

# Introduction to Cryogenics for accelerators

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# Préambule

## Reference

Great thanks to predecessors for this type of exercise, particularly to Ph. Lebrun and his “legacy” of slides

## Disclaimer

Being an engineer and new in this domain as “teacher”, I will try to share with you some information with emphasis on “applied cases” with a “pragmatic approach” rather than only a theoretical one.

*There are plenty of books, previous CAS courses with lot's of formulas and various equations. I leave it to you to check bibliography if this is what you are looking for!*

# Contents

- Introduction
- Cryogenic fluids
- Heat transfer & thermal insulation
- Cryogenic distribution & cooling schemes
- Refrigeration & liquefaction
- Various complements
- Concluding remarks, references

- **cryogenics**, that branch of physics which deals with the production of very low temperatures and their effects on matter

*Oxford English Dictionary*

2<sup>nd</sup> edition, Oxford University Press (1989)

- **cryogenics**, the science and technology of temperatures below 120 K

*New International Dictionary of Refrigeration*

3<sup>rd</sup> edition, IIF-IIR Paris (1975)

Temperature in Celsius (C): unit defined with 0 C (ice) and 100 C (vapour)

Temperature in Kelvin (K): 1 K = 1 C, but 0 K = -273.15 C (absolut zero)

# Densification, liquéfaction & séparation des gaz

## LNG



130 000 m<sup>3</sup> LNG carrier  
with double hull

Air separation by cryogenic  
distillation

Up to 4500 t/day LOX

## LIN & LOX



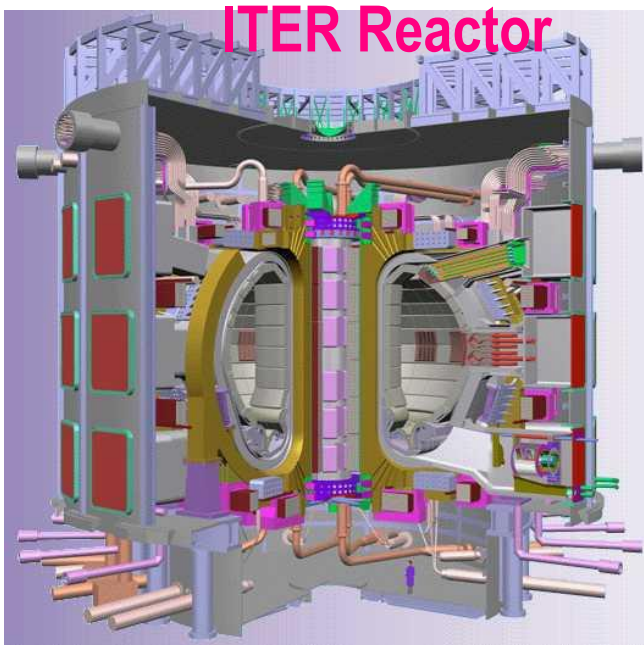
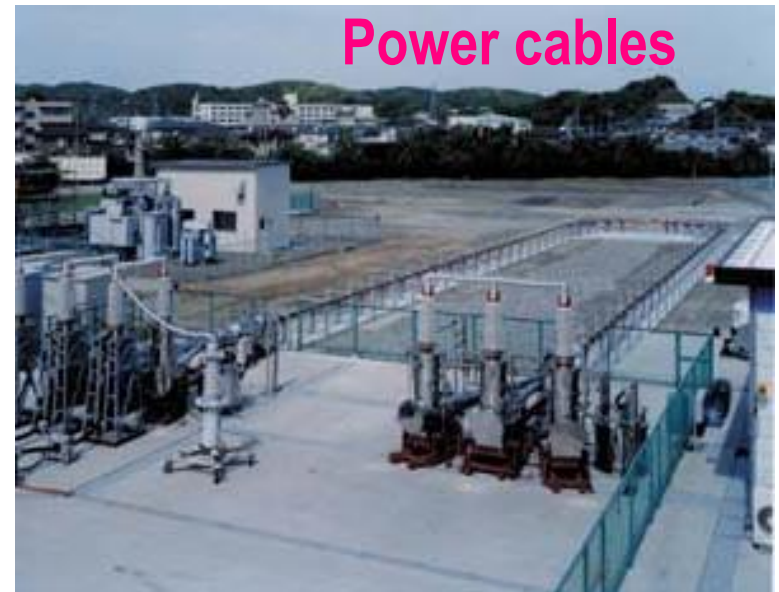
## Rocket fuels



## Ariane 5

25 t LHY, 130 t LOX

# Cooling of superconducting devices



# Main reasons to superconducting

*For accelerators in high energy physics*

- Compactness through higher fields

Capital Cost

$$E_{\text{beam}} \approx 0.3 \cdot \mathbf{B} \cdot r$$

[Gev]            [T]   [m]

$$E_{\text{beam}} \approx \mathbf{E} \cdot L$$

[Gev]            [MV/m]   [m]

At design stage, working at highest possible temperature is always considered, but often not selected to maximise beam energy ...

Cryogenic systems takes longer to recover from failures than conventional ones !  
*(but there is work on it!)*

- Saving operating energy

Operating Cost

Electromagnets:

Resistive:             $P_{\text{input}} \approx E_{\text{beam}}$

Superconducting:    $P_{\text{input}} \approx P_{\text{ref}}$

Acceleration cavities

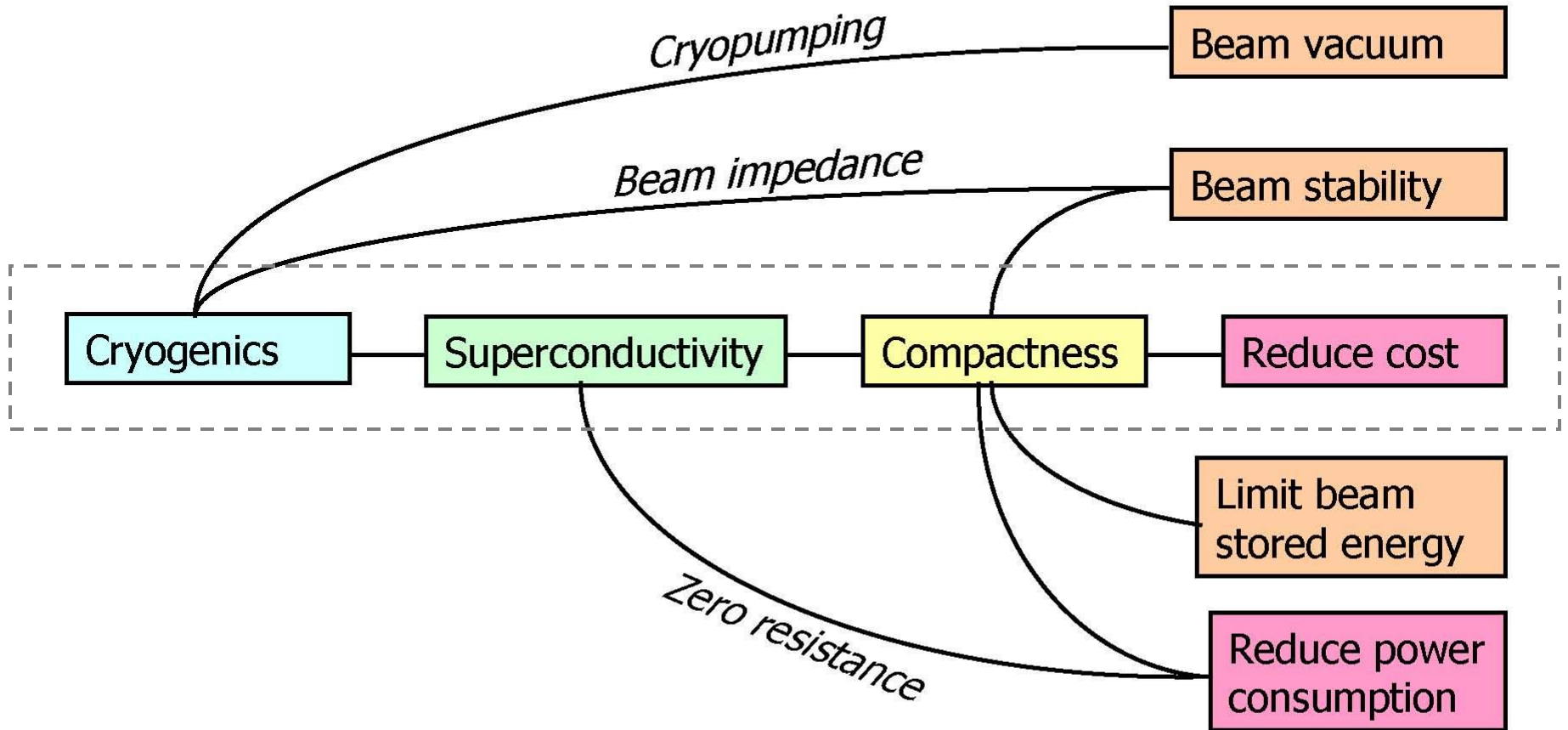
$$P_{\text{input}} \approx R_s \cdot L \cdot \mathbf{E}^2 / w$$

$$R_s \approx R_{\text{BCS}} + R_0$$

$$R_{\text{BCS}} \approx (1/T) \exp(-BT_c/T)$$



# Rationale for superconductivity & cryogenics in particle accelerators

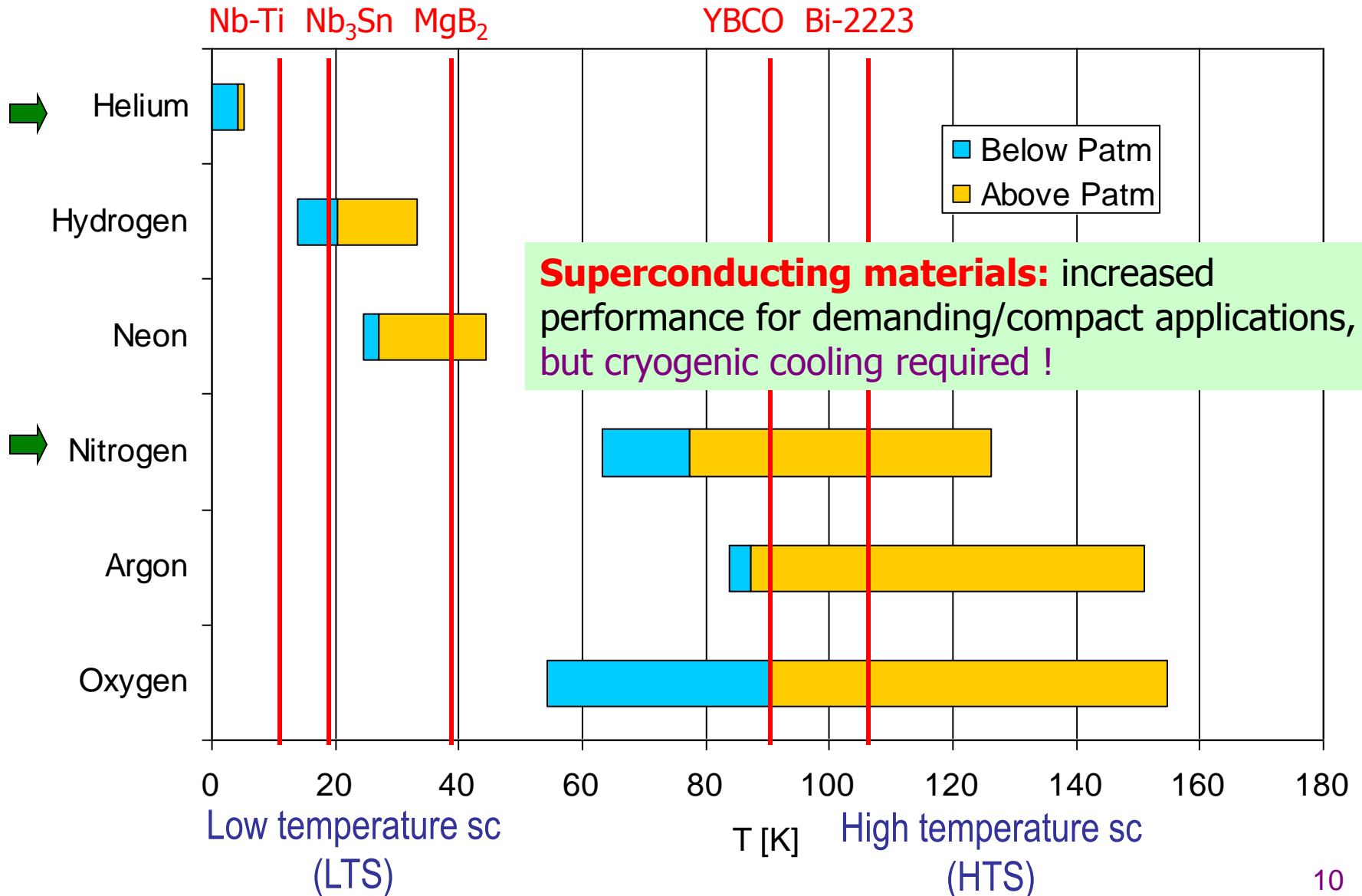




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# Useful range of cryogenes, and potential applications



# Characteristic temperatures of cryogenes

<b>Cryogen</b>	<b>Triple point [K]</b>	<b>Normal boiling point [K]</b>	<b>Critical point [K]</b>
Methane	90.7	111.6	190.5
Oxygen	54.4	90.2	154.6
Argon	83.8	87.3	150.9
Nitrogen	63.1	77.3	126.2
Neon	24.6	27.1	44.4
Hydrogen	13.8	20.4	33.2
Helium	2.2 (*)	4.2	5.2

(\*):  $\lambda$  point

# Vaporization of normal boiling cryogenics under 1 W applied heat load

$$\text{Power} \approx \dot{m}' \cdot \text{Latent\_Heat}$$

[W]      [g/s]      [J/g]

Cryogen	[mg.s <sup>-1</sup> ]	[l.h <sup>-1</sup> ] (liquid)	[l.min <sup>-1</sup> ] (gas NTP)
Helium	48	1.38	16.4
Nitrogen	5	0.02	0.24

# Amount of cryogenics required to cool down 1 kg iron

$$\text{Power} \approx m' \cdot \text{Latent\_Heat}$$

[W]      [g/s]      [J/g]

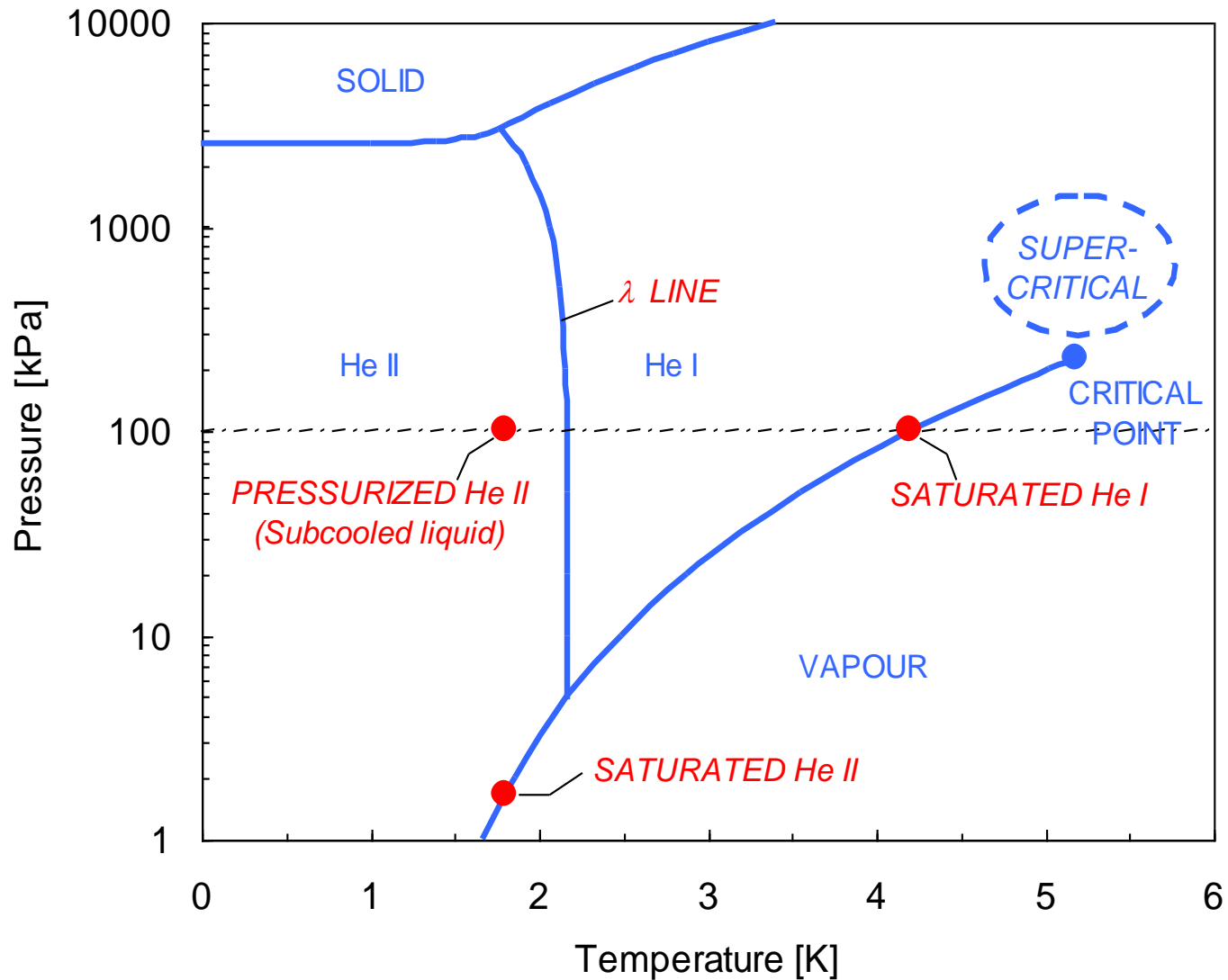
$$\text{Power} \approx m' \cdot \text{Specific\_Heat} \cdot \Delta T$$

[W]      [g/s]      [J/g.K]      [K]



Using	Latent heat only	Latent heat and enthalpy of gas
LHe from 290 to 4.2 K	29.5 liter	0.75 liter
LHe from 77 to 4.2 K	1.46 liter	0.12 liter
LN2 from 290 to 77 K	0.45 liter	0.29 liter

# Phase diagram of helium



# Helium as a cooling fluid

<b>Phase domain</b>	<b>Advantages</b>	<b>Drawbacks</b>
Saturated He I	Fixed temperature High heat transfer	Two-phase flow Boiling crisis
Supercritical	Monophase Negative J-T effect	Non-isothermal Density wave instability
He II	Low temperature High conductivity Low viscosity	Second-law cost Subatmospheric

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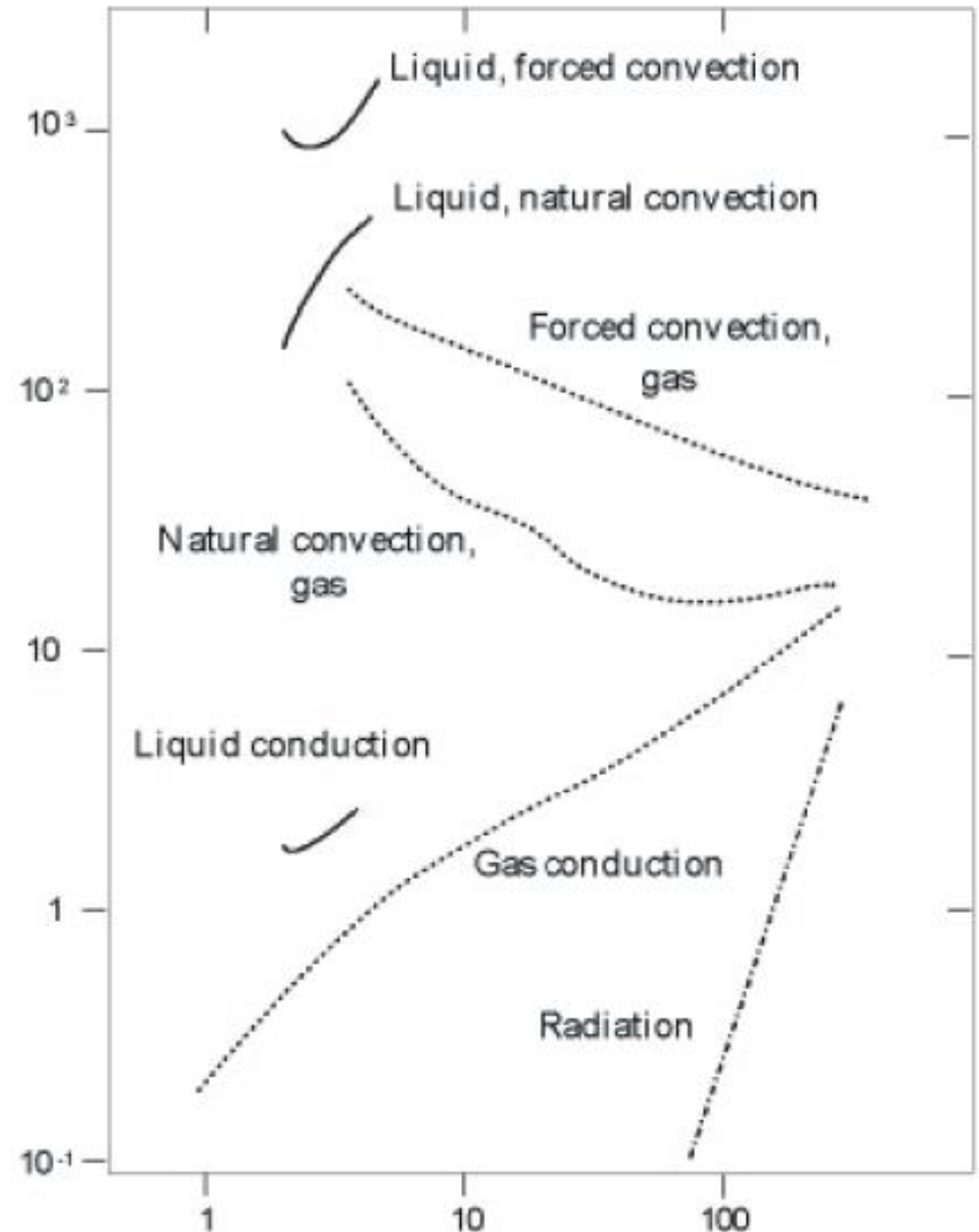


