



Model Predictive Control applied to the LHC magnets temperature control

Advanced Control Engineering
EN/ICE Automation Seminars
CERN, 2nd, 3rd June 2014

Contents

- Introduction
 - 1.8 K Cooling Loop Process
 - Challenges
- Advanced control
 - Model-Based Predictive Control
 - Performance
- Present & Future

LHC Accelerator

World Largest accelerator

27km length
100m underground

Over 1600
Superconducting
magnets

Cryogenics
Coldest place in
Universe:

-271° C
(1.9 K)

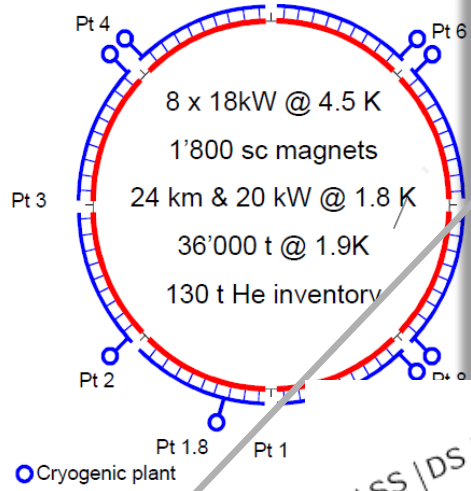


LHC Cryogenics

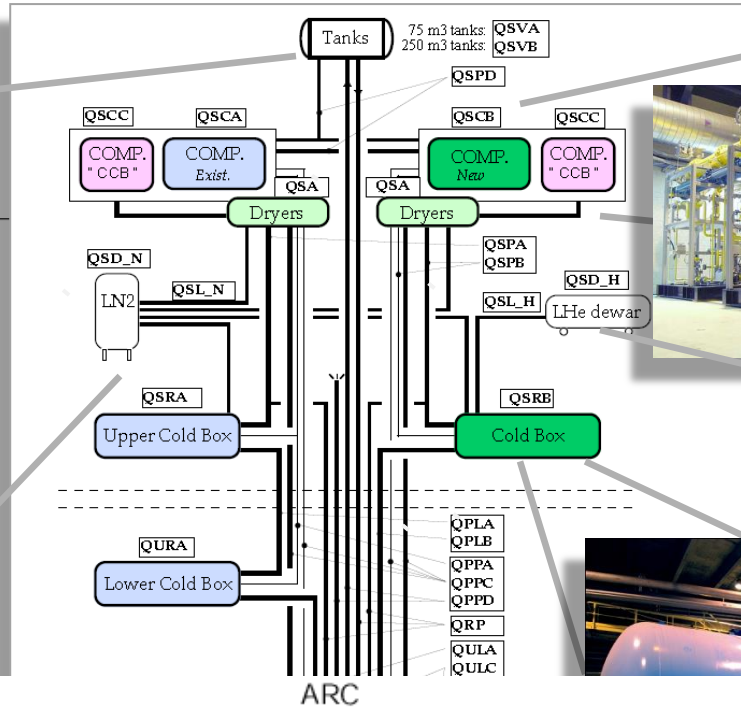
helium storage



Pt 5



LHC sector: 3.3 km

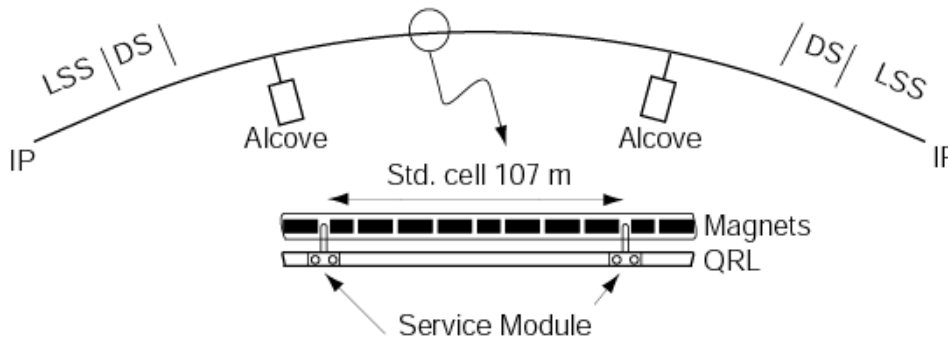


compressor stations



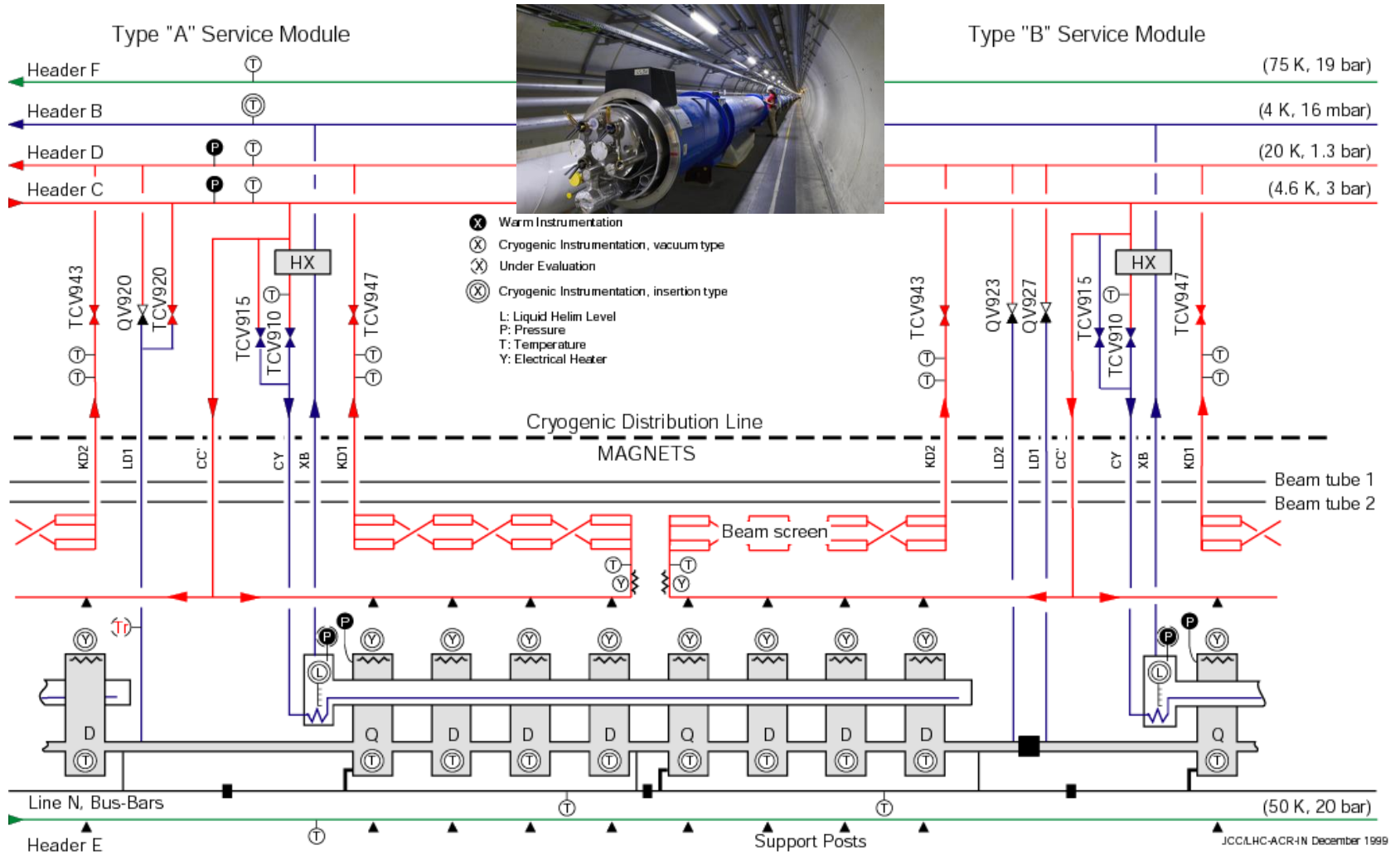
cold boxes

liquid helium storage



LHC Standard cell

LHC cryo standard cell PI&D (~100 meters)

