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# Activated Carbon-Hydrogen Based Continuous Sorption Cooling in Single Adsorbent Bed with LN<sub>2</sub> Heat Sink

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# Outline

- Introduction
- New concept
- Objective
- Theory and validation
- Results and discussion
- Conclusions

# Introduction – Solid Sorption Cooling

## Advantages

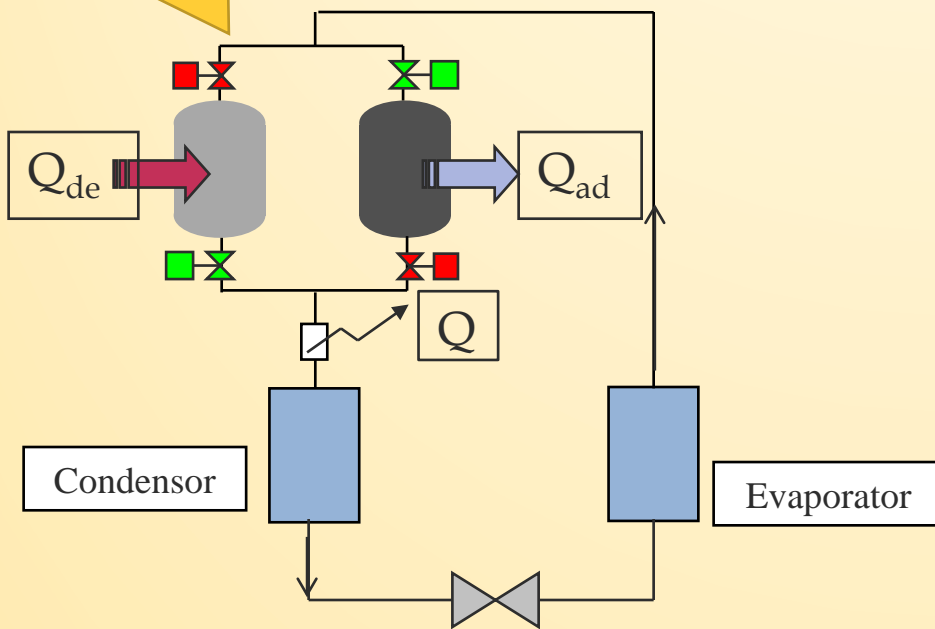
- Zero global warming potential
- High heat of adsorption of working fluid
- Wide temperature domain