# Typical heat transfer coefficients at cryogenic temperatures

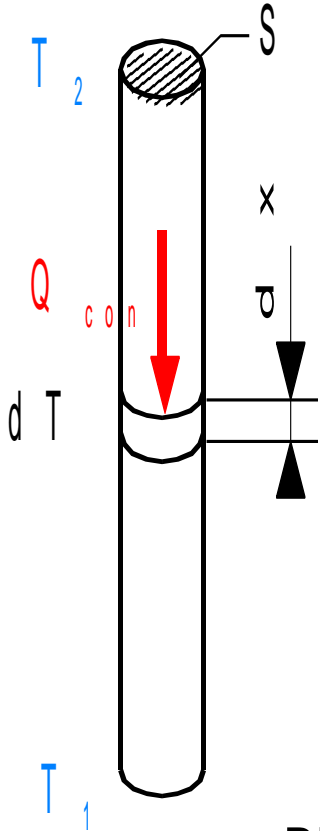
3 mechanisms involved:

- Conduction
- Radiation
- Convection

$Q/(\Delta T.A)$  [ $W/(m^2.K)$ ]



# Heat conduction in solids



Fourier's law:  $Q_{\text{con}} = k(T) \cdot S \cdot \frac{dT}{dx}$

$k(T)$ : thermal conductivity [W/m.K]

Integral form:  $Q_{\text{con}} = \frac{S}{L} \cdot \int_{T_1}^{T_2} k(T) \cdot dT$

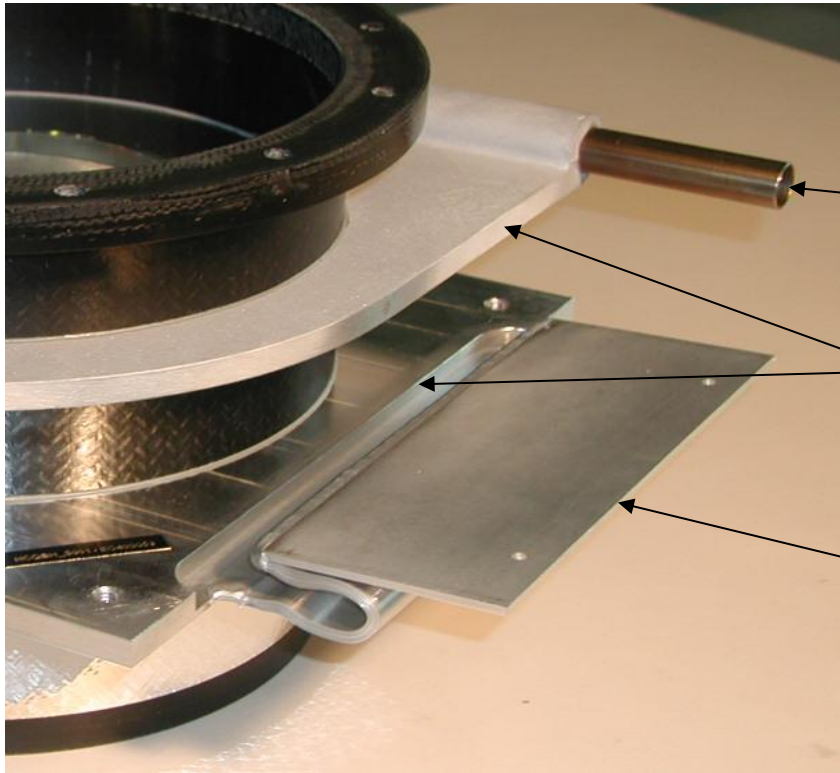
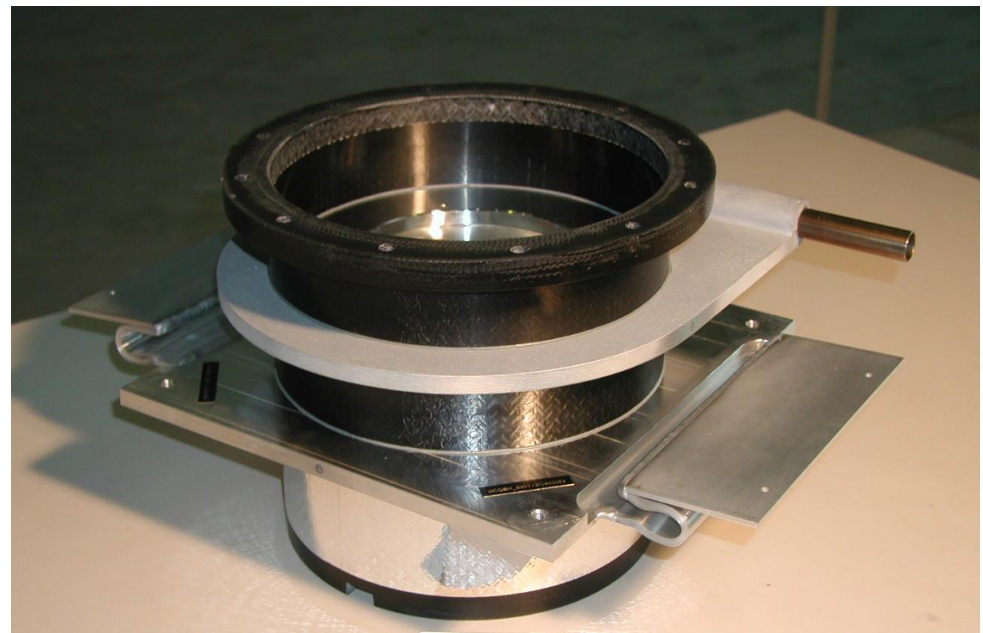
$\int k(T) \cdot dT$  : thermal conductivity integral [W/m]

Thermal conductivity integrals for standard construction materials are tabulated

Risks associated with "optimisation":

- small section  $S$ : towards limit for material resistance
- long length  $L$ : towards limits for mechanical stability
- insulators (large)  $K$ : transfer of forces in compression

# Non-metallic composite support post with heat intercepts for LHC magnets

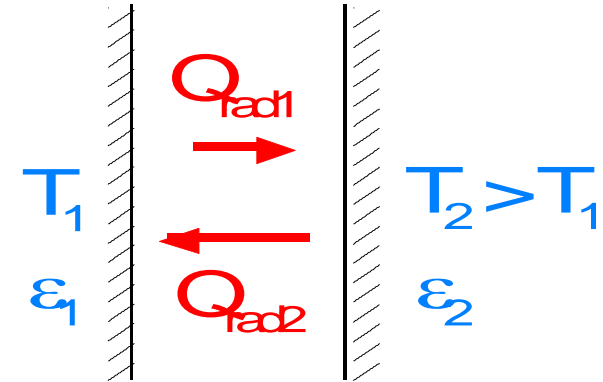


5 K cooling line (SC He)

Aluminium intercept plates  
glued to G-10 column

Aluminium strips to thermal  
shield at 50-75 K

# Thermal radiation



- Wien's law
  - Maximum of black body power spectrum  
 $\lambda_{max} T = 2898 \text{ } [\mu\text{m.K}]$

- Stefan-Boltzmann's law
  - Black body
  - "Gray"body
  - "Gray" surfaces at  $T_1$  and  $T_2$

$$Q_{rad} = \sigma A T^4$$

$$\sigma = 5.67 \times 10^{-8} \text{ W/m}^2.\text{K}^4$$

(Stefan Boltzmann's constant)

$$Q_{rad} = \varepsilon \sigma A T^4$$

$\varepsilon$  emissivity of surface

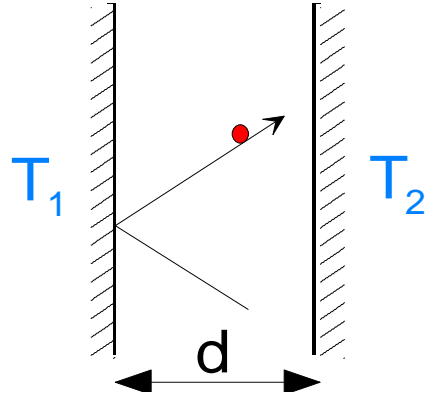
$$Q_{rad} = E \sigma A (T_1^4 - T_2^4)$$

$E$  function of  $\varepsilon_1, \varepsilon_2, \text{ geometry}$

$$E \cdot T^4$$

Best would be to have a reflective (high E) "parasol" to intercept T4 ...

# Residual gas conduction



$\lambda_{molecule}$  : mean free path of gas molecules

Best would be to avoid residual gas ...

- Viscous regime

- At high gas pressure  $\lambda_{molecule} \ll d$
- Classical conduction  $Q_{res} = k(T) A dT/dx$
- Thermal conductivity  $k(T)$  independent of pressure

- Molecular regime

- At low gas pressure  $\lambda_{molecule} \gg d$
- Kennard's law  $Q_{res} = A \alpha(T) \Omega P (T_2 - T_1)$
- Conduction heat transfer proportional to pressure, independent of spacing between surfaces  
 $\Omega$  depends on gas species
- Accommodation coefficient  $\alpha(T)$  depends on gas species,  $T_1$ ,  $T_2$ , and geometry of facing surfaces

# Multi-layer insulation (MLI)



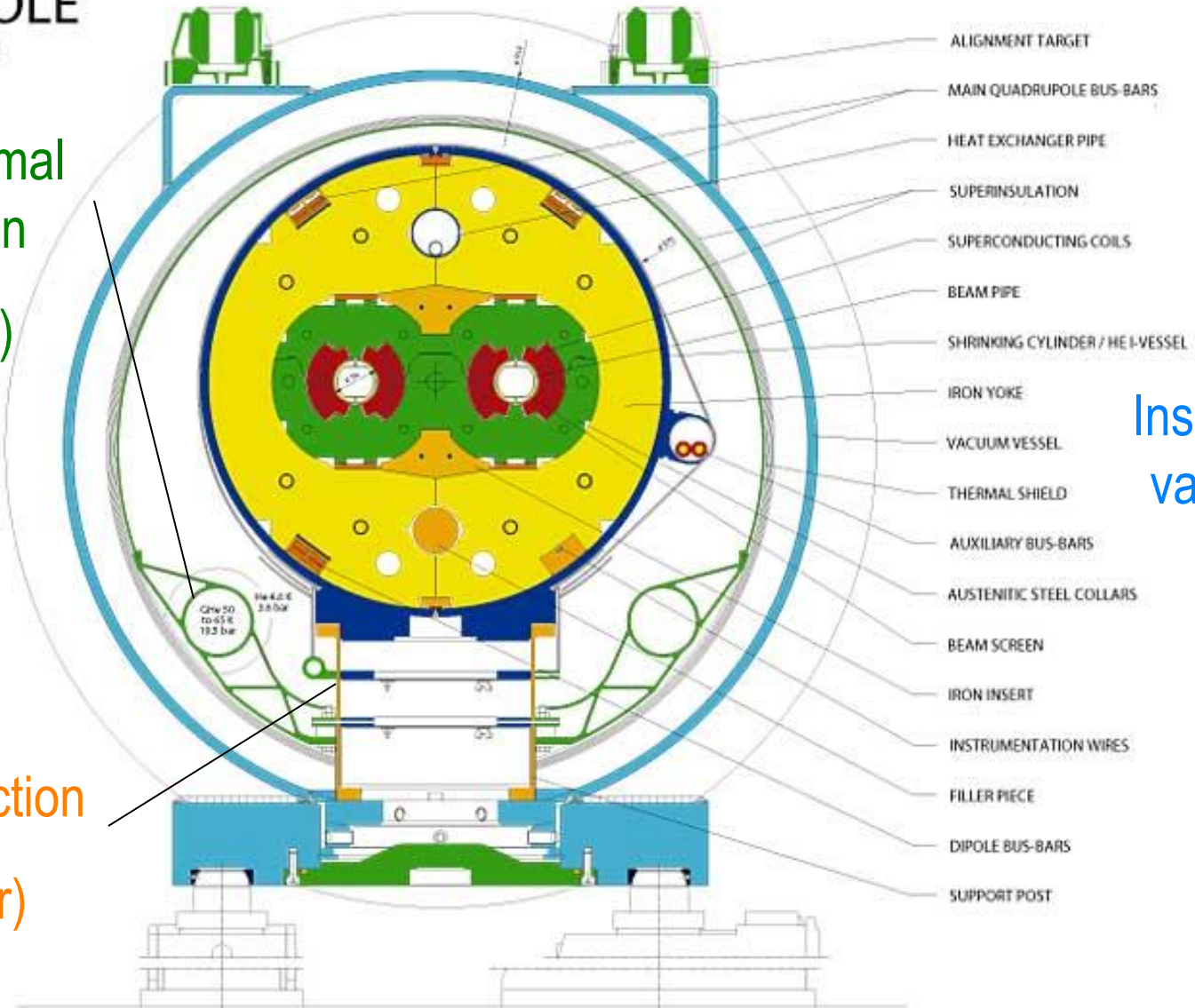
- Complex system involving three heat transfer processes
  - $Q_{MLI} = Q_{rad} + Q_{sol} + Q_{res}$
  - With  $n$  reflective layers of equal emissivity,  $Q_{rad} \sim 1/(n+1)$
  - Due to parasitic contacts between layers,  $Q_{sol}$  increases with layer density
  - $Q_{res}$  due to residual gas trapped between layers, scales as  $1/n$  in molecular regime
  - Non-linear behaviour requires layer-to-layer modeling
- In practice
  - Typical data available from (abundant) literature
  - Measure performance on test samples

# Cross section of a LHC dipole

## LHC DIPOLE CROSS SECTION

Low thermal  
radiation  
(shield)

Low conduction  
(insulator)

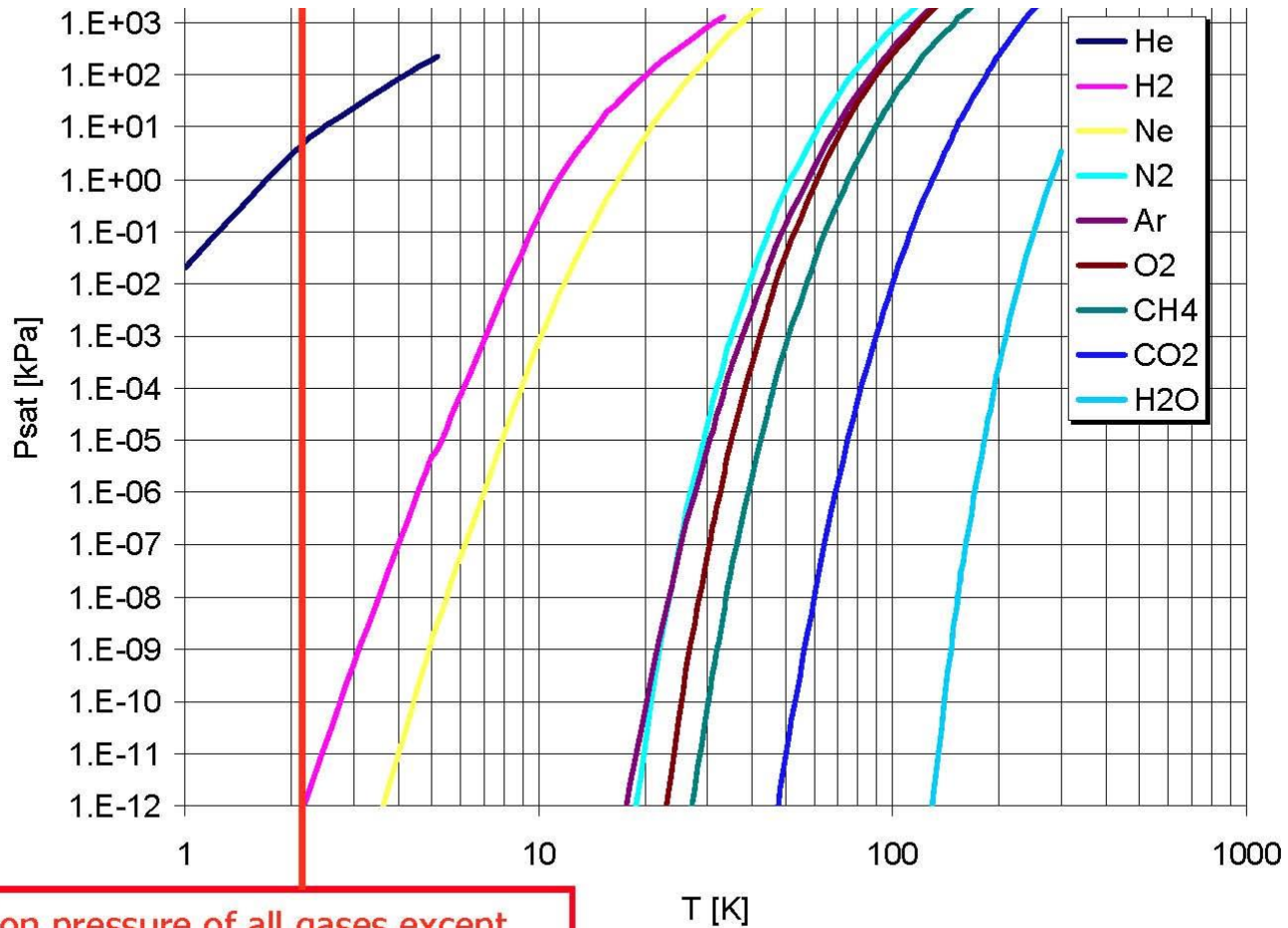


Insulation  
vacuum



# Cryopumping maintains good vacuum

## Vapour pressure at cryogenic temperatures



Saturation pressure of all gases except helium vanish at cryogenic temperature

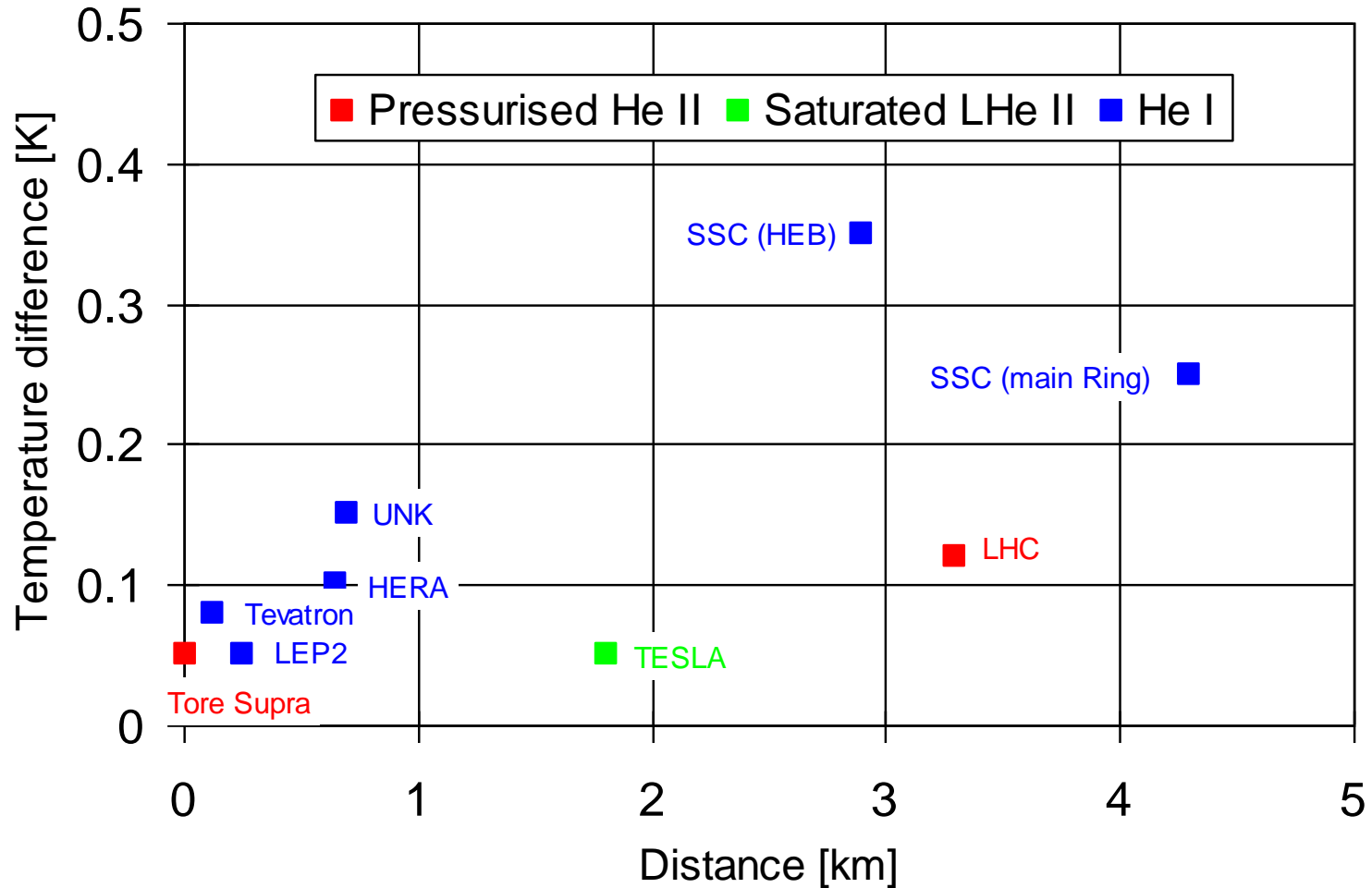
Cryopumping maintains good vacuum



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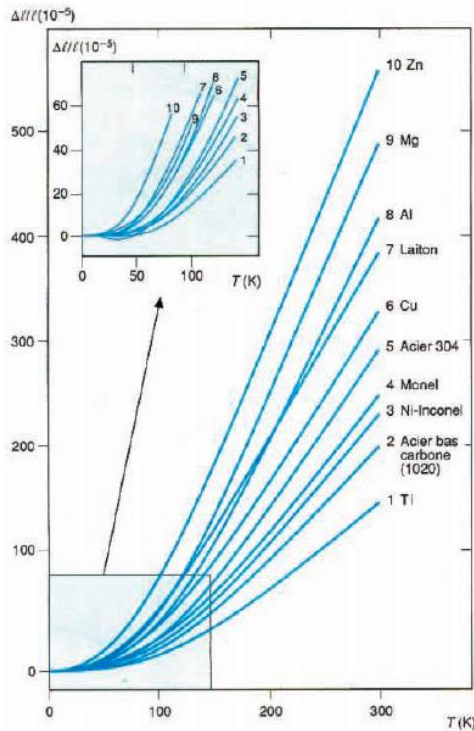
# Transport of refrigeration in large distributed cryogenic systems



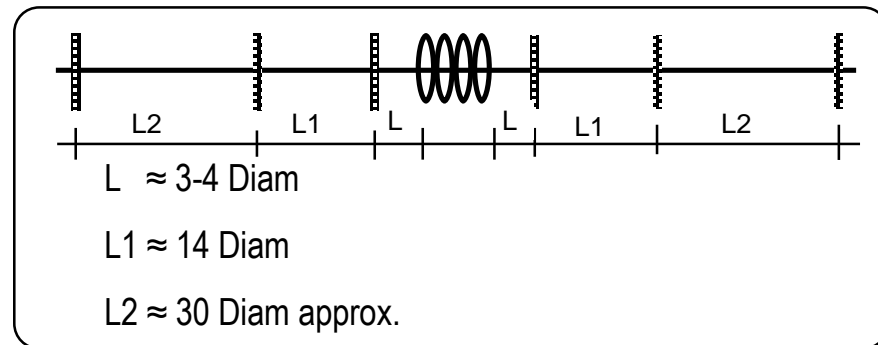
# Cryogenic distribution scheme: design issues

- Monophase vs. two-phase
  - temperature control
  - hydrostatic head & flow instabilities
- Pumps vs. no pumps
  - efficiency & cost
  - reliability & safety
- LN<sub>2</sub>
  - cooldown and/or normal operation
  - capital & operating costs of additional fluid
  - safety in underground areas (ODH)
- Lumped vs. distributed cryoplants
- Separate cryoline vs. integrated piping
- Number of active components (valves, actuators)
- Redundancy of configuration

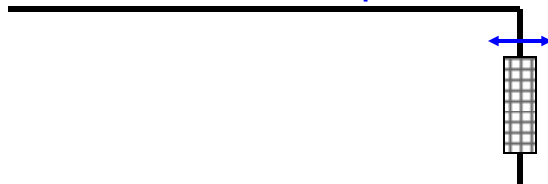
# Thermal contraction for cryo lines



3 mm / m of thermal contraction  
=> Compensation required !

