

HVAC OVERVIEW and VALUE ENGINEERING ITEMS

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CLIC Working Group CES

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RDR - Air treatment Design Basis

- **Tunnel Ventilation** – Conditioned dehumidified air from surface mounted equipment is ducted into the service tunnel at each shaft. A volume of 15000cfm (425meter³/min) flows at approximately 88fpm (1.6km/hr) to the midpoint between shafts where it is routed into the beam tunnel and returned to the shaft area. Fresh air at a rate of 20% (air change/16hr) is mixed into the air then conditioned and it is recirculated back to the service tunnel. Air volumes for the DR and BDS are similar.
- **Hazardous Conditions** - The air direction is reversible and capable of being doubled (unconditioned) during hazardous situations.
- **Design temperature ML** - The design temperature for the ML service and beam tunnels is 80-90F (27-32C). ML electronics' heat rejection is mainly to CHW direct cooling and FCUs with small amounts of heat to the ventilation air. AHU and FCUs are used at alcoves and shaft areas.
- **Design temperature DR** - The design temperature for the DR tunnel is 104F (40C), using process water fan coil units, and the tunnel wall as a heat rejection source.

RDR - Air treatment Design Basis

- **Design temperature BDS** - The design temperature for the BDS is 85-90F (29-32C). The low “heat to air” load is mainly absorbed by the tunnel wall. Air mixing fans will be used for temperature stability as required by the BDS.
- Used the basis that airflow could pass from the service tunnel to the beam tunnel through fire/smoke/ODH/radiation protected passages between the tunnels. This assumes that radiation/oxygen deficiency hazards (ODH) do not exist or can be mitigated between the tunnels from the standpoint of air mixing. This item needs concurrence from rad/ODH groups.
- AHU and FCU sizes in the alcoves and tunnels did not consider heat absorption by the rock wall. These units use chilled water from the surface as the heat rejection source.

