



# Plasma Source Development at MPP

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# Overview

- Two Plasma Source Candidates: Alkali Metal Sources
- Low ionization Potential

- **Heat Pipe Oven**

WHY BUILT?

- Has been built before

MAIN ISSUE

- The uniformity is not certain  
Yet.

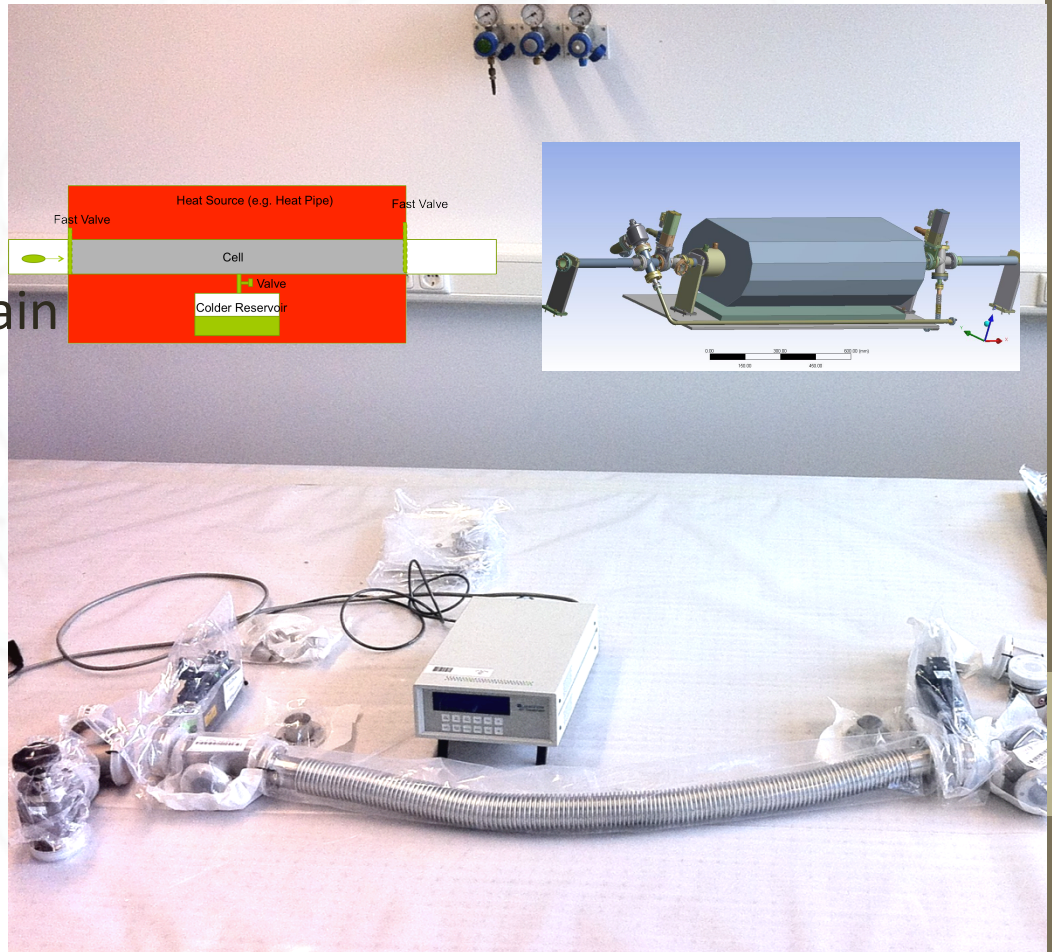
- **Vapor Cell**

WHY?