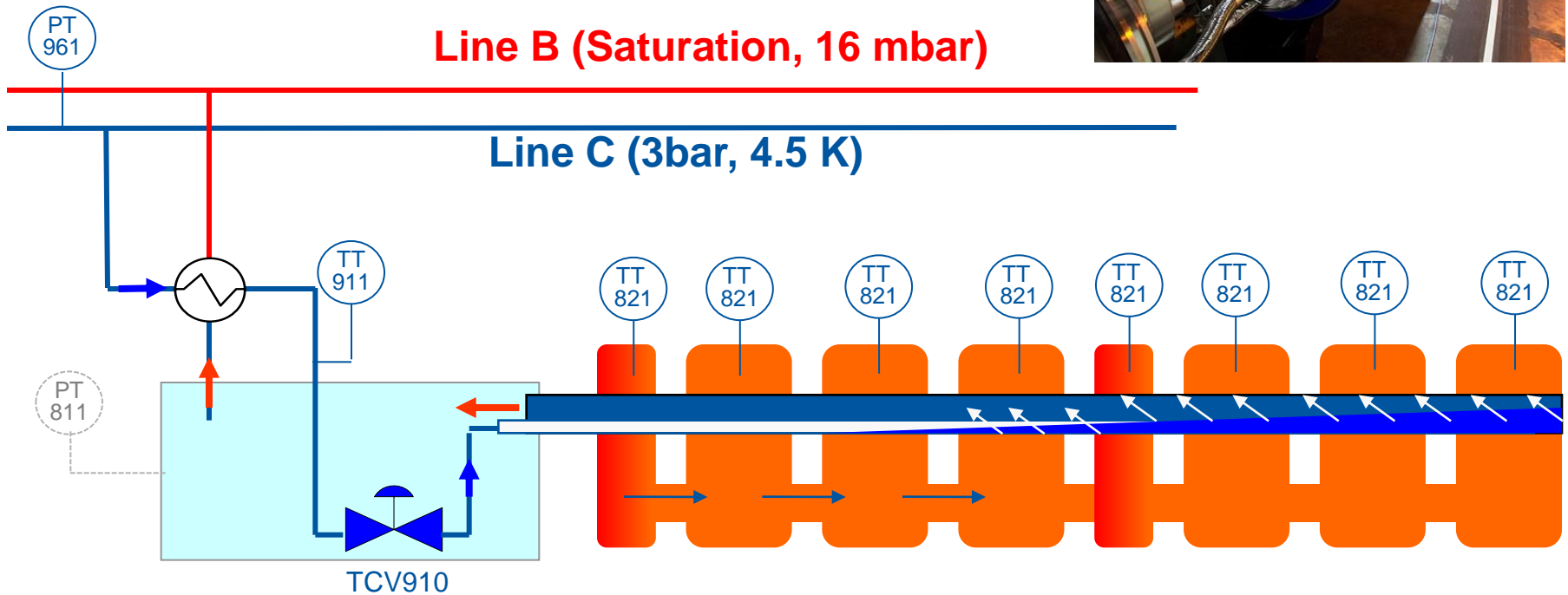


1.8 K Cooling Loop



Line B (Saturation, 16 mbar)

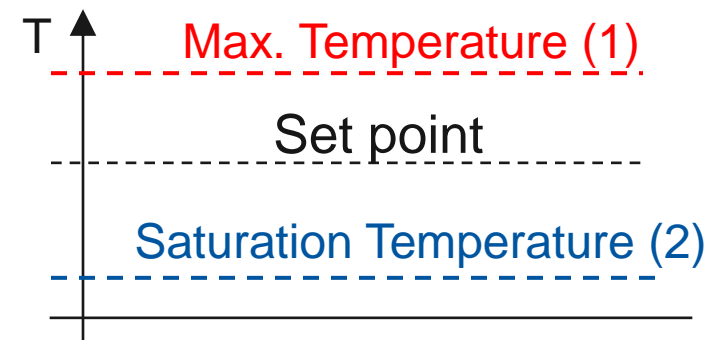
Line C (3bar, 4.5 K)



LHC cryogenics standard cell (~100 meters)

Objectives

- Keep the temperature of the superconducting magnets as constant as possible within strict operating constraints imposed by:
 - Allowed maximum temperature (1) for the magnets (**1.9 K = -271 °C**)
 - Cooling capacity of the cryogenic system (2)
 - Disturbances: Dynamic heat loads
 - Instrumentation accuracy



Challenges

Highly non-linear process

- Non-minimum phase system: Inverse response
- Variable dead time
- Non-self regulating process

