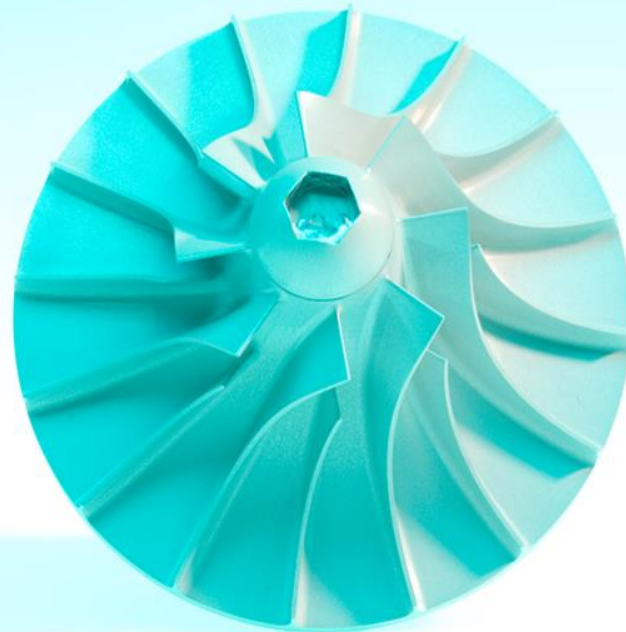


ICEC/ICMC

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University of Twente, Enschede, The Netherlands

## **Cold Compressor String.** for the Superfluid Cryogenic Plant at Fermilab's CMTF.



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# Cold Compressor Development

## From the past to the present



### PAST

- Custom-made machine design
- Long commissioning duration
- Control system design from scratch
- Long pump-down time
- First observation of performance during commissioning
- System observation only based on sensor values



### PRESENT

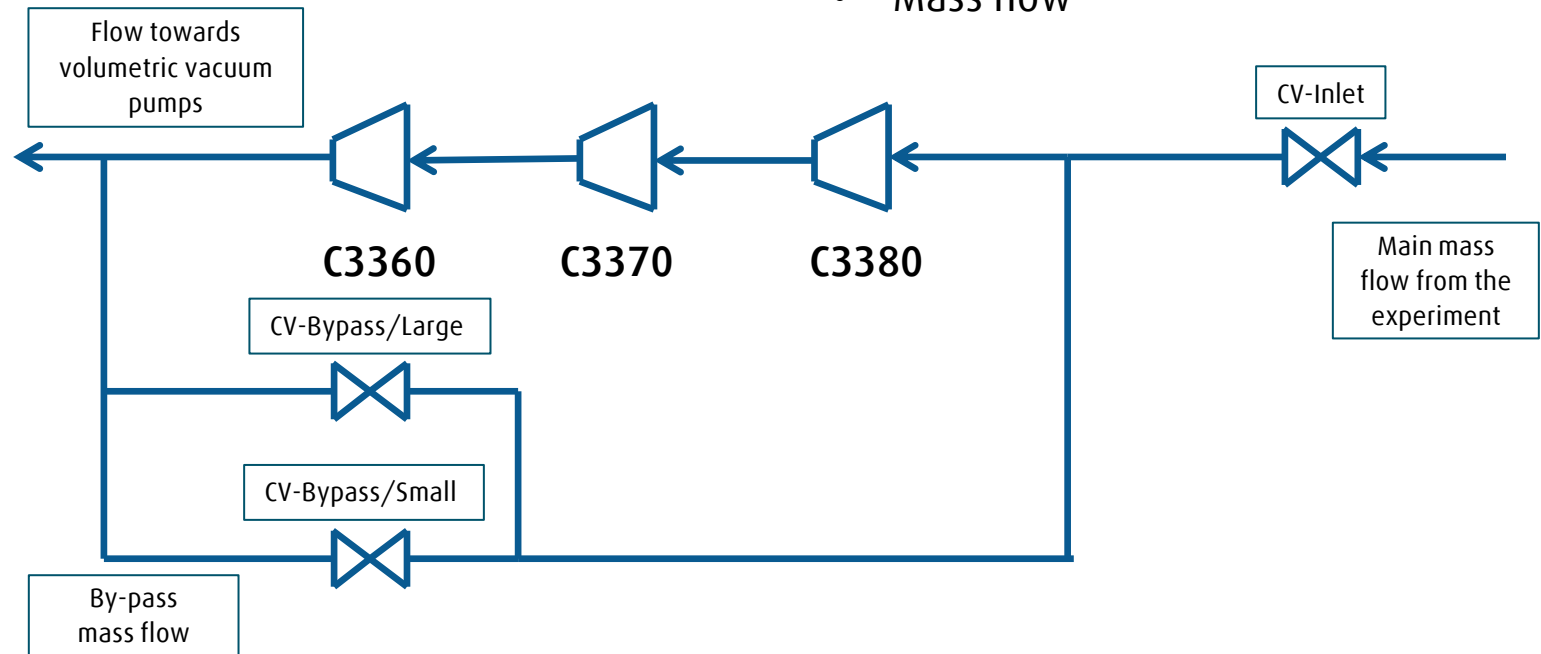
- Standard machinery, custom-made flow parts
- Very fast commissioning
- Standardized control system
- High pump-down speed
- Dynamic simulation of system model prior to commissioning
- Dynamic operating point visualization on compressor maps