Better uniformity

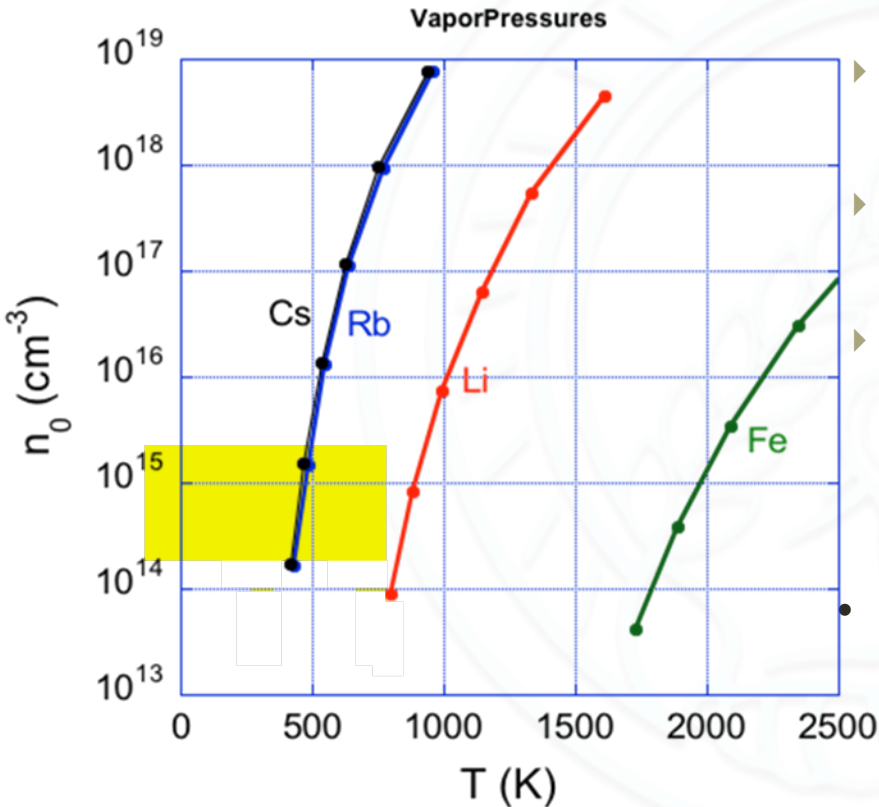
MAIN ISSUE

- Engineering Challenge





# Element of Choice



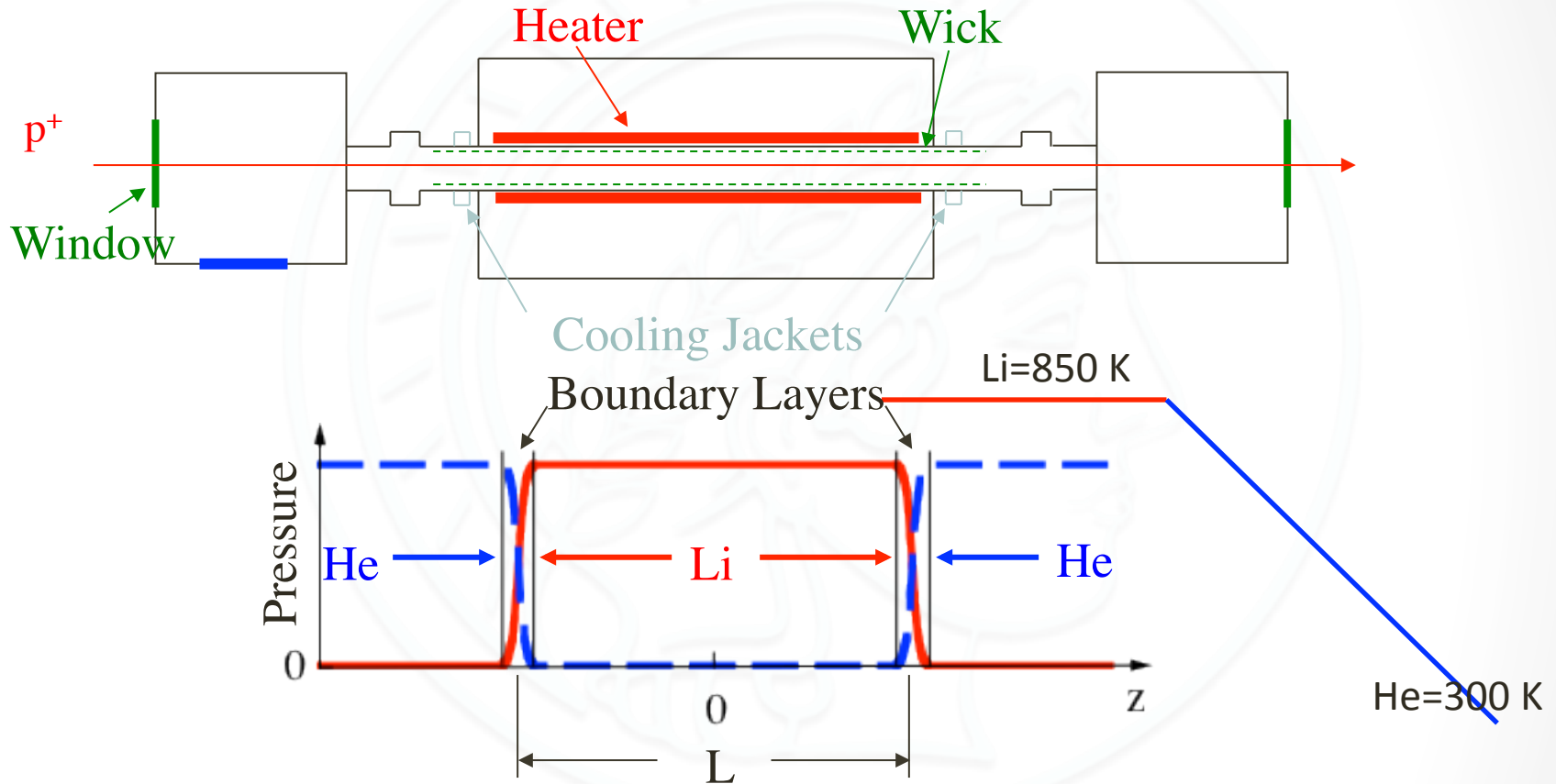
- ▶ Li:  $F=5.45\text{eV}$ ,  $T_{\text{melt}} \sim 184^\circ\text{C}$ ,  $T \sim 500\text{-}600^\circ\text{C}$ ,  $Z=3$ ,  $A=7$   
light ion
- ▶ Rb:  $F=4.18\text{ eV}$ ,  $T_{\text{melt}} \sim 39^\circ\text{C}$ ,  $T \sim 130\text{-}200^\circ\text{C}$ ,  $Z=37$ ,  $A=85$
- ▶ Cs:  $F=3.89\text{eV}$ ,  $T_{\text{melt}} \sim 28.5^\circ\text{C}$ ,  $T \sim 130\text{-}200^\circ\text{C}$ ,  $Z=55$ ,  $A=133$   
liquid at room temperature (needs refrigeration)
- P-T relation Described by Clausius-Clapeyron

$$P = P_i \exp\left(\frac{h}{k_B} \left(\frac{1}{T_i} - \frac{1}{T}\right)\right)$$