## Different Domain of Application

- Air conditioning
- Refrigeration
- **Cryogenic cooling**

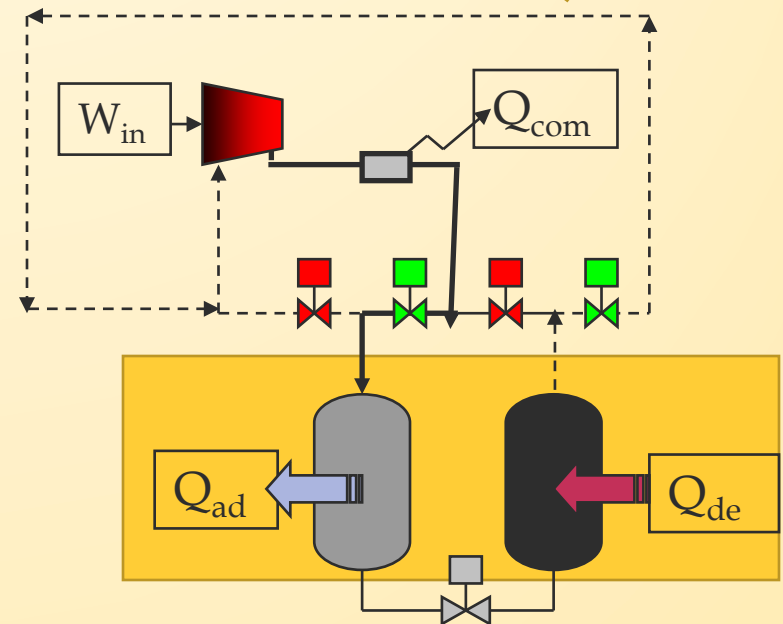
## Classification

well-documented



Thermal compressor driven cycle

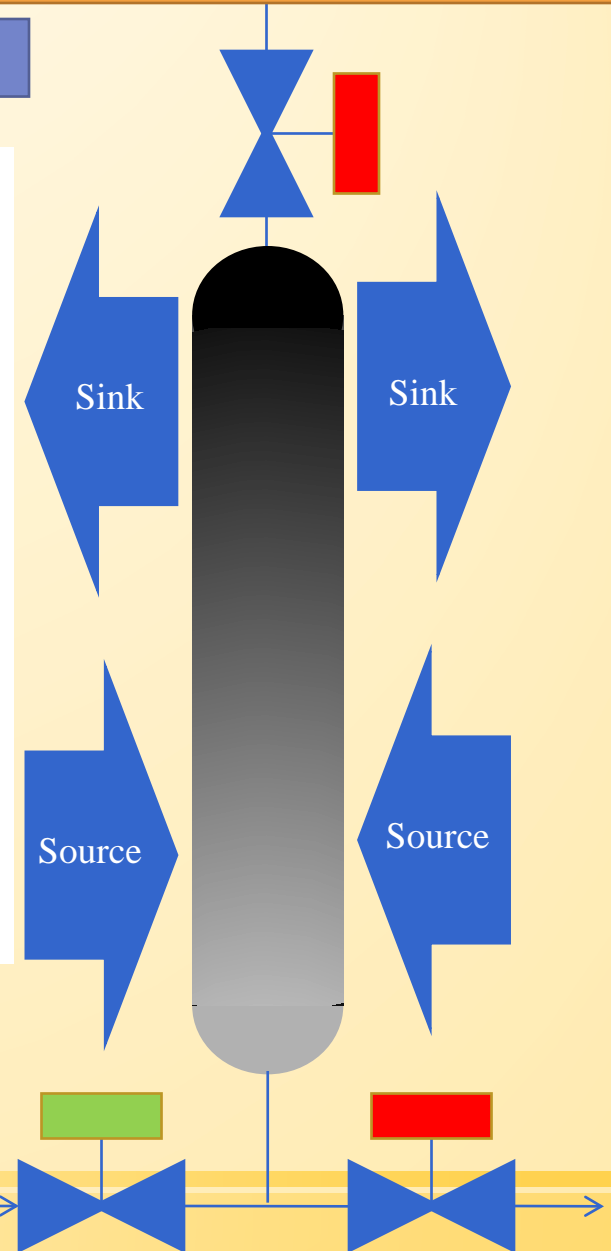
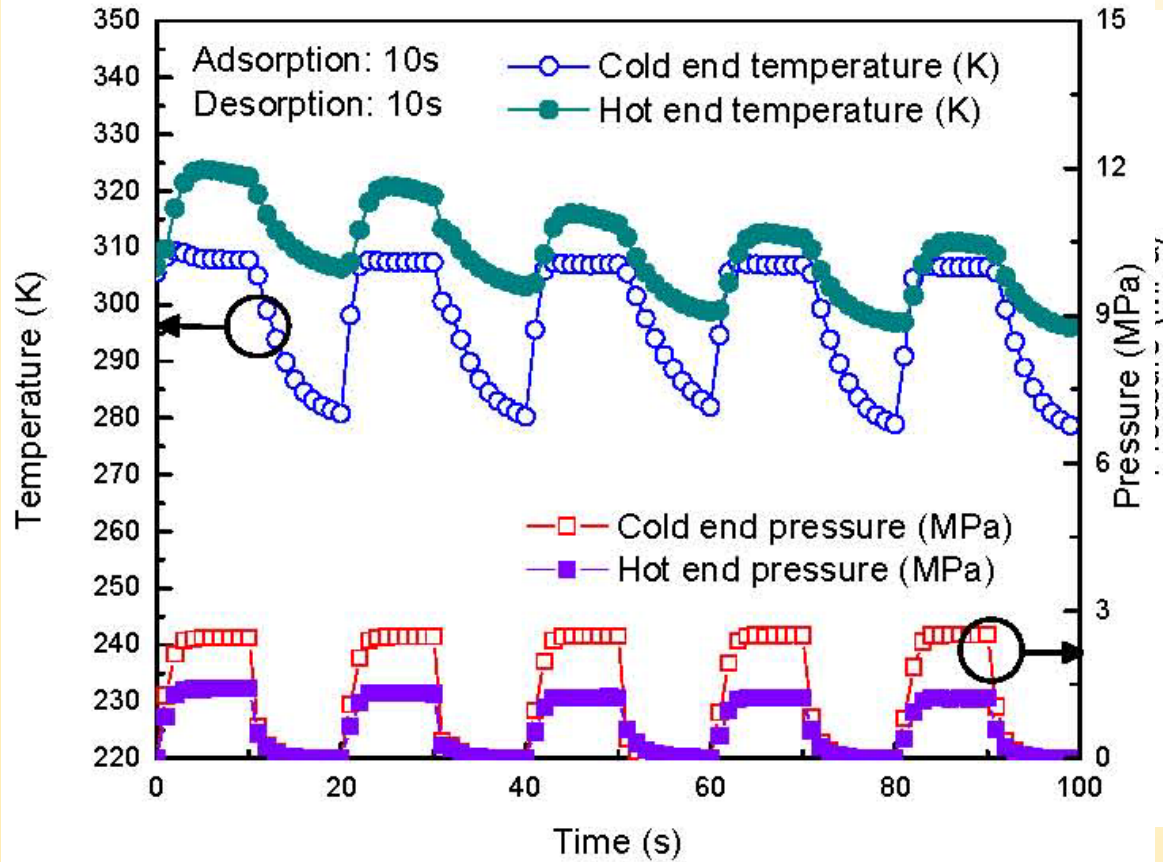
less-familiar