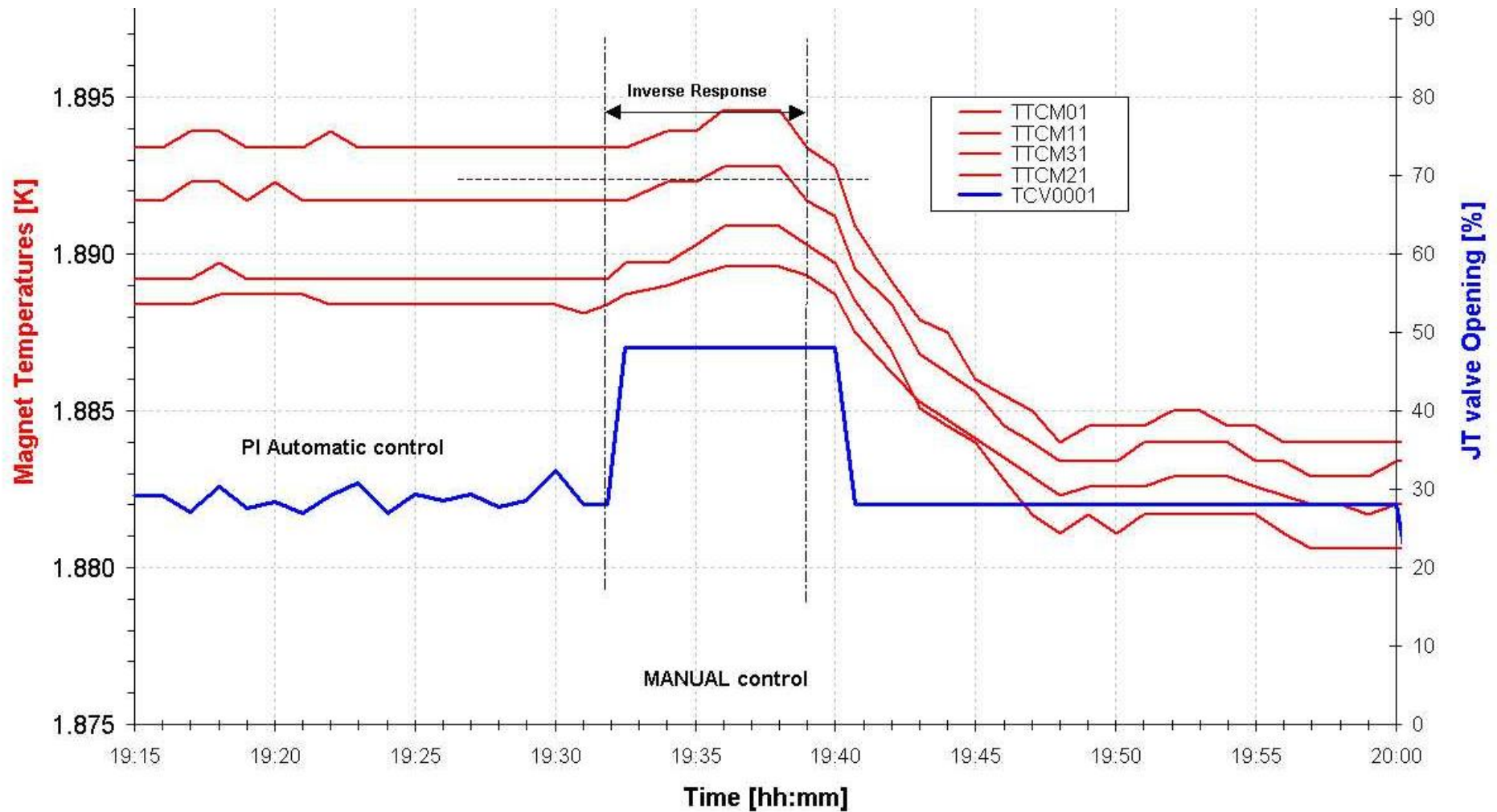
Wide operational conditions

- Heat loads, Temperature, Pressure

Problematic tuning

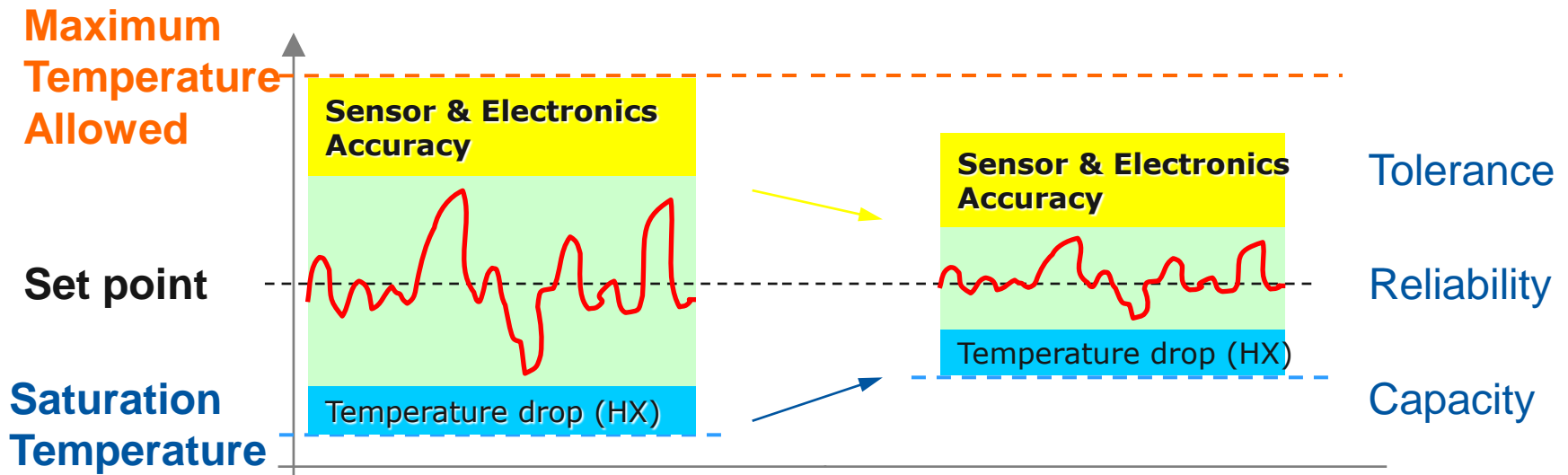
- LHC architecture: multiple controllers

Challenges



Advanced regulation motivation

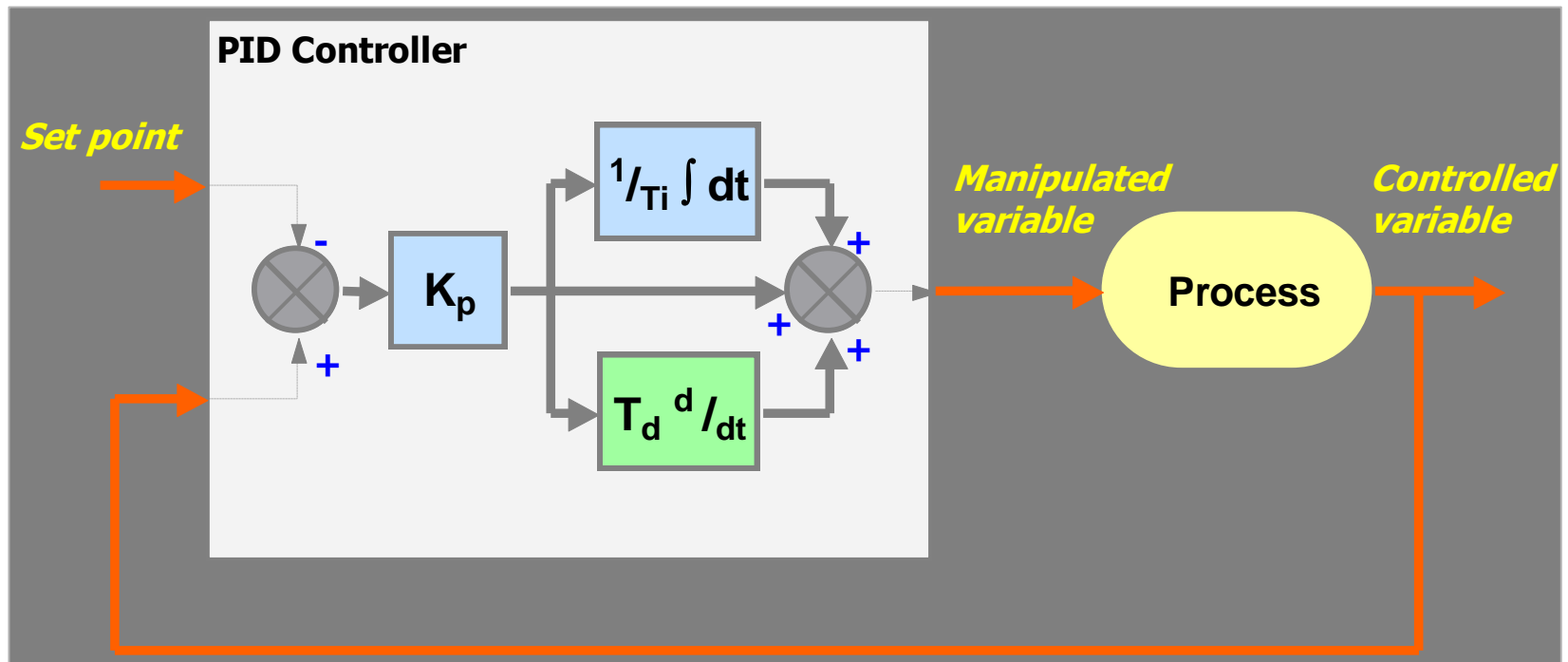
- Reducing temperature variability, squeezing the control band and place it optimally.



Contents

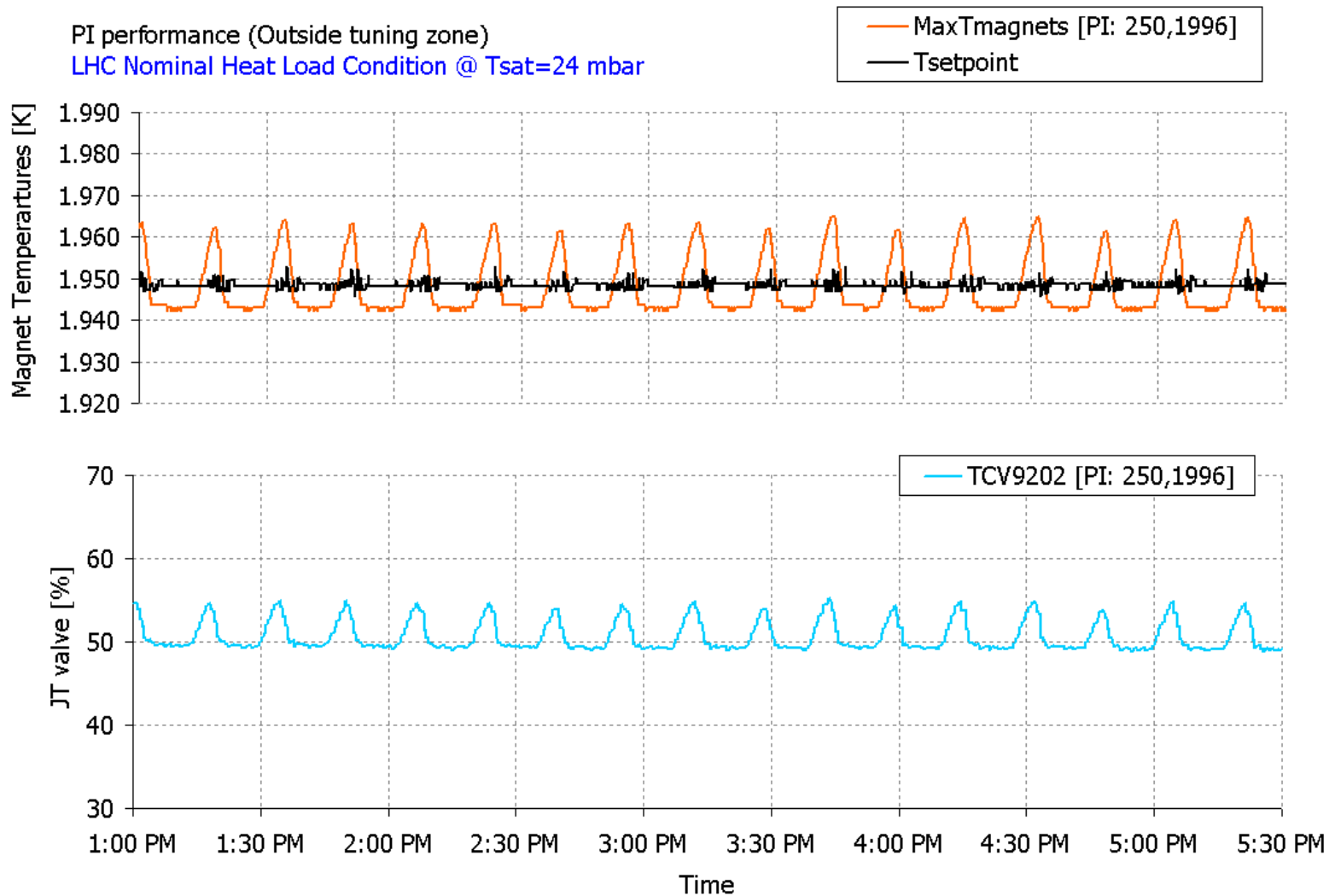
- Introduction
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 - Challenges
- **Advanced control**
 - Model based Predictive Control
 - Performance
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Basic Control