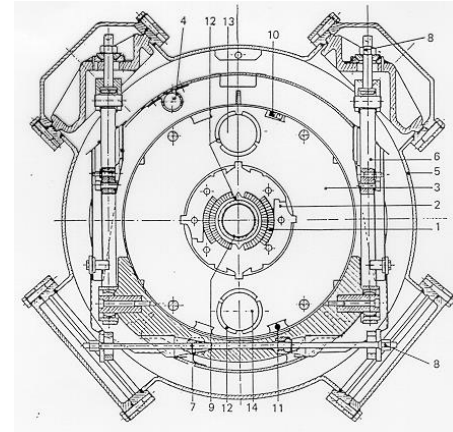
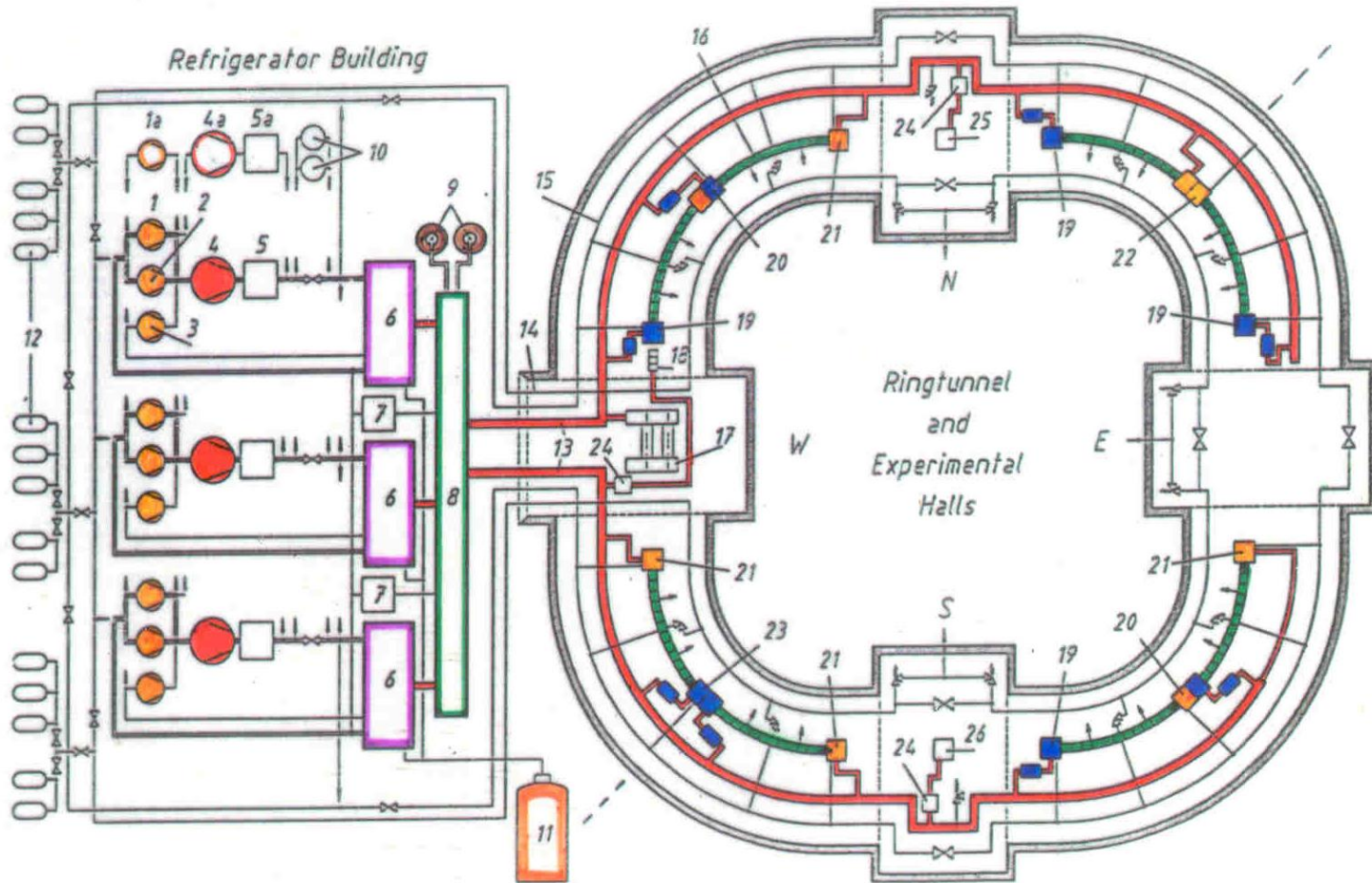


Thermal compensation



This is **THE** delicate part in the design of a cryogenic line, as thermal performance can only be considered once the line withstand mechanical forces !!!

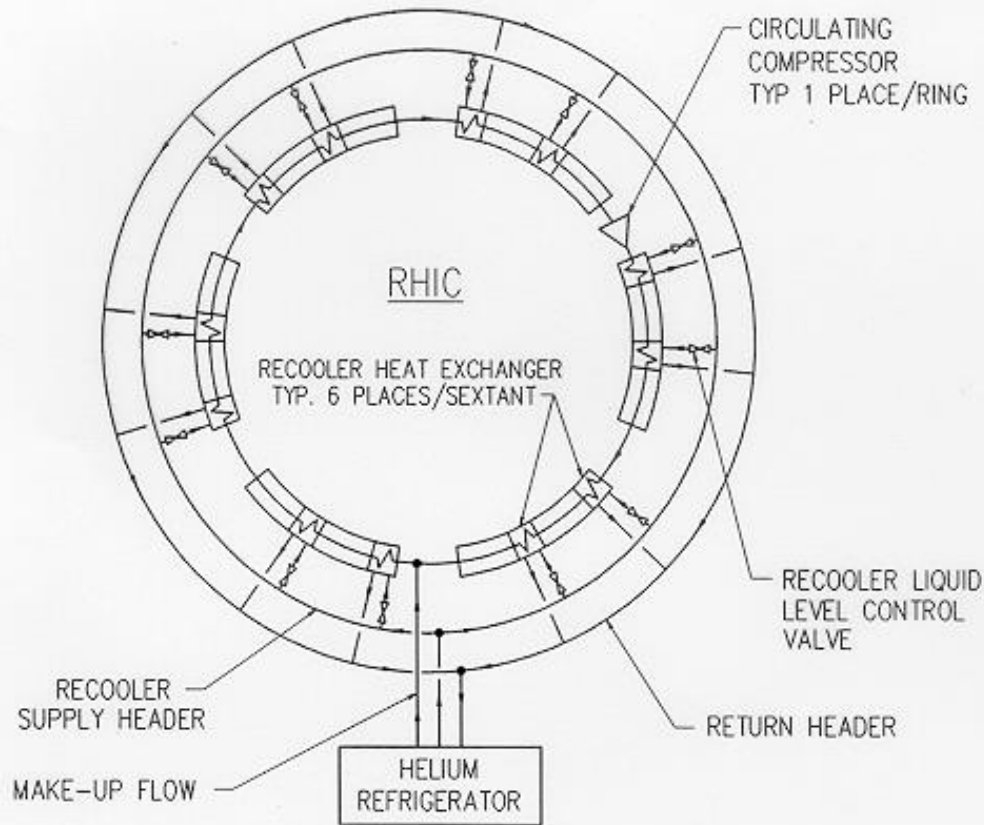
# HERA distribution scheme



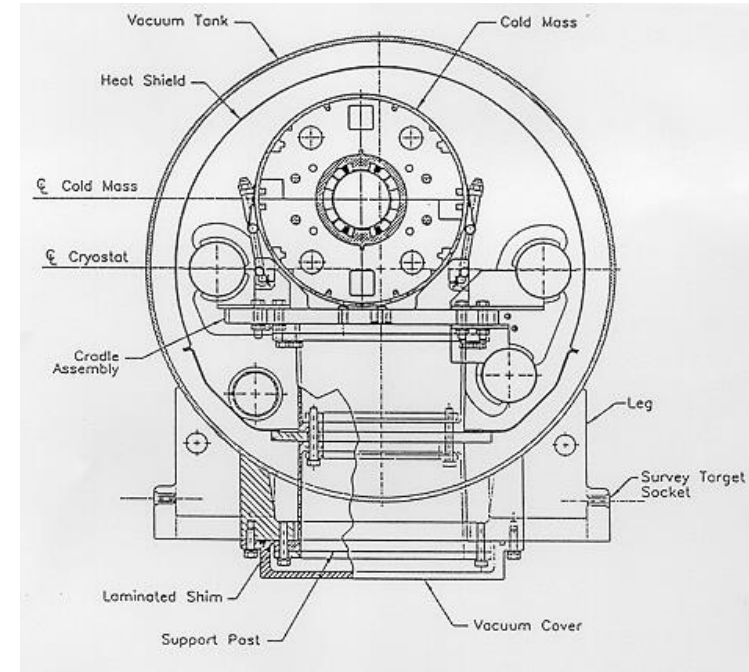
Central cryoplat and separate ring cryoline

Refrigeration 4.3 K	6775 W	total mass flow	0.871 kg/s
Refrigeration 40/80 K	20000 W	Primary power	2845 kW
Current lead flow	$20.5 \times 10^{-3}$ kg/s	Specif. power consumption	281 W (300 K)/W (4.3 K)

# RHIC distribution scheme



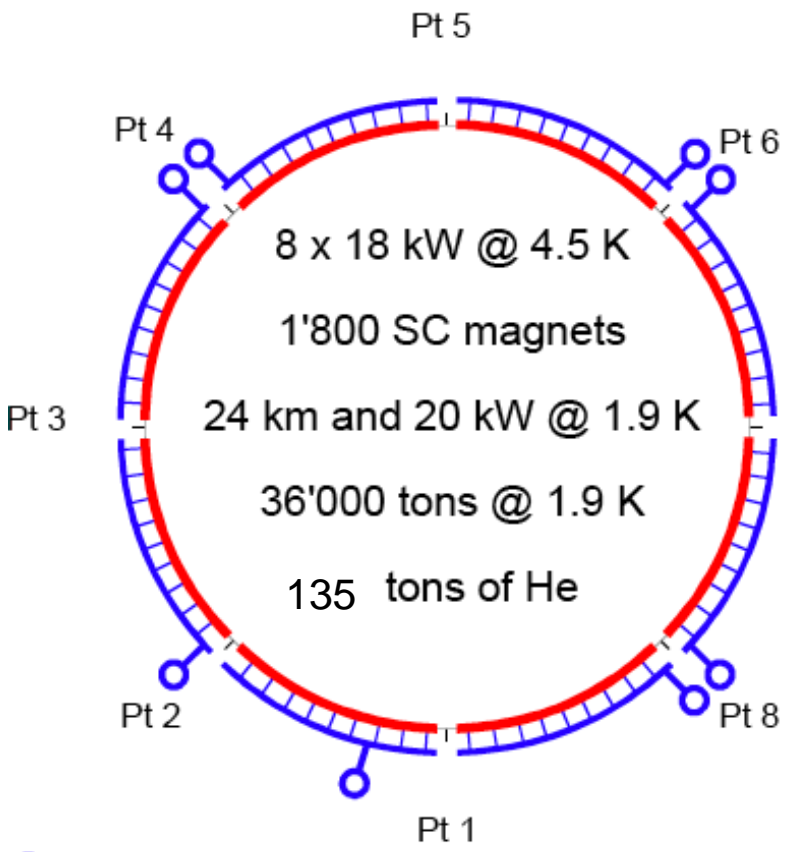
HELIUM PRIMARY FLOW CIRCUIT FOR STEADY-STATE OPERATION.  
ONLY ONE OF THE RINGS IS SHOWN.



Central cryoplant and piping integrated in magnet cryostat

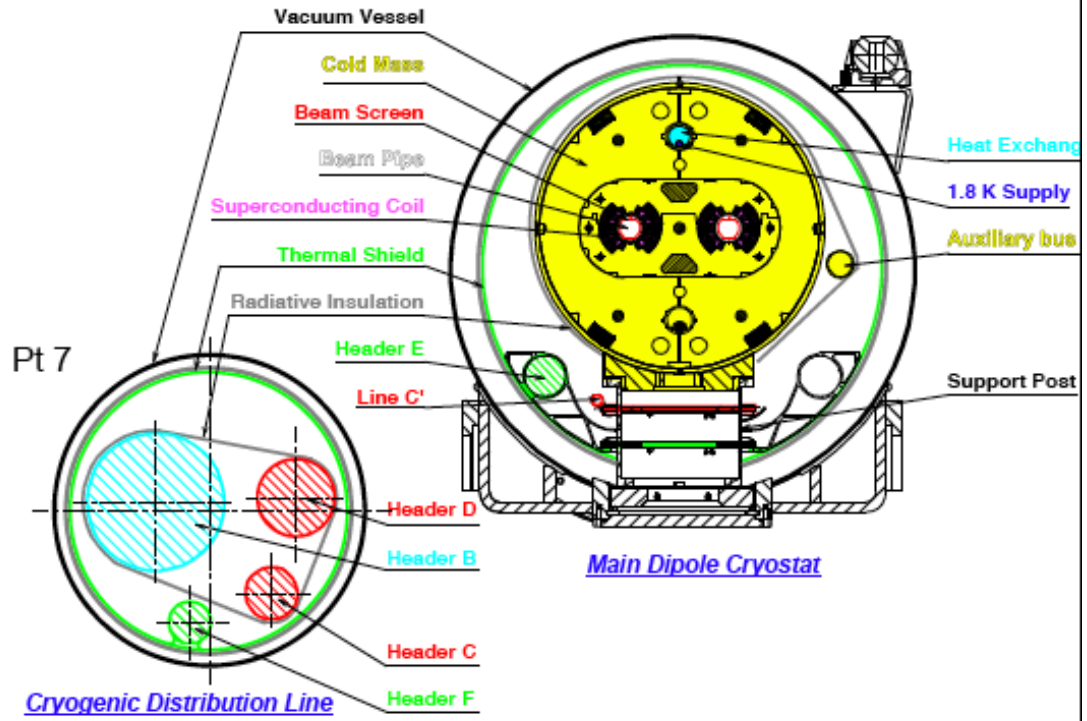


# LHC distribution scheme



○ Cryogenic plant

## Typical LHC Cross-section



Cryoplants at five points, separate ring cryoline, 107 m long strings

# Superconducting Linac (Tesla\_based)

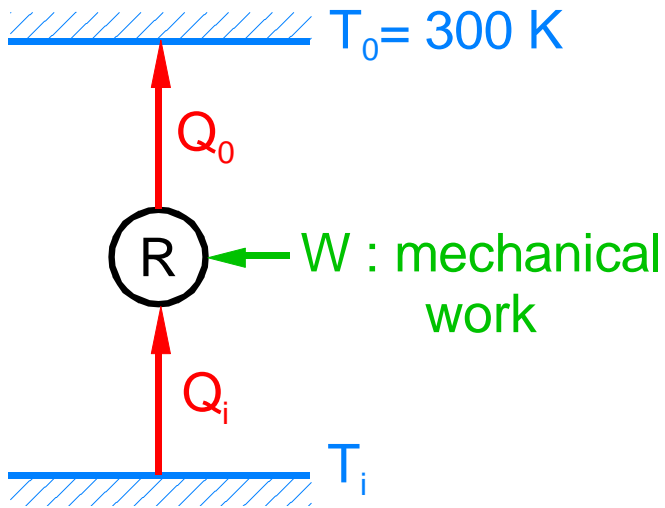




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# Thermodynamics of cryogenic refrigeration



First principle [Joule]

$$Q_0 = Q_i + W$$

Second principle [Clausius]

$$\frac{Q_0}{T_0} \geq \frac{Q_i}{T_i}$$

(= for reversible process)

Hence,  $W \geq T_0 \cdot \frac{Q_i}{T_i} - Q_i$  which can be written in three different ways:

①  $W \geq T_0 \cdot \Delta S_i - Q_i$  introducing **entropy S** as

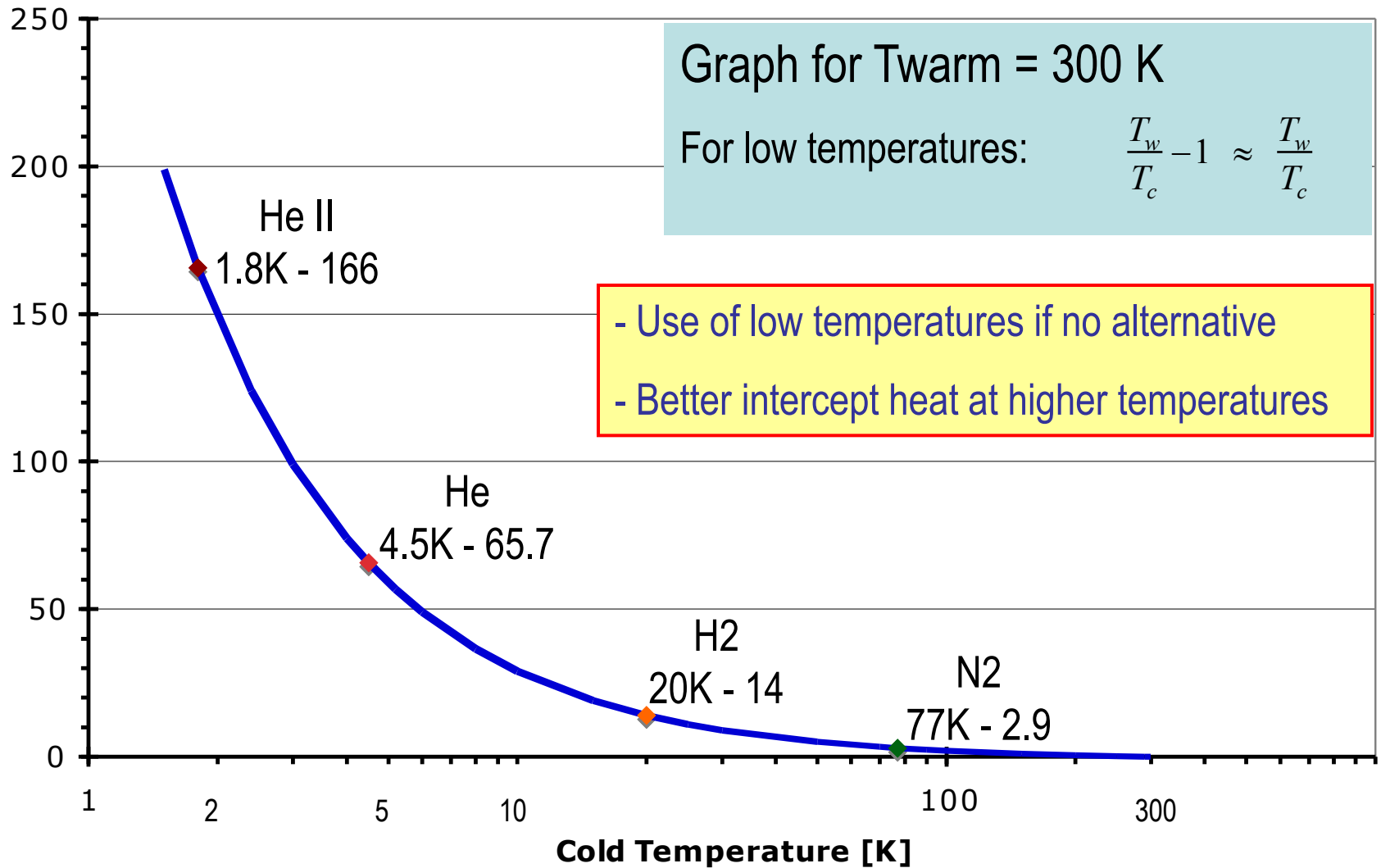
$$\Delta S_i = \frac{Q_i}{T_i}$$

②  $W \geq Q_i \cdot \left( \frac{T_0}{T_i} - 1 \right)$  ← Carnot factor

③  $W \geq \Delta E_i$  introducing **exergy E** as

$$\Delta E_i = Q_i \cdot \left( \frac{T_0}{T_i} - 1 \right)$$

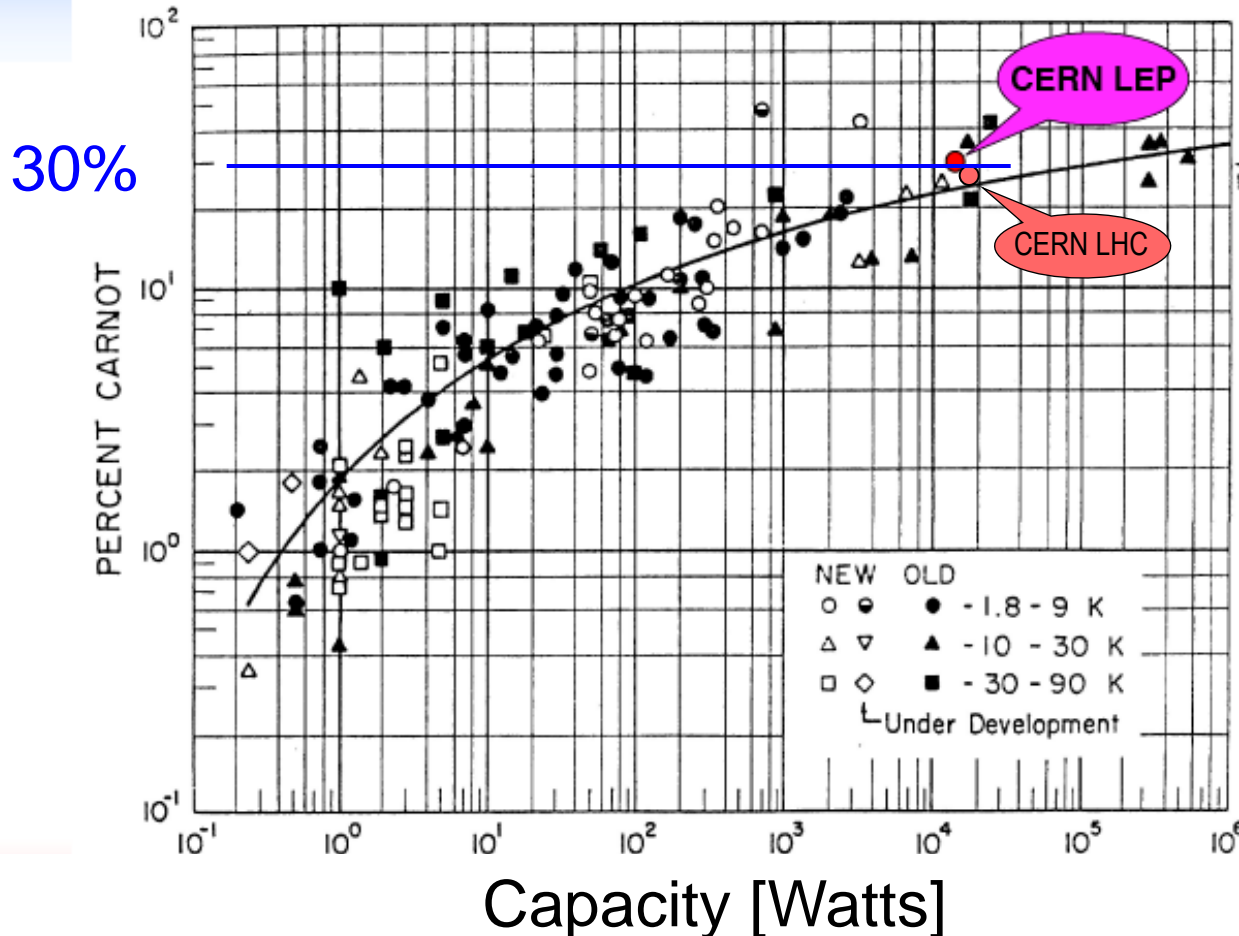
# The Carnot Factor



# Helium refrigerators

Power Input  $\approx$  Power@cold x Carnot / %w.r.tCarnot

## LE DIAGRAMME DE STROBRIDGE



The efficiency w.r.t Carnot does not depend on the temperature, but rather on the size

The largest possible, the best !