Mechanical compressor driven cycle

# Novel Concept

Activated carbon-Nitrogen system at room temperature

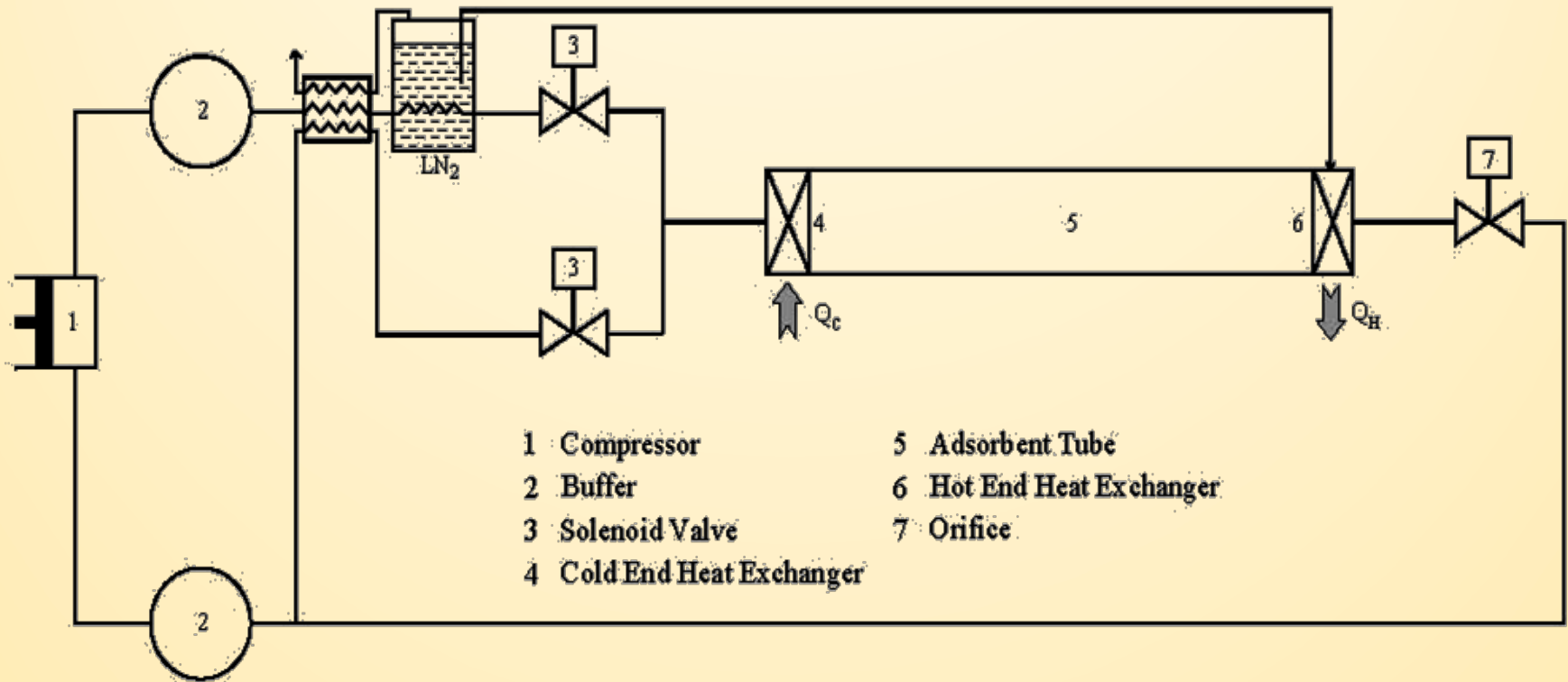


- Koley S. Ghosh I., 2013. Applied Thermal Engineering; 55, 33-42.
- Koley S., Ghosh I., 2014. Int. Journal of Heat and Mass Transfer; 72, 470-478.

# Objective

- Theoretical investigation of LN<sub>2</sub> pre-cooled continuous solid sorption cooling in activated carbon-hydrogen system
- Parametric studies of the cooling process

# Physical Model



- |                           |                          |
|---------------------------|--------------------------|
| 1 Compressor              | 5 Adsorbent Tube         |
| 2 Buffer                  | 6 Hot End Heat Exchanger |
| 3 Solenoid Valve          | 7 Orifice                |
| 4 Cold End Heat Exchanger |                          |

# Governing Equations

## Mass Balance Equation

$$\varepsilon \frac{\partial \rho}{\partial t} + \varepsilon \frac{\partial}{\partial x} \left[ u\rho - D_{ax} \frac{\partial \rho}{\partial x} \right] + (1 - \varepsilon) \rho_s M_g \frac{\partial q(x,t)}{\partial t} = 0$$

## Energy Balance Equation

$$\begin{aligned} & \left[ \varepsilon A_1 \rho C_p + (1 - \varepsilon) A_1 \rho_s C_{ps} + \varepsilon A_2 \rho_w C_{pw} - \varepsilon A_1 \bar{R} \rho \right] \left( \frac{\partial T}{\partial t} \right) - (1 - \varepsilon) A_1 \Delta H \rho_s \frac{\partial q(x,t)}{\partial t} \\ & = \frac{\partial}{\partial x} \left[ A_1 k_b \frac{\partial T}{\partial x} - \varepsilon A_1 \rho C_p u T \right] - h_{amb} (\pi D_0) (T - T_0) \end{aligned}$$