PID performance

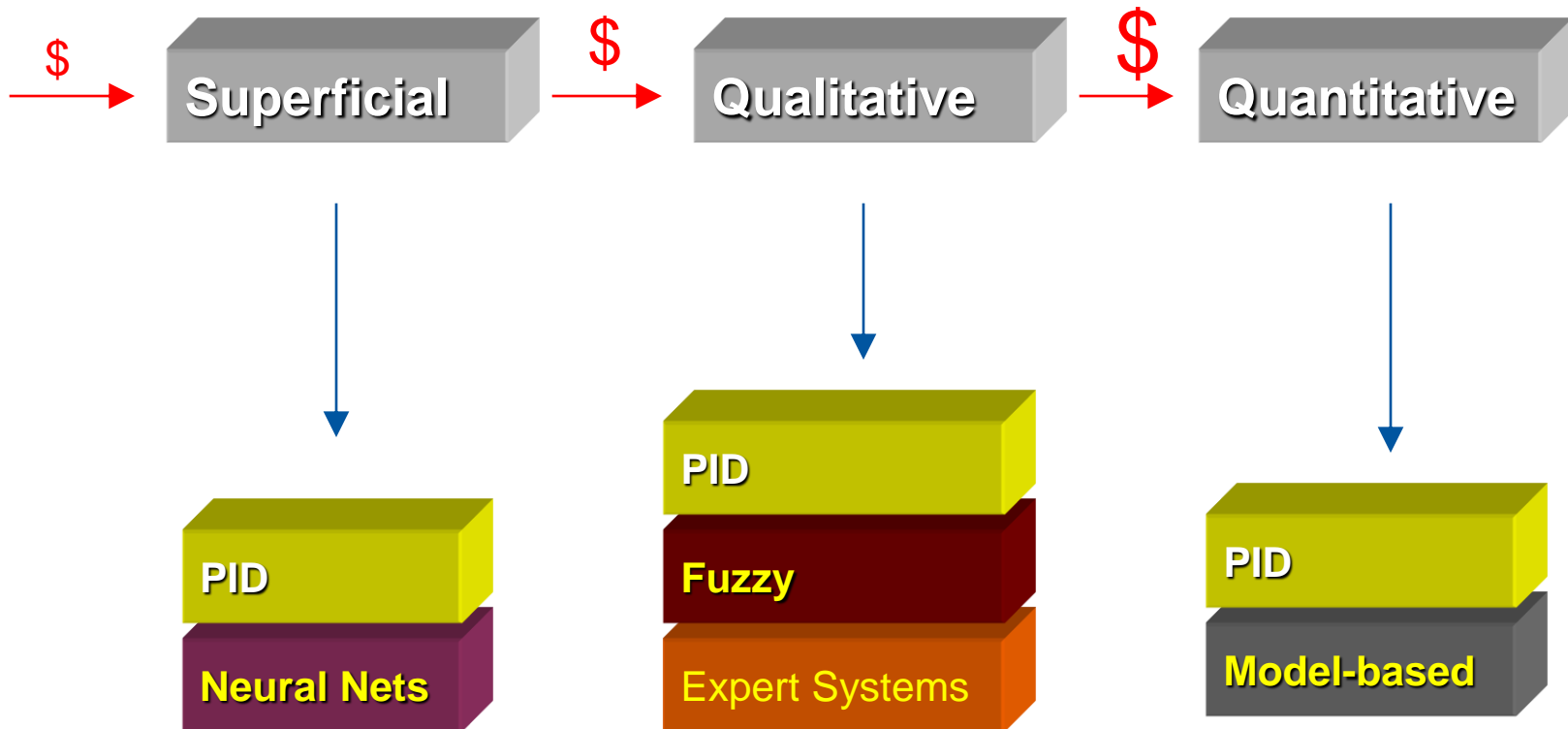
PI performance (Outside tuning zone)
LHC Nominal Heat Load Condition @ Tsat=24 mbar



Advanced Control

- What is the right choice?

Available process knowledge

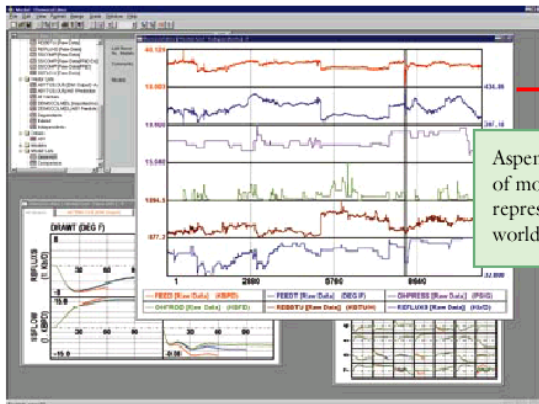


From Control Engineering

Model-Based Predictive Control

An Industrial solution

DMCplus™



The new GUI-based system makes DMCplus easy to use

AspenTech's installed base of model predictive control represents over 50% of the world's applications.

New Generation Controller

Honeywell

HONEYWELL INTRODUCES ENHANCED TECHNOLOGY FOR COMPLEX PROCESS CONTROL

PHOENIX, AUGUST 16 -- Honeywell today introduced an enhanced technology for controlling and optimizing highly interactive industrial processes that can increase product throughput, improve product quality, and reduce property give-away.

Robust Multivariable Predictive Control Technology (RMPCT) is the result of an evolution of two previous leading multivariable control technologies: Honeywell's Robust Multivariable Predictive Control (RMPC) and Honeywell Profimatic's Predictive Control Technology (PCT).

Predictive Adaptive Control Aids Pulp Digestion

New software provides closed-loop control at Skeena Cellulose; \$0.60/ton cost reduction cooks up into \$100,000 savings per year for each digester.

Predictive software embedded in processors

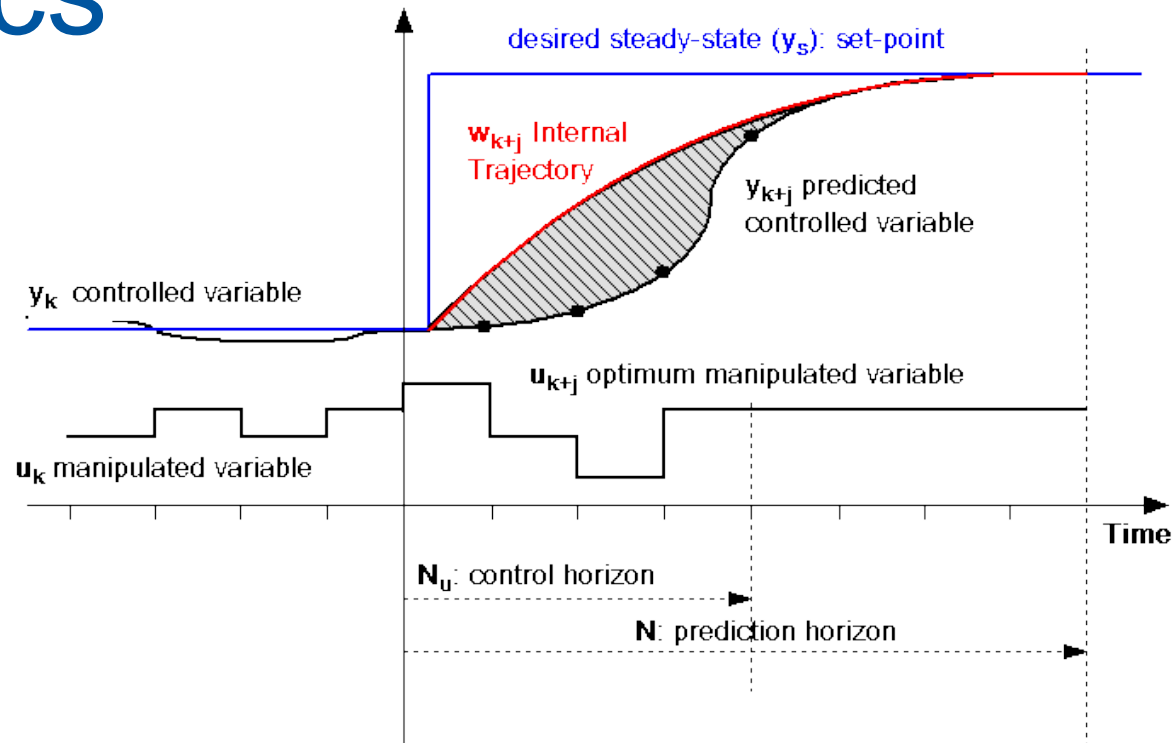
Foxboro, Mass.—Embedded Connoisseur places Multivariable Predictive Control (MPC) software in fault-tolerant I/A Series Control Processors to build and deliver robust, responsive MPC solutions to fast acting processes such as combustion and surge control. I/A Series embedded Connoisseur supports developing mathematical process models, establishment of constraint limits, and automatic control of the process to maximize economic, quality, and production objectives. *Foxboro* www.foxboro.com