# Compression Process Design Flow diagram



## Measured variables

- Rotational speed
- Temperature
- Pressure
- Mass flow



# Cold Compressor Design Specifications



## 2K Mode

500W

$M^* = 26.8 \text{ g/s}$

$P_{in} = 24 \text{ mbar}$

## 1.8K Mode

250W

$M^* = 14.0 \text{ g/s}$

$P_{in} = 13 \text{ mbar}$

$CC_1 \rightarrow N_{des} = 540 \text{ Hz} ; N_{max} = 767 \text{ Hz}$

$CC_2 \rightarrow N_{des} = 706 \text{ Hz} ; N_{max} = 917 \text{ Hz}$

$CC_3 \rightarrow N_{des} = 706 \text{ Hz} ; N_{max} = 917 \text{ Hz}$

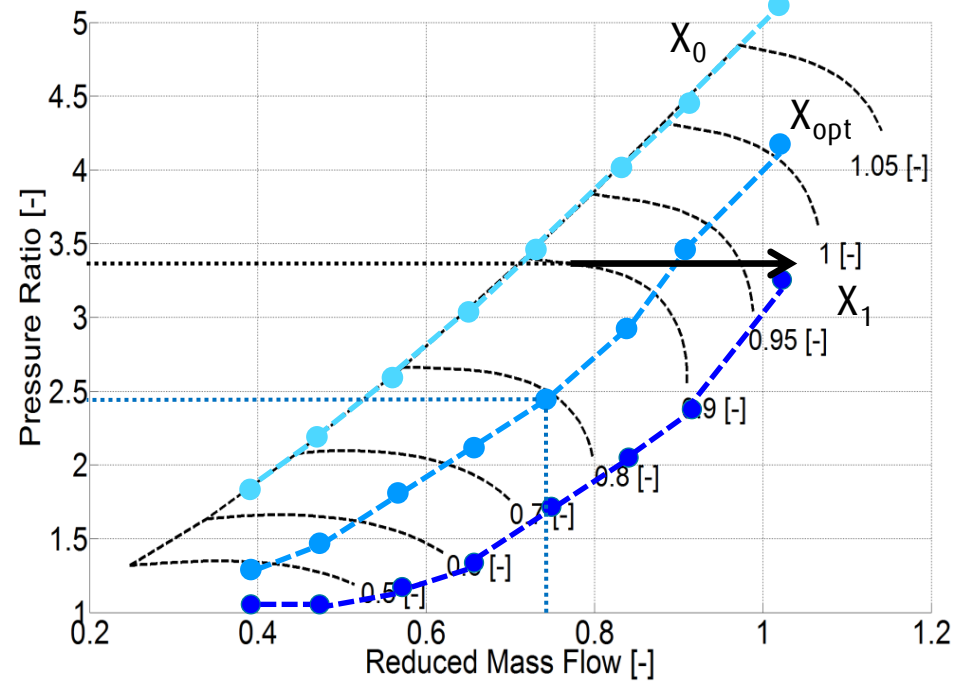


# Cold Compressor String Model

## Concept – Example Stage 1 (CC1)



- At each reduced flow different reduced speed lines
- Effect on the input conditions of the next stage
- Capacity (X) curves are created along the map
- Capacity (X) value is the control variable