## Initial Conditions for Adsorption

$$\rho(x, t=0) = \rho_0 \text{ and } T(x, t=0) = T_0$$

## Initial Conditions for Desorption

$$\rho(x, t=0) = \rho_x(T_x, P_x) \text{ and } T(x, t=0) = T_x$$

## Boundary Conditions

At  $x=0$ ;

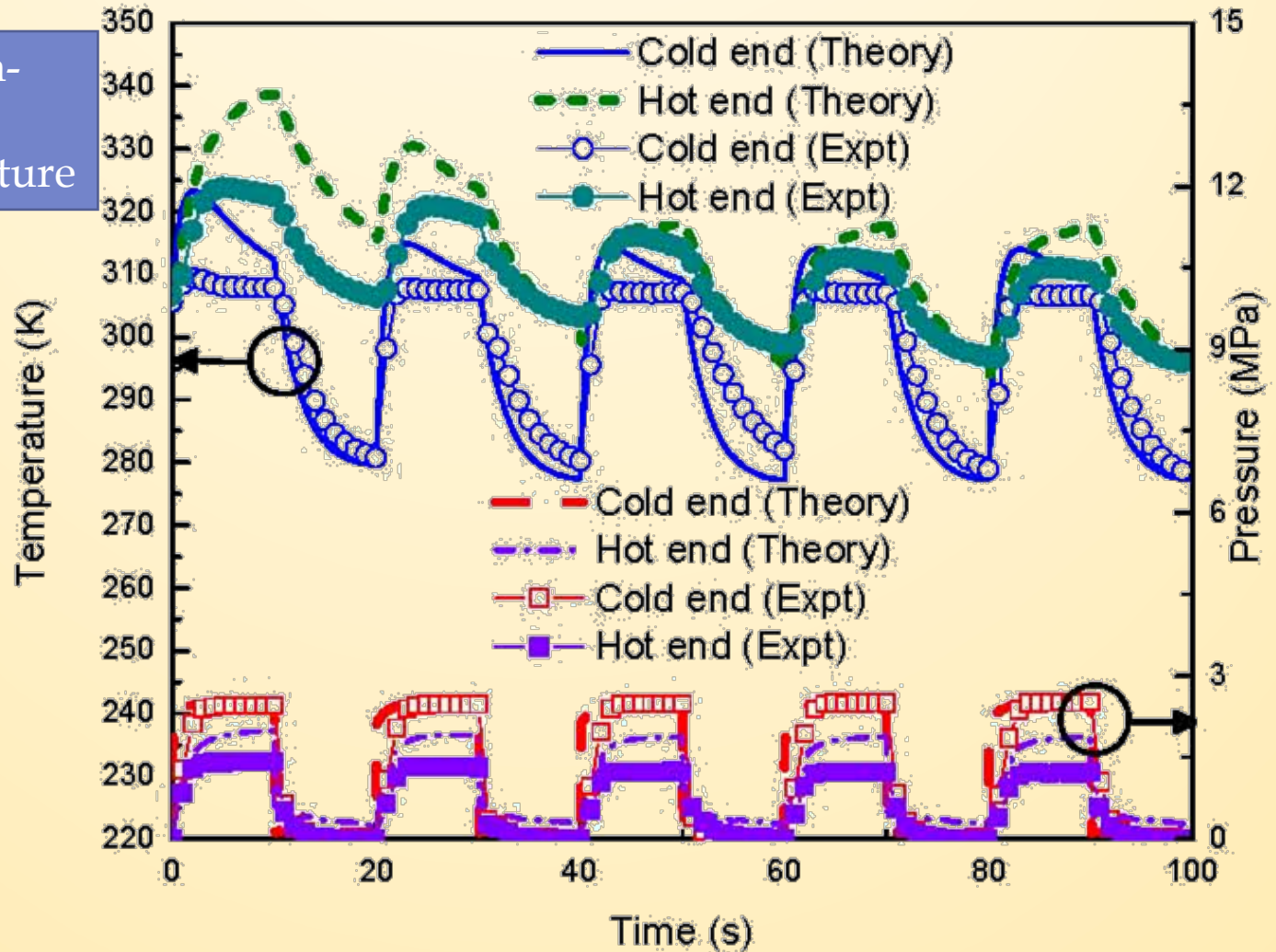
$$u\rho(0,t) - D_{ax} \frac{\partial \rho}{\partial x}(0,t) = u\rho_0 \text{ and } T(0,t) = T_0$$

At  $x=L$

$$\frac{\partial \rho}{\partial x}(L,t) = 0 \text{ and } \frac{\partial T}{\partial x}(L,t) = 0$$