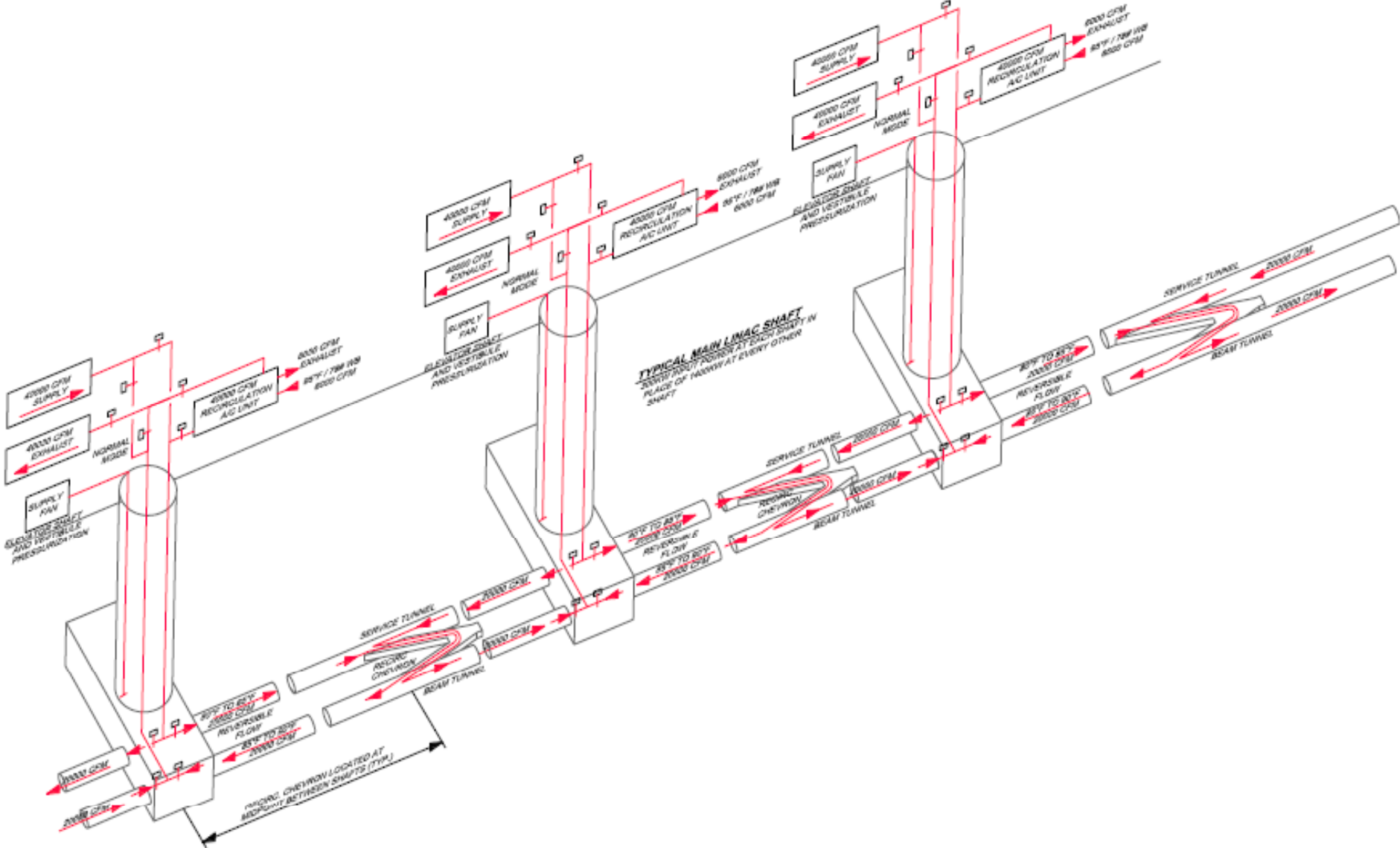
Air Treatment WBS

- Air Treatment Cost is about 1% of CFS
 (or 5.5% when CHW system is moved to the air treatment WBS)

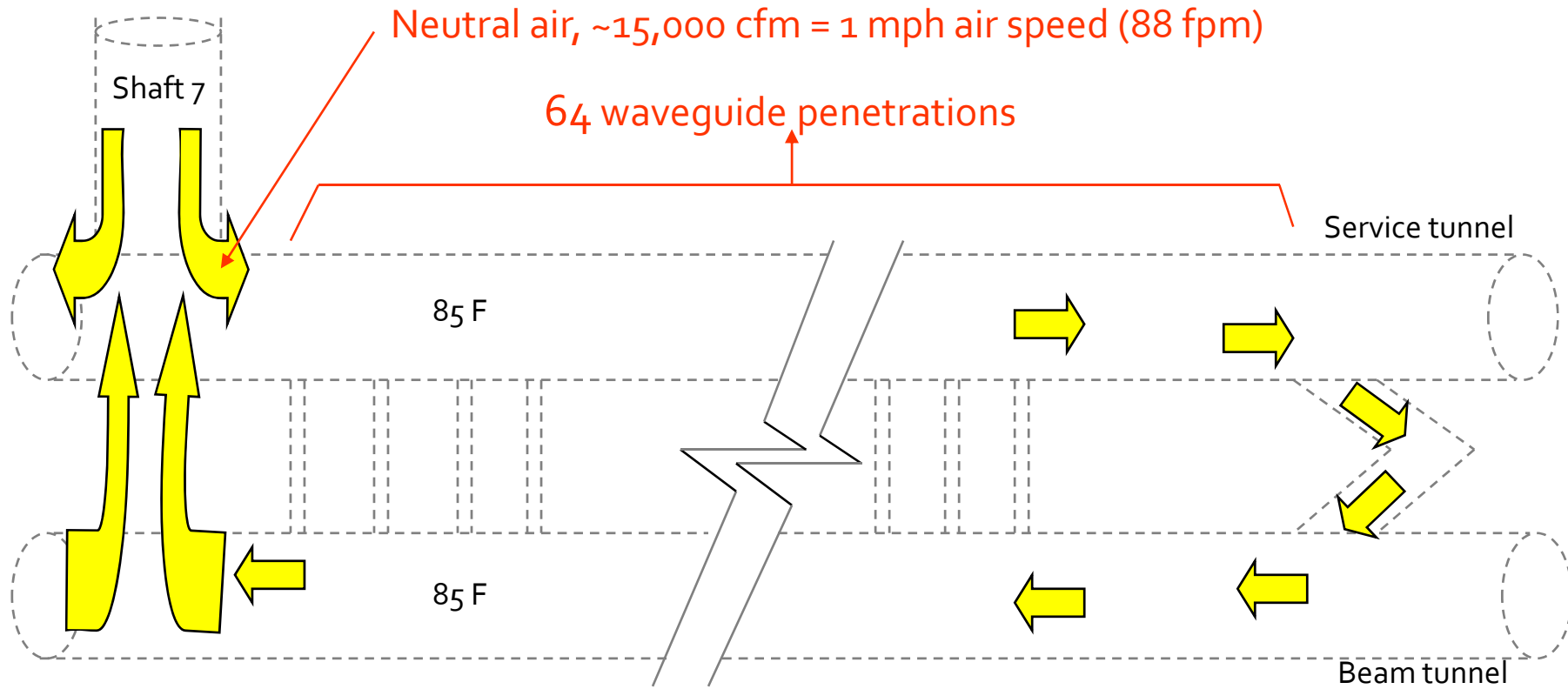
| RDR | | RDR Cost (America) | | RDR with CHW adjustment |
|-------|-------------------------|-----------------------|-----------------|-------------------------------|
| 1.7.1 | Civil Engineering | 64.3% | | 64.3% |
| 1.7.2 | ELECTRICAL | 13.2% | | 13.2% |
| 1.7.3 | AIR TREATMENT EQUIPMENT | 1.0% | | 5.5% |
| 1.7.4 | PIPED UTILITIES | 0.1% | | 0.1% |
| 1.7.5 | PROCESS (COOLING) WATER | 14.9% | Includes CHW | 10.3% |
| 1.7.6 | Handling Equipment | 1.6% | | 1.6% |
| 1.7.7 | Safety Equipment | 1.3% | | 1.3% |
| 1.7.8 | Survey and Alignment | 3.7% | | 3.7% |
| | | 100.0% | | 100.0% |