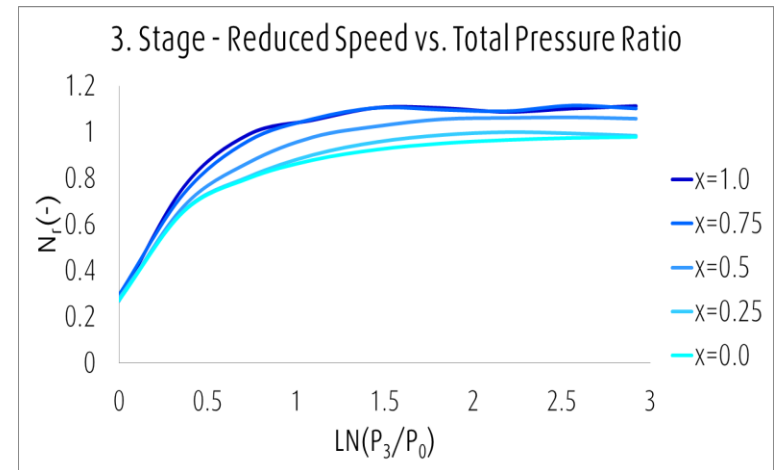
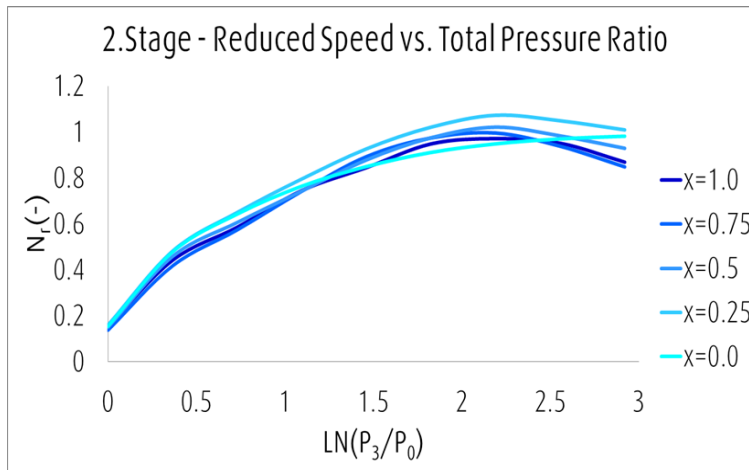
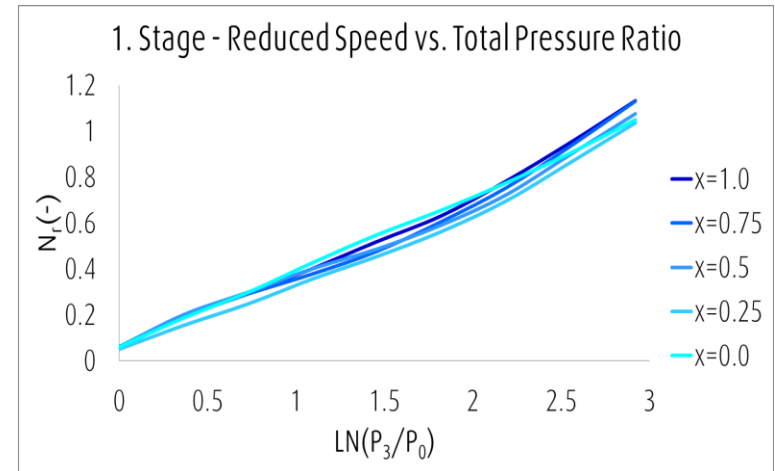


# Cold Compressor String Model

## Look-up graphs



- X is the output of the PI controller
- The same X for all compressors
- For saturated X at 0.9, the controller increases  $\text{LN}(P_3/P_0)$