- ▶ Li at SLAC experiments
- ▶ Rb or Cs may work better for PDPWA (lower ionization and lower temperature of operation)
- ▶ Secondary ionization issues?



# Heat Pipe Oven



Rb(  $n_0=10^{14} \text{ cm}^{-3}$ :  $T=142^\circ\text{C}$ ,  $P=3.3\text{mT}$ )  
 $n_0=10^{15} \text{ cm}^{-3}$ :  $T=260^\circ\text{C}$ ,  $P=36 \text{ mT}$ )  
Li (  $n_0=10^{14} \text{ cm}^{-3}$ :  $T=518^\circ\text{C}$ ,  $P=6.8\text{mT}$ )  
 $n_0=10^{15} \text{ cm}^{-3}$ :  $T=611^\circ\text{C}$ ,  $P=76 \text{ mT}$ )



# Progress with metal vapor source

## @MPP

- Li/Cs/Rb metal vapor;  $l=1$  m,  $D=3$  cm

- ▶ Source in the design/purchasing phase



“if we can draw it we can build it!”

- Heaters are purchased  
To be delivered by the end of summer
- Operation by Christmas



12.38



# What is $Dn/n$ for heat-pipe oven?

- Except for the short boundaries ISOTHERMAL system (T constant)(orders of magnitude higher thermal conductivity than comparable size metals)

• Boundary length independent of heating power ( on the order of several He-Li mean free path)

$$l = \frac{1}{\sqrt{2}\sigma_c n} \quad l = 1 = 1/(5 \times 10^{14} \times 2.5 \times 10^{-15}) = 0.6 \text{ cm}$$

- 1-D analytic estimates quoted :  $0.005 \text{ } ^\circ\text{C}/\text{cm}^*$  (for 1 m, 0.005 % in T)
- Thermocouple measurements quoted :  $1 \text{ } ^\circ\text{C} / 1000 \text{ } ^\circ\text{C}$  (0.1 % in T) from the center to the condenser\*\*
- For an ideal gas  $Dn/n = DT/T$  ( $pv=nkT$ )

- Not true for vapor 
$$P = P_i \exp\left(\frac{h}{k_B} \left(\frac{1}{T_i} - \frac{1}{T}\right)\right)$$

Because of steep vapor-pressure curve  $Dn/n$  is larger than  $DT/T$

- Simulations

$$l = \frac{1}{\sqrt{2}\sigma_c n}; K_n = \frac{l}{D} \approx 0.2 \quad ; D = 3 \text{ cm}$$

free-molecular flow  $Kn > 1.0$ ;  
 transition flow  $0.01 < Kn < 1.0$ ;  
 continuum flow  $Kn < 0.01$ .

## Transition & molecular Flow Regime

- Not fluid
- Can't use Navier Stokes
- Wall collisions are important

- Difficult to measure  $DT/T$  with accuracy better than 0.1 %
- Quartz tuning forks?

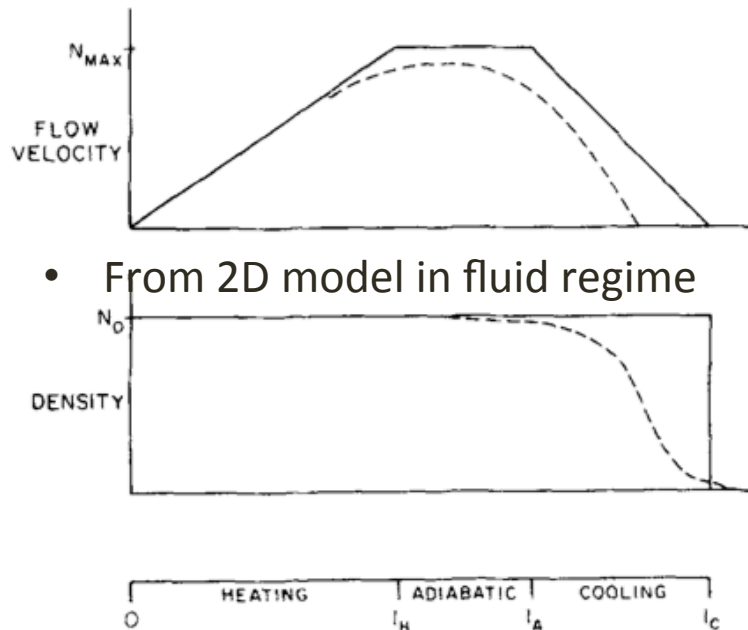
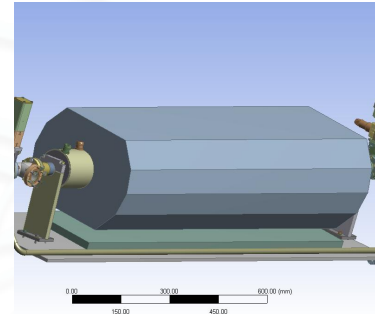
\*G. M. Grover, T. P. Cotter, and G. F. Erickson, Journal of Applied Physics 35, 1990 (1964),