Same Totals

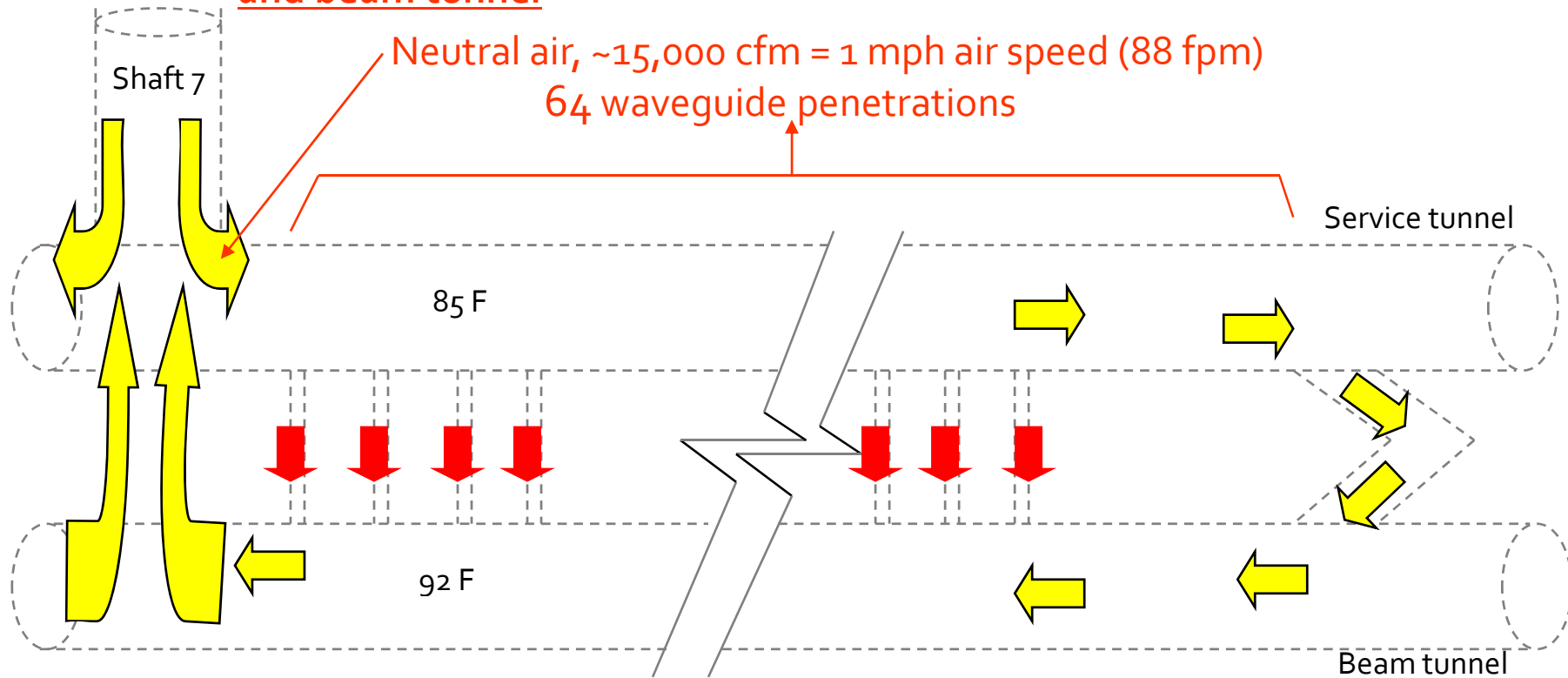
CFS Air Treatment Layout



AIR SYSTEM CONCEPT (assume no issues with mixing airflow between service and beam tunnel)



Possible waveguide cooling - IF "Waveguide at Penetration" is aircooled and no issues with mixing airflow between service and beam tunnel



0.676 KW per waveguide pene ~300cfm @ 7 air delta T X 64 = additional 19,200 cfm air

- Waveguide load in the beam tunnel will still need be picked up by fancoils
- Means of air balancing at each penetration needed
- Some part of tunnel will have ~200 fpm air speed

POST RDR

| | Heat Load KW per RF | | |
