



TRANSVERSE HEAT TRANSFER COEFFICIENT IN THE ITER TF CICC_s

Part II. Analysis of transient temperature responses observed during heat slug propagation tests

Monika LEWANDOWSKA¹, Robert HERZOG², Leszek MALINOWSKI¹

(1) West Pomeranian University of Technology, Szczecin, Poland

(2) was EPFL-CRPP, Villigen PSI, Switzerland

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Outline



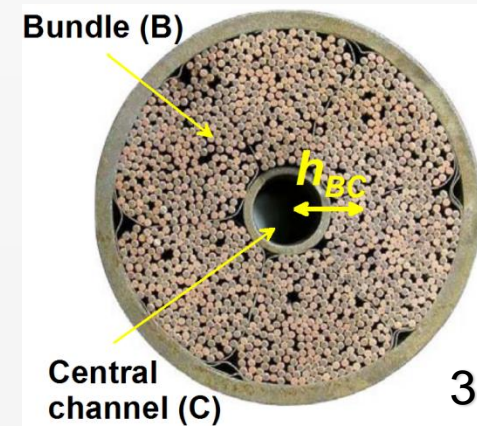
- Motivation
- Experimental setup and conductor characteristics
- Evaluation of the heat transfer coefficient
 - Method proposed in [1] and its modifications
 - Method proposed in [2]
- Results
- Summary and conclusions

[1] Bottura L, Bruzzone P, Marinucci C, Stepanov B. Cryogenics 2006; 46: 597–605

[2] Renard B, Martinez A, Duchateau J-L, Tadrist L. Cryogenics 2006; 46: 530–40.

Motivation (I)

- The simple „meso-scale” representation of a CICC with a central channel is a 1-D dual channel model, which requires constitutive relations, i.e. friction factors f_B and f_C , and transverse heat transfer coefficient h_{BC} .
- Reliable predictive correlation for h_{BC} does not exist.
- The results of theoretical efforts [3-5] are neither comprehensive nor free of contradictions.
- The database of h_{BC} data obtained by interpretation of experimental data using simple models [1,2,6,7] is very modest.



- [3] Long AE. M. Sc. Thesis, MIT, Cambridge-MA, 1995.
- [4] Nicollet S, Ciazynski D, *et al.* Proceedings of ICEC 20, Beijing, China, 2005, 589-92.
- [5] Zanino R, Giors S, Savoldi Richard L. Cryogenics 2010; 50: 158-166.
- [6] Renard B, Duchateau J-L, Rousset B, Tadrst L. Cryogenics 2006; 46: 629-42.
- [7] Marinucci C, Bottura L, Bruzzone P, Stepanov B. Cryogenics 2007; 47: 563-76.



Motivation (II)

- Two thermal-hydraulic test campaigns of two full-size ITER TF conductors were carried out in SULTAN at EPFL-CRPP in 2008 and 2009 [8,9] .
- Unique instrumentation was used:
 - large number of thermometers and heaters,
 - ‘intrusive’ instrumentation mounted inside the cable space.
- Main goal of these experiments was to study the occurrence of the flow – reversal effect, but ...

Why not to use the collected data for other analyses?

A systematic investigation of h_{BC} in the ITER TF CICCs can be performed using different approaches [1,2,6].

[8] Herzog R, Lewandowska M, Bagnasco *et al* . IEEE Trans Appl Supercond 2009; 19: 1488-91.

[9] Herzog R, Lewandowska M, Calvi M, Bessette D. J Phys: Conf Ser 2010; 234: 032022 (8 pp)



Motivation (III)



- In Part I ^[10] we derived h_{BC} values using method based on analysis of steady state temperature profiles along the sample resulting from the local annular heating ^[6] .
- In the present study the results of the heat – slug propagation tests will be interpreted using two different approaches proposed in [1] and [2].

EXPERIMENTAL (I) [9]

CONDUCTOR:

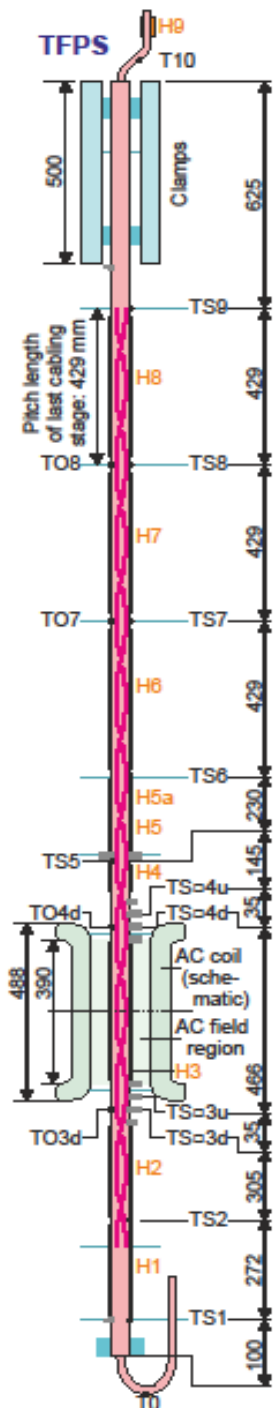
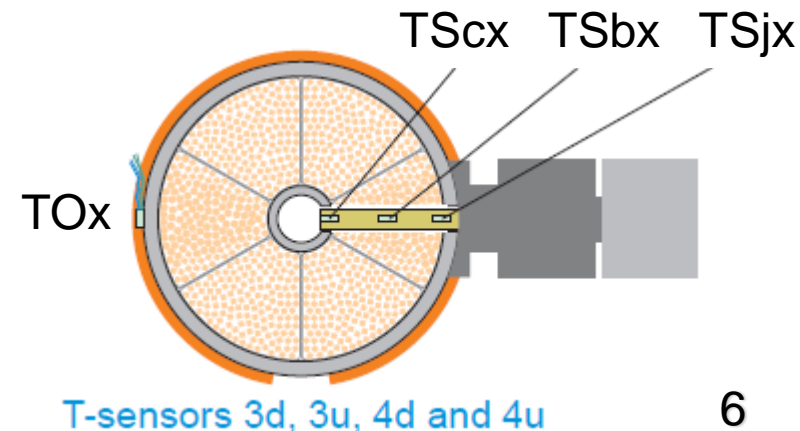
- ALSTOM B TF Performance Sample (TFPS)