# Minimum refrigeration work

Consider the extraction of 1 W at 4.5 K, rejected at 300 K  
The minimum refrigeration work (equation 2) is:

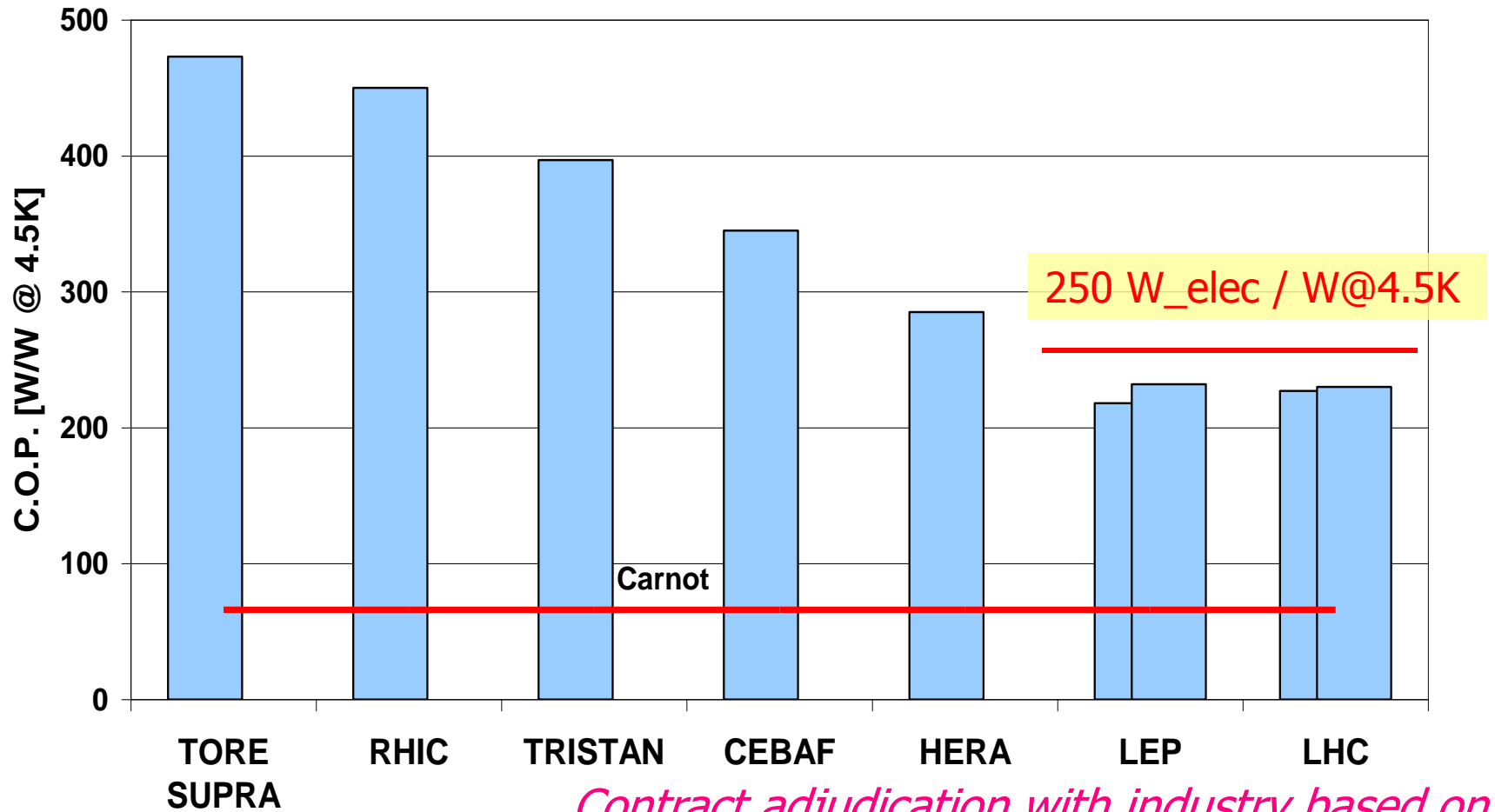
$$W_{\min} = Q_i \cdot \left( \frac{T_o}{T_i} - 1 \right) = 1 \cdot \left( \frac{300}{4.5} - 1 \right) = 65.7 \text{ W}$$

In practice, the most efficient helium refrigerators have an efficiency of about 30% w.r. to the Carnot limit.

$$\Rightarrow W_{\text{real}} = \frac{W_{\min}}{\eta} = \frac{65.7}{0.3} = 220 \text{ W}$$

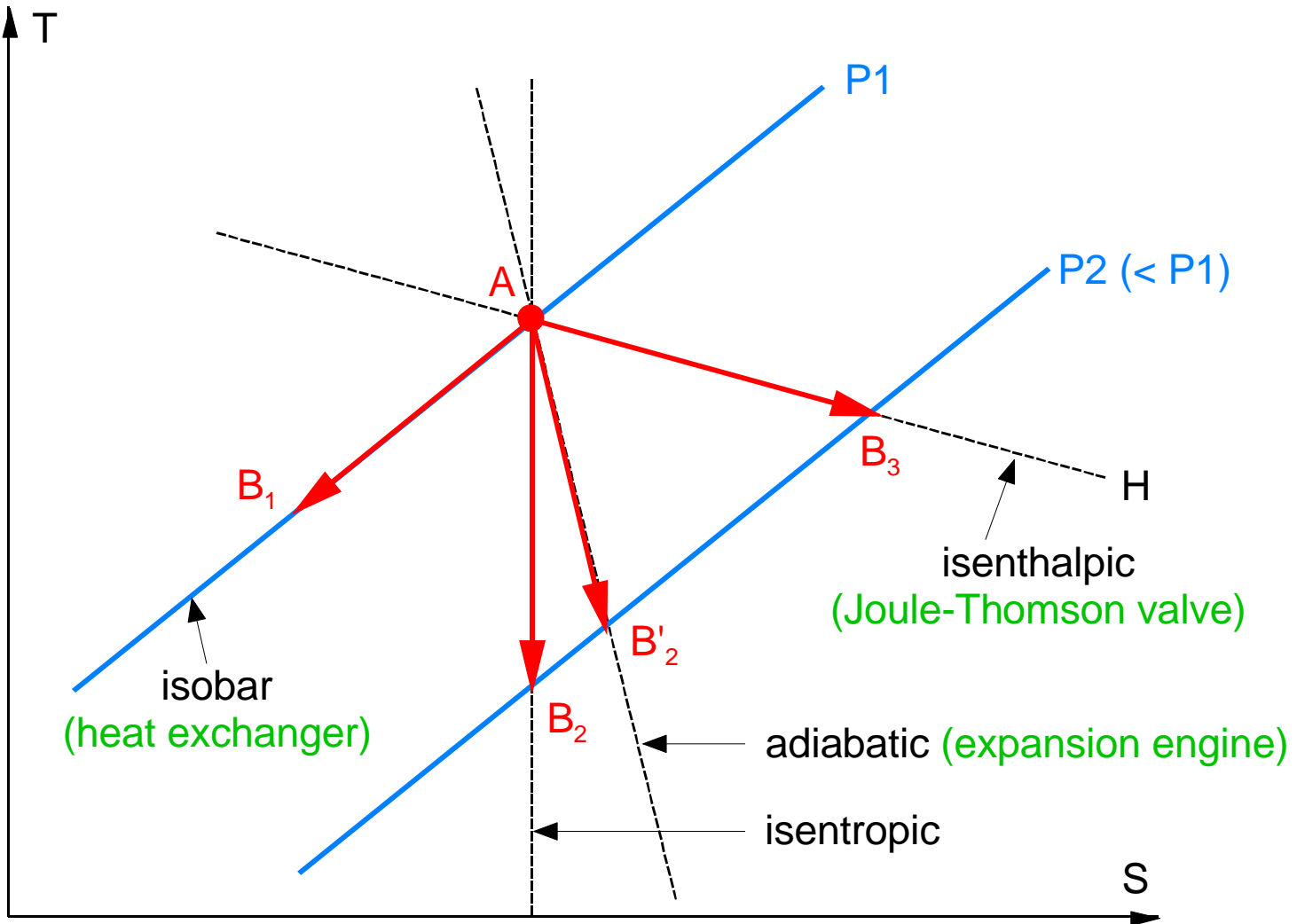
# C.O.P. of large cryogenic helium refrigerators

*Time (left to right) is not the only factor for improvement*

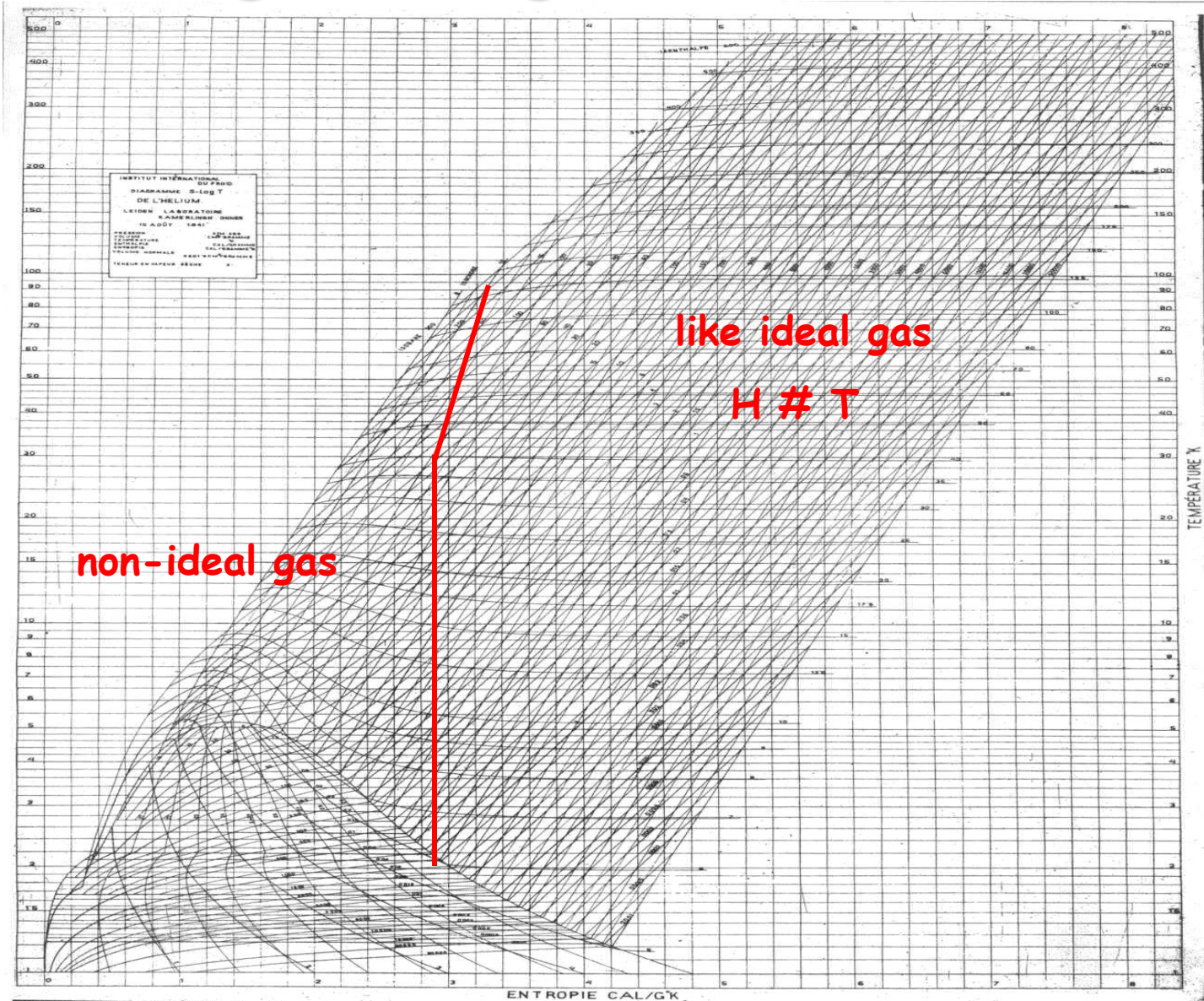


*Contract adjudication with industry based on Capital+Operation(10yrs) costs*

# Elementary cooling processes on T-S diagram



# Log T-s Diagram for Helium





# Maximum Joule-Thomson inversion temperatures

Cryogen	Maximum inversion temperature [K]
Helium	43
Hydrogen	202
Neon	260
Air	603
Nitrogen	623
Oxygen	761

While air can be cooled down and liquefied by JT expansion from room temperature, helium and hydrogen need precooling down to below inversion temperature by heat exchange or work-extracting expansion (e.g. in turbines)

# LE CYCLE DE JOULE THOMSON

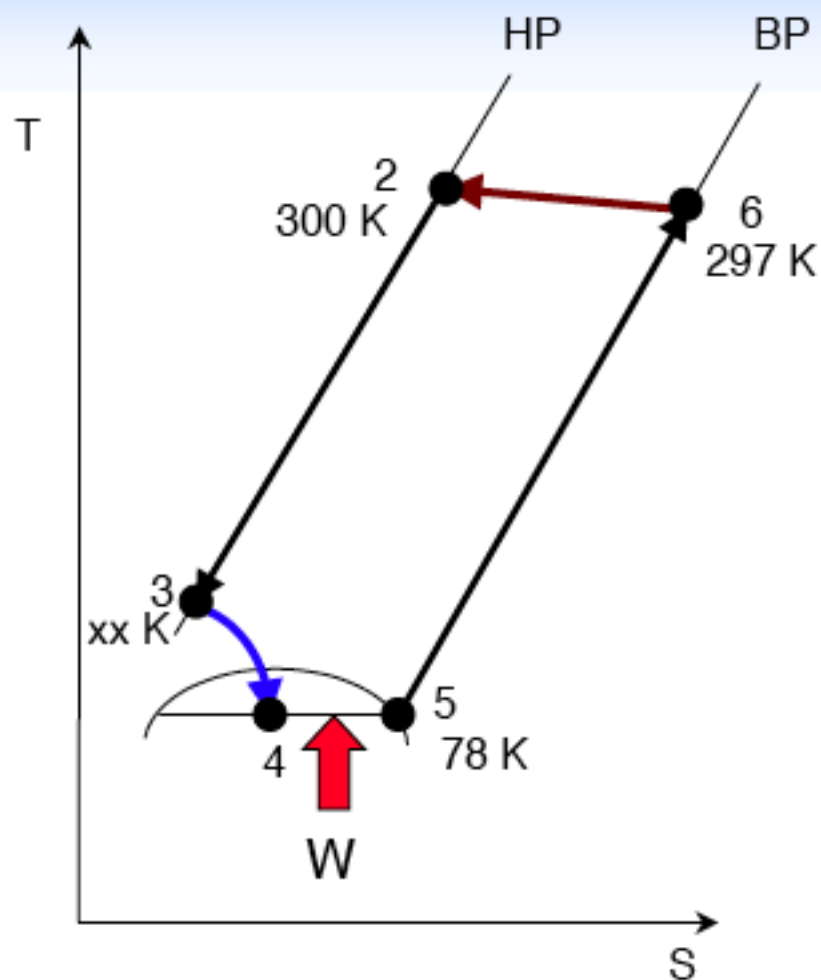
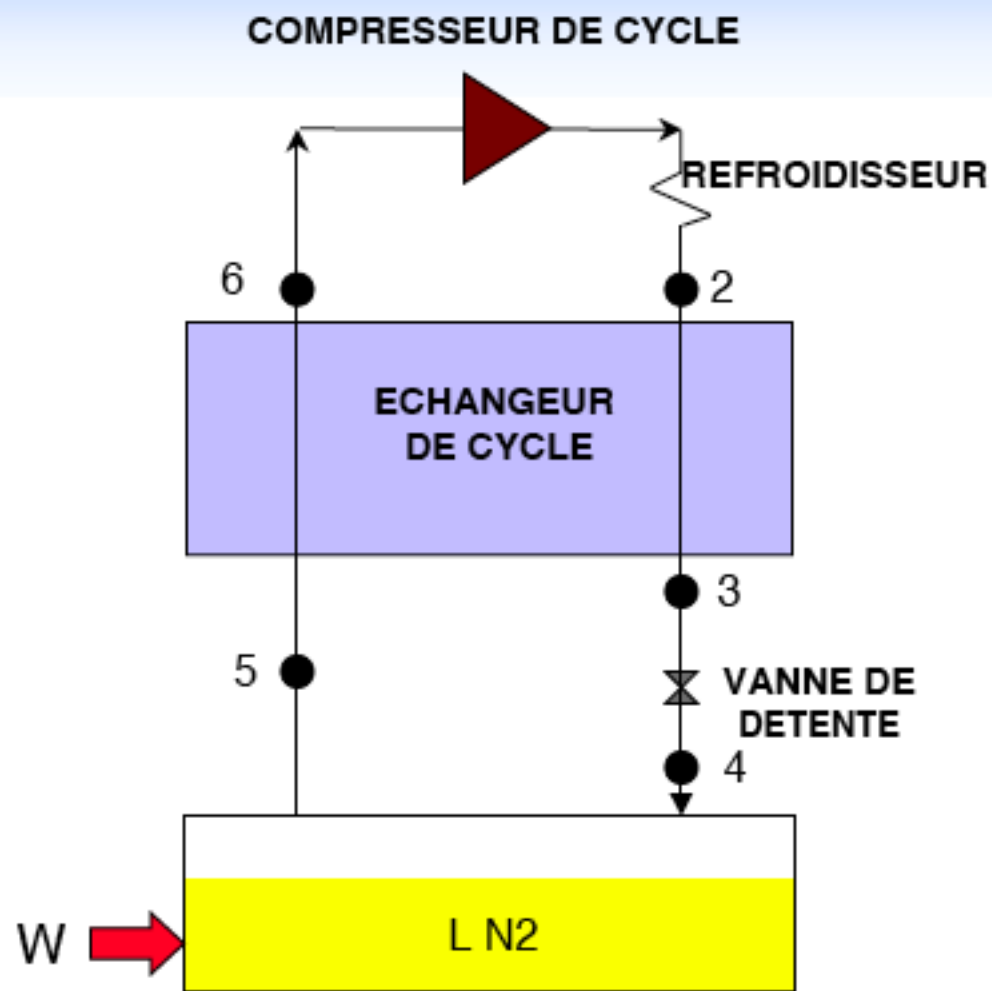