# Validation

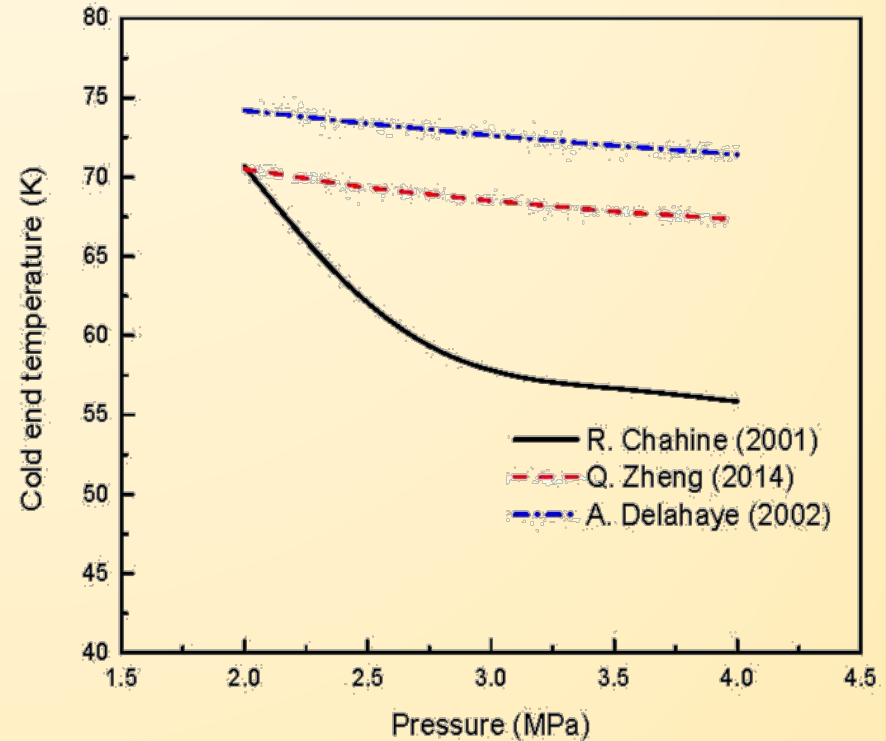
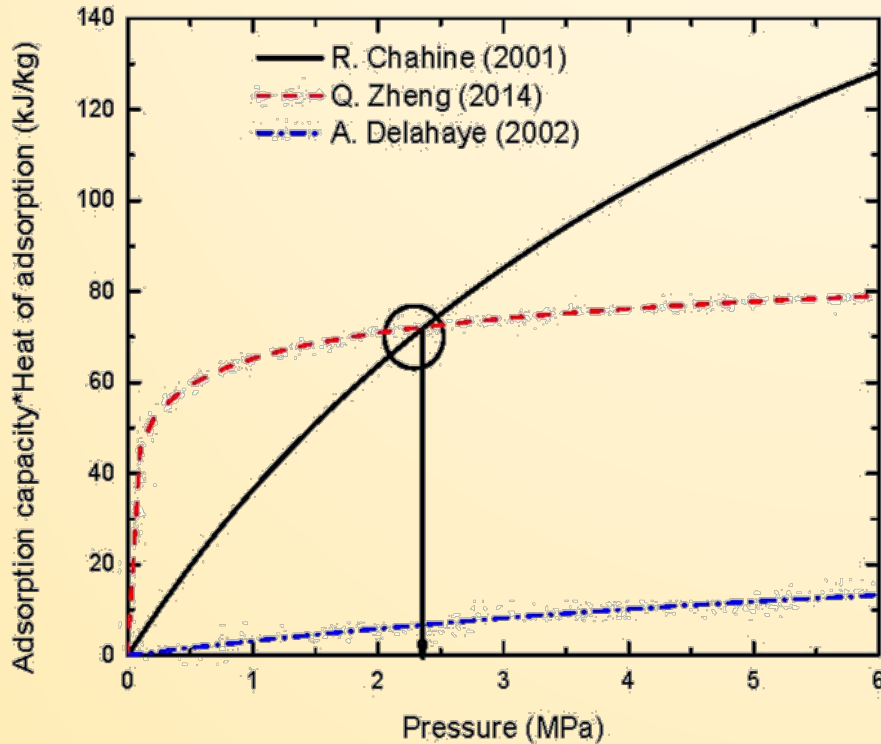
Activated carbon-Nitrogen system at room temperature