\*\*C.R. and Vidal, in Atomic, Molecular, and Optical Physics: Atoms and Molecules, (Academic Press, 1996), vol. 29, Part B of Experimental Methods in the Physical Sciences, pp. 67 -83

# Quantifying Density Uniformity Challenge at Low Pressure

(Li 850 K  $n=5 \times 10^{14} \text{ cm}^{-3}$   $P \sim 0.05 \text{ Torr} \sim 6 \text{ Pa}$ )

- Density uniformity depends on flow



- From 2D model in fluid regime

- For the densities we have We don't know.



FIG. 4. Velocity and density profiles: solid line—ideal heat pipe, no diffusion,  $\beta = 1$ ; dashed line—ideal heat pipe with diffusion,  $\beta = 1$ .



# 1D Model energy and pressure balance shows\*

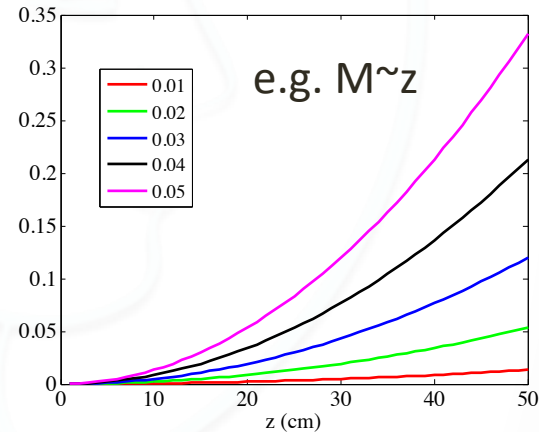
- $g_{max} = \sqrt{\frac{1+\gamma}{\gamma}} A \left( \frac{\epsilon_t D}{d^2} \right) \propto M = \frac{v_{flow}}{c}$  where  $A = 4\sigma(T_0^4 - T_r^4) \frac{(2kT_0 m)^{1/2}}{l_A P_0}$

- $A \propto P_0^{\frac{9\kappa}{2}-1}$  where  $\kappa = \frac{kT_0}{l_A}$

- For our parameters  $A \propto P_0^{-0.8}$

- The lower the pressure the more flow we have and more Non-uniformity

$$\frac{n}{n_0} = \frac{1 + \frac{1}{2} M^2 (\gamma - 1)}{1 + \gamma M^2}$$



- Low pressure could cause issues
- We need to look more carefully

\*C. Vidal J. Appl. Phys. 44 2225 (1973)



# Simulations

- ANSYS FLUENT

Does not strictly apply in molecular regime however in short term could be used as a guide and cross check for molecular codes in

- Simulating all the coupled process especially in this regime requires highly sophisticated code and a long term Project

- In contact with experts to collaborate

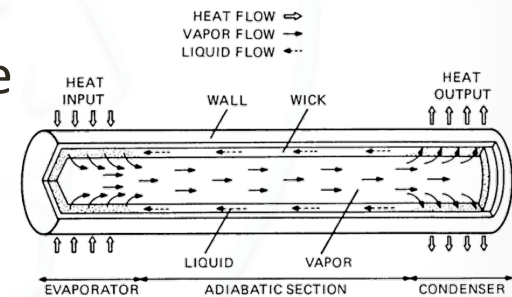


FIGURE 2.1. Illustration and Principle of Operation of a Conventional Heat Pipe.

### Liquid Flow in the Wick

$$\frac{\partial}{\partial t} [\gamma(\rho_h)_s + \epsilon(1-\gamma)(\rho_h)_l + (1-\epsilon)(\rho_h)_m]$$

$$+ \text{div}[(\rho_h)\mathbf{q}] = \text{div}[\mathbf{k}_{eff}\nabla T]$$

S: Solid  
 L: Liquid  
 M: Mixture  
 a: velocity

Volume averaged enthalpy Method to model melting process

Liquid flow in saturated isotropic wick  
 Brinkman Forchheimer extended Darcy continuity and momentum equations  
 For  $k \rightarrow \infty$  becomes Navier-Stokes