Conductor parameter (unit)	Symbol	Value
Central spiral diameter (mm)	D_{in}/D_{out}	8/10
Spiral gap fraction (-)	$perf$	0.30
Bundle He cross section (mm ²)	A_B	384.8
Central channel He cross section (mm ²)	A_C	58.7
Bundle /channel wetted perimeter (mm)	p_{BC}	28.3

$$A_C = \pi[(1 - perf)D_{in}^2 + perfD_{out}^2]/4 \quad [2]$$

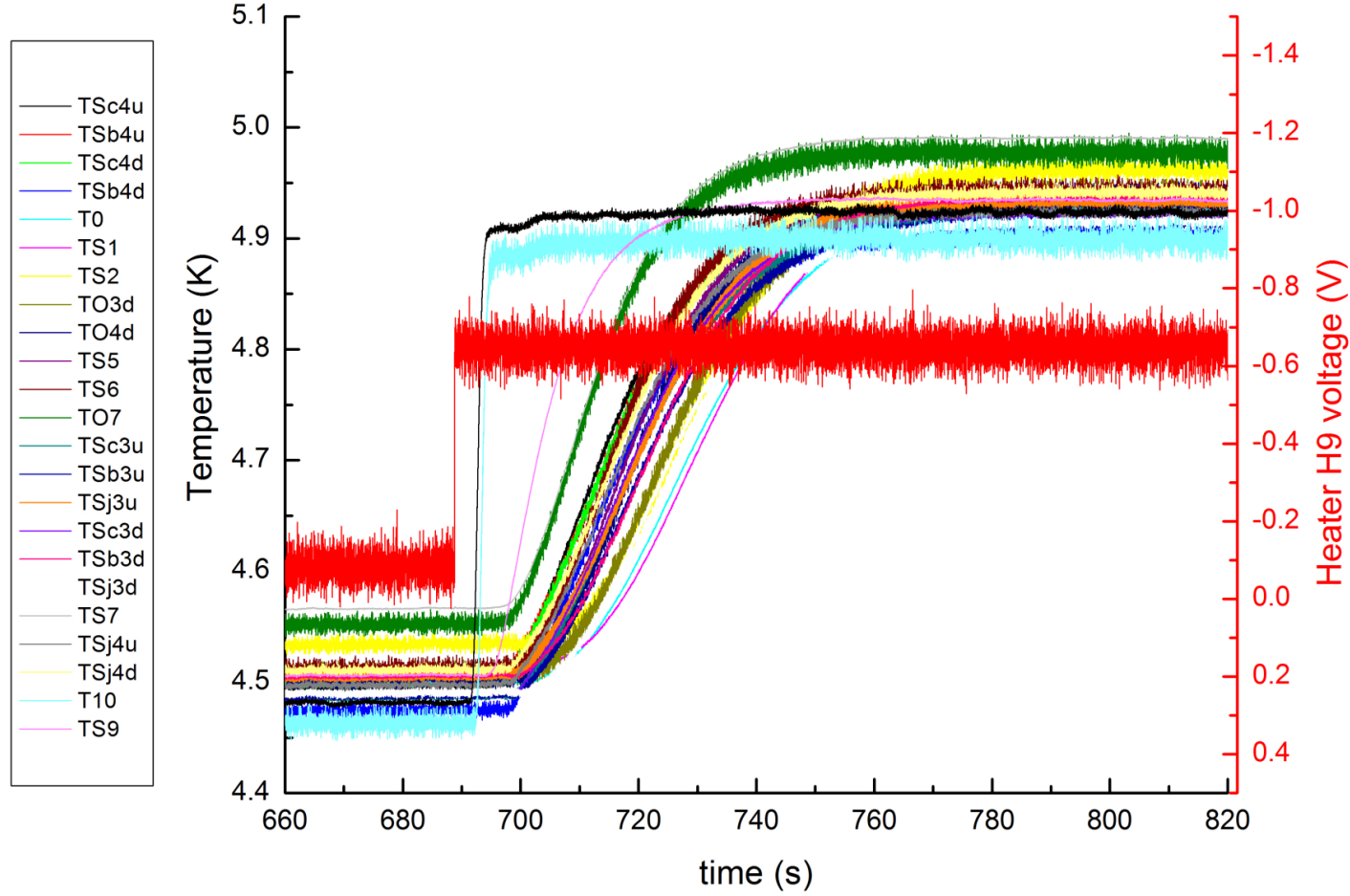
TEST CONDITIONS:

- Supercritical He at 4.5 K and 10 bar
- downward flow direction
- $\dot{m} = 4$ to 10 g/s
- 4 consecutive pulses of 0.45 K were generated by heater H9 at each mass flow rate





Experimental (II)



Typical example of raw data set



Method proposed in [1]

Mathematical model (I)



$$\left\{ \begin{aligned} \dot{m}_C C_p \frac{\partial T_C}{\partial t} + \rho C_p v_C \frac{\partial T_C}{\partial x} &= \frac{p_{BC} h_{BC}}{A_C} (T_B - T_C) \\ \dot{m}_B C_p \frac{\partial T_B}{\partial t} + \rho C_p v_B \frac{\partial T_B}{\partial t} &= \frac{p_{BC} h_{BC}}{A_B} (T_C - T_B) \end{aligned} \right.$$



$$\frac{\partial T}{\partial t} + v \frac{\partial T}{\partial x} - k \frac{\partial^2 T}{\partial x^2} = 0$$

Where:

$T(x, t) = [T_C(x, t) + T_B(x, t)] / 2$ - average temperature field in a CICC

$v = \frac{A_C v_C + A_B v_B}{A_C + A_B}$ - average flow velocity

$k = \frac{A_C^2 A_B^2}{(A_C + A_B)^3} \left(\frac{\rho C_p}{p_{BC} h_{BC}} \right) (v_C - v_B)^2$ - diffusion coefficient



Method proposed in [1]

Mathematical model (II)



МЭСЭСЭСЭСЭСЭ
ТЭСЭСЭСЭСЭСЭСЭ
ПЭСЭСЭСЭСЭСЭСЭ

$$\frac{\partial T}{\partial t} + v \frac{\partial T}{\partial x} - k \frac{\partial^2 T}{\partial x^2} = 0$$