# Results and Discussions

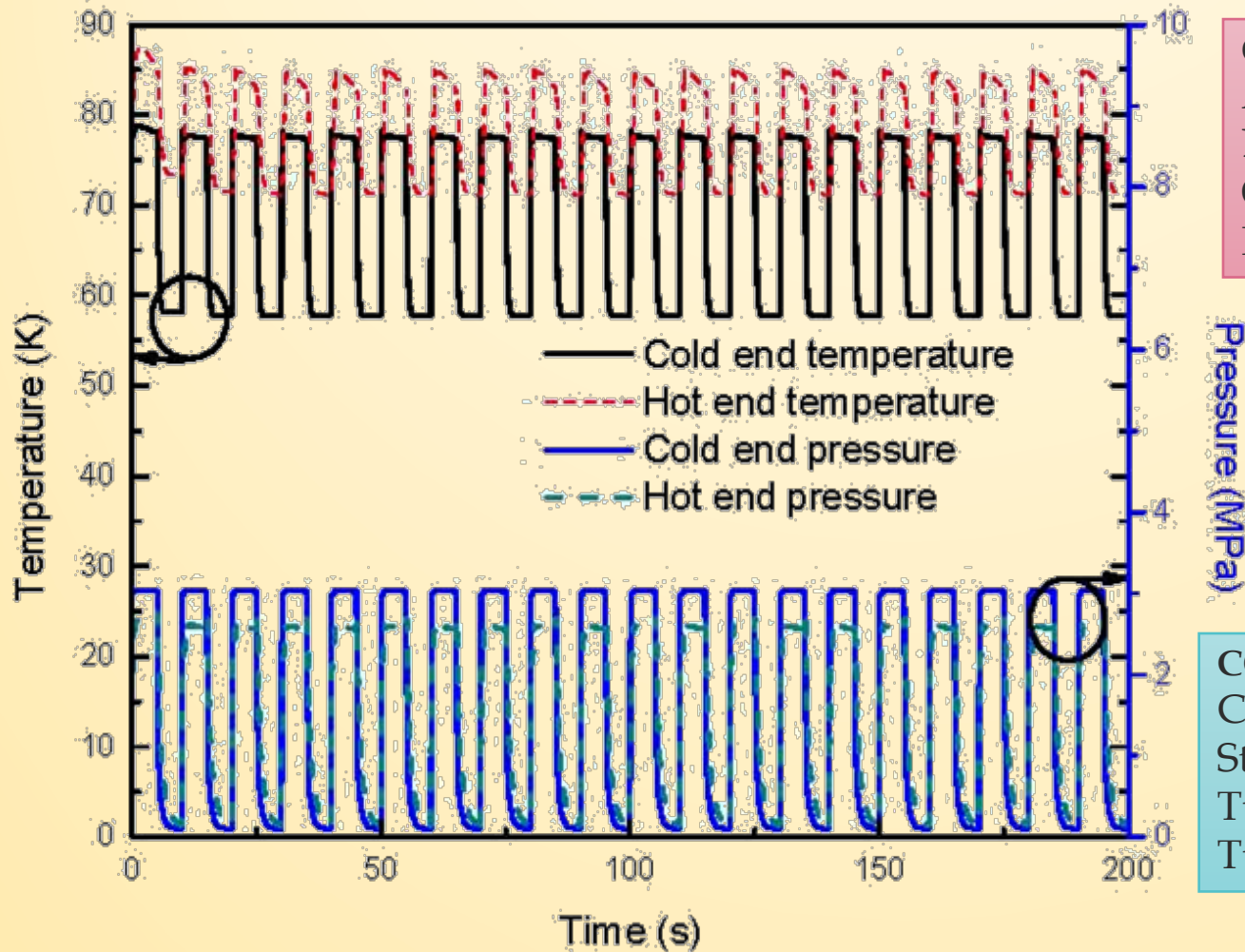
## Different activated carbon



- Benard P., Chahine R., 2001. Langmuir 17, 1950-1955.
- Zheng Q., Wang X., Gao S., 2014. Cryogenics 61, 143-148.
- Delahaye A., Aoufi A., Gicquel A. Pentchev I., 2002. Energy and environmental engineering 48, 2061-2073.