15

MBPC basics

- Process Model
- Internal trajectory
- Optimization



$$I = \sum_{j=0}^N [w(t+j) - \hat{y}(t+j)]^2 + \beta \sum_{j=0}^{N_u} [\Delta u(t+j)]^2$$

$$\Delta u_L \leq \Delta u \leq \Delta u_H$$

$$u_L \leq u \leq u_H$$

$$y_L \leq y \leq y_H$$

- Constraints Management

MBPC: Modeling

Various techniques depending mainly on objectives, plant availability and knowledge

- Linear vs. Non-linear models
- Approaches:
 - Empirical approach: System Identification
 - NARMAX, Neural nets, fuzzy sets, Hammerstein models, Volterra...
 - First principles modelling



1.8 K Cooling Process Model

$$m_{cm} \cdot \frac{d}{dt} (Cp(T_{mag}) \cdot T_{mag}) = Q_{ss} - q_{cool}$$

$$q_{cool} = H \cdot A_w \cdot (T_{mag} - T_{sat})$$

$$\frac{dm_{hx}}{dt} = f_{in} - f_{out} - f_{vap}$$

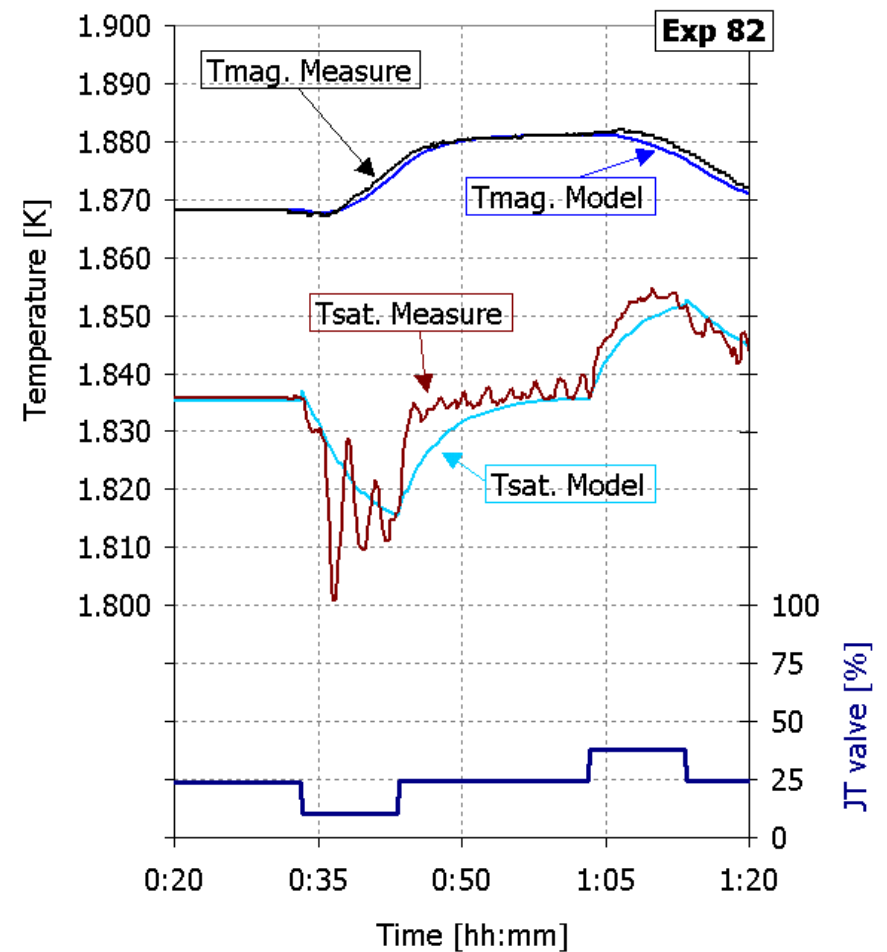
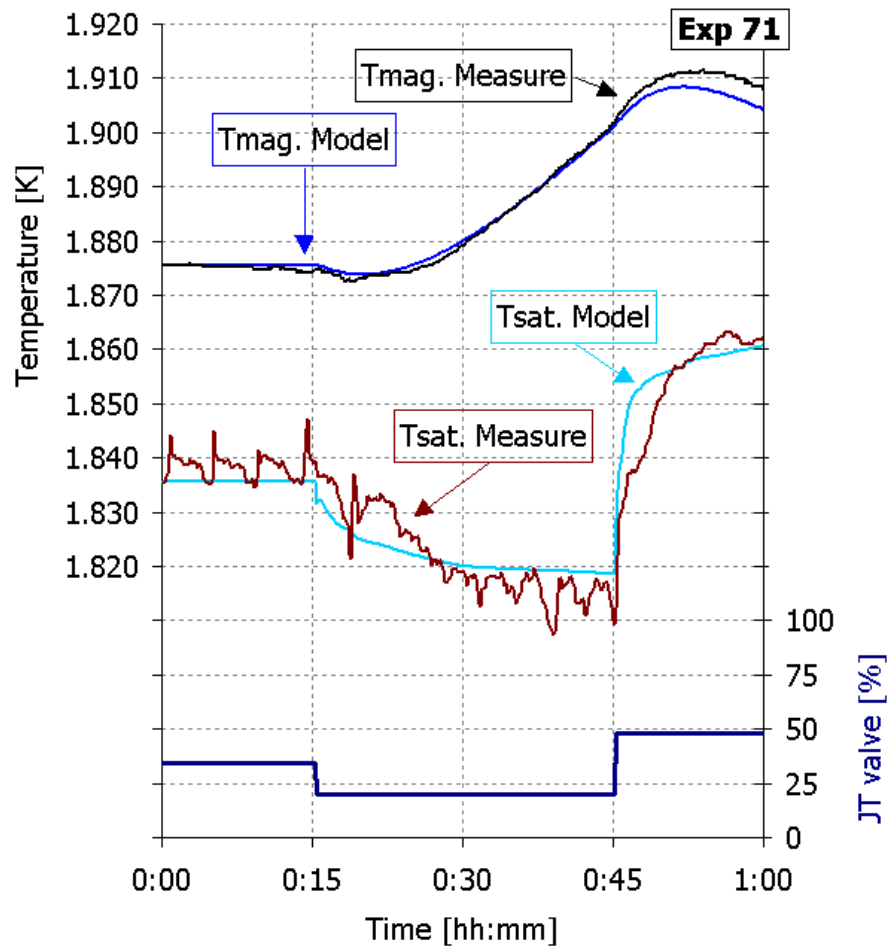
$$\Delta p = f \frac{\rho \mu_m^2}{2D} \int_{x_1}^{x_2} dx$$

- Controlled Variable
 - × Magnet Temperature
- Manipulated variable
 - × JT valve
- **UNMEASURED variables**
 - × He II mass accumulation
 - × Dynamic heat load