Rates of evaporation sublimation resolidification by kinetic theory

Vapor and liquid wick coupling:  
 Radial momentum jump condition  
 R: c: Curvature of meniscus:  
 Volume of fluid

$$\frac{\partial \rho_l}{\partial t} + \text{div}[\rho_l \mathbf{q}] = 0$$

$$\frac{\partial \rho_l}{\partial t} + \frac{\rho_l}{\epsilon} \text{div}[\mathbf{q}] = 0$$

$$\frac{\rho_l}{\epsilon} \frac{\partial \mathbf{q}}{\partial t} + \frac{\rho_l}{\epsilon} \mathbf{q} \text{div}[\mathbf{q}] = \rho_l \frac{\mathbf{F}}{m} - \nabla p_l - \frac{\rho_l \mathbf{q}}{K}$$

$$-\frac{C}{\sqrt{K}} \rho_l |\mathbf{q}| \mathbf{q} + \frac{\rho_l}{\epsilon} \Delta \mathbf{q}$$

$$\dot{m} = \left( \frac{m}{2\pi k T_w} \right)^{1/2} [p_v - p_{sat}(T_w)]$$

$$(\rho_l - \rho_v) + 2 \frac{\sigma}{R_c} + \left( \frac{1}{\epsilon \rho_l} - \frac{1}{\rho_v} \right) \dot{m}^2 = 0$$

### Vapor Flow

- Based on Knudsen number transition temperatures are used to define regimes
- For transition and Molecular Flow
- Wall collisions are important and fluid equations can't be used
- 1-D transient model of Dusty Gas Model based on microscopic Boltzmann equation is used
- Wall is treated as giant stationary molecules

For cylindrical channel

Boundary conditions  
 no slip,  
 zero liquid and vapor velocity at solid boundaries

$$\frac{\partial p_v}{\partial t} + \frac{\partial}{\partial z} (\rho_v U_z^v) = - \frac{2}{R_{int}} \dot{m}$$

$$\frac{\partial}{\partial t} (\rho_v U_z^v) + z_2 \frac{\partial}{\partial z} (\rho_v (U_z^v)^2)$$

$$= \rho_v \frac{F_z}{m} - \frac{\partial p_v}{\partial z} + \frac{1}{\text{Vol}} \int_{S_{wall}} \mathbf{t}(\mathbf{Z}) \cdot \mathbf{N} dA$$

$$\frac{\partial}{\partial t} \left[ \rho_v \left[ h^v + z_2 \frac{1}{2} (U_z^v)^2 \right] \right]$$

$$+ \frac{\partial}{\partial z} \left[ \rho_v \left[ h^v + z_2 \frac{1}{2} (U_z^v)^2 \right] \right]$$

$$= \frac{F_z}{m} \rho_v U_z^v + \frac{\partial p_v}{\partial t} - \frac{\partial Q_z^v}{\partial z}$$

$$- \frac{2}{R_{int}} \left\{ \dot{m} \left[ h^v + \frac{1}{2} \left( \frac{\dot{m}}{\rho_v} \right)^2 \right] + Q_z^v \right\}_{z=z_{in}}$$

$$\frac{1}{\text{Vol}} \int_{S_{wall}} \mathbf{t}(\mathbf{Z}) \cdot \mathbf{N} dA = \left[ \frac{\partial p_v}{\partial z} \right]_{z=0}^{z=L}$$

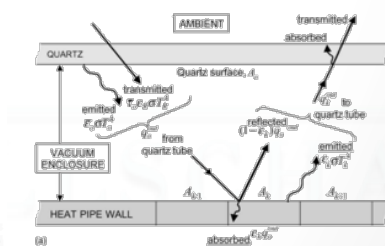
$$= - \frac{k T_w}{m} \times \frac{\rho_v U_z^v}{[D]_{eff}^{2D}}$$

deviatoric component of pressure tensor,  $t_{\alpha\beta} = p_{\alpha\beta} - p_{\alpha} \delta_{\alpha\beta}$  [N]

$$\int_V (\mathbf{U}^v)^T \cdot \mathbf{r} dA = z_2 (U_z^v)^2$$

Alfa is defined by  
 Changes according to Flow characteristic but Taken as 1, predicts by a factor of 2  
 Wrong axial momentum and kinetic energy but because the pressure gradient and loss Dominates acceptable.

## Radiative Exchange in HPTAM





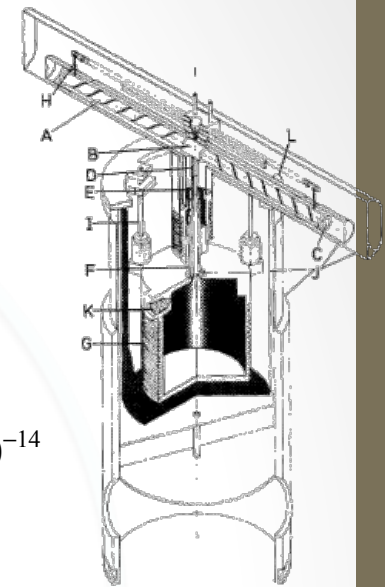
# What is a Vapor Cell?