↓

$$\xi = x - vt$$

$$\frac{\partial T}{\partial t} - k \frac{\partial^2 T}{\partial \xi^2} = 0$$

$$T(\xi < 0, 0) = T_1 \quad T(\xi = 0, 0) = (T_0 + T_1)/2 \quad T(\xi > 0, 0) = T_0 \quad - \text{initial conditions}$$

$$T(-\infty, t) = T_1 \quad T(+\infty, t) = T_0 \quad - \text{boundary conditions}$$

$$T(\xi, t) = T_0 + \frac{1}{2} (T_1 - T_0) \operatorname{erfc} \left(\frac{\xi}{2\sqrt{kt}} \right) \quad - \text{solution in moving frame}$$

$$T(x, t) = T_0 + \frac{1}{2} (T_1 - T_0) \operatorname{erfc} \left(\frac{x - vt}{2\sqrt{kt}} \right) \quad - \text{solution in laboratory frame}$$

The analytical solution could be matched to temperature response of T -sensors $\rightarrow k$
 In practice it is impossible to obtain in this way reproducible results for all T -sensors



Method proposed in [1]

Mathematical model (III)



- The characteristic time constant τ of the temperature rise at half height is a useful tool to determine k .
- Time constant τ is defined by matching an exponential model:

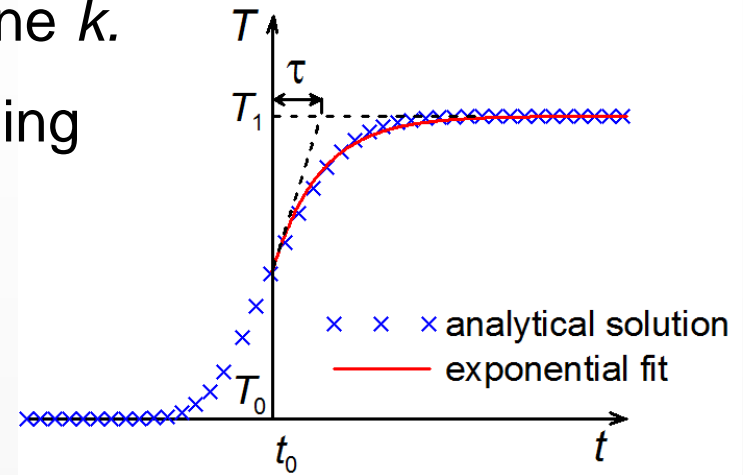
$$T(t, t_0) = T_1 - \left(\frac{T_1 - T_0}{2} \right) \exp\left(\frac{t_0 - t}{\tau} \right)$$

to the analytical solution,

t_0 is the time in which the temperature at the location of observation x reaches the value $(T_0 + T_1)/2$.

- By repeating matching at various values of k , v and x the scaling law for τ was obtained in [1]:

$$\tau \approx \sqrt{\pi} \sqrt{\frac{kx}{v^3}}$$



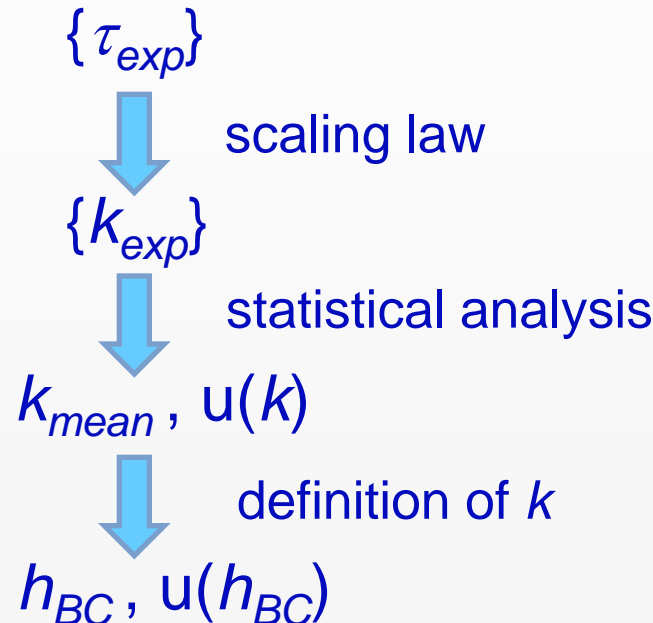


Method proposed in [1]



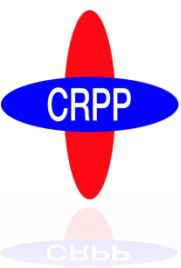
Method of h_{BC} evaluation

By fitting the exponential model to the temperature responses of thermometers located along the sample, a set of experimental values of the characteristic time $\{\tau_{exp}\}$ can be obtained.



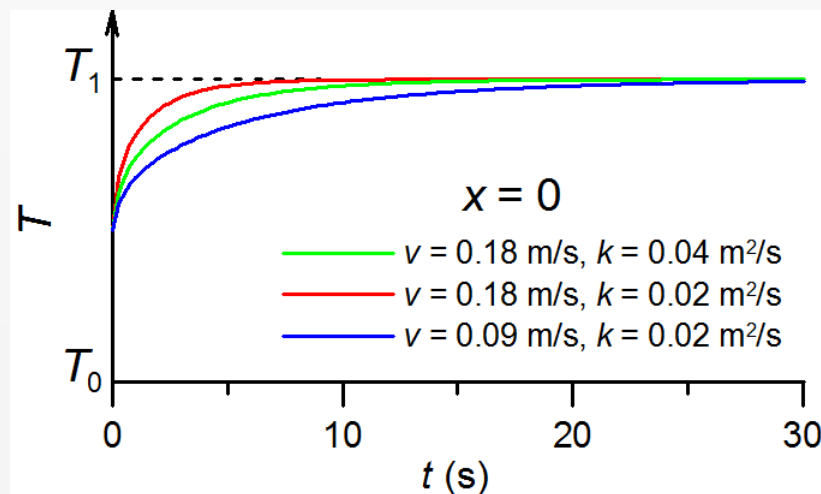
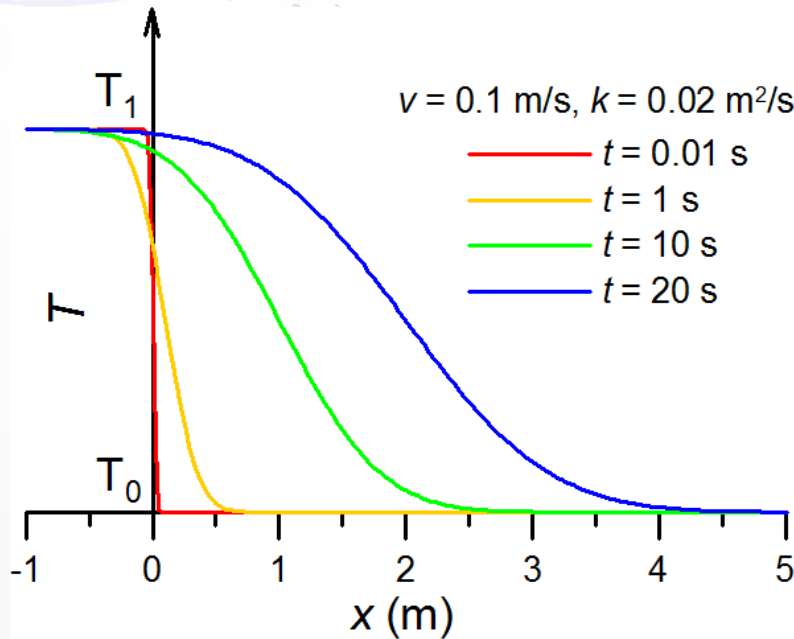
**Method
fast and
convenient in
practical use**