|---------------------------------|---------------------|------------------------------------|------------------------------------|
| | RDR | Post RDR <u>as of</u> Dec 07 | Post RDR <u>after</u> Dec 07 |
| Service Tunnel (ML RF) | | | |
| to water | 100 | 104 | |
| to air | 26 | 21.4 | |
| racks | 11.5 | 11.5 | |
| beam tunnel (ML RF) | | | |
| to water | included | included | |
| to air (wvguide) | 0 | 5.9 | |
| Load to air, servc tunnel, w /m | ~ 684 | | |
| Servc tunnel temp F | 85 | 104 | > 104??? |
| DR tunnel temperature F | 104 | 85 (cooler LCW) | |
| Metrology reqmnt (GDE Oct 2007) | | < 90F | |
| Air Stability | | + - 0.1 C | |
| Water Supply stability | | + - 0.2 C | |

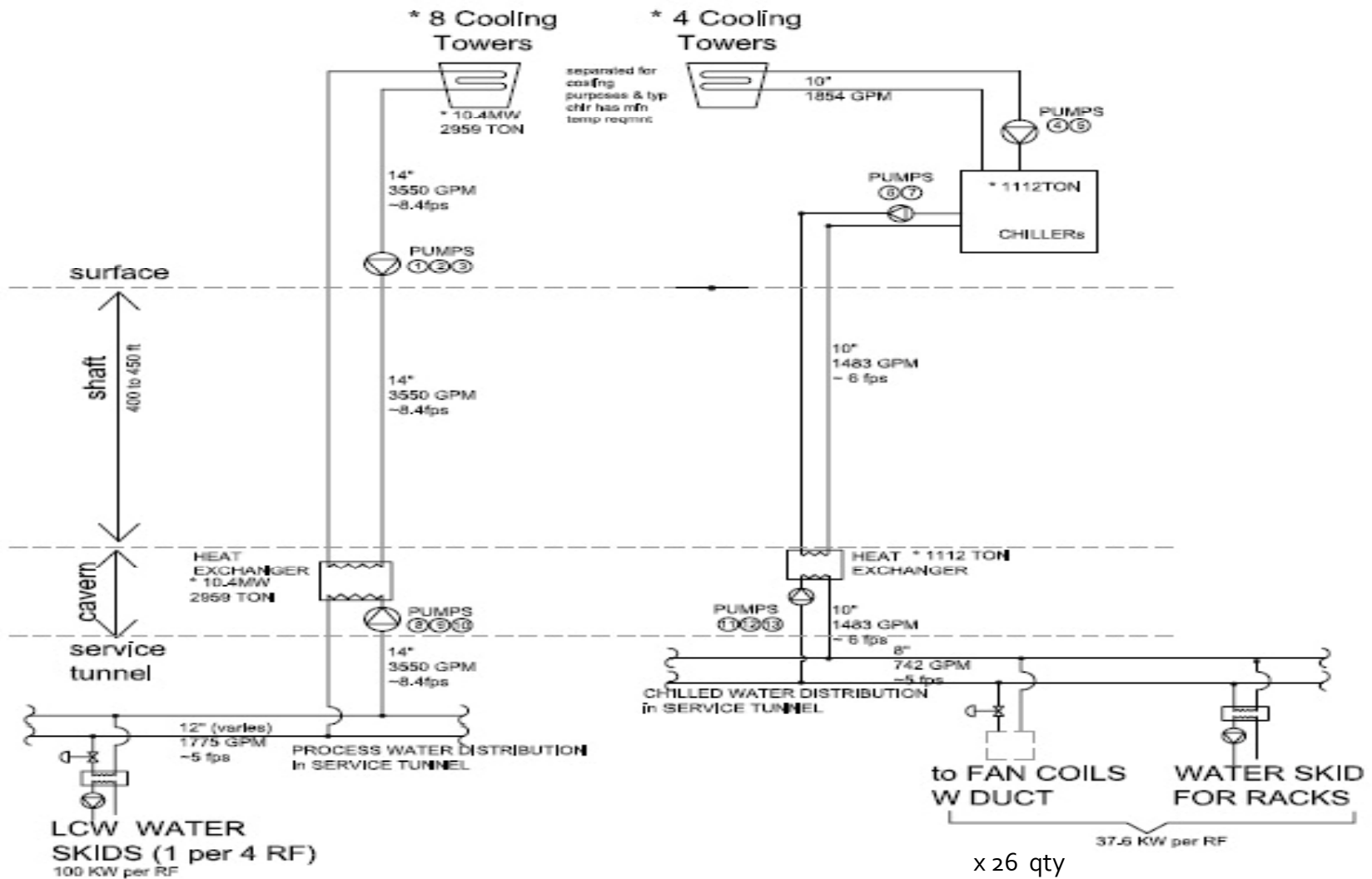
Rock Contribution?