- No buffer gas, no wick, no liquid
- Just the vapor as the ideal gas
- $DT/T = Dn/n \quad \langle (\Delta T)^2 \rangle = \frac{kT}{C_v}$
- Why don't people do it?
- Alkali metals are extremely corrosive, hard to confine, blacken glass, quartz

Requires special sealing, special materials especially for windows, high failure rate

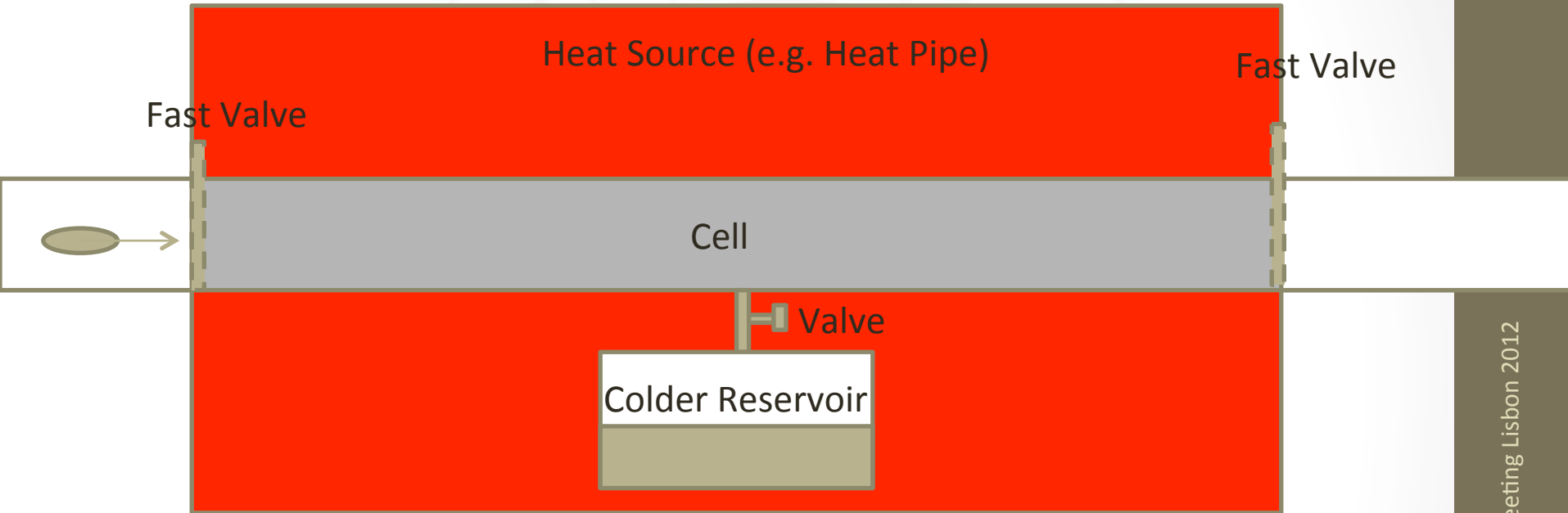
- Literature: Vapor cells with separate liquid reservoir (coldest point) or random condensation
  - No report on just gas : liquid provides density control
  - Supply of vapor compensate for leaks
  - Heated windows to prevent condensation on window which can be very problematic.

$$\frac{\sqrt{\langle (\Delta T)^2 \rangle}}{T} = \sqrt{\frac{k}{C_v T}} \sim 10^{-14}$$





# Sketch: Vapor Cell



- Two key factors: corrosion resistance and even compression of seal for a range of temperatures (0-700 C) (matching thermal expansion coefficients)
- Fast Valves?
- Choice of element (Rb, Li, Cs)?



# Back of the envelope calculations tolerance on valve opening

Speed of sound  
In Lithium or Rubidium

$$c = \sqrt{\frac{5kT}{3M}} \text{ for Li = 850 K } c \sim 1300 \text{ m/s, for Rb=500 K } c \sim 285 \text{ m/s.}$$

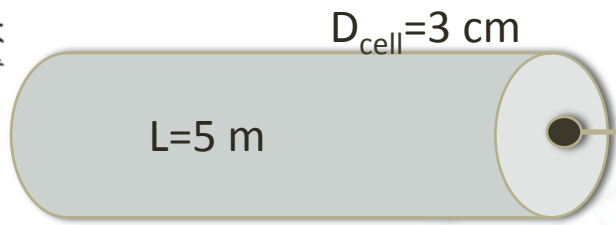
In Steel

$$c = \sqrt{\frac{Y}{\rho}} \text{ where } Y \text{ is the young's modulus for steel } Y=200 \text{ GPa; } \rho = 8000 \text{ kg / m}^3$$

$c \sim 5000 \text{ m/s.}$

for a 10  $\mu\text{s}$  opening time this would be a distance of 5 cm in steel, 0.3 cm in Rb and 1.3 cm in Li.