# Theoretical Results

## Time-temperature-pressure profile

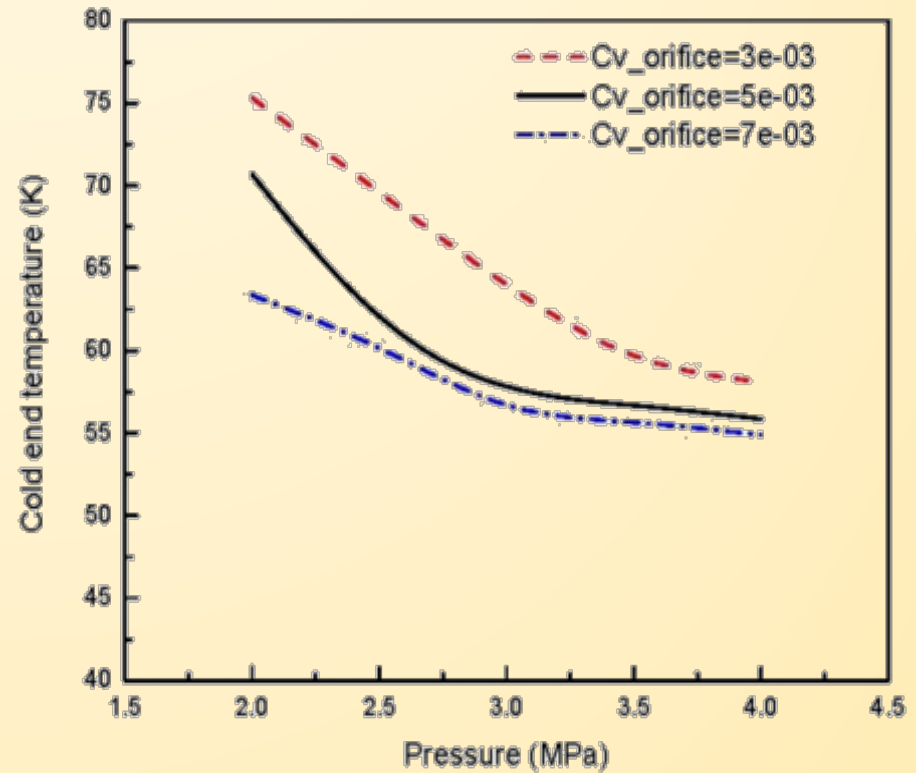
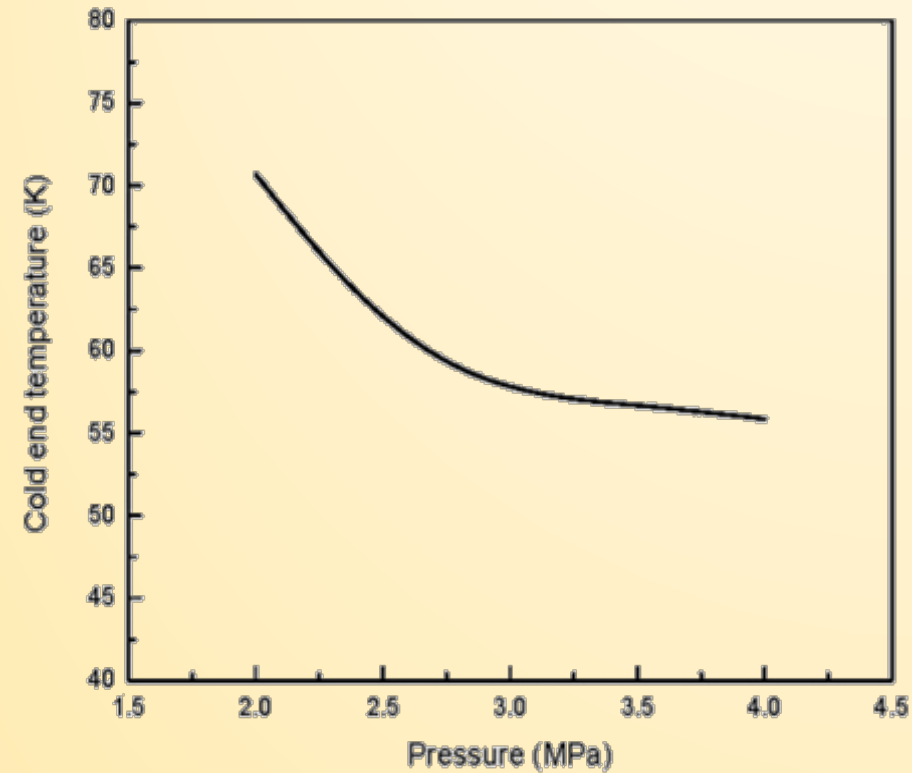


**OPERATING CONDITION**  
Adsorption time: 5s  
Desorption time: 5s  
Operating pressure: 3MPa  
Initial Temperature: 77K