DIAGRAMME TEMPERATURE/ENTROPIE



SCHEMA

# LE CYCLE DE BRAYTON

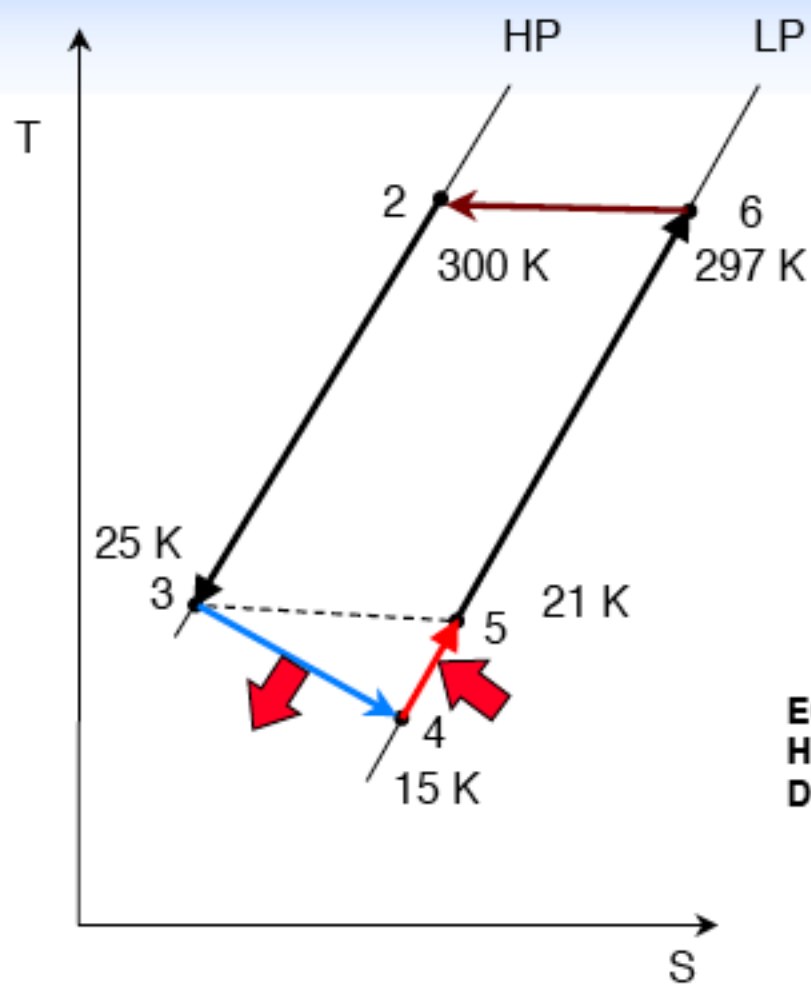
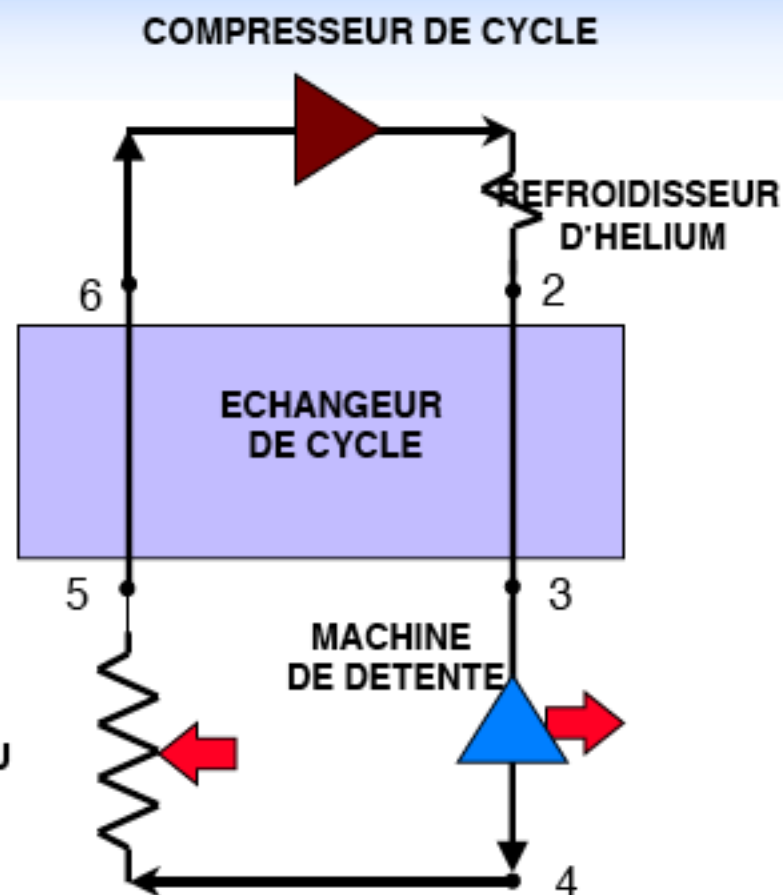
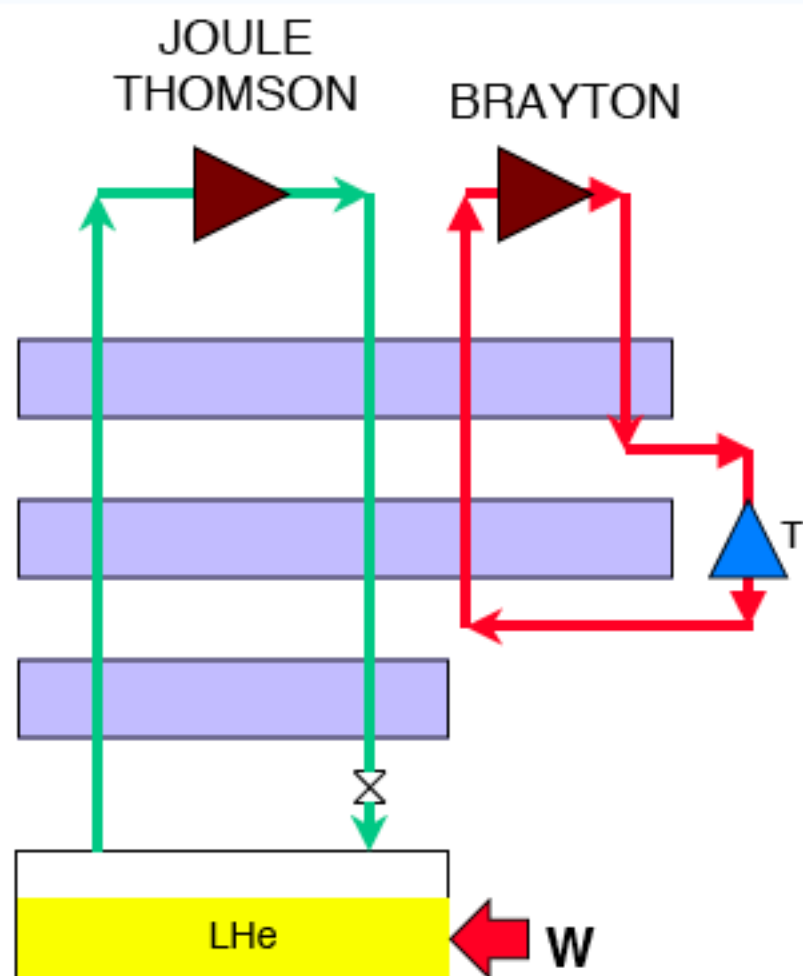


DIAGRAMME TEMPERATURE/ENTROPIE

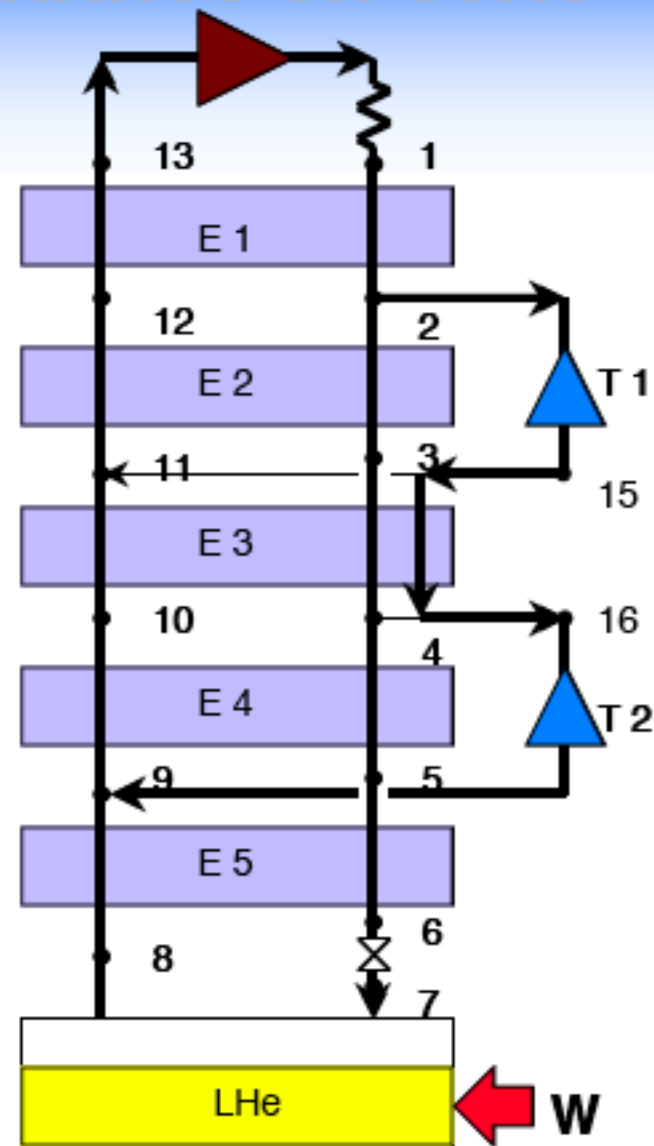
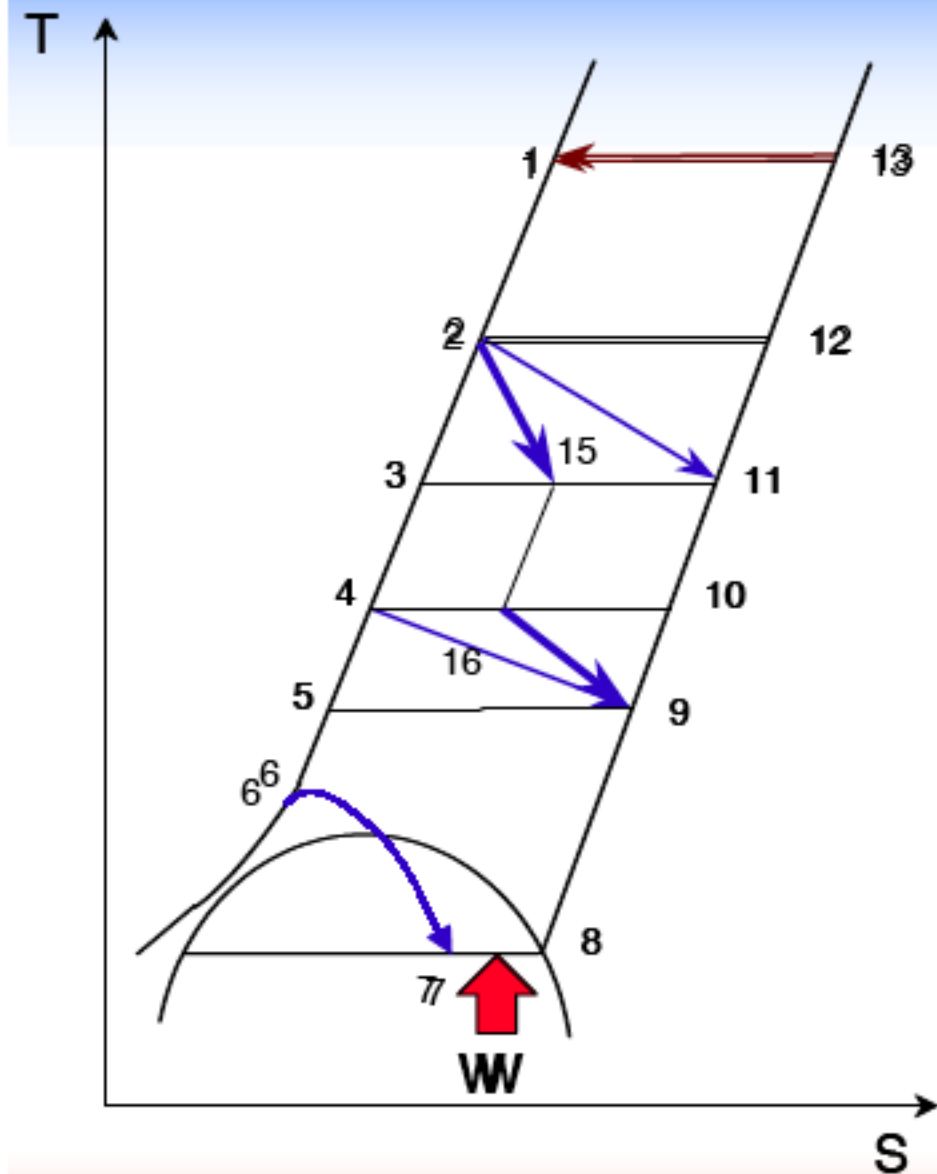


SCHEMA

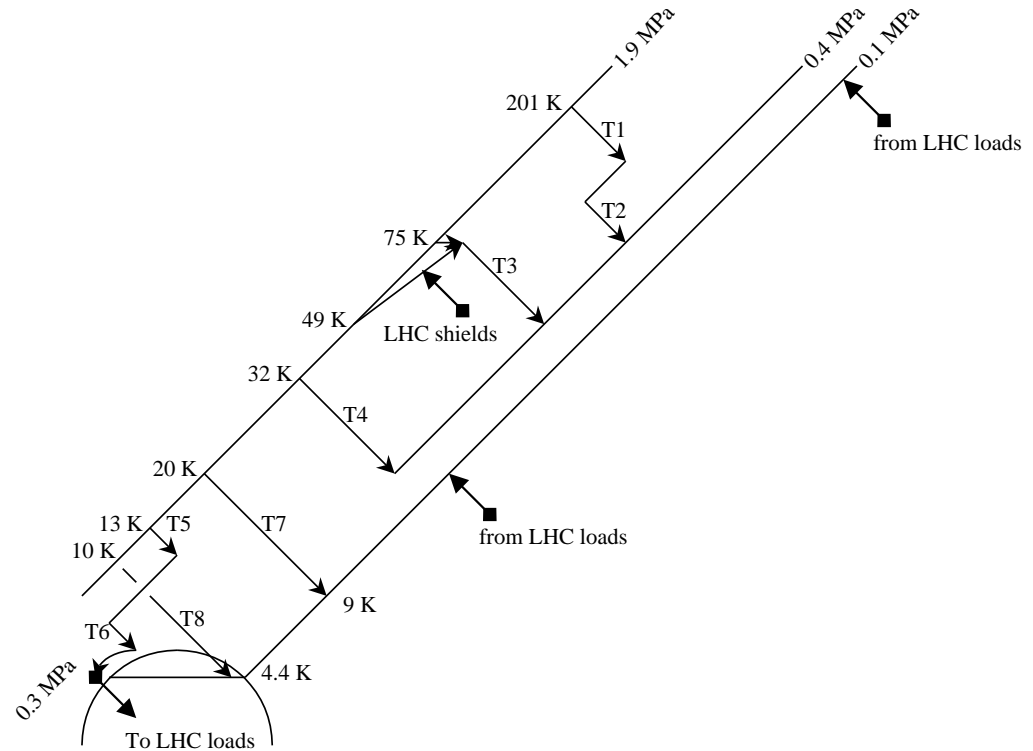
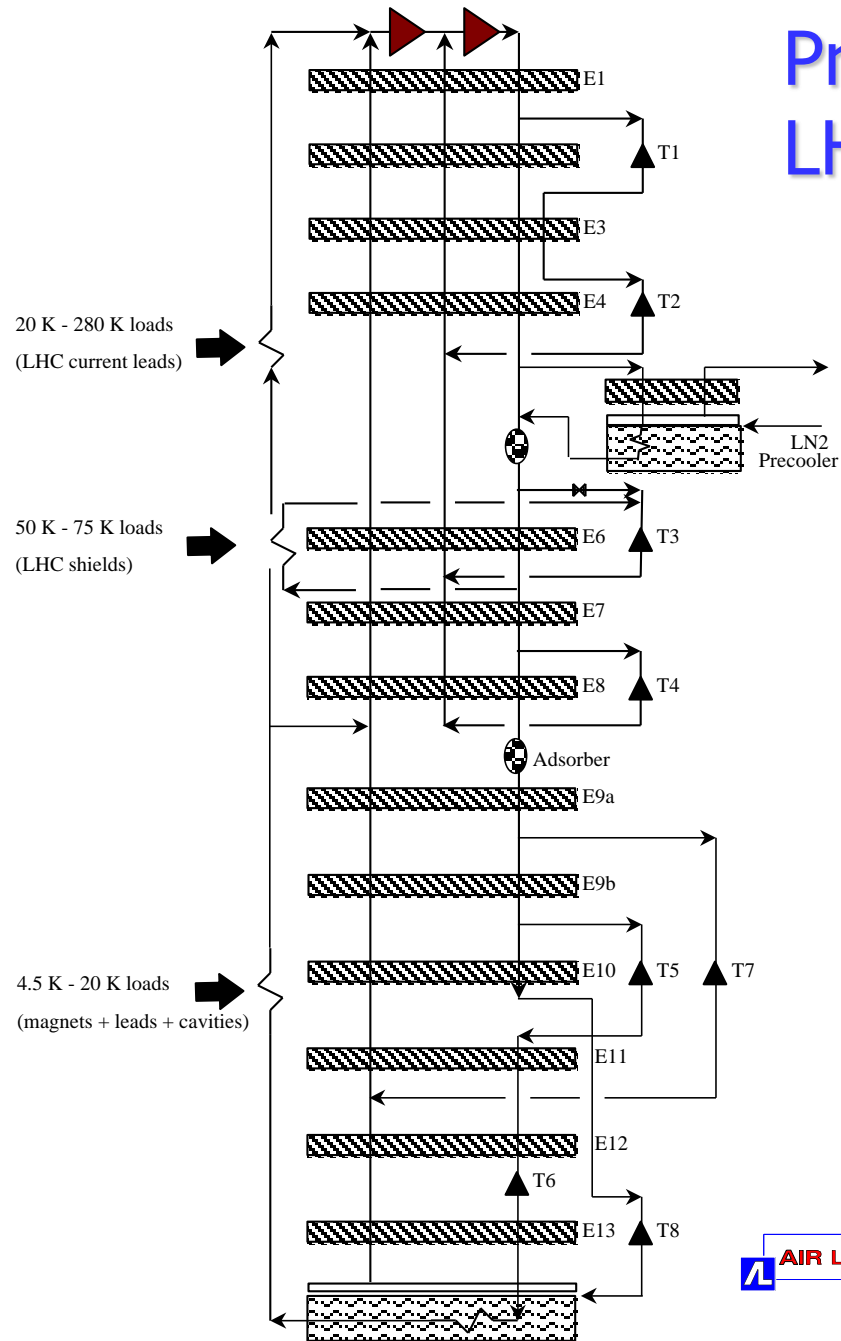
# LE CYCLE DE CLAUDE 1 turbine



# LE CYCLE DE CLAUDE 2 turbines en série

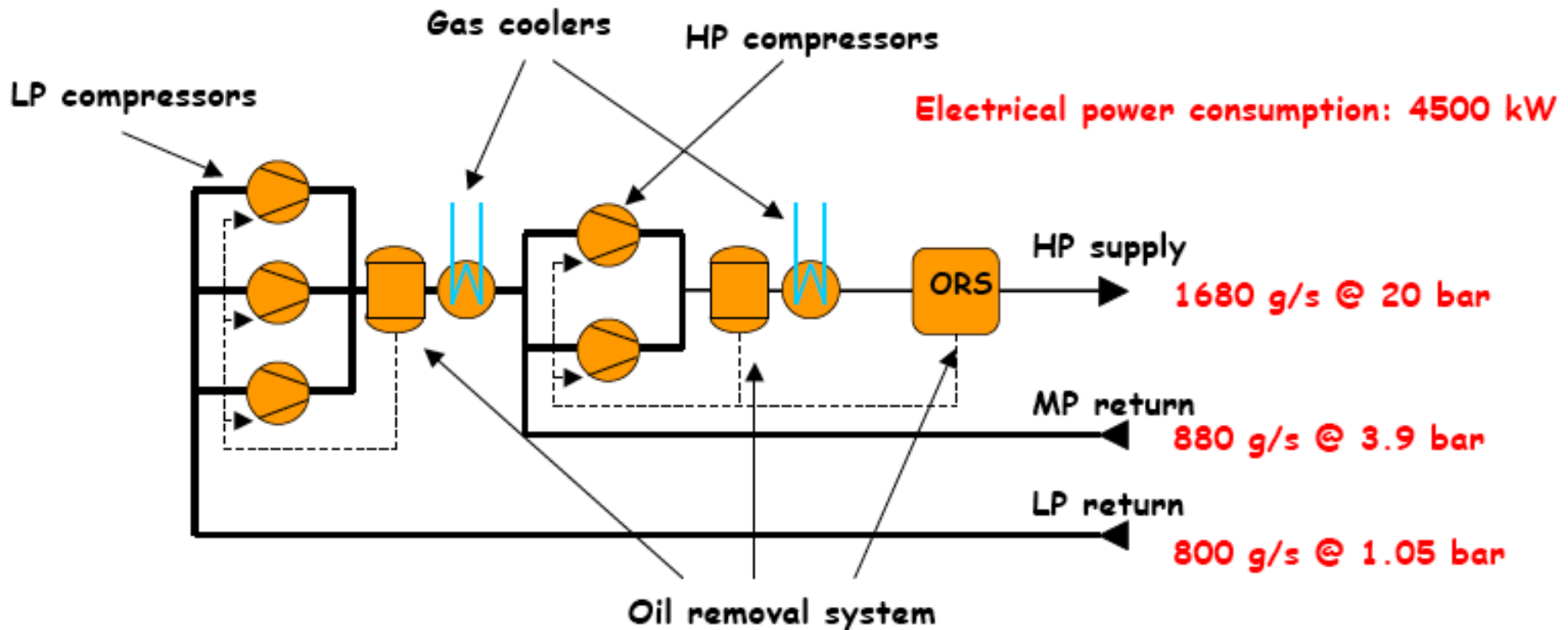


# Process cycle & T-S diagram of LHC 18 kW @ 4.5 K cryoplant



# Process diagram, LHC compressors 18 kW @ 4.5 K

Oil lubricated screw compressors, water cooled, oil separation included



Machine derived from industrial refrigeration (or compressed air)

No more piston (high PR, low flow), not yet centrifugal (high flow, low PR)