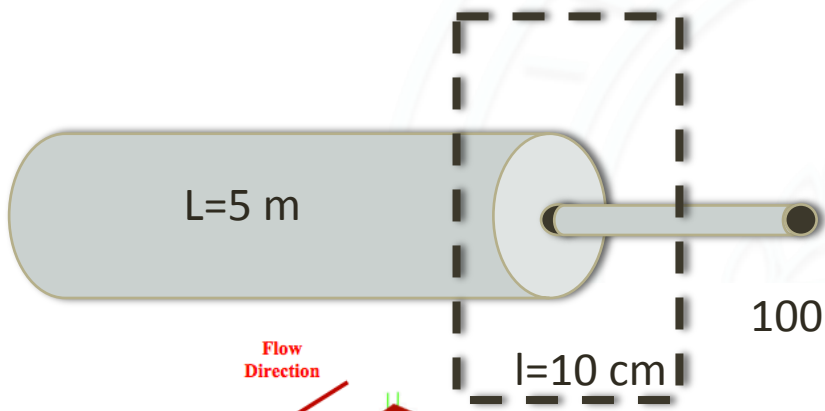




$$\Gamma = \frac{n c \pi r^2}{4}$$

$r_{\text{hole}}=2\text{ mm}$   
 $n=5 \times 10^{14}\text{ cm}^{-3}$

$$\Gamma = 2 \times 10^{18}\text{ Atoms/s}$$



$$\Gamma = 10^{15}$$

Molecular flow  
with long narrow tube

100 ms opening

$$\frac{dV}{V} = 0.2\%$$

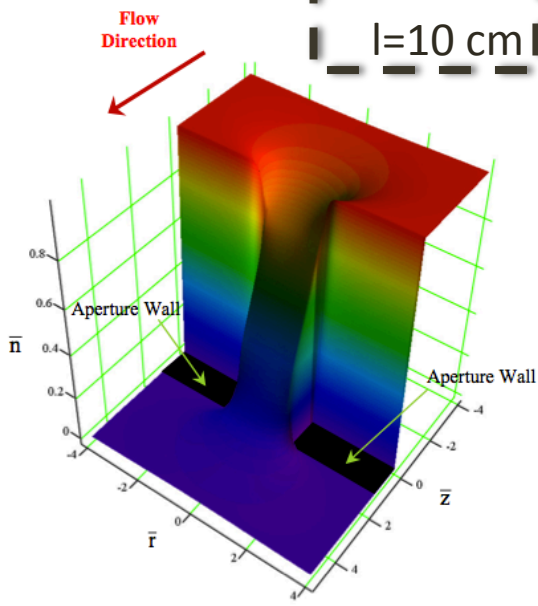
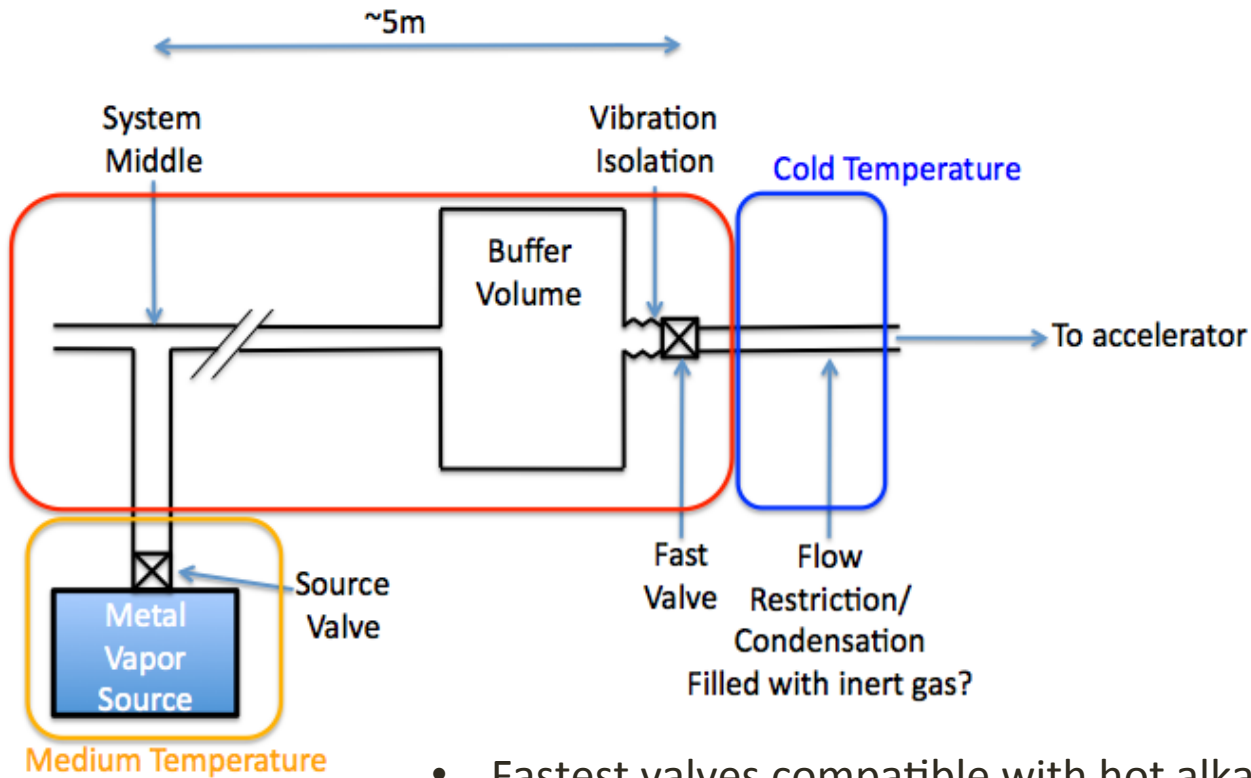


Figure 20.—Particle density surrounding a cylindrical aperture with a thickness-to-radius ratio of 1.25.