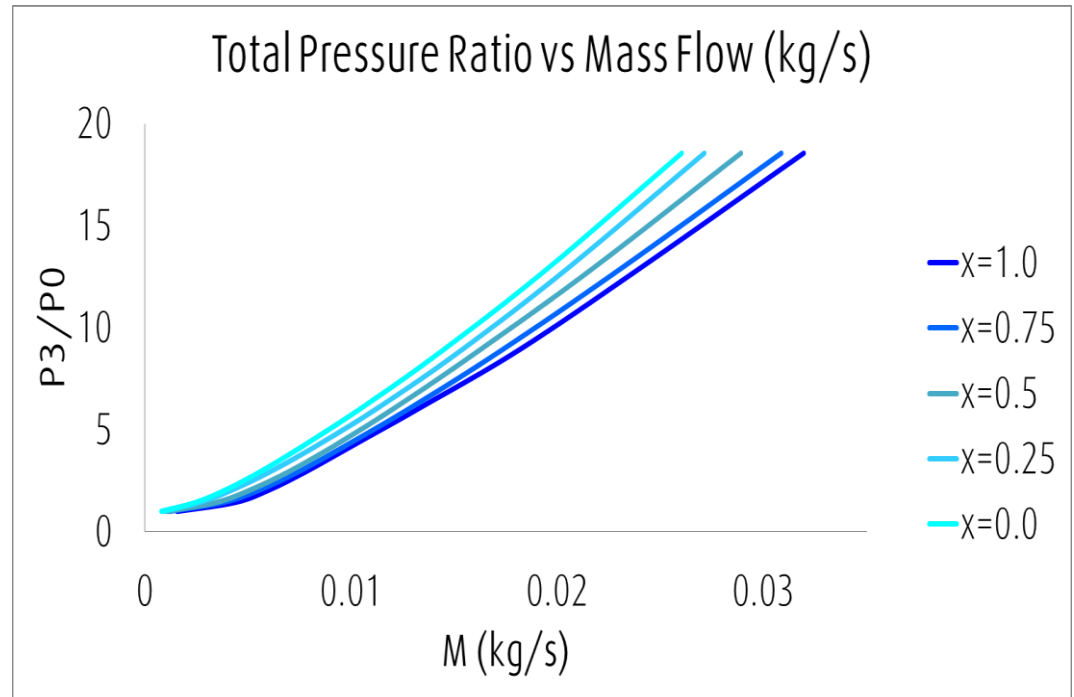


# Cold Compressor String Model

## Range of the real mass flow

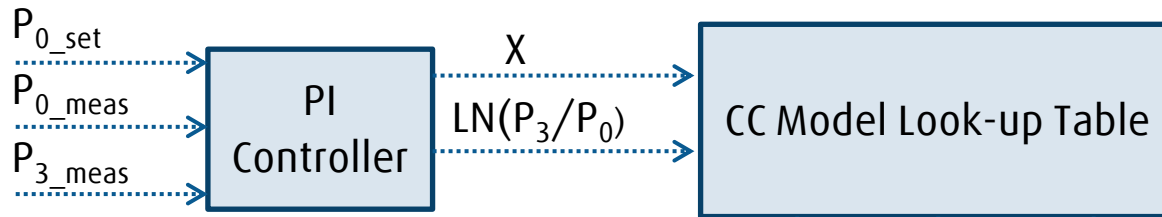


- At high  $P_3/P_0$  mass flow range becomes higher
- $X$  and  $P_3/P_0$  can be used to find mass flow set point