# Compressor station of LHC 18 kW@ 4.5 K helium refrigerator

4.2MW input power

Bldg: 15m x 25m



Oil/Helium Coolers

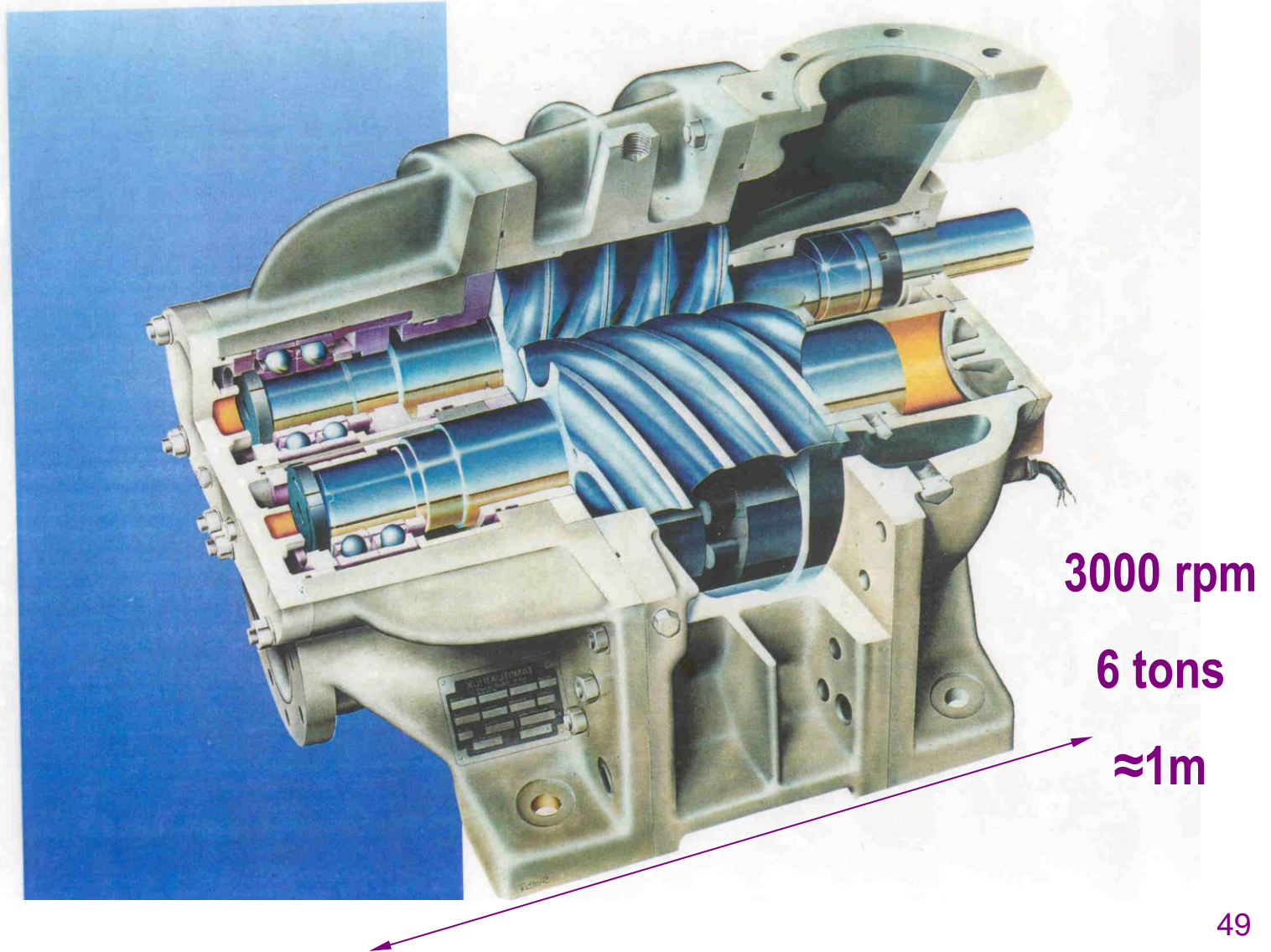
Compressors

Motors

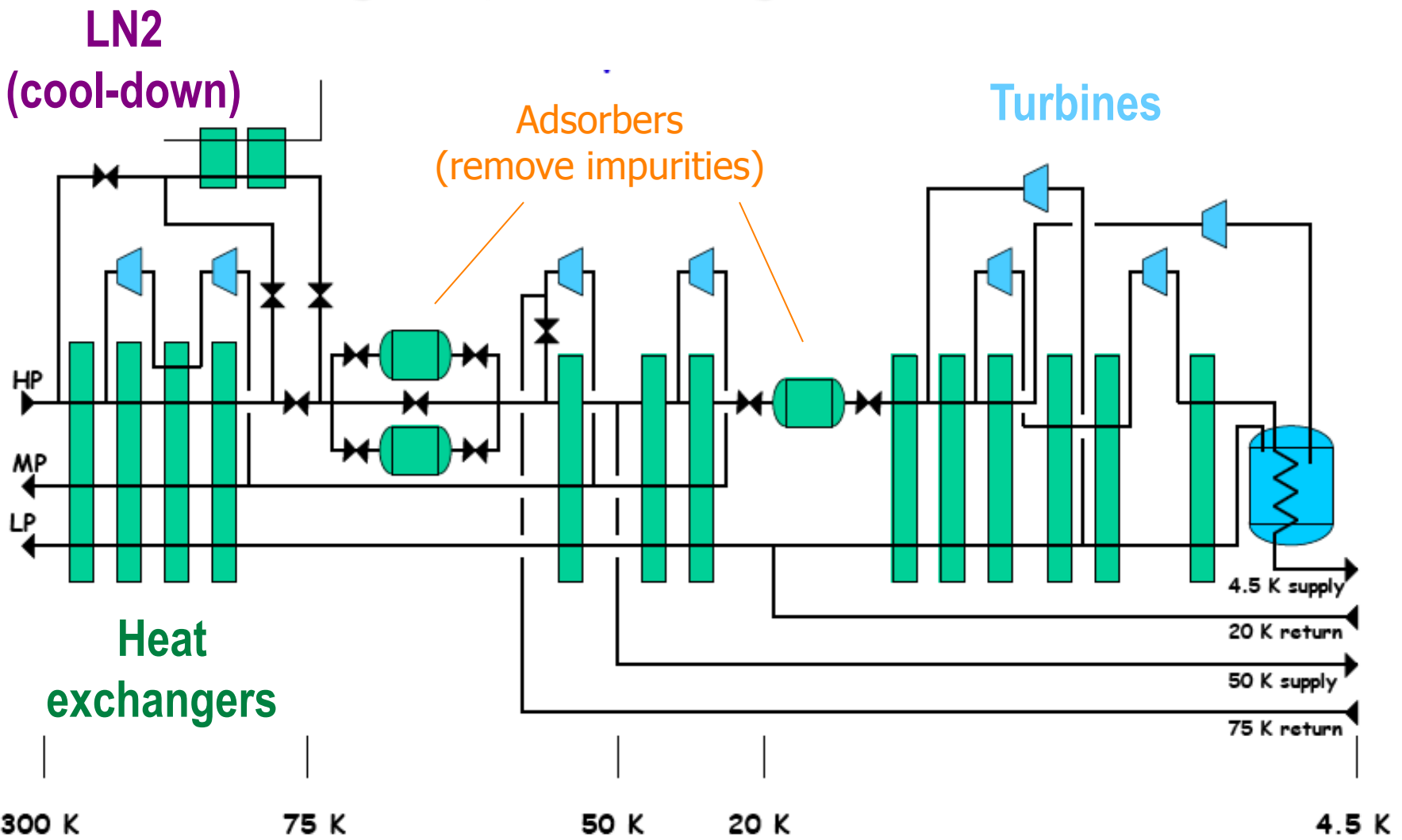


# Oil-injected screw compressor

*(derived from Industrial refrigeration, compressed air)*



# Process diagram, LHC refrigerator 18 kW @ 4.5 K



# LHC 18 kW @ 4.5 K helium cryoplants

33 kW @ 50 K to 75 K, 23 kW @ 4.6 K to 20 K, 41 g/s liquefaction

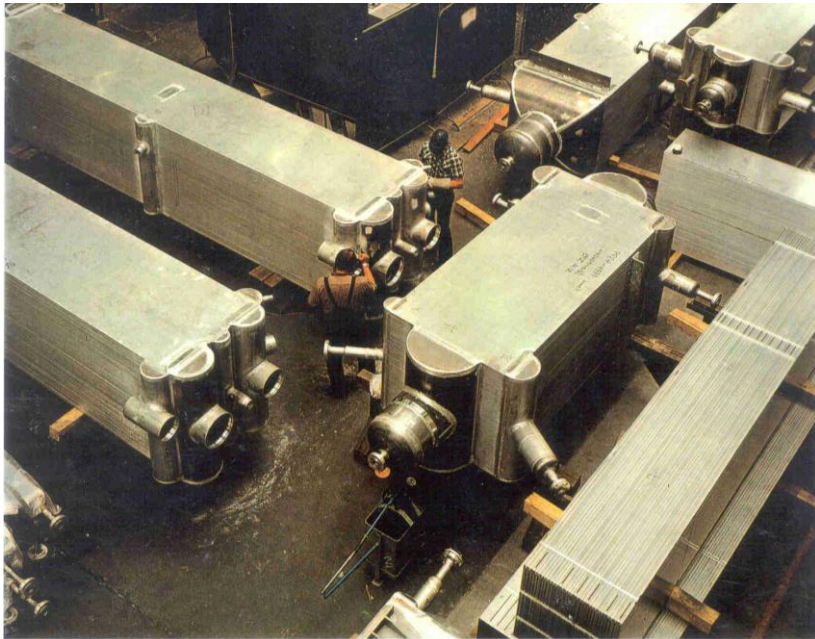
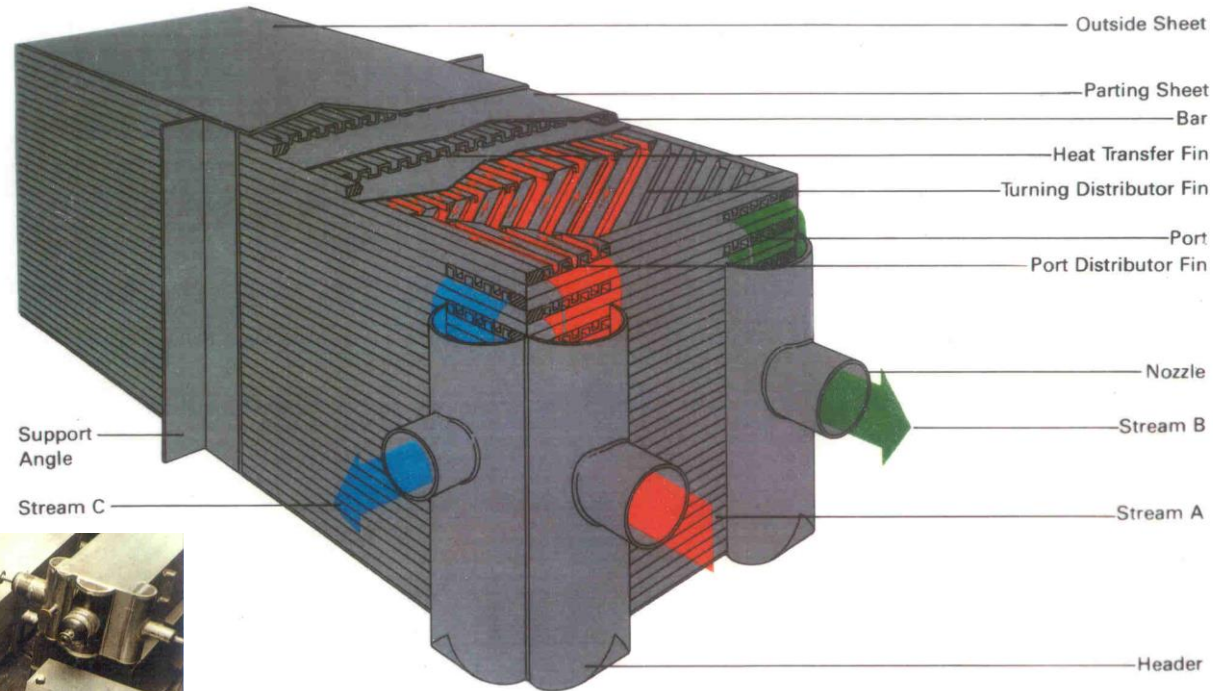
Diameter: 4 m  
Length: 20 m  
Weight: 100 tons  
600 Input/Output signals



Air Liquide 

Linde 

# Brazed aluminium plate heat exchanger

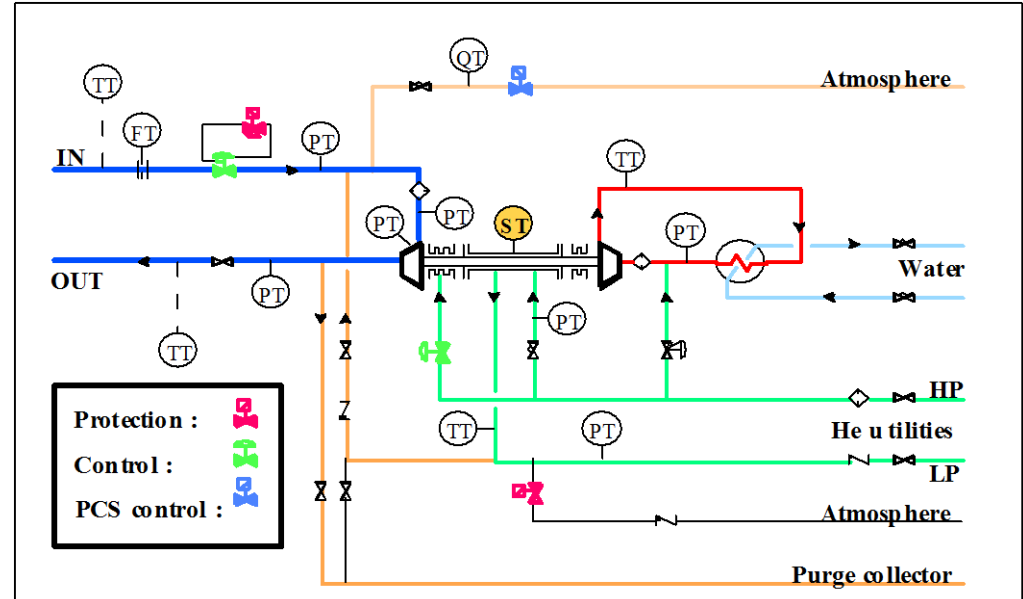
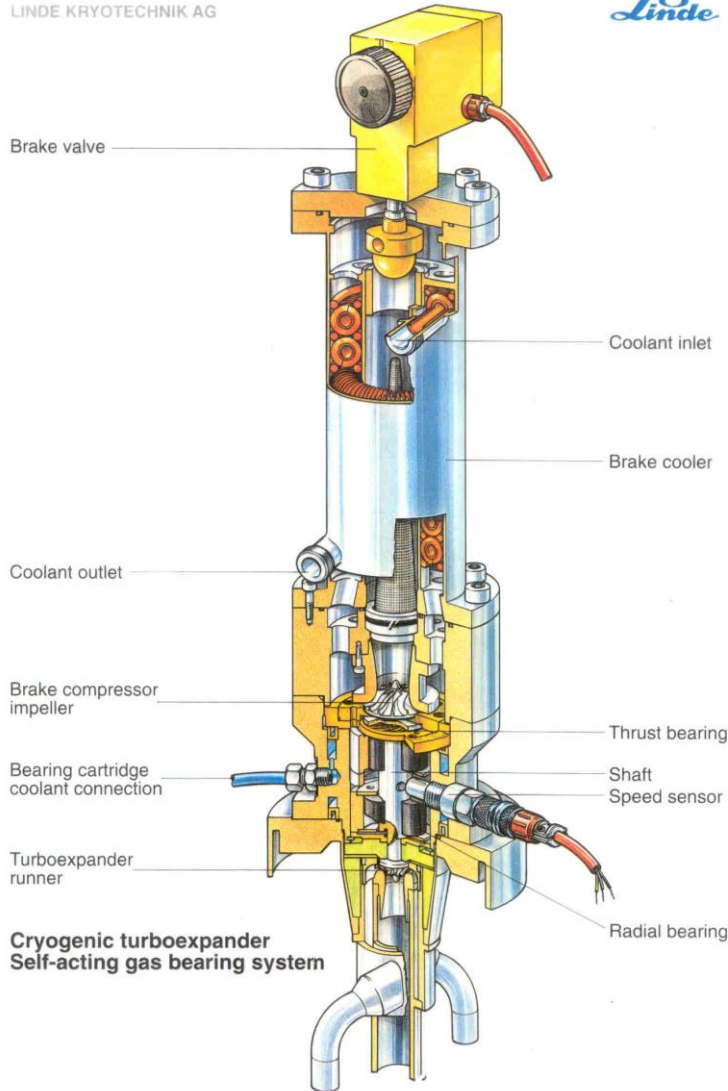


Largest used: 1.4 m x 1.4 m x 8 m  
(10 tons)

# Cryogenic turbo-expander

*Specific technology "contact free" gas bearings operated at 120'000 rpm*

LINDE KRYOTECHNIK AG

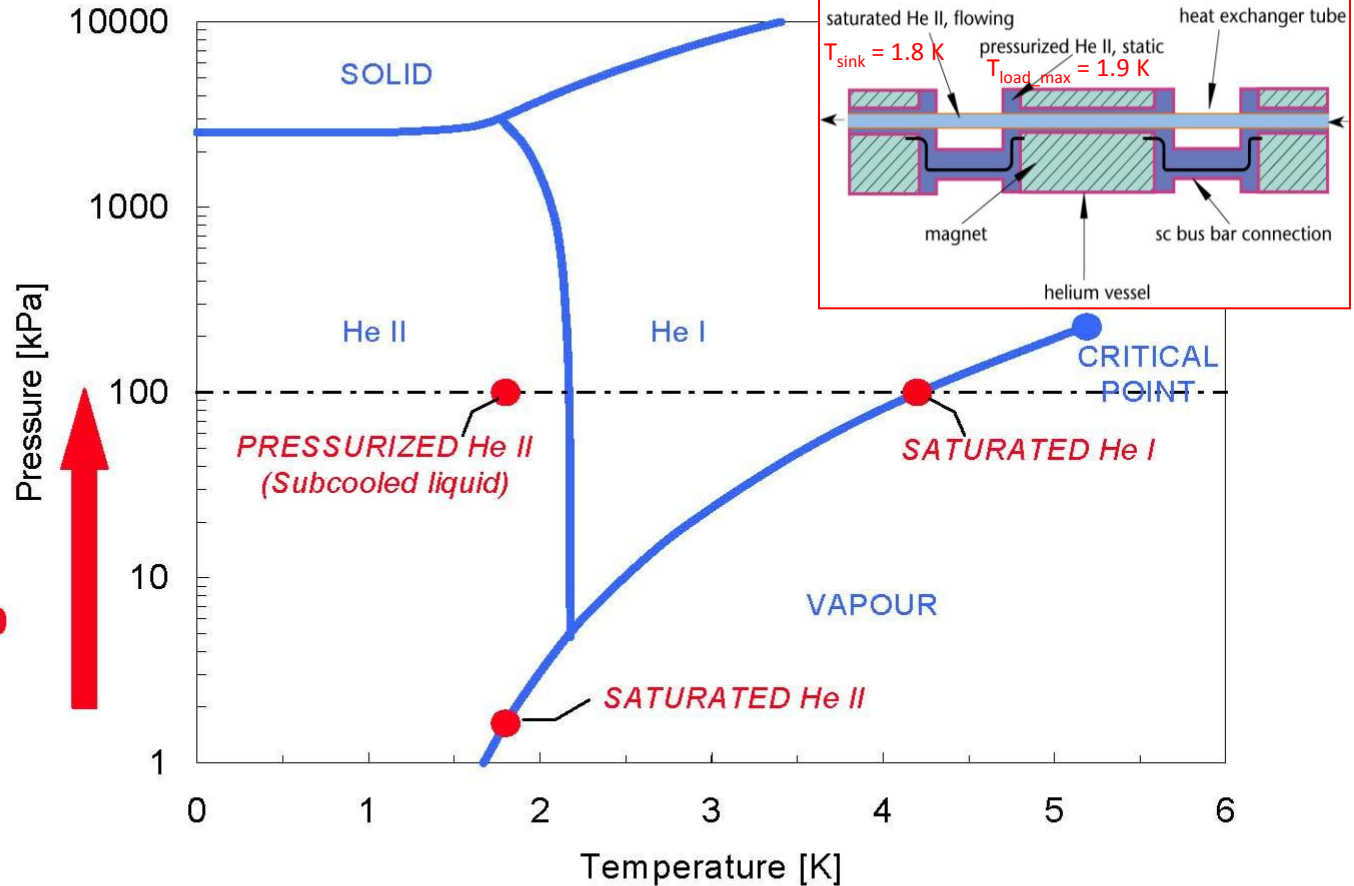


Wheel diameter: 5-15 cm

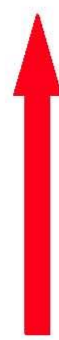
Shaft length: 20 cm

Rotation: 60'000 to 150'000 rpm

# Challenges of power refrigeration at 1.8 K

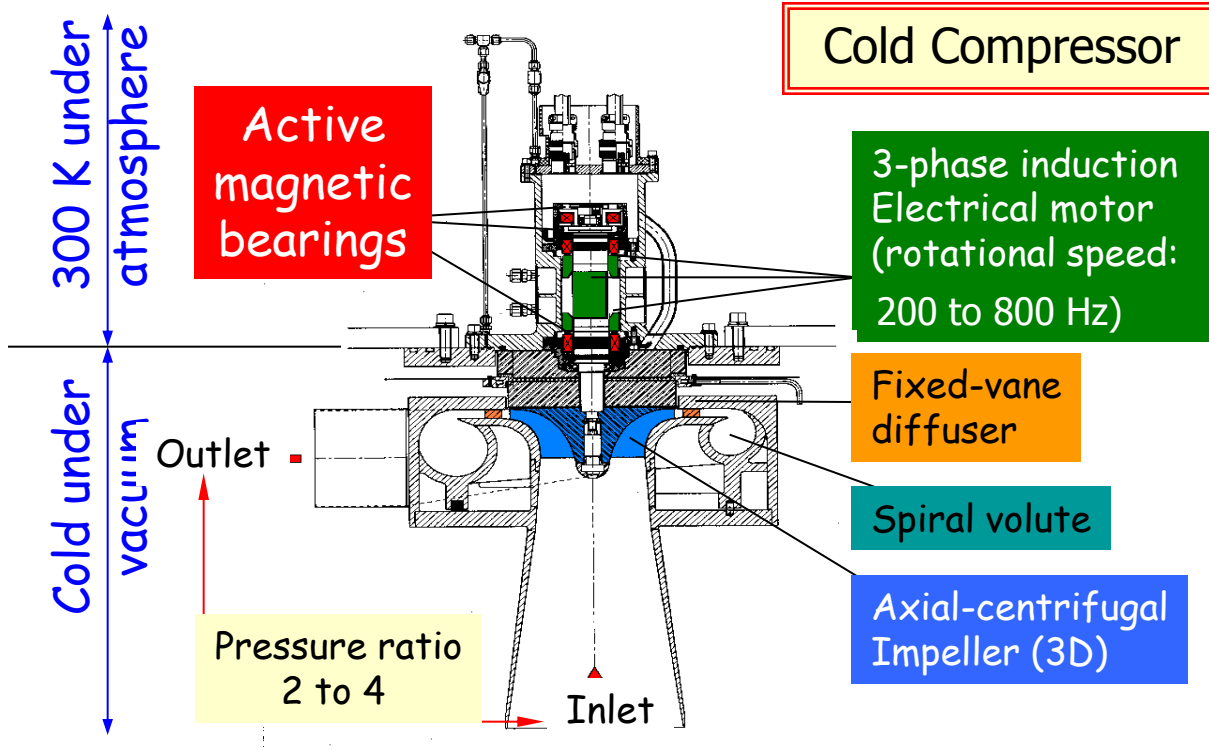


**Compression > 80**



- Compression of large mass flow-rate of He vapor across high pressure ratio  
 ⇒ intake He at maximum density, i.e. cold
- Need contact-less, vane-less machine ⇒ hydrodynamic compressor
- Compression heat rejected at low temperature ⇒ thermodynamic efficiency