**CONSTRUCTION PARAMETER**  
C034 Activated carbon  
Stainless steel tube  
Tube length: 250mm  
Tube diameter: 28mm

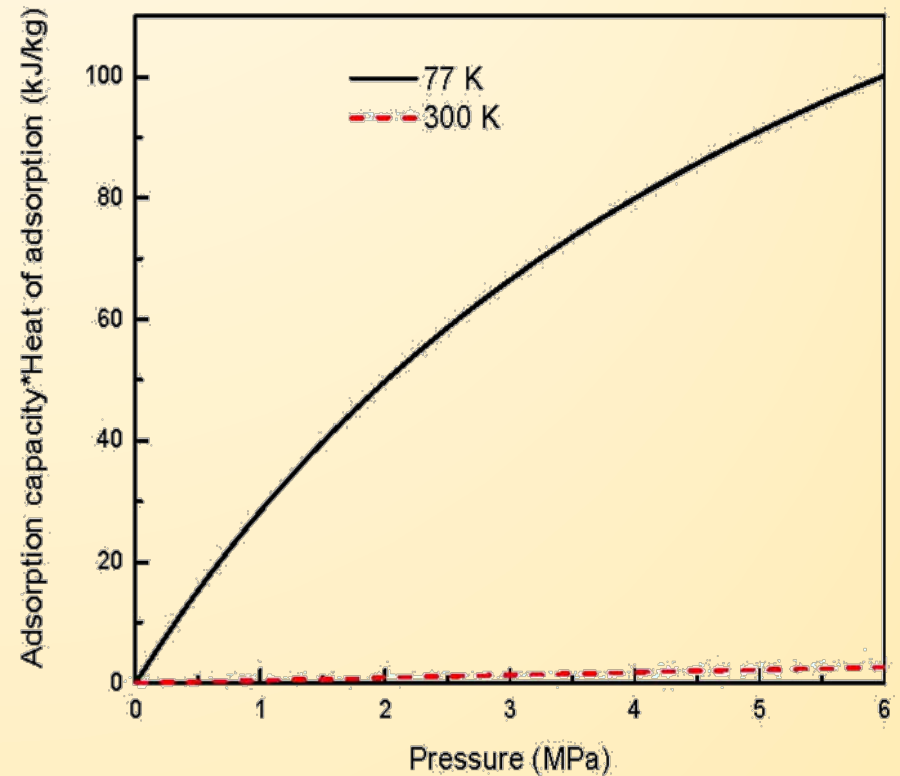
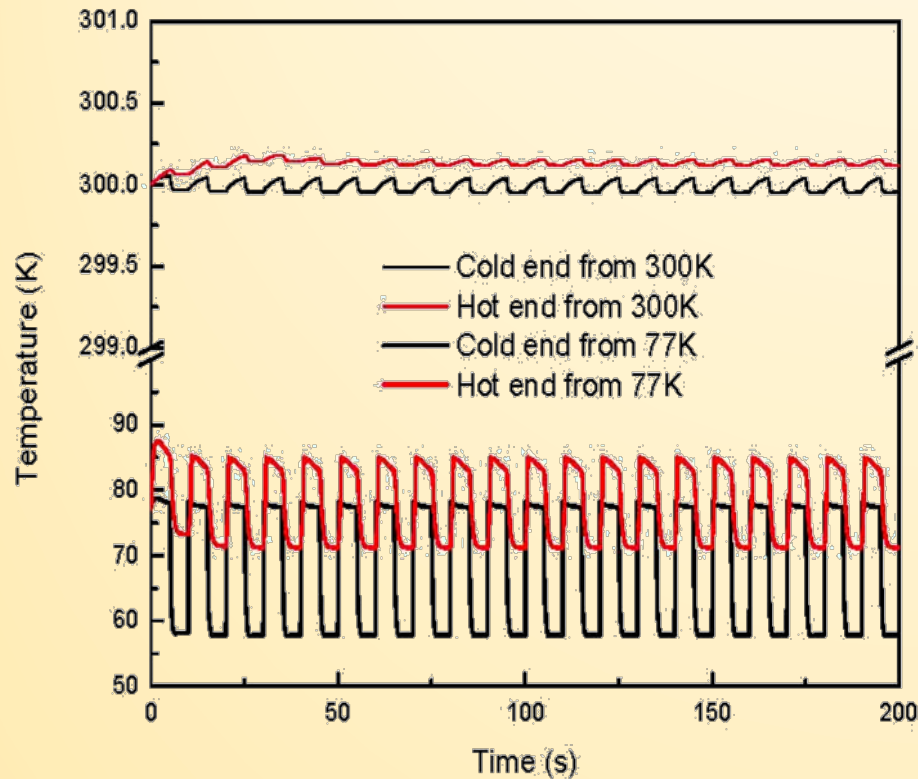
# Theoretical Results

## Different orifice opening



# Theoretical Results

## Effect of pre-cooling



$$\begin{aligned} & \left[ \varepsilon A_1 \rho C_p + (1 - \varepsilon) A_1 \rho_s C_{ps} + \varepsilon A_2 \rho_w C_{pw} - \varepsilon A_1 \bar{R} \rho \right] \left( \frac{\partial T}{\partial t} \right) - (1 - \varepsilon) A_1 \Delta H \rho_s \frac{\partial q(x, t)}{\partial t} \\ & = \frac{\partial}{\partial x} \left[ A_1 k_b \frac{\partial T}{\partial x} - \varepsilon A_1 \rho C_p u T \right] - h_{amb} (\pi D_0) (T - T_0) \end{aligned}$$

# Conclusions

- ❖ Generation of cooling at LN<sub>2</sub> temperature is possible using activated carbon and hydrogen as adsorbent/adsorbate pair
- ❖ Higher operating pressure and wider orifice opening are favorable for larger temperature drop
- ❖ Suitability of working pair for a given temperature and pressure zone of interest is decided by the product of equilibrium adsorption capacity and heat of adsorption

# THANK YOU

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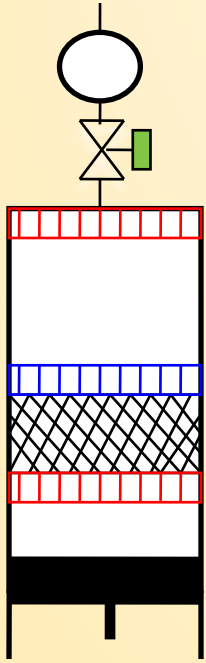
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# Comparison with Pulse-Tube Refrigerator



- Empty tube
- Heat of expansion causes cooling
- Frequency in Hertz order

- Filled with adsorbent
- Heat of desorption causes cooling
- Frequency in milli-Hertz order