This method was applied in [1] to determine h_{BC} in PFIS_W and PFIS_{NW} CICC. The same experimental data were analysed in [2] using another method.



Method proposed in [1]

Problem with the model (I)



- The model formulated in [1] considers time evolution of the rectangular temperature step at $x=0$ imposed as the initial condition.
- According to the analytical solution presented in [1] temperature at $x = 0$ (corresponding to the sample inlet) varies with time:

$$T(x = 0, t) = T_0 + \frac{1}{2}(T_1 - T_0) \operatorname{erfc} \left(\frac{-v}{2} \sqrt{\frac{t}{k}} \right)$$
- As a result of the mathematical model adopted in [1] a smeared step of the helium inlet temperature occurs.
- The case considered in [1] is not equivalent to the case of rectangular step change of the inlet temperature.



Method proposed in [1]

Problem with the model (II)

In the ideal case the temperature step entering the sample should be rectangular, however ...

- heat exchange between the heater and helium is not instantaneous,
- heat pulse travels a distance between the heater and the sample inlet, which results in some diffusion,
- helium flow may be disturbed at the sample inlet or due to the presence of joints (if any).

The actual time dependence of the inlet temperature cannot be verified - thermometers have not been installed at the sample inlet ☹

Is the scaling law for τ (and the resulting h_{BC}) affected by the way of the model formulation ???



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Method modifications

Case 1: rectangular T - step imposed at the boundary $x = 0$



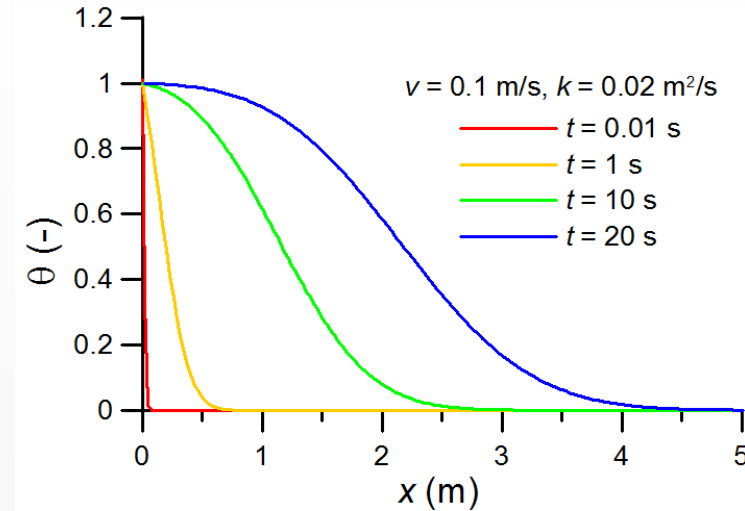
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$$\theta = \frac{T - T_0}{T_1 - T_0} \quad \text{- dimensionless temperature}$$

$$\left\{ \begin{array}{l} \frac{\partial \theta}{\partial t} + v \frac{\partial \theta}{\partial x} - k \frac{\partial^2 \theta}{\partial x^2} = 0 \\ \theta(x, 0) = 0 \quad \text{- initial condition} \\ \theta(0, t) = \begin{cases} 0 & \text{for } t \leq 0 \\ 1 & \text{for } t > 0 \end{cases} \quad \text{- boundary conditions} \\ \theta(\infty, t) = 0 \end{array} \right.$$



$$\theta(x, t) = \frac{1}{2} \left[\operatorname{erfc} \left(\frac{x - vt}{2\sqrt{kt}} \right) + \exp \left(\frac{vx}{k} \right) \operatorname{erfc} \left(\frac{x + vt}{2\sqrt{kt}} \right) \right] \quad \text{- analytical solution}$$

$$\tau \approx \frac{4}{3} \sqrt{\frac{kx}{v^3}} \quad \text{- scaling law providing } h_{BC} \text{ values } (16/9\pi) \approx \mathbf{1.8 \text{ times smaller}} \text{ than the scaling law obtained in [1]}$$

A very dissatisfactory disambiguity ☹️

Method modifications

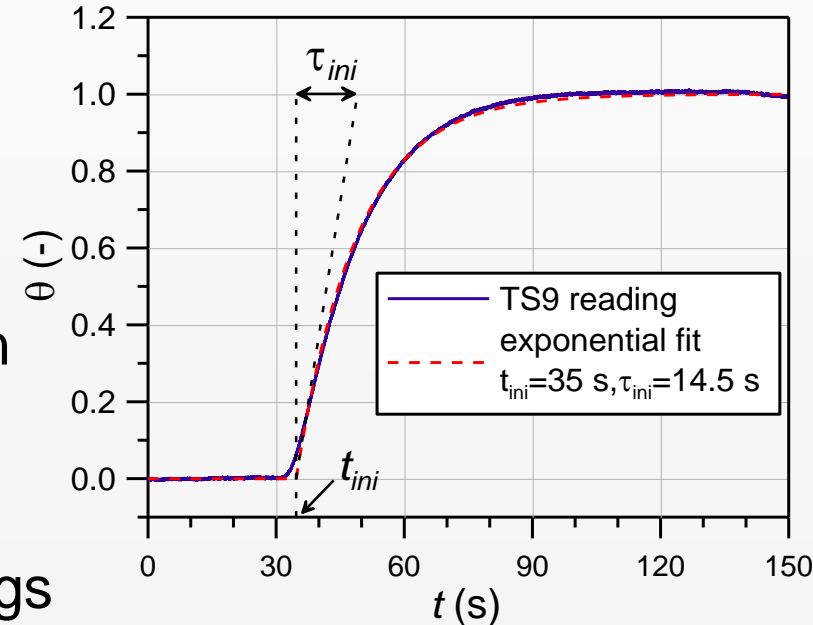
Case 2: TS9 reading used as the boundary condition (I)

- We chose the origin of the x coordinate at the location of the **thermometer closest to the sample inlet** (TS9 in our case).
- Reading of TS9-sensor for each pulse is approximated by an exponential model

$$\theta(0, t) = \begin{cases} 0 & \text{for } t \leq t_{ini} \\ 1 - \exp\left(\frac{t_{ini} - t}{\tau_{ini}}\right) & \text{for } t > t_{ini} \end{cases}$$

to be used as the boundary condition at $x = 0$.