# 1.8K Units with cold compressors (x8)



Specific technology to allow large capacity below 2K



# Contents

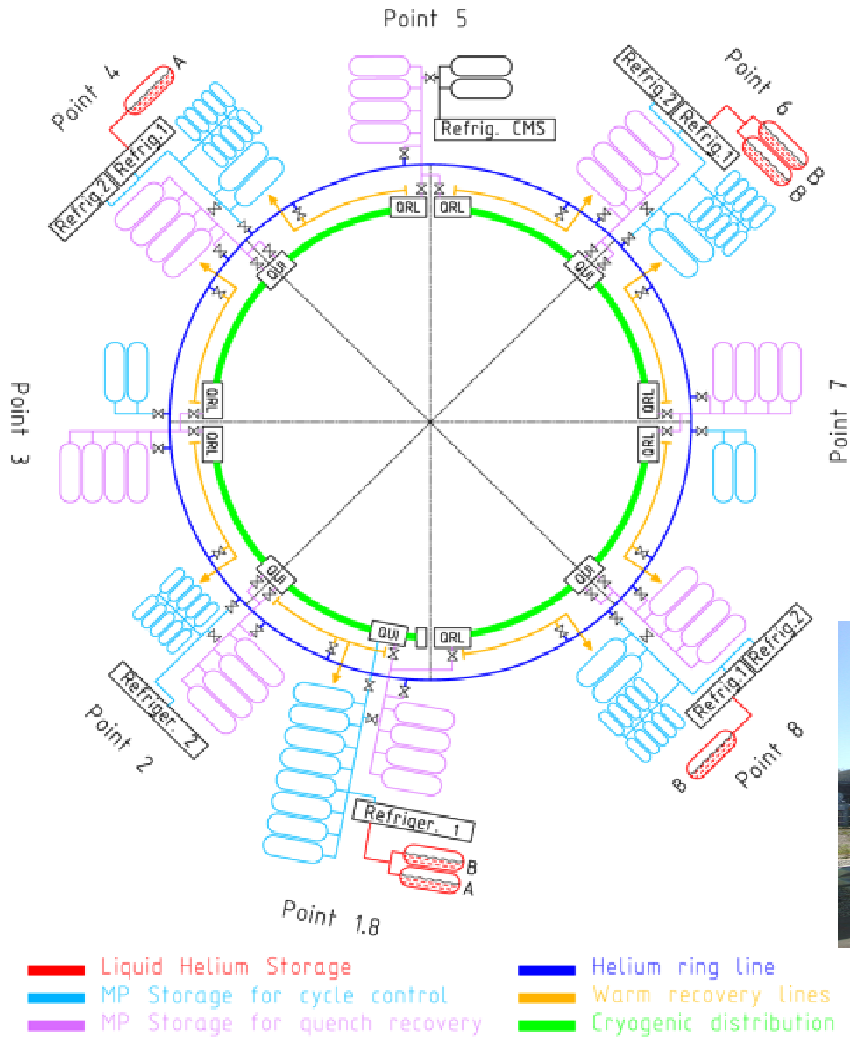
- Introduction
- Cryogenic fluids
- Heat transfer & thermal insulation
- Cryogenic distribution & cooling schemes
- Refrigeration & liquefaction
- **Various complements**
- Concluding remarks, references



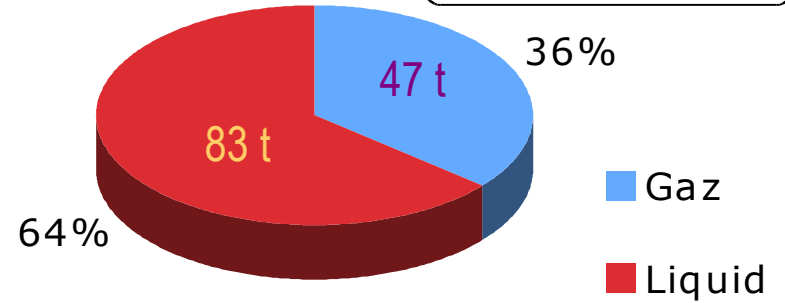
# Safety notes

- Major risks associated with cryogenic fluids at low temperatures:
  - **Asphyxia:** Oxygen is replaced by a pure gas
  - **Cold burns:** in case of contact with cold surfaces
  - **Explosion:** pressure rise in case of warm-up at constant volume (1l Liq  $\approx$  700 l gas)
  - **Embrittlement:** Thermal contractions, potential fragile at cold
- Be informed about valid standards, like for pressure vessels, safety devices, transport of cryogenes, ...

# LHC on-site helium storage



Total storage: 130 t



Total: 6 ,120 m3 LHe



1 LHe 120 m3 tanks

Total: 50 ,GHe 250 m3



2 x 6 GHe 250 m3 tanks

# Bulk Liquid & Gaseous cryogen storage solutions



Deliveries in Liquid form:

- 60 trucks LN2 to cool a LHC sector to 80K (14 days-1'200t)
- 20 trucks for external storage of helium (4 months - 90tons)



250m<sup>3</sup> Gaseous He  
(20B - 850kg He)

# How to deal with impurities

- Any liquid or gas other than helium would solidify during the cooling process. This could block the helium flow or degrade moveable components (valves, turbines)
- Typical treatment applied for: Water, air (N<sub>2</sub> and O<sub>2</sub>), H<sub>2</sub> (adsorption on porous medium like activated charcoal, molecular sieve)

## Recommendation:

- ⇒ evacuation of air once circuits are leak-tight (pur helium)
- ⇒ on-line treatment of what could remain or arrive during operation, with target of fraction of ppm(v)

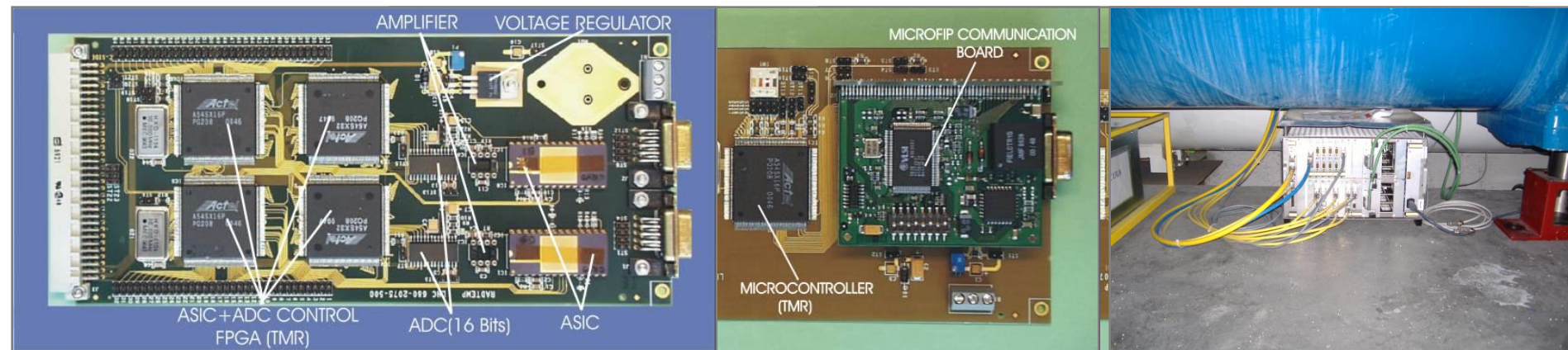
# Thermometry

Industrial instrumentation whenever possible, specific developments when necessary

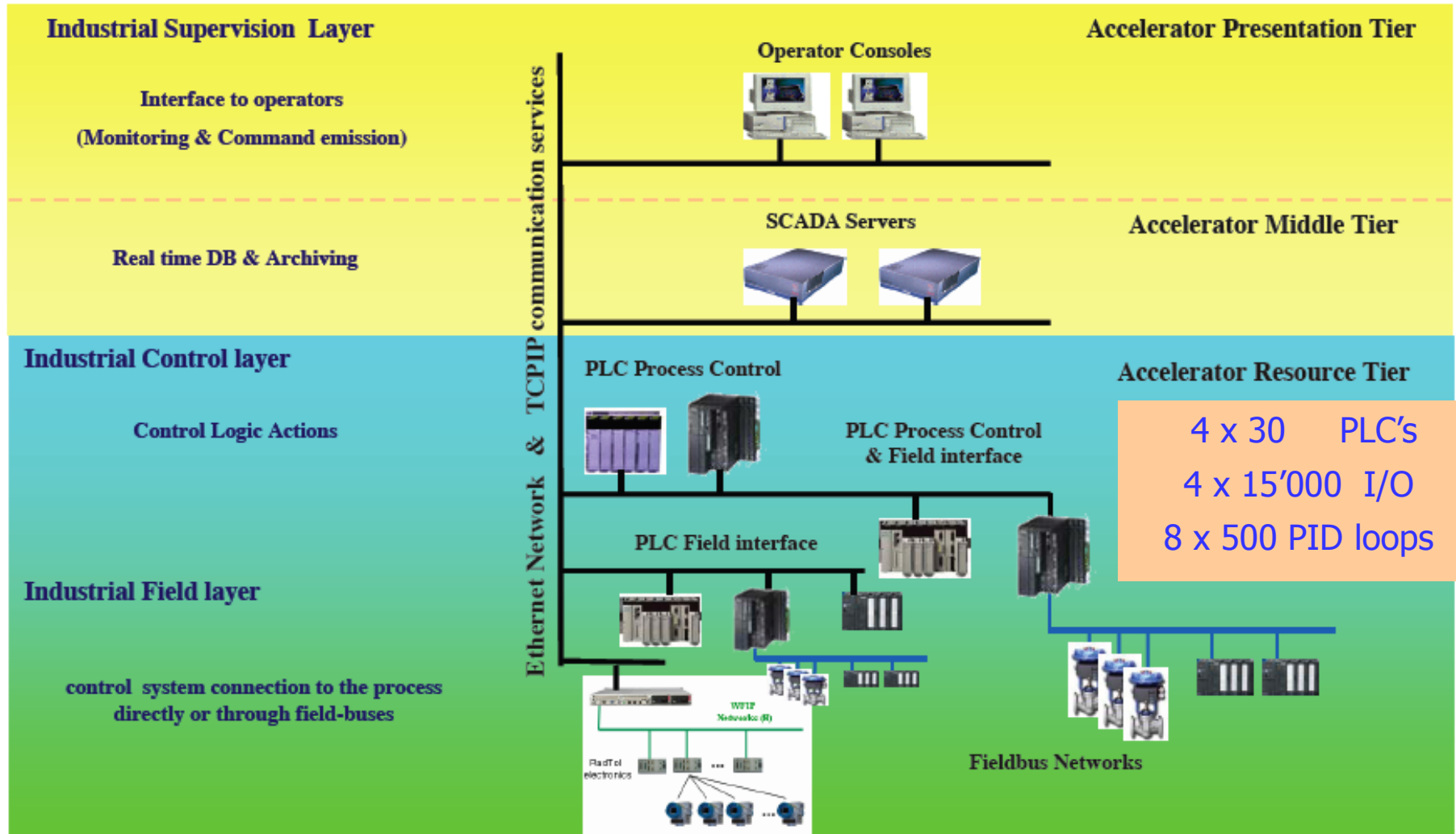
6'000 units, +/- 10 mK @ 2K in LHC radiation conditions



From 'sensor' to 'thermometer' with signal processing



# Industrial Control Architecture



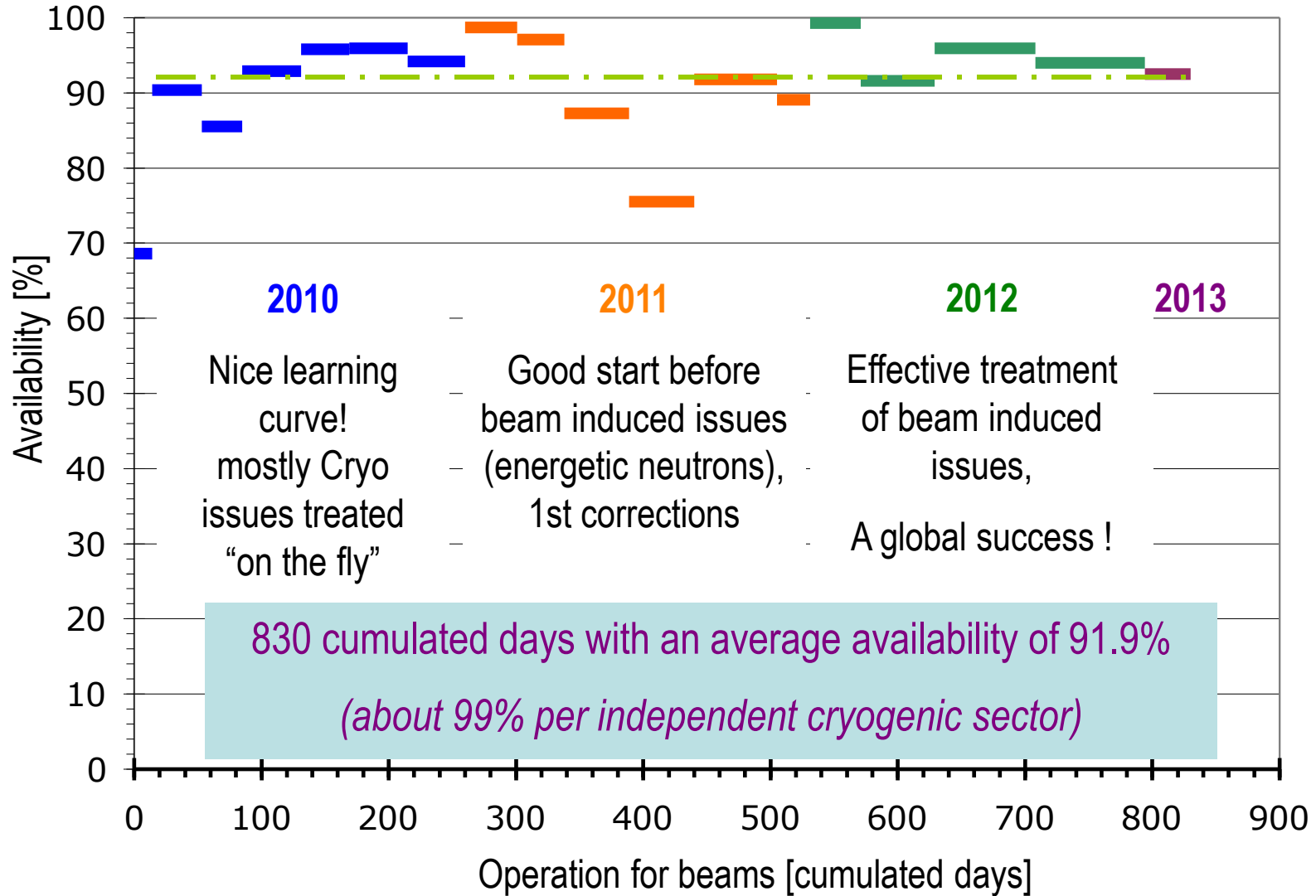
# Cryo operator in Cern Central Control room

Shift 24/7



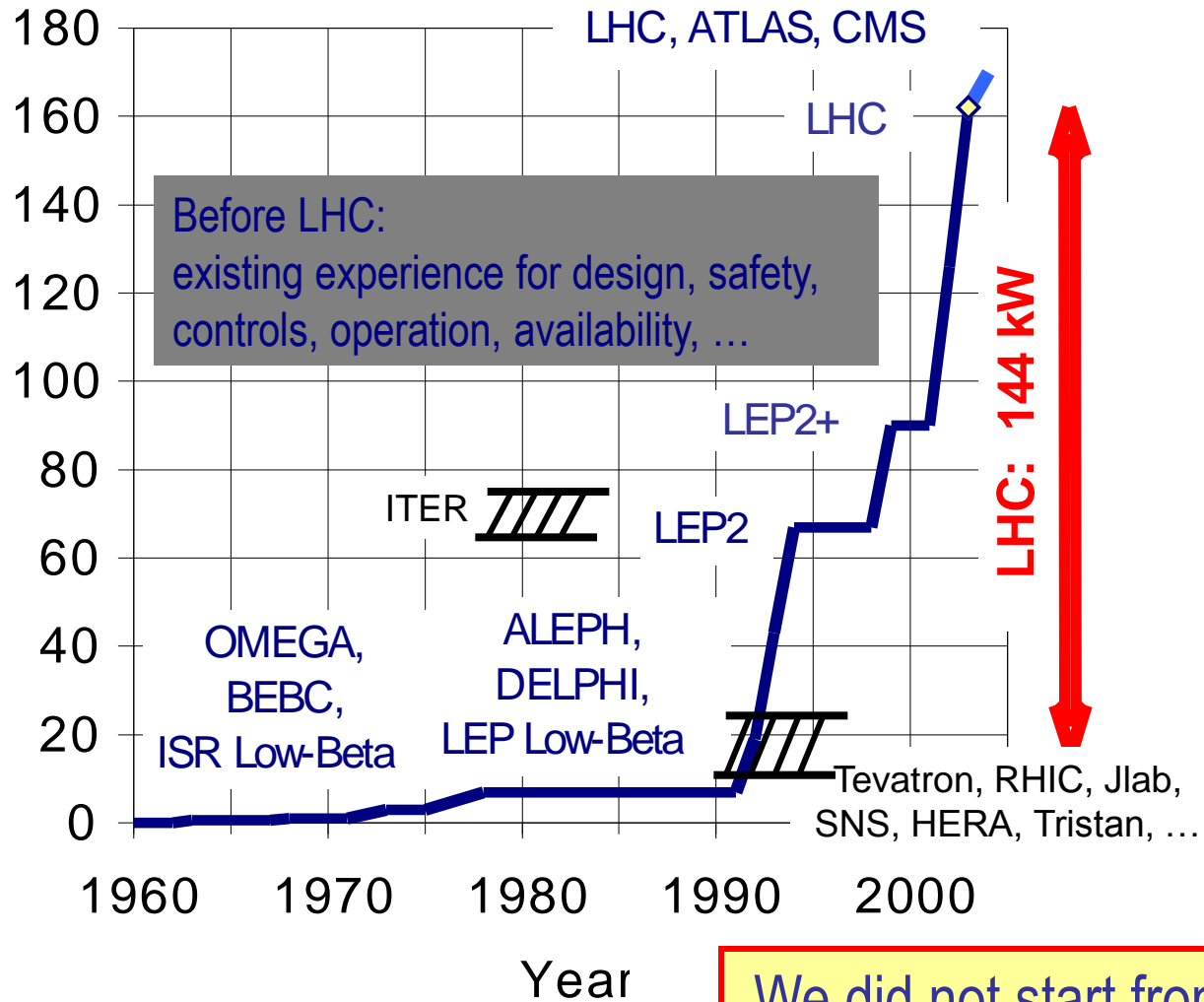
Fully automated, supervised by a single operator

# LHC Cryo global availability





# How does it compare ?



# Concluding remarks

- Cryogenics serving superconducting systems is now part of all major accelerators and future projects.
- While advanced applications tend to favor "below 2K", many almost industrial applications are based on "4.5K" and RnD (or demonstrators) continues for "high temperature" applications
- If cryogenic engineering follows well defined rules and standards, there are variants depending on boundary conditions, continents, time of a project...

I could only recommend that demonstrated experience be evaluated and adapted to specific requirements you may have !