\*Gas flux and density surrounding a cylindrical aperture in the free molecular flow regime, George C Soulas; NASA Glenn Research Center.



# Vapor Cell



(Cs, Rb)



MBE-Komponenten GmbH Gutenbergstr. 8  
71263 Weil der Stadt, (Germany)

- Fastest valves compatible with hot alkali metal vapor?
- What is the density perturbation? (Simulations)
- How to provide uniform temperature?



## Heat Pipe Oven Applications. I. Isothermal Heater of Well Defined Temperature. II. Production of Metal Vapor-Gas Mixtures

C. R. VIDAL AND F. B. HALLER

National Bureau of Standards, Boulder, Colorado 80302

(Received 30 July 1971)

A concentric heat pipe oven is described, which serves as an oven with a highly homogeneous temperature distribution as required by such applications as crystal growing, thermal treatment of materials, and radiation standards. The design is simpler than conventional ovens with similar temperature stability and homogeneity. The temperature control is replaced by a pressure control. This device is used in a modification of the heat pipe oven that generates homogeneous mixtures of a vapor (such as a metal vapor) and an inert gas at well defined total pressure, partial pressure, temperature, and optical path length. All the features of the previously described heat pipe oven are maintained with the additional option that allows quantitative total and partial pressure pressure curves.

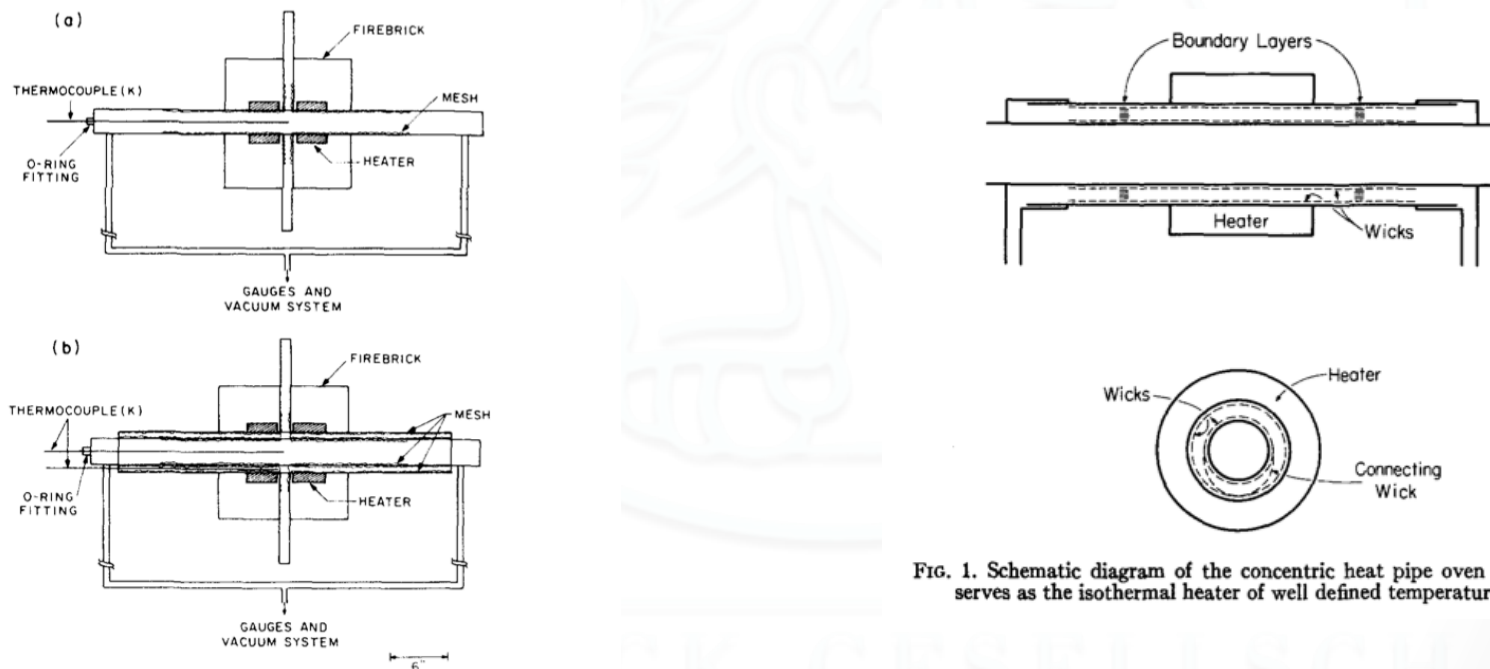


FIG. 1. Schematic diagram of the concentric heat pipe oven which serves as the isothermal heater of well defined temperature.

FIG. 1. Heat pipe used in experimental studies. (a) Simple heat pipe, (b) concentric heat pipe.

\*L. A. Melton and P. H. Wine J. Appl. Phys. 51, 4059 (1980);



# PLANS AND FUTURE WORK

- Finish 1-m long heat-pipe
- Design and test vapor cell
- Study ideal heat pipe case with numerical simulations
- Characterize neutral temperature and density profiles in both systems with various diagnostics
- Characterize plasma density profile in both systems with various diagnostics

Thank you for listening. Any questions?