- Least square fitting is used to match the exponential model to TS9 readings for each pulse $\rightarrow t_{ini}$ and τ_{ini} .



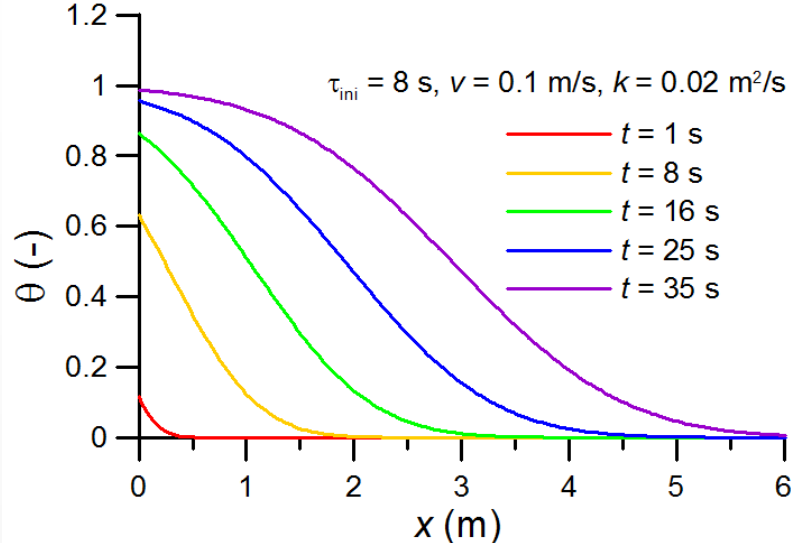


Method modifications

Case 2: TS9 reading used as the boundary condition (II)



$$\left\{ \begin{array}{l} \frac{\partial \theta}{\partial t} + v \frac{\partial \theta}{\partial x} - k \frac{\partial^2 \theta}{\partial x^2} = 0 \\ \theta(x, 0) = 0 \\ \theta(0, t) = \begin{cases} 0 & \text{for } t \leq 0 \\ 1 - \exp(-t / \tau_{ini}) & \text{for } t > 0 \end{cases} \\ \theta(\infty, t) = 0 \end{array} \right.$$



$$\theta(x, t) = \theta_1(x, t) - \theta_2(x, t)$$

$$\theta_1(x, t) = \frac{1}{2} \left[\operatorname{erfc} \left(\frac{x - vt}{2\sqrt{kt}} \right) + \exp \left(\frac{vx}{k} \right) \operatorname{erfc} \left(\frac{x + vt}{2\sqrt{kt}} \right) \right]$$

$$\theta_2(x, t) = \frac{1}{2} \exp \left(\frac{-t}{\tau_{ini}} \right) \exp \left(\frac{vx}{2k} \right) \frac{x}{\sqrt{\pi k}} \int_0^t \xi^{-3/2} \exp \left[\xi \left(\frac{1}{\tau_{ini}} - \frac{v^2}{4k} \right) - \frac{x^2}{4k\xi} \right] d\xi$$



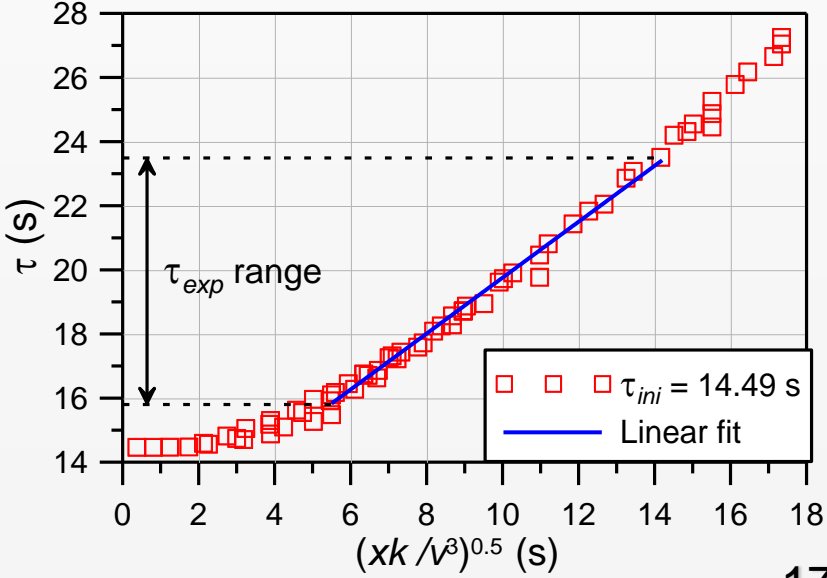
Method modifications

Case 2: *TS9* reading used as the boundary condition (III)