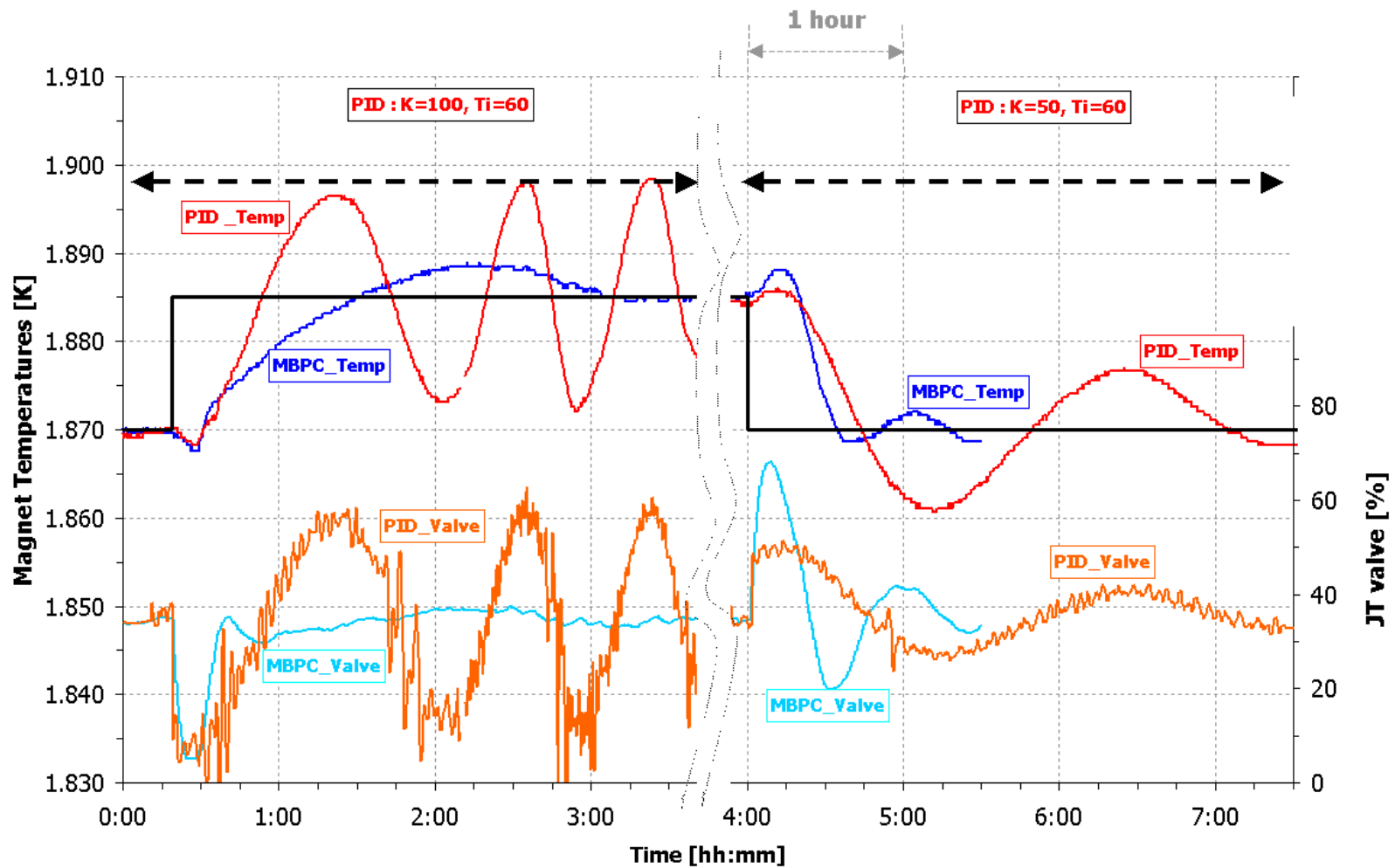
LHC prototypes



Model performance



First results: GPC vs PID

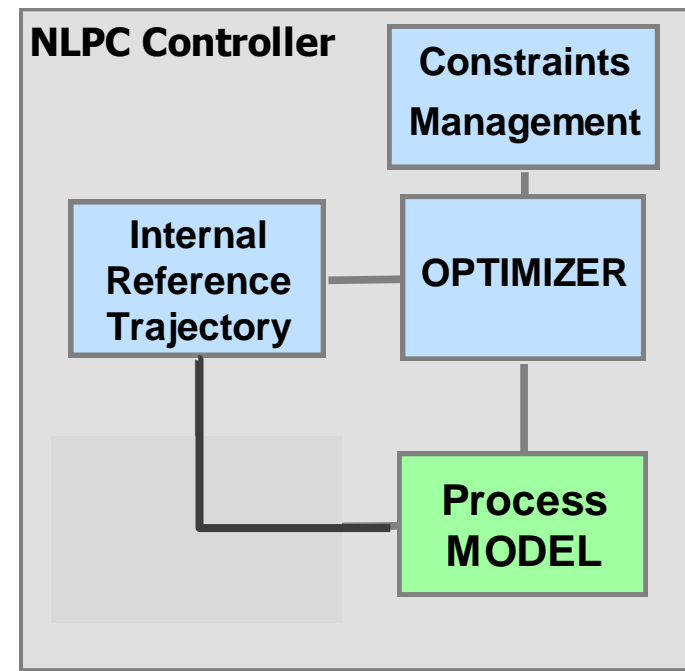


GPC: Generalized Predictive Controller

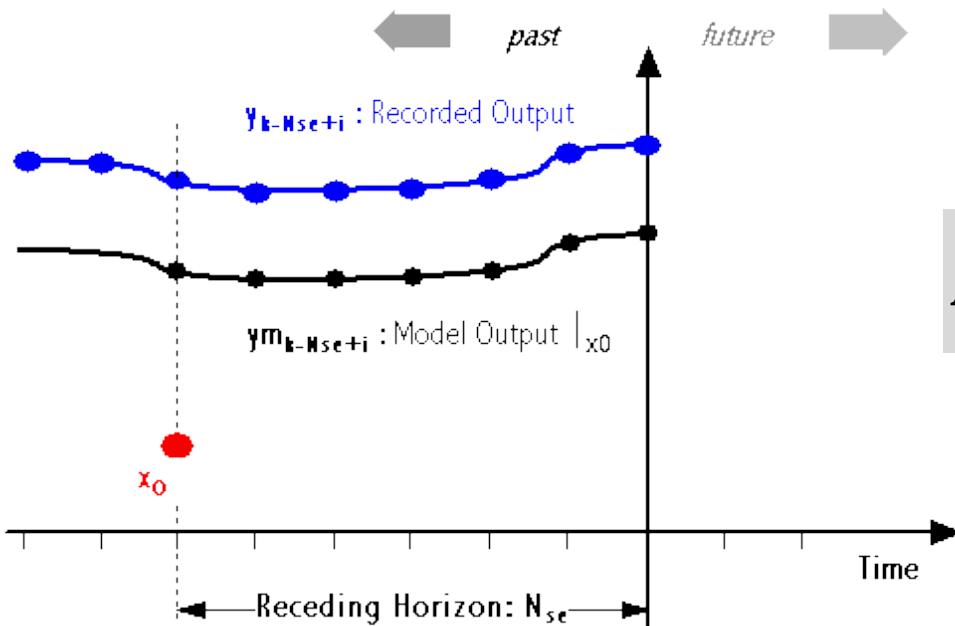
Regulation methodology

Nonlinear Model-Based Predictive Control (NLPC)

- **Process Model**
 - DAE solution: DASSL Newton-Raphson (EcosimPro simulation toolbox)
- **Nonlinear Optimization (under constraints)**
 - Commercial Numerical routines (NAG)
 - SQP: Sequential Quadratic Programming
- **State Estimator**
 - Un-measurable variables
 - Receding Horizon Estimation (RHE)



State Estimation (RHE)



$$x_{k+1} = f(x_k, u_k, v_k, w_k)$$

$$y_k = g(x_k) + \zeta_k$$

$$\text{Min}_{X_0} J = \gamma_1 \sum_{j=0}^{N_{se}-1} [y_{k-N_{se}+j} - y_{m_{k-N_{se}+j}}]^2 + \gamma_2 \sum_{j=0}^{N_{se}-1} [p_{k-N_{se}+j}]^2$$

$$\text{Min}_{X_0} J = \gamma_0 [A]^2 + \gamma_1 \sum_{j=0}^{N_{se}-1} [B]^2 + \gamma_2 \sum_{j=0}^{N_{se}-1} [C]^2$$