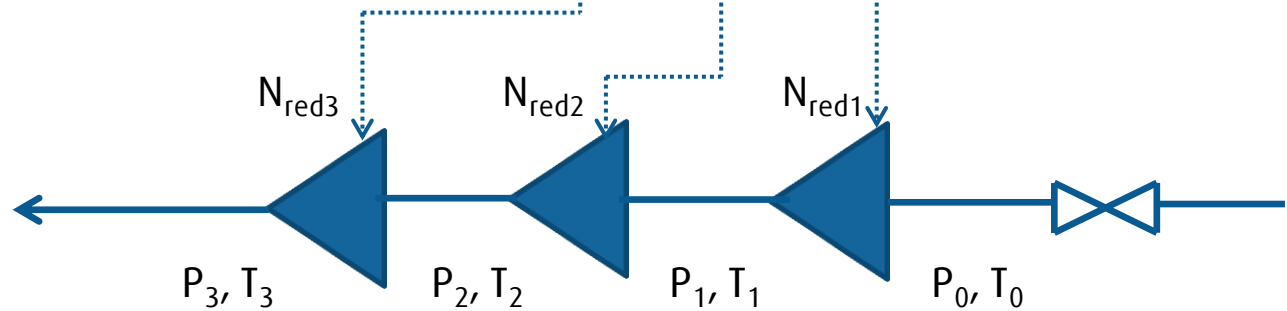




# Controller Design Overview

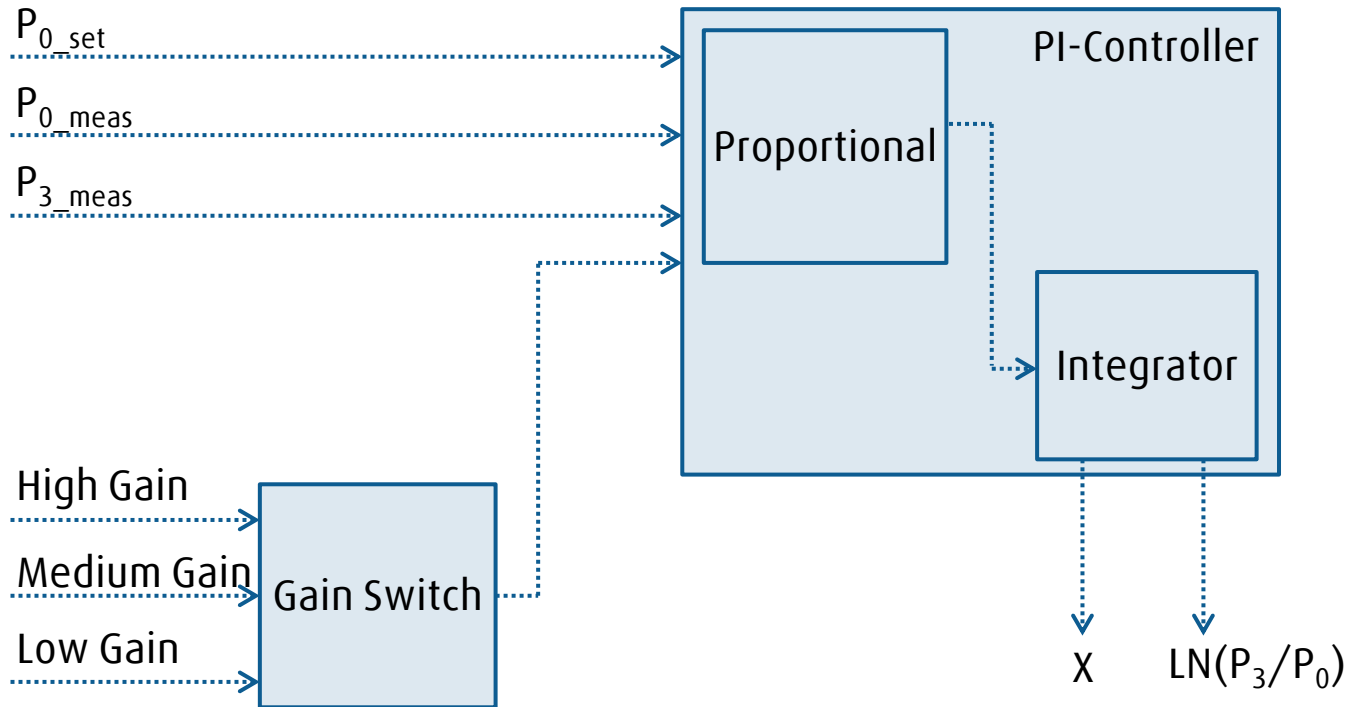


- $X$  and  $\ln(P_3/P_0)$  are inputs to the model
- $X_{max}$  is 0.9 to avoid choke
- $X_{min}$  is 0.05 to avoid surge