- We did not manage to formulate a universal scaling law, which is a disadvantage of this approach.
- In principle a separate scaling equations should be obtained for each τ_{ini} value (i.e. for each considered pulse). However, for similar values of τ_{ini} we used their average.
- Least square fitting was used to obtain scaling equations in the linear form:

$$\tau \approx a\sqrt{kx/v^3} + b$$

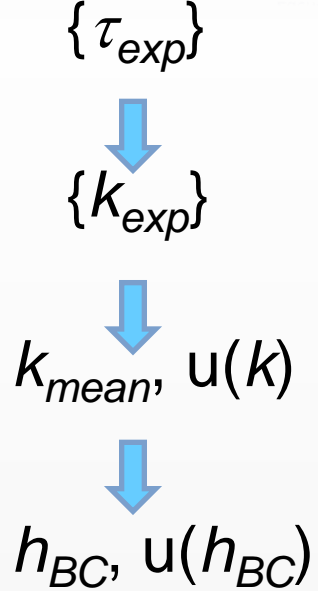




Method proposed in [1] and its modifications



Uncertainties evaluation



$$h_{BC} = \frac{1}{k} \frac{A_C^2 A_B^2}{(A_C + A_B)^3} \left(\frac{\rho C_p}{p_{BC}} \right) \left[v_C \left(1 + \frac{A_C}{A_B} \right) - \frac{\dot{m}}{A_B \rho} \right]^2$$

$$u(k_{mean}) = \sqrt{\frac{\sum_{i=1}^n (k_{exp_i} - k_{mean})^2}{n(n-1)}}$$

Relative uncertainties:

$$u(\dot{m}) / \dot{m} = 5\%$$

$$u(v_C) / v_C = 25 / 5 \% \text{ (upper/lower bound) [9]}$$

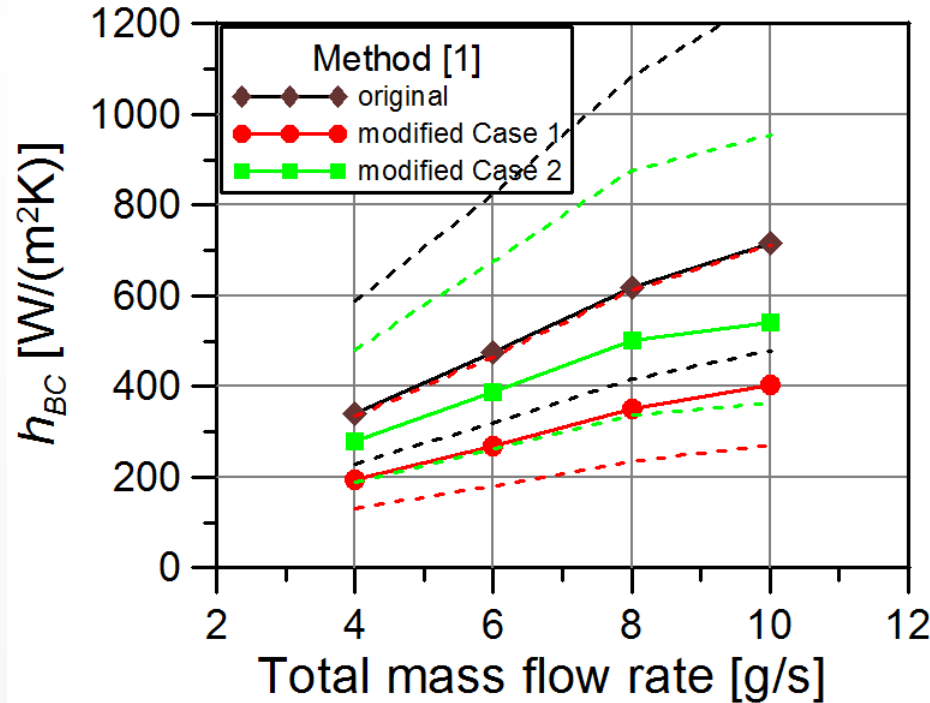
$$u(A_C) / A_C = 15 \% \text{ (lower), due to different definitions}$$

$$u(h_{BC}) = \sqrt{\left(\frac{\partial h_{BC}}{\partial v_C} \right)^2 u^2(v_C) + \left(\frac{\partial h_{BC}}{\partial A_C} \right)^2 u^2(A_C) + \left(\frac{\partial h_{BC}}{\partial \dot{m}} \right)^2 u^2(\dot{m}) + \left(\frac{\partial h_{BC}}{\partial k} \right)^2 u^2(k)}$$

The resulting uncertainties of h_{BC} are large ☹ (up to 70% for the upper bound)

Method proposed in [1] and its modifications

Results



- All methods are **very sensitive** to small changes of the v_C and A_C values used in the evaluation of h_{BC} (v_C is the most critical).
- Accurate knowledge of the flow partition in a cable is necessary to obtain reliable h_{BC} values, which seems challenging with the existing methods.



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Method proposed in [2]

Mathematical model



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$$\left\{ \begin{aligned} \dot{m}_C C_p \frac{\partial T_C}{\partial t} + \rho C_p v_C \frac{\partial T_C}{\partial x} &= \frac{p_{BC} h_{BC}}{A_C} (T_B - T_C) \\ \dot{m}_B C_p \frac{\partial T_B}{\partial t} + \rho C_p v_B \frac{\partial T_B}{\partial x} &= \frac{p_{BC} h_{BC}}{A_B} (T_C - T_B) \\ T_B(x, t = 0) = T_C(x, t = 0) &= T_0 \\ T_B(x = 0, t) = T_C(x = 0, t) &= \begin{cases} T_0 & \text{for } t < 0 \\ T_1 & \text{for } t \geq 0 \end{cases} \end{aligned} \right.$$

$$\theta_B(x, t) = \begin{cases} 0 & \text{for } t \leq x/v_C \\ 2\alpha \exp(-\alpha) \int_0^\delta \beta \exp(-\alpha\beta^2) I_0(2\alpha\beta) d\beta & \text{for } x/v_C < t < x/v_B \\ 1 & \text{for } t \geq x/v_B \end{cases}$$

$$\alpha(x, t) = \frac{h_{BC} p_{BC}}{\rho A_i C_p} \cdot \frac{x - v_B t}{v_C - v_B} \quad \delta(x, t) = \sqrt{\frac{(v_C t - x) A_C}{(x - v_B t) A_B}}$$

Following [1] we assume that readings of TSx, TOx, TSbx and TSjx sensors can be approximated by the analytical solution θ_B



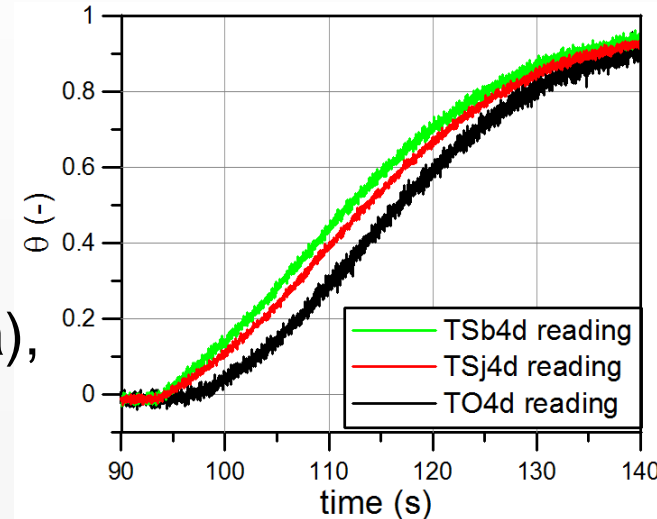
Method proposed in [2]