| Analysis by | W/M | <u>KW</u> in 36m RF | Material (K in W/m- K) | Temp in (F) | Tunnel Dia-m | Temp up to what radius |
|-----------------------|------------|--------------------------------|------------------------------------|------------------------|-------------------------|---------------------------------------|
| Ztang - Sep 2006 | 130 | -4.68 | Rock (4.6) | 86 | 5 | 55F (25m) |
| Gbowden -Jul 2003 | 73 | -2.63 | Earth, Sandstone, Conc (varies) | 113 | 3 | 77F (10m) |
| SSC TP/JT - Feb 1985 | 29 | -1.04 | Dolomite (3.5) | 65 | 2.5? | 55F (30m) |
| A Enomoto - June 2008 | 100 | -3.60 | | | | |

Some discussions and preliminary investigation, but not considered

There still is considerable KW load to the air per RF - chilled fancoils are needed to maintain temperatures

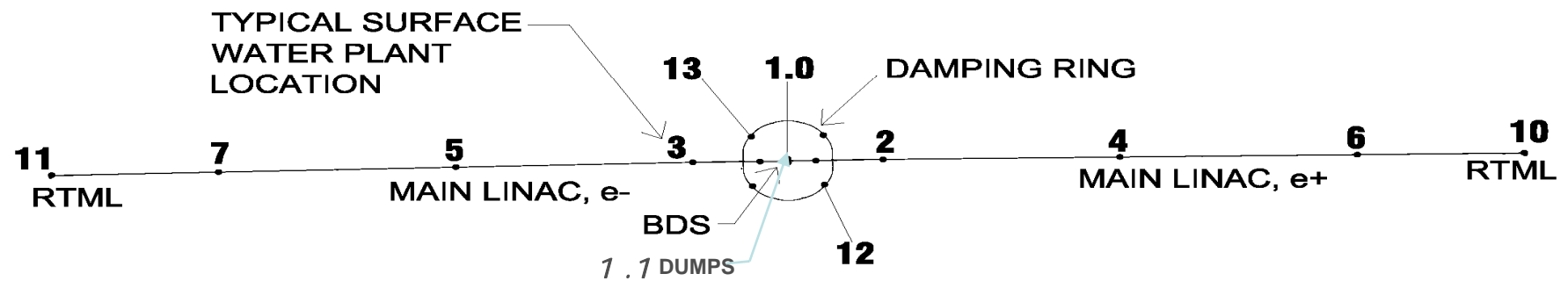
RDR Chilled Water Schematic



CHW Plant at Shaft 7

x 26 qty

Surface Air/CHW Plant locations



Air Treatment Summary

- Air Treatment Components in RDR:
 - Large air handling systems providing heating, cooling, dehumidification, humidification.
 - Fans for air purge, tunnel and shaft pressurization
 - Miscellaneous ducting and accessories, dampers, insulation, etc
- Chilled water systems including chillers, cooling towers, piping and accessories will be moved to the Air Treatment WBS
- Air treatment design is dependent on the ventilation requirements and the heat load criteria received from the area systems
- Air treatment and purge systems have not been fully investigated for radiation and ODH issues. **Need further input on air flow configuration concerning radiation and ODH issues**
- Air treatment and purge systems configuration were not developed with consensus of any AHJ (authority having jurisdiction, even who this is may not be identified for some time). **Need fire protection consultant.**

POST RDR

Specific V.E. List

| DESCRIPTIONS & "color" legend (DRAFT Dec 18 2007) | | Who is reviewing about Dec 2007 |
|--|--------|---------------------------------|
| Optimize wire not used to lose system | White | Not sure |
| Wet heat may result to heating and less power loss (potential cost savings 10M) | White | Not sure |
| Eliminate the need for cooling towers in the process water system | Red | Marc |
| Put the power plant in the tunnel to reduce the need for cooling towers and reduce system cost | Red | Marc |
| Use electrical flows for the first time | Green | Not sure |
| Provide one high efficiency cogeneration plant on site and distribute power and 33 degree F chilled water throughout the facility, remove the power generation and chilling cost from the project cost | Green | Not sure |
| Eliminate one piping system by using process water as primary rejection for chilled water system w/9 (using refrigerated head pump as fan coils and standalone chillers for racks) | Yellow | Not sure |
| Eliminate one piping system by using process water as primary rejection for chilled water system w/9 (using process cooled fan coils), wet air tunnel (Item E 15) | Yellow | Not sure |
| Increase the delta T in the LCR and chilled water systems to 30 degrees, reduce flow, pipe size w/9 | Yellow | Not sure |
| Add a chiller on the process water side w/9 | Yellow | Not sure |
| Lower the temperature in the tunnel to 65 or 70 degrees to increase operating efficiency, extend equipment life, and improve operating environment w/9 | Yellow | Not sure |
| Consider use of renewable energy source for use with cogeneration w/9 | Yellow | Not sure |
| Provide a cost analysis for reducing the overall cooling load by 5% and 10% w/9 | Yellow | Not sure |
| Centralize the cooling system | Yellow | Not sure |
| Provide distributed cogeneration / cryo (similar to #1 & 2) | Yellow | Not sure |
| Decentralize the 345 KV substation function w/ 11, 20, 30, & 33 | Gray | Not sure |
| Electrically engineer the distribution system to optimize and reduce cost w/9 | Gray | Not sure |
| Provide connection to electrical utility system at all shafts (w/ #9) | Gray | Not sure |
| Optimize substation spacing w/9 | Gray | Not sure |
| Let the electrical utility construct substations and don't include that cost in the project construction cost w/9 | Gray | Not sure |