$$A = x_0 - mHX_{k-N_{se}}^{rec}$$

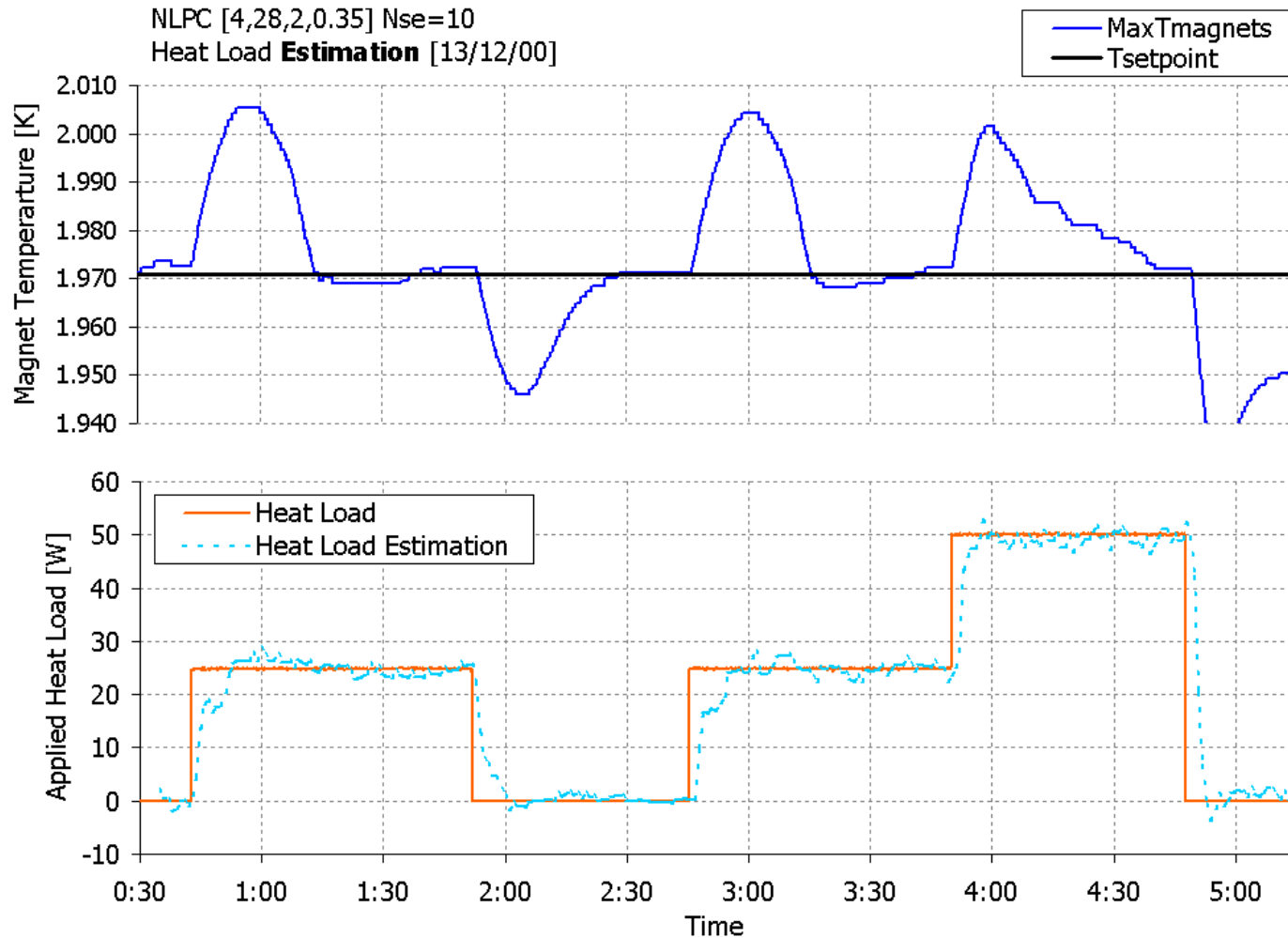
$$B = \frac{mHX_{i+1}^{rec} - mHX_i^{cal}}{1 + [vopen_{i+1}^{rec} - vopen_i^{rec}]}$$

$$C = Qtr_i^{cal} - Qtr_i^{rec}$$

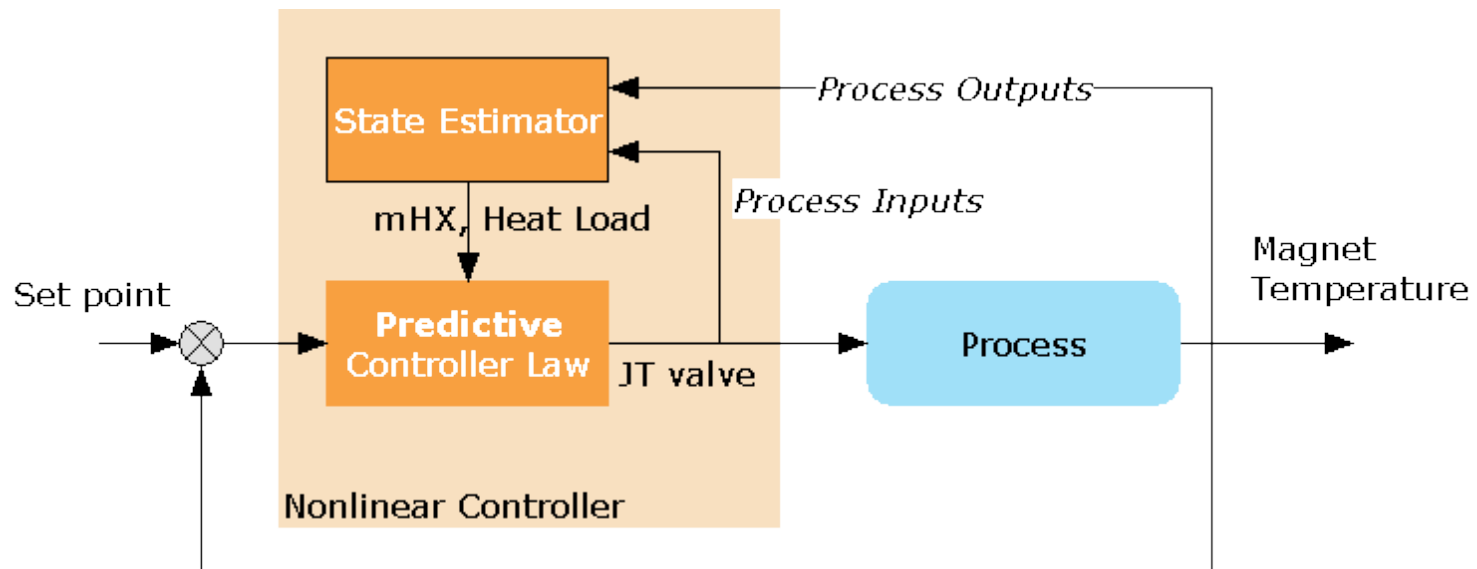
Non measurable states:

- Helium mas in the HX exchanger
- Heat load

State Estimation: Performance

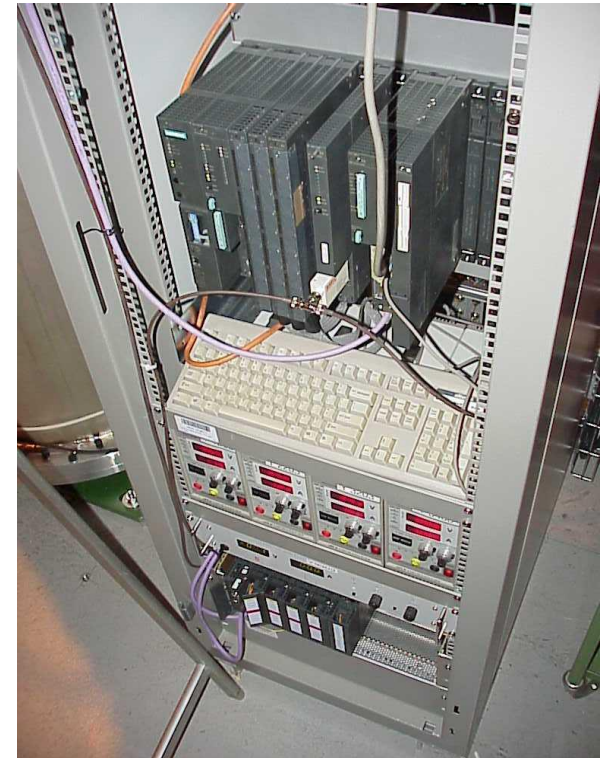
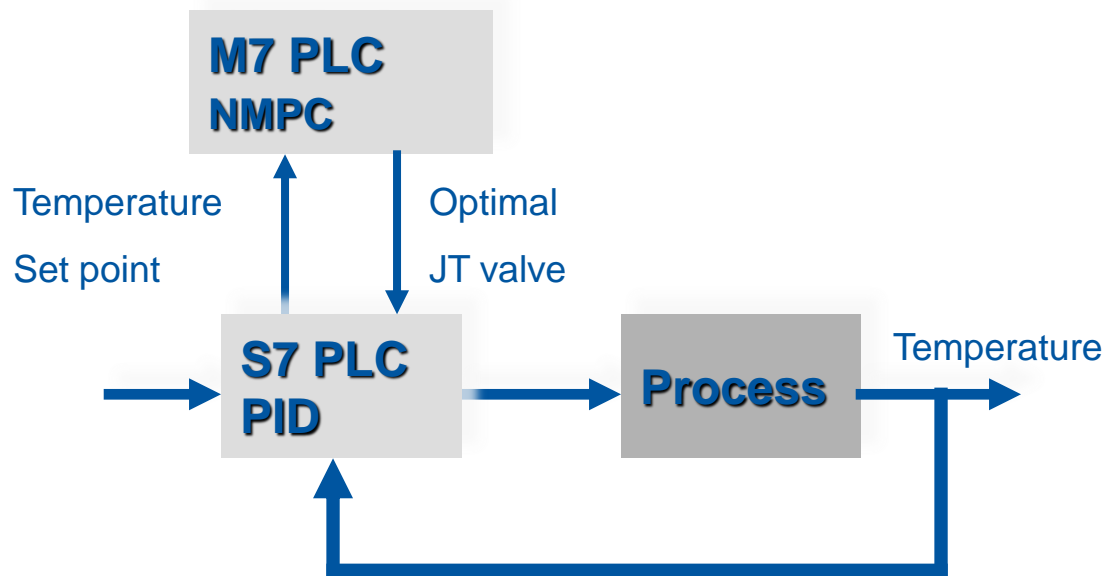