Starting delay

Time at which the temperature rise is registered by the T -sensor located at a distance x depends on:

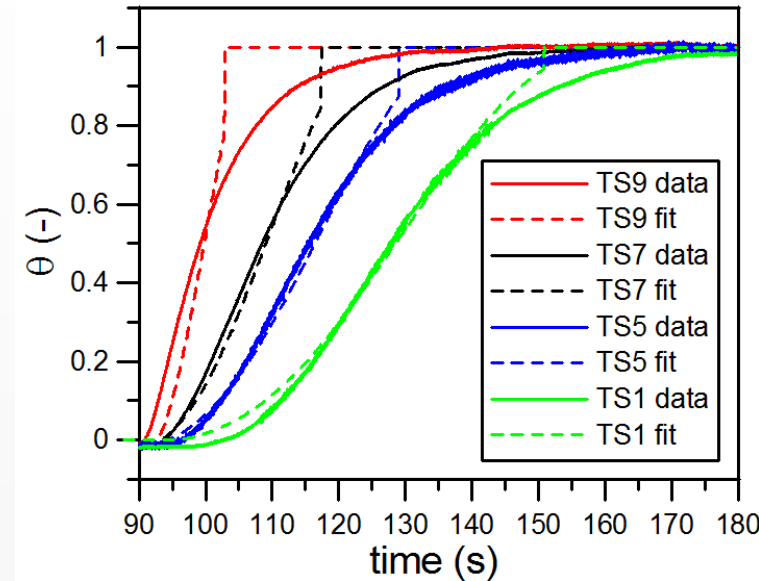
- the time t_0 at which the heater is switched on,
- the time delay Δt_h , after which the heat pulse reaches the sample inlet,
- the time delay related to the duration of heat transfer in the radial direction (difficult to estimate, but visible in our data),
- the time during which the heat pulse travels a distance x within the sample (taken into account in the analytical solution).



The first three effects are lumped together into one parameter called „**starting delay**” [2]. Its value can be determined by matching the solution to experimental data.

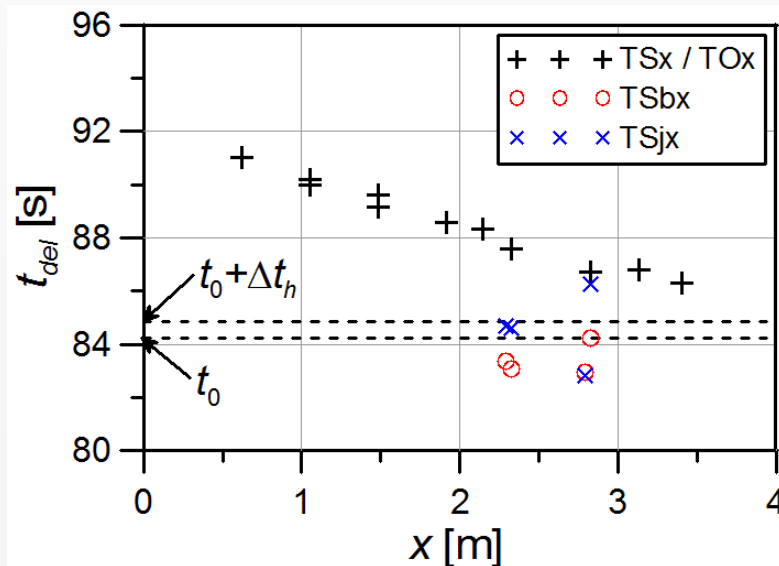
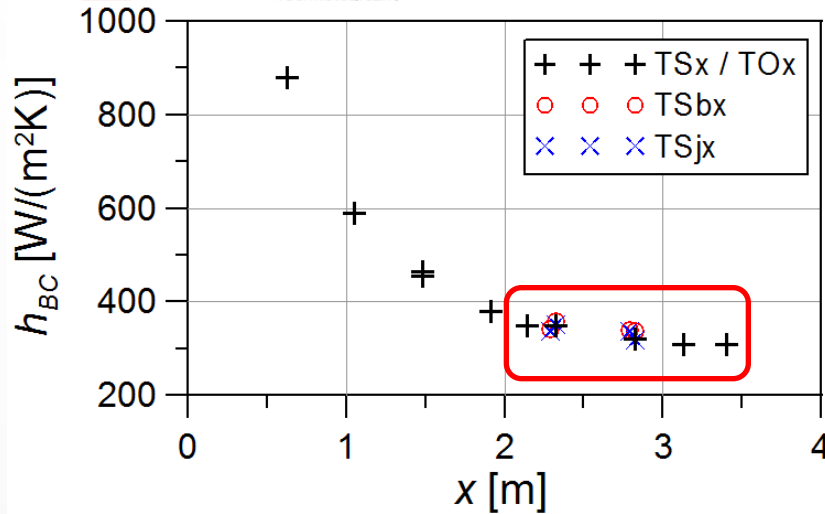
Fitting

- We used the least square fitting procedure with the two free parameters h_{BC} and t_{del} .
- A characteristic feature of the analytical solutions is a **sharp temperature front at $t = t_{del} + x/v_B$** , where x is the sensor position.
- Such a temperature jump is not observed in T -sensors' readings.
- The smaller is x the higher is the temperature front and the poorer the agreement between the fits and the data.



For small x parameters h_{BC} and t_{del} , obtained from fitting, are pushed towards higher values.