| Centralize the HVAC and reconfigure air flow from the shafts | Yellow | Not sure |
| Pipe two chilled water coils in series, chilled water recirculate, size one for 33 degree delta T w/10 | Yellow | Not sure |
| Let the temperature in the tunnel go to 55 degrees F during normal operation and go as low as 50 degrees where people are, consider increased cost for more frequent replacement | Yellow | Not sure |
| Raise tunnel temperature to 55 degrees at all times (per OSHA requirements) w/10 | Yellow | Not sure |
| Provide air conditioned suits for personnel working in tunnel and let the temp go higher than OSHA requirements w/10 | Yellow | Not sure |
| Consider oversizing electrical cables and transformers to reduce heat | Yellow | Not sure |
| Reassign the RP loads for more optimal process water flow | Yellow | Not sure |
| Modify top shaft HVAC to only process make up air, add blowers down shaft for recirculation | Yellow | Not sure |
| Reduce lighting level to green limits | Yellow | Not sure |
| Reduce water pressure drop across components, minimize head pressure | Yellow | Not sure |
| Combine possibility of going to 2 condenser water loops instead of 3 as presently planned | Yellow | Not sure |
| Consider using low mineral content water instead of LCR w/9 (design water system for low mineral water) | Yellow | Not sure |
| Allow different types of pipe materials: PVC, CPVC, HDPE, carbon fiber wrapped PE, etc. in lieu of stainless steel | Yellow | Not sure |
| Consider replacing the fan coil units with a chilled water beam (radiant cooling) | Yellow | Not sure |
| Put the water piping in the concrete slab, eliminate pipe supports | Yellow | Not sure |
| Use water cooled weaver in the accelerator tunnel in lieu of air cooling | Yellow | Not sure |
| Provide passive convection tunnel using cooling shafts during colder months | Yellow | Not sure |
| Provide multiple modes of operation dependent on outdoor temperature | Yellow | Not sure |
| Develop loads that do not require low conductivity water | Yellow | Not sure |
| Use the weaver/pre-irradiation system for cooling the weaver (flow cooled gas inside the weaver) | Yellow | Not sure |
| Pulse the power source for selected loads when not being used | Yellow | Not sure |
| Use pressure regulators to control the hydrostatic pressure in the collectors | Yellow | Not sure |
| Define the maximum hydrostatic pressure for the collectors | Yellow | Not sure |
| Consider expandability of systems - modular vs centralized | Yellow | Not sure |
| Reexamine the tee design of modular power supplies | Yellow | Not sure |
| Plan for a 4 month downtime during the summer | Yellow | Not sure |
| Limit the operation of the system to 72 degree wet bulb | Yellow | Not sure |
| Use CO2/iodon monitoring and limit the intake of outside air to what is necessary to maintain a safe environment | Yellow | Not sure |
| Use a deaerator to deaerate ventilation air | Yellow | Not sure |
| Calculate water head conductivity to determine requirements | Yellow | Not sure |
| Establish power budgets for the relay racks (400 W / RP + 50% of power supplies) | Yellow | Not sure |
| Provide power supply that will work with warm water if necessary (quasi self-heating) | Yellow | Not sure |
| Use on site ponds for make up water | Yellow | Not sure |
| Consider using cooling ponds in lieu of cooling towers | Yellow | Not sure |
| Give or sell heat from chillers to neighboring communities | Yellow | Not sure |
| Increase the number of RP stations per LCR skid | Yellow | Not sure |
| Use vapor phase cooling on the collector and generate electricity from excess energy | Yellow | Not sure |
| Use the lowest kVA transformer to reduce heat load | Yellow | Not sure |
| Consider use of geothermal cooling | Yellow | Not sure |
| Use the first river for once thru primary cooling, eliminate the cooling towers | Yellow | Not sure |
| Use modular systems for all equipment | Yellow | Not sure |
| Eliminate Rack 541d and replace with jet pump | Yellow | Not sure |
| Eliminate one piping system by using chilled water only as primary rejection, minimize process water distribution | Yellow | Not sure |