Regulator architecture

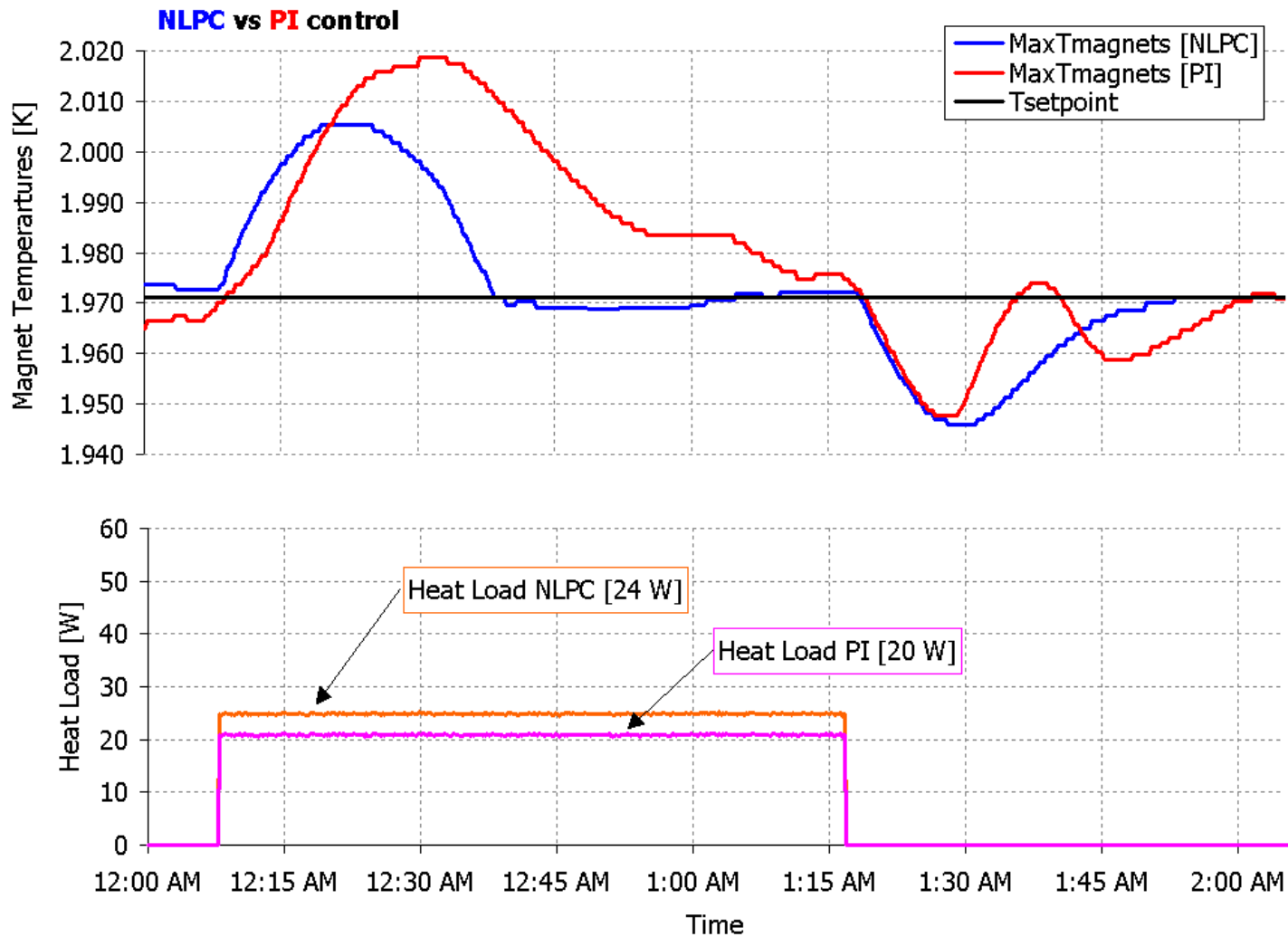


Controller deployment

- IPC M7: running a real time operating system
- PLC S7: “backup” PID control

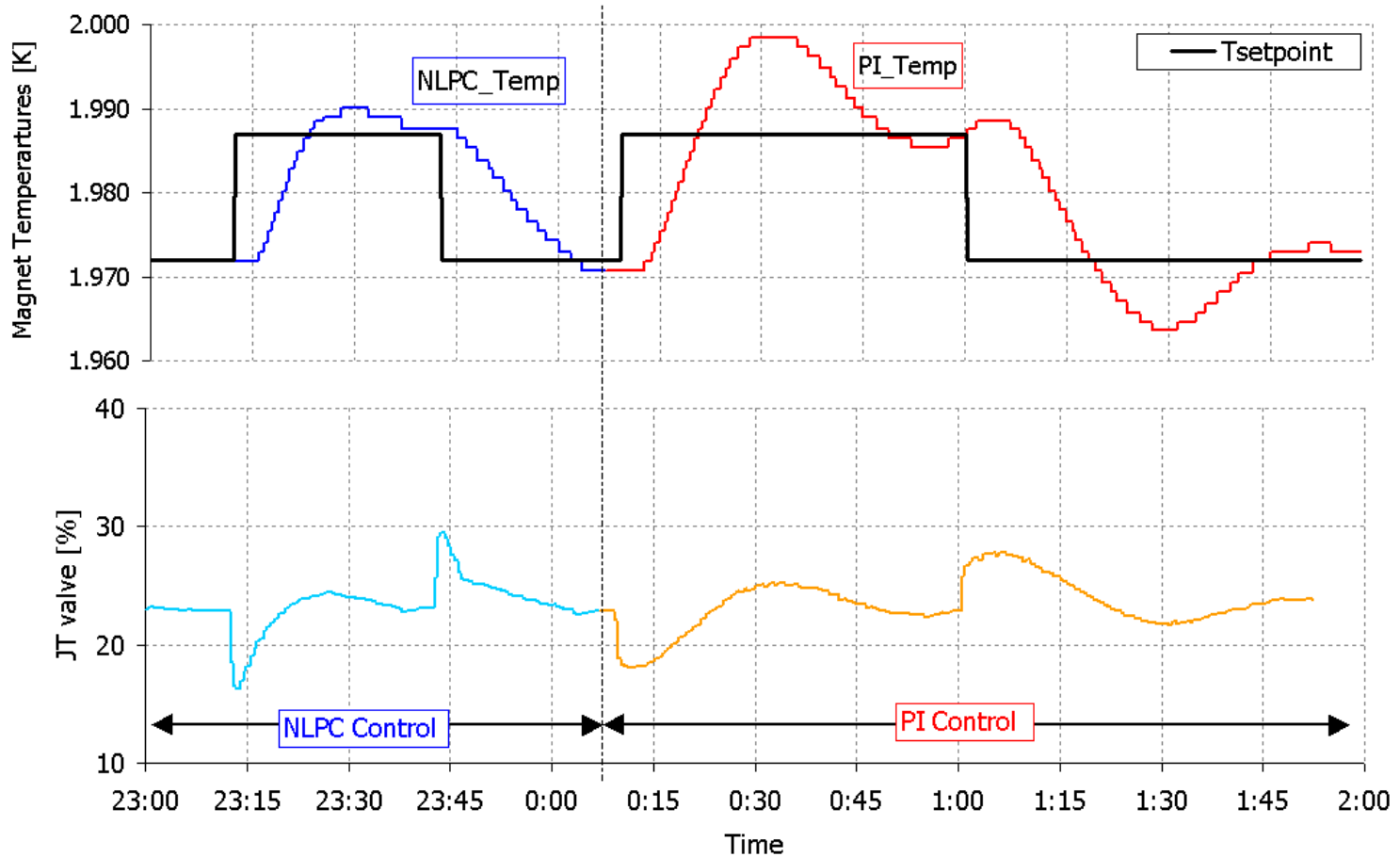


NLPC vs. PID: heat load change



NLPC vs. PID: set point change

NLPC + PI performance
IT-HXTU Nominal Heat Load + Setpoint Change



Contents

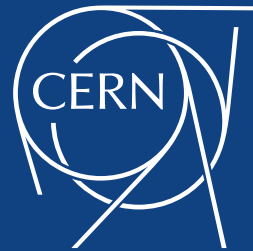
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Present & Future

- Refining models and algorithms
 - Enriching the model performance
 - Previous tests were performed mainly in the Inner Triplet & String prototypes.
 - LHC adjacent cells thermally coupled
- Multi-objective MBPC
 - Full LHC sector vs. single cell
- Implementation feasibility
 - How to smoothly integrate the nonlinear model and optimization algorithms in the control system

Thanks for your time





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