Observed trends



- For the further statistical analysis we used only h_{BC} values obtained for thermometers at $x > 2$ m, for which the dependence on x is weak.
- The h_{BC} values for the sensors TOx, TSjx and TSbx located at the same distance are consistent 😊
- The dependence of the starting delay on x cannot be explained by the presence of joints.
- The values of t_{del} for thermometers mounted inside the cable are very small (**some are smaller than t_0 !**).
- **Parameter t_{del} does not have a clear physical interpretation??**



Method proposed in [2]

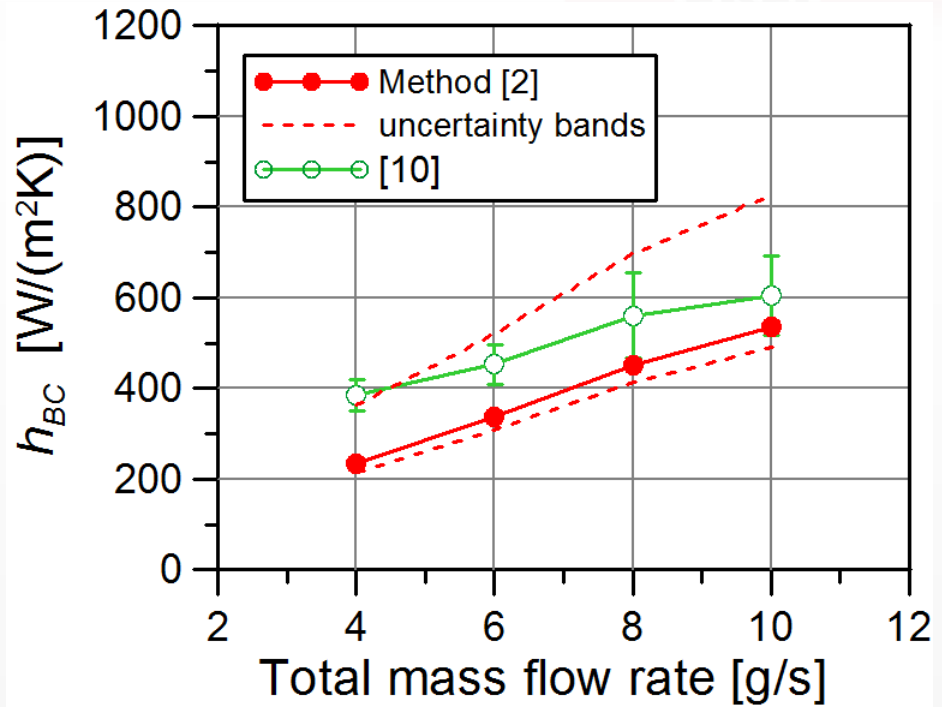
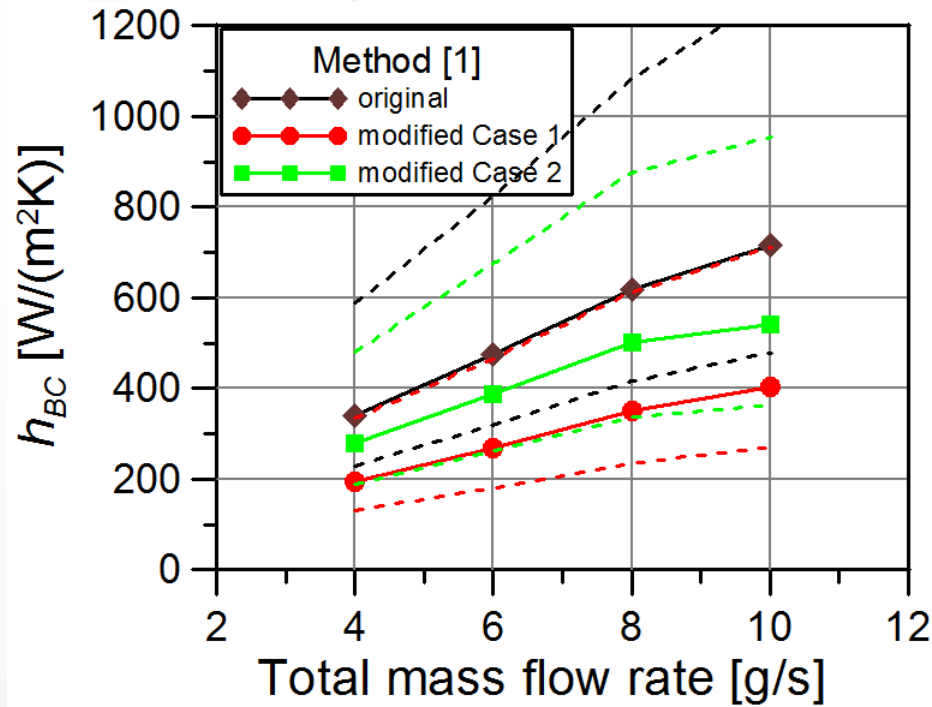
Uncertainties evaluation

- The uncertainties of h_{BC} resulting from the fitting procedure and standard deviations of the mean are very small (of about 2%).
- To assess the contributions of the uncertainties of v_C , A_C and \dot{m} used in the calculations to the uncertainty of h_{BC} , we performed a sensitivity analysis.
- We increased (or decreased) the value of one of the parameters v_C , A_C or \dot{m} by the value of the respective error bar and repeated the fitting procedure for several selected thermometers. Then we estimated the respective relative change of the h_{BC} value.
- All these contributions were lumped together resulting in an **upper band of the h_{BC} uncertainty of 54% and lower one of 8.4%**.
- The values of t_{del} were much more stable than h_{BC} with respect to the changes of parameters v_C , A_C and \dot{m} .



The surprisingly small values of t_{del} obtained for the sensors mounted in the cable space **cannot result** from the inaccurately measured v_C used in the calculations.

Results



The h_{BC} values obtained in [1] for the PFIS_W and PFIS_{NW} conductors were systematically smaller (about 30%) than those in [2].

Here we see the opposite trend.

Different methods of v_C evaluation and different A_C definitions used in [1] and [2] can be the possible reason of inconsistent results.

- We derived the h_{BC} values for the final-design ITER TF conductor from the measurements of a heat slug propagation experiment.
- Two different models proposed in [1] and [2] were used for interpretation of experimental data.
- To the former we added 2 modifications and assessed their impact on the results.
- Results obtained with **both methods are sensitive to uncertainties of v_C , A_C and \dot{m} values used in the calculations** (v_C is the most critical). The resulting uncertainties of h_{BC} are particularly large (up to 70%) with the method proposed in [1] and its modifications.
- The original method [1] and its 1st modification are rapid in practical use, but they can provide the approximate range in which h_{BC} value should fall.
- The 2nd modification proposed by us does not involve any unverified assumptions about the helium inlet temperature, but requires more efforts, since no universal scaling equation for τ was formulated.
- Method proposed [2] is based on unrealistic assumption that the temperature step is rectangular which affects the results → **modification could be proposed ?**
- Method based on analysis of steady state temperature profiles resulting from annular heating [6] seems more accurate.



Thank you for your attention



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Question Time



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