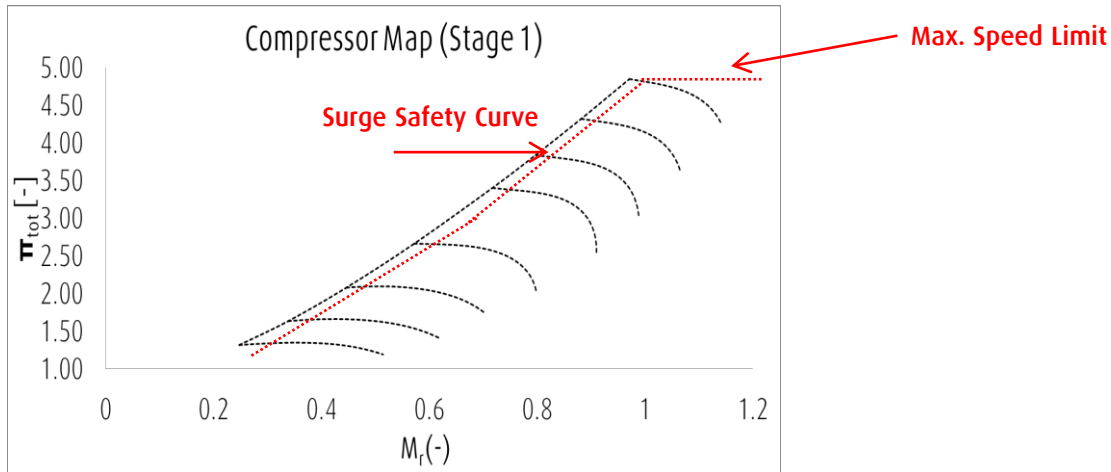
# Controller Design

## Control System Detail



- High gain is activated during pump-down to saturate  $X$  faster
- Saturated  $X$  increases the speed of pump-down

# Surge and High Speed Protection Safety Levels



**Before setting the speeds**

Safety Level 1 (Controller switch/option)

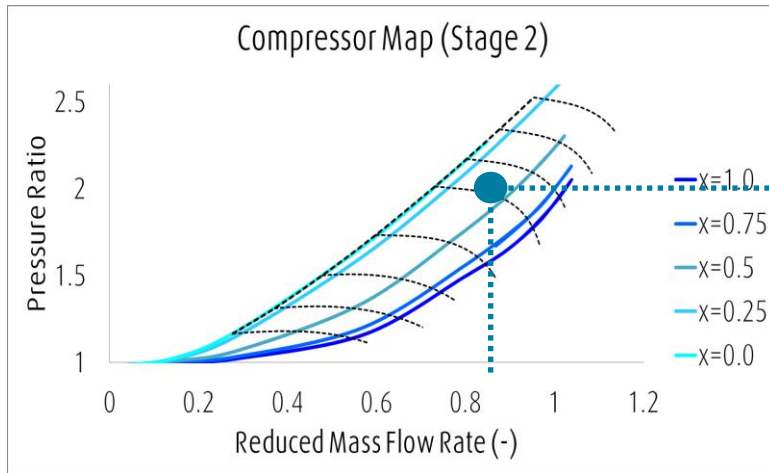
Safety Level 2 ( X limit)

Safety Level 3 ( Set speed limit)

**Speed measurement and surge  
counter**

Safety Level 4 ( Smooth operation)

