimensional parameters of heat exchangers
- > Numerical model of two types of heat exchangers are established.
- \succ Effects of dimensions, Kapitza resistance and viscous heating are investigated. > Both heat exchangers are optimized.

Physical Models



(1) Outlook and internal design of a CHEX

- \succ The concentrated phase flows into the inner tube while the dilute phase flows into the annular space.
- \succ The spiral inner tube is used to increase the heat exchange area and suppress heat transfer deterioration due to evaporation.
- \succ The material of both inner and outer tube is *CuNi* in order to reduce axial heat transfer and enhance radial heat conduction simultaneously.



- area of the upper one.

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channel while the dilute phase in the lager channel which is 4 times the cross-sectional

> The Ag block can increase the heat transfer area by several orders of magnitude to compensate for Kapitza resistance below 100mK.

 \succ The optimal dimensions: $L=2.6 \text{ m } d_{ic}=0.6 \text{ mm } D_{od}=4 \text{ mm}.$

0.0 0.4 0.8 1.2 1.6 2.0 2.4 2.8 3.2

Length (m)

	According to the conservation of energy, the coupled heat transfer governing equation of the heat exchangers below 1K can be summarized as:					
Concentrated phase Inner tube wall Outer tube wall	$X \frac{d}{dx} \left(\frac{dT_{i}}{dx} \right) + Y \frac{128\dot{n}^{2}}{\pi} + Z \left(T_{c}^{4} - T_{d}^{4} \right) = \dot{n}C_{i} \frac{dT_{i}}{dx}$ axial heat viscous lateral interface conduction heating heat transfer					(
hase — Sintered Ag	The c phase	coefficients e in both hea	of the equation for at exchangers are	or the concentration given in the tal	ited and dilute ole below.	
Shell		CHEX (c-phase)	CHEX(d-phase)	DHEX(c-phase)	DHEX(d-phase)	
 Connecting tube 	Х	$\frac{\pi d_{\rm ic}^2}{4}k_{\rm c}$	$\frac{\pi (D_{\rm od}^2 - D_{\rm id}^2)}{4} k_{\rm d}$	$\left(\varphi A_{\text{sintered-Ag}} + \frac{\pi D_{\text{c}}^2}{4}\right) k_{\text{c}}$	$\left(\varphi A_{\text{sintered-Ag}} + \frac{\pi D_{\text{d}}^2}{4}\right) k_{\text{d}}$	
	Y	$\frac{\eta_{\rm c} V_{\rm c}^2}{d_{\rm ic}^4}$	$\frac{\eta_{\rm d} V_{\rm d}^2}{(D_{\rm od} - D_{\rm id})^2 (D_{\rm od}^2 - D_{\rm id}^2)}$	$\frac{\eta_{\rm c} V_{\rm c}^2}{D_{\rm c}^4}$	$rac{\eta_{ m d} {V_{ m d}^2}}{D_{ m d}^4}$	
elow 1 K	Z	$\frac{A_{\rm ic}}{4R_{\rm k,c}}$	$\frac{A_{\rm od}}{4R_{\rm k,d}}$	$\frac{\gamma A_{\rm sintered-Ag}}{4R_{\rm k,c}}$	$\frac{\gamma A_{\rm sintered-Ag}}{4R_{\rm k,d}}$	
Discu	ssi	on an	d Optim	ization		



Relationship between thermal and flow parameters and dimensions in the CHEX

- With the optimal dimensions, taking the CHEX and DHEXs as a whole, the effects of Kapitza resistance and viscous heating are shown below.
- ➤ When the concentrated side is cooled below 0.1 K, the Kapitza thermal resistance becomes extremely large.
- > Therefore, the impendence of HEXs should be confined below 2×10^{14} m⁻⁴ to avoid the degradation of heat transfer characteristics caused by pressure drop.





Cold fluid (*d*-phase)

 \succ The numerical model is established to calculate the thermal performance based on the finite volume method.

 $\bullet T_{swith}$

 \succ The heat exchangers are regarded as a one-dimensional model, and divided into N segments along the length.

 \succ The boundary working conditions are given by:

 $T_{\rm cN+1} = T_{\rm s} = 0.7 \text{ K}$ $T_{\rm d,1} = T_{\rm mc}$ $T_{\rm c,1} = T_{\rm in}$ $\dot{n} = 200 \ \mu \text{mol/s}$

 $\bullet T_{\rm sw 1}$

 $\bullet T_{\rm exc}$

Conclusions

Separating wall

Concentrated phase

Hot fluid

- The numerical model of heat exchangers in the dilution refrigerator is established to investigate its cooling performance.
- ◆ The optimal dimensions of the continuous heat exchanger should achieve a trade-off between cooling performance and irreversible loss.
- For the discrete heat exchanger, the heat transfer and flow characteristics are strongly influenced by the Kapitza thermal resistance and impedance below 1 K.
- ◆ With the optimized heat exchangers, the cooling capacity of the dilution refrigerator can be improved by 30% in this study to accommodate more qubits for the booming superconducting quantum computers.