• About 50+ list from V.E. in Nov 2007, List from value engineering sessions in Nov 2007. Some appear to have very good cost reduction potential.

• No pros/cons and cost impact evaluation done yet

• Color coded

Red=Marc selected on Dec 4 2007

Yellow=potential VE but not necessarily cost reduction?

Green= by others (HLRF), not CFS

Gray=ignore

White=not sure

• Most VE work effort stopped on Dec 18 07

HVAC/CHW Value Engineering Studies

- Provide one hi-efficiency cogen power/cooling plant on site and distribute power and 33°F (0.6°C) CHW throughout the facility,
 - Removes power/CHW production systems costs from the project cost.
 - Removes one piping system from project.
 - 33°F CHW = smaller pipes, lower HP pumps, smaller HXs, very HI delta T (90°F/50°C+)
 - Cogen plant builder/operator finances, builds, operates, and maintains power plant then sells utility power and CHW to ILC.
 - Allows cooling of tunnel and electronics mitigating high temperature disadvantages.
 - Centralize plant reduces shaft/support area footprints.
- Centralize the HVAC and reconfigure airflow from tunnel ends or center.
- Modify top-of-shaft HVAC to only process make up air, add blowers at tunnel level for recirculation.
- Investigate use of desiccants to dehumidify make up air. Could use heat recovery from cogen plant.
- Investigate alternate piping materials, PVC, copper, HDPE, etc.