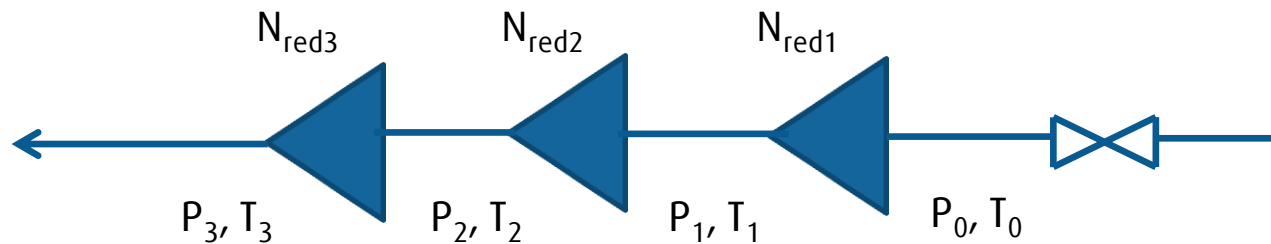
# Correction of Measured Data



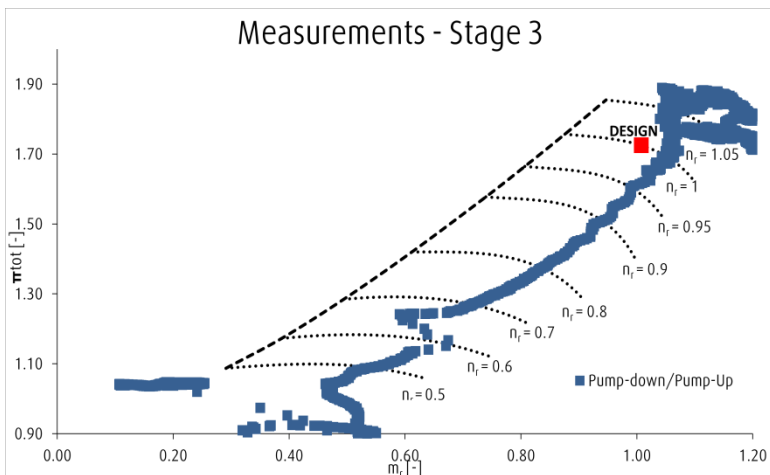
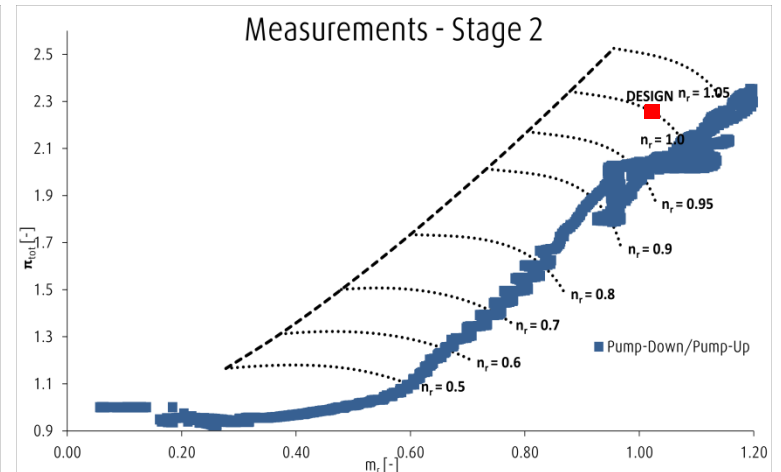
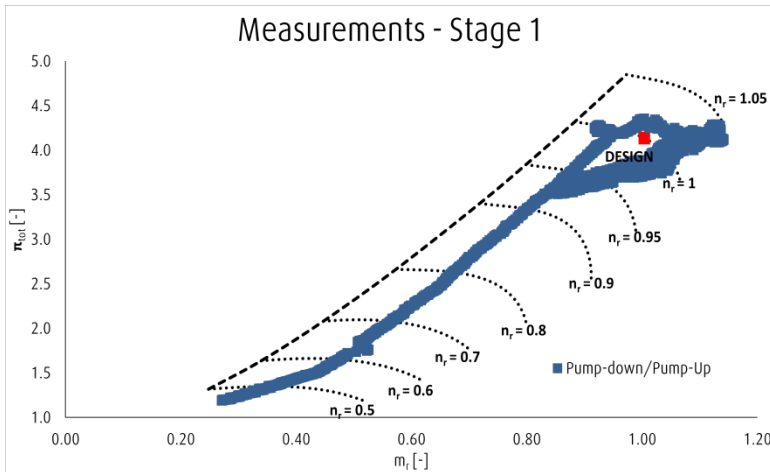
## Model Output

- Expected Pressure Ratio
- Expected Efficiency
- Expected Temperature Ratio

- Compensation of measurement errors



# Real System Performance Transient and steady state



- Pump-down to 24 mbar
- Pump-up to 30 mbar

# Summary



- **Modularized approach which can be easily adapted to systems with different number of compressors (e.g. for the cryoplant of DESY's XFEL Project with 4 compressors)**
- **Extremely quick and uncomplicated commissioning within a few days only**
- **Reliable and robust operation**
- **Pump-down, steady-state, pump-up for 2K and 1.8K covered by the same control logic**
- Different levels of surge and over-speed protection
- Model-based control algorithms derived using Euler turbo-machinery equations
- Single PI controller with adjustable gains for fast pump-down performance
- One control variable for all compressors
- Integrated mass flow and inlet temperature control

**Thank you for your attention.**