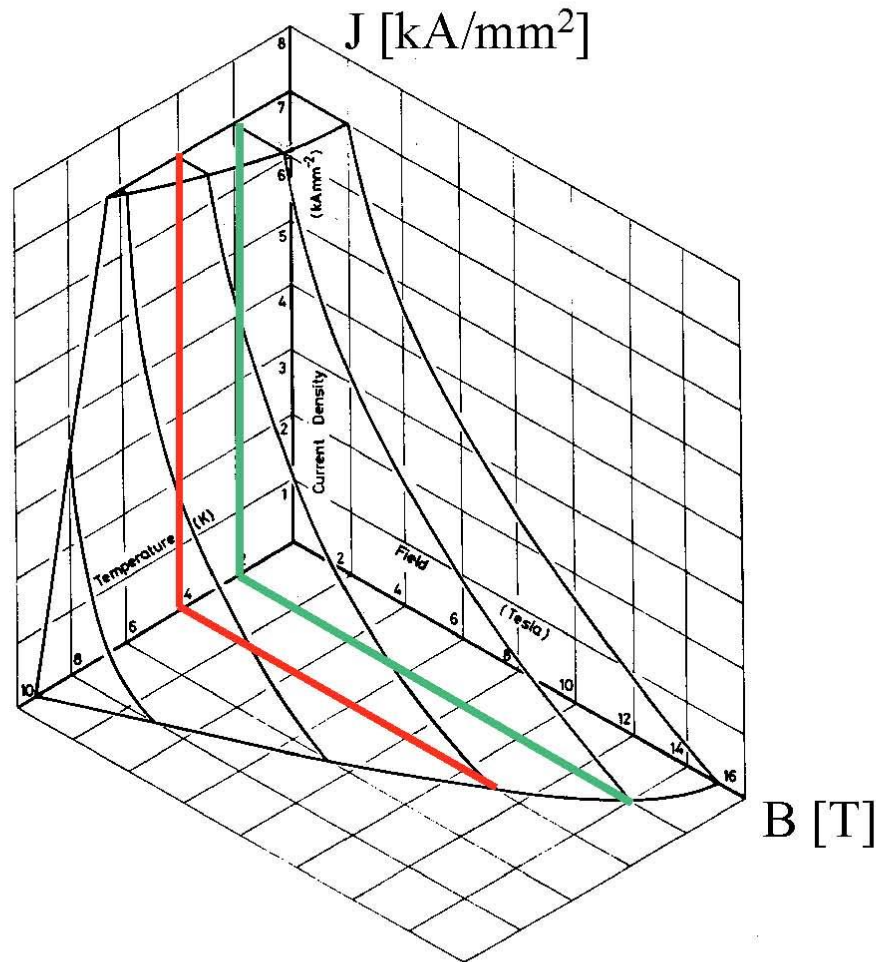
*Thanks for your attention,  
and hoping you would (now) be more aware with cryogenics !!!*

## Some references

- K. Mendelssohn, *The quest for absolute zero*, McGraw Hill (1966)
- R.B. Scott, *Cryogenic engineering*, Van Nostrand, Princeton (1959)
- G.G. Haselden, *Cryogenic fundamentals*, Academic Press, London (1971)
- R.A. Barron, *Cryogenic systems*, Oxford University Press, New York (1985)
- B.A. Hands, *Cryogenic engineering*, Academic Press, London (1986)
- S.W. van Sciver, *Helium cryogenics*, Plenum Press, New York (1986)
- K.D. Timmerhaus & T.M. Flynn, *Cryogenic process engineering*, Plenum Press, New York (1989)
- Proceedings of *CAS School on Superconductivity and Cryogenics for Particle Accelerators and Detectors*, Erice (2002) (+2013)
  - U. Wagner, *Refrigeration*
  - G. Vandoni, *Heat transfer*
  - Ph. Lebrun, *Design of a cryostat for superconducting accelerator magnet*
  - Ph. Lebrun & L. Taviani, *The technology of superfluid helium*
- Proceedings of ICEC and CEC/ICMC conferences

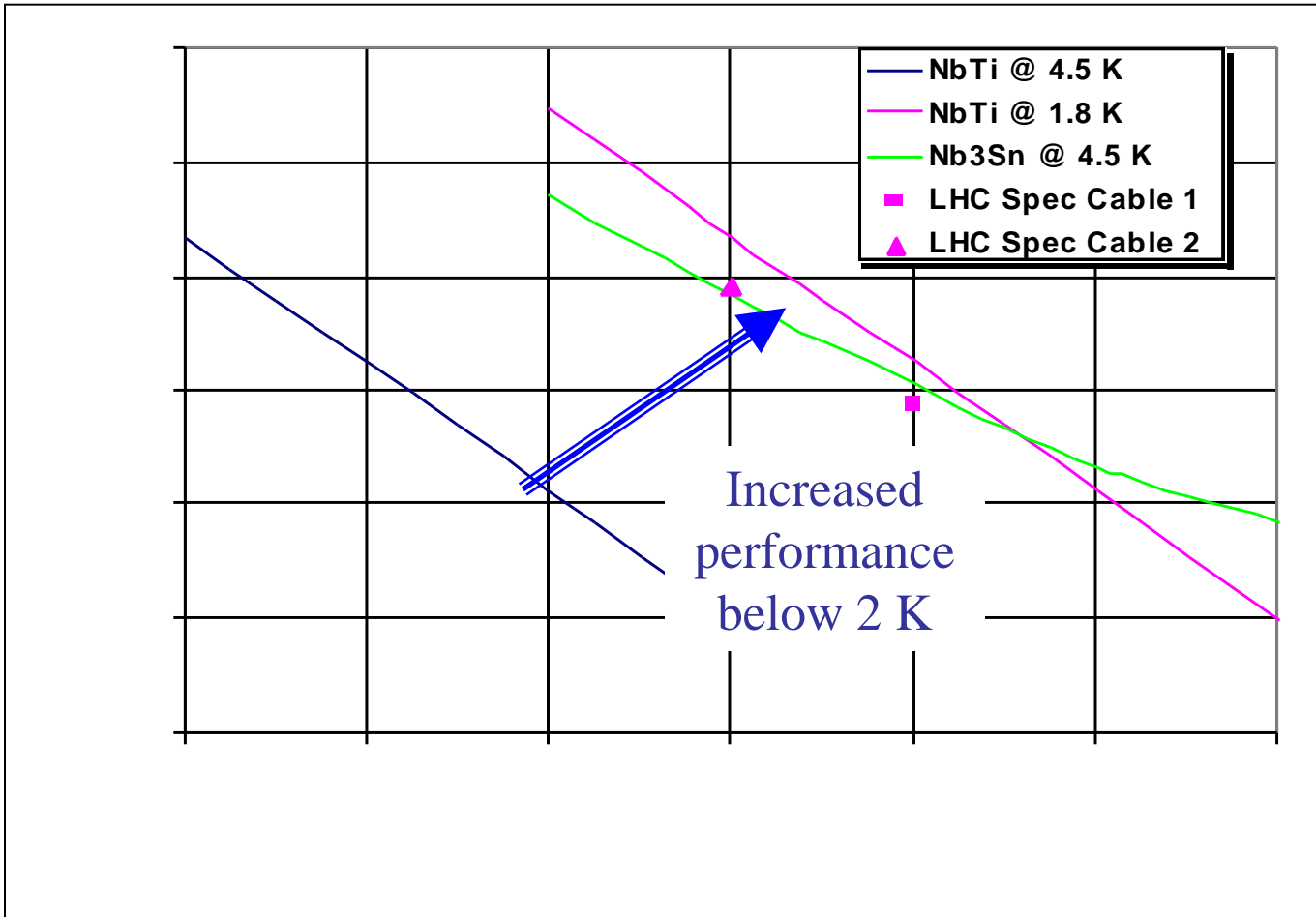
**Bonus slides**

# Operating temperature & performance of superconductors

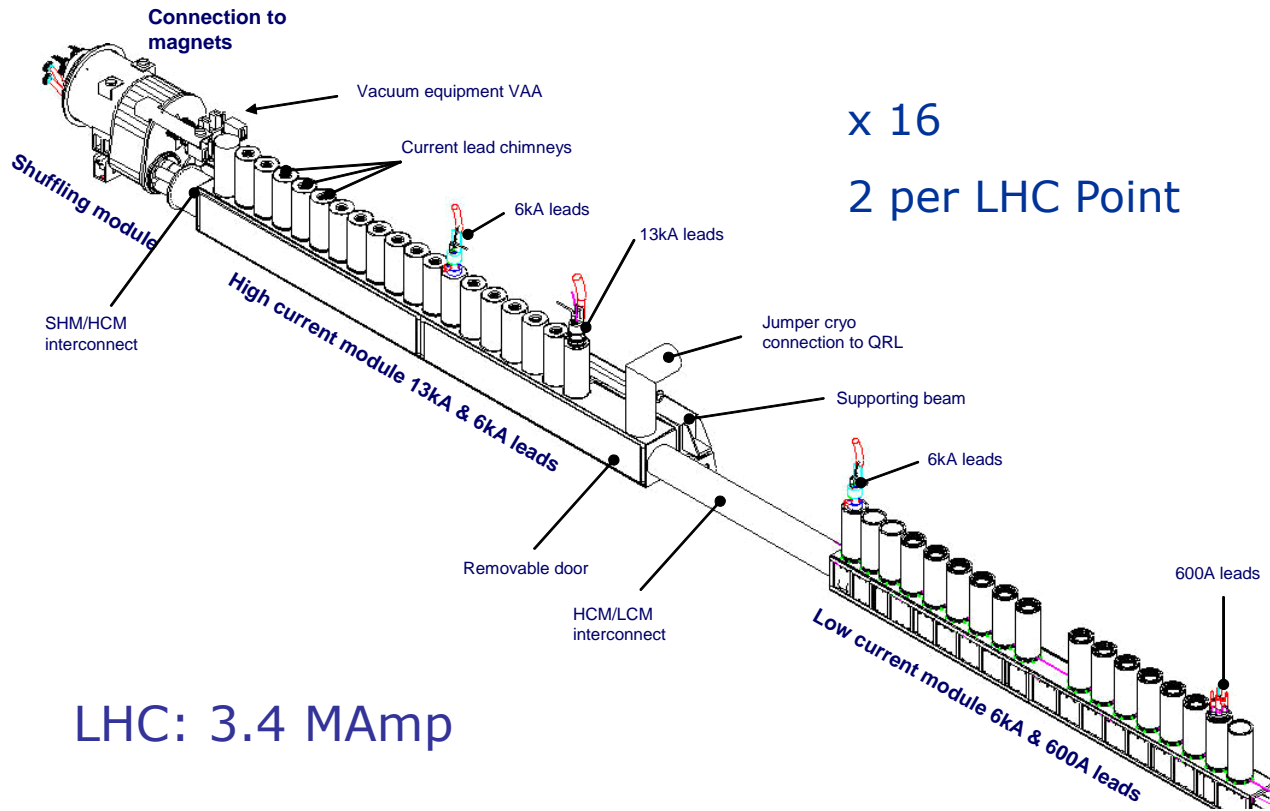


- Superconductivity only exists in a limited domain of temperature, magnetic field and current density
- Electrotechnical applications require transport current and magnetic field
- Operating temperature of the device must therefore be significantly lower than the critical temperature of the superconductor

# Superconducting magnets



# Electrical Feed Box for current leads



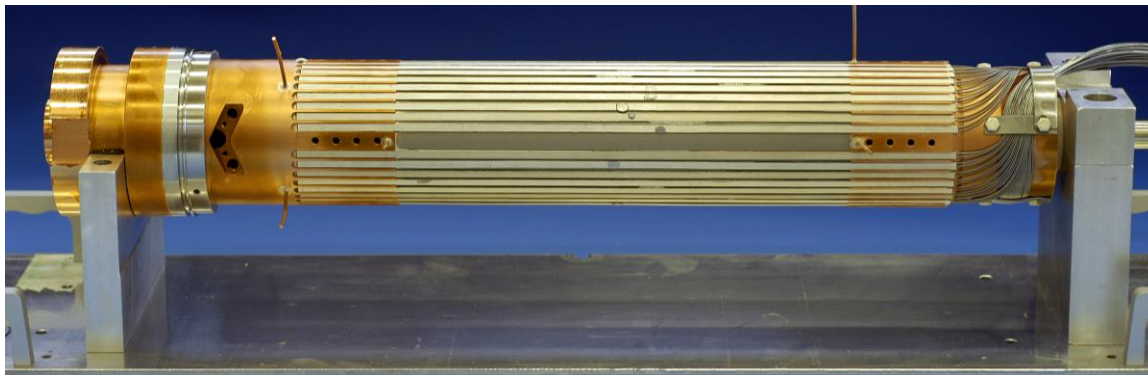
LHC: 3.4 MAmp

1.9K

4.5K

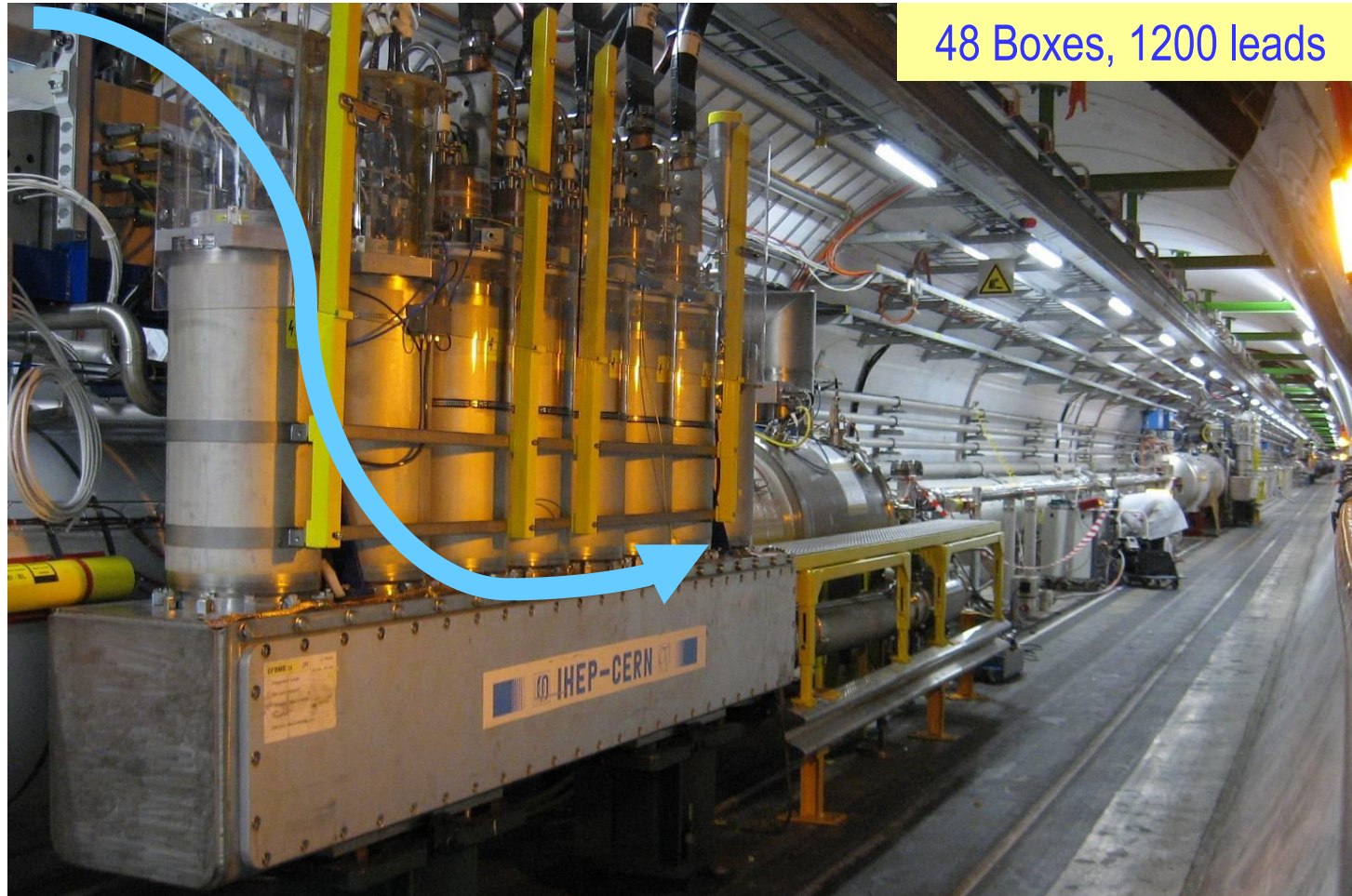
# Beating the WFL law: HTS current leads

- The WFL law essentially states that good electrical conductors are also good thermal conductors
- Current leads need good electrical conductors with low thermal conductivity
- Superconductors are bad thermal conductors with zero resistivity
- Build current lead with superconductor up to temperature as high as possible, i.e. HTS





## Electrical feed boxes for current leads



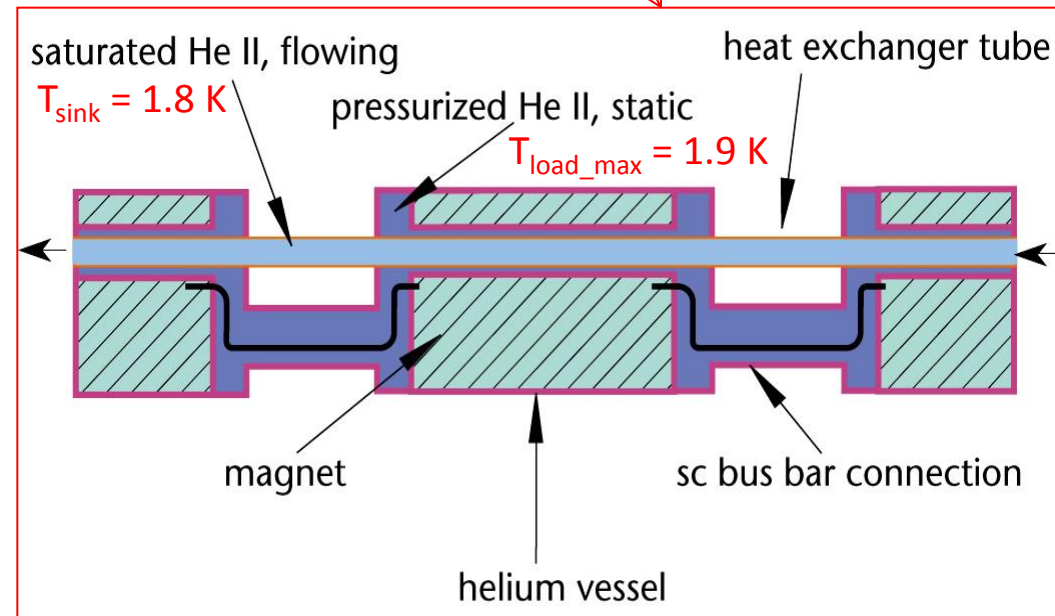
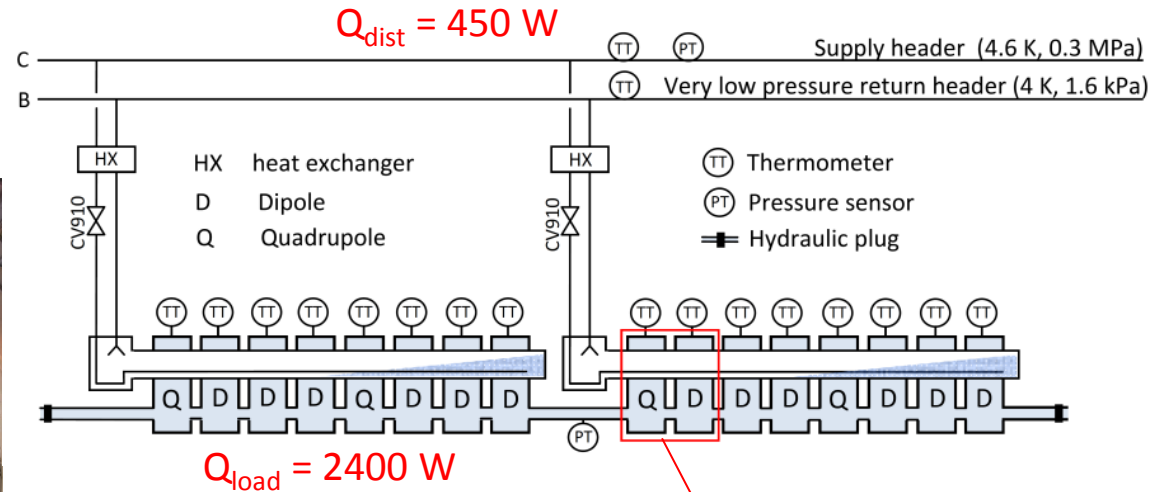
More than 10'000 Amperes per chimney, from room temperature down to 4.5K in about a meter

# LHC sector cooling scheme

Pressurized/saturated He II

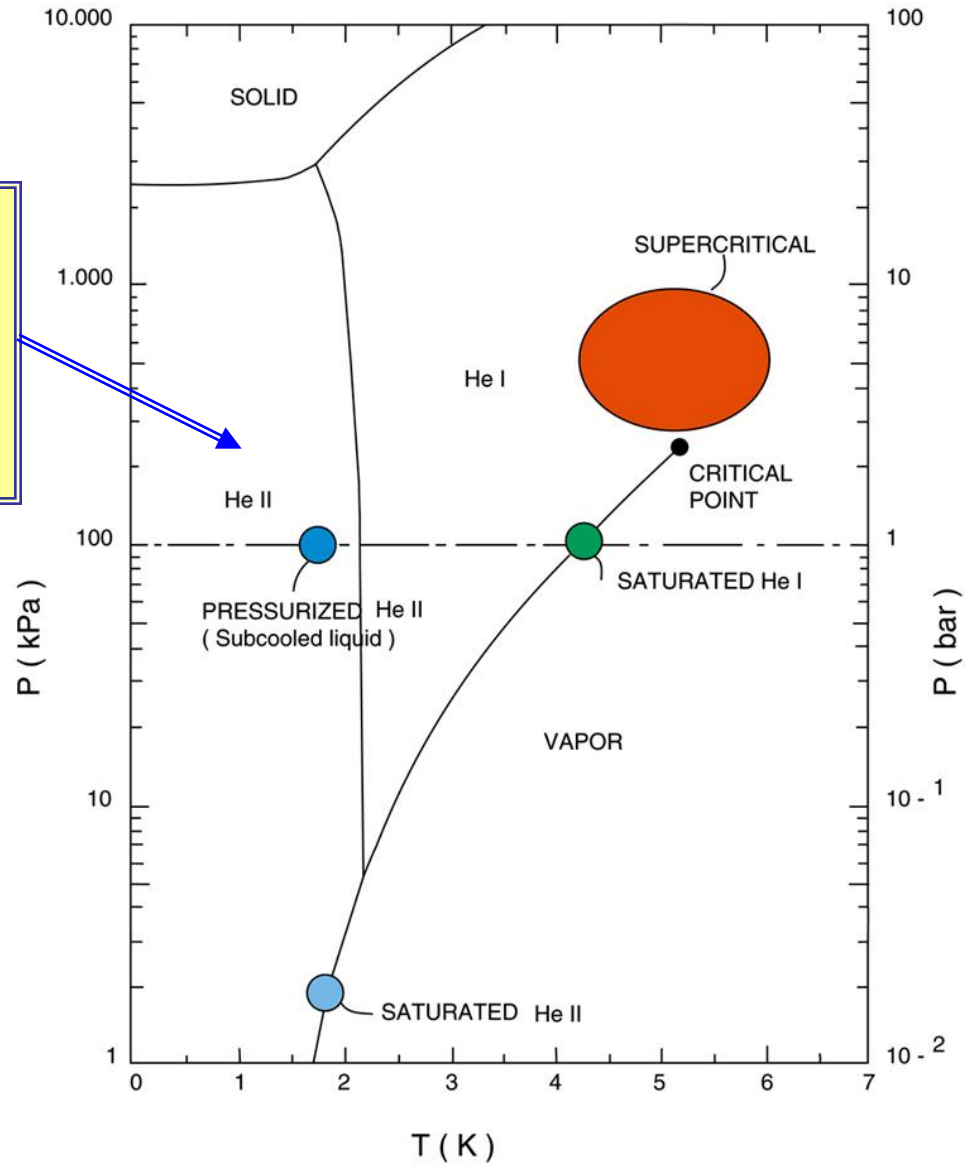


37'500 tons at 1.9 K



# Helium phase diagram

Superfluid Helium:  
- Lower viscosity  
- Larger heat transfer capacity



# Basic thermodynamics at low temperature

- Minimum refrigeration work  $W_{\min}$  to extract heat  $Q$  at temperature  $T$  and reject it at ambient temperature  $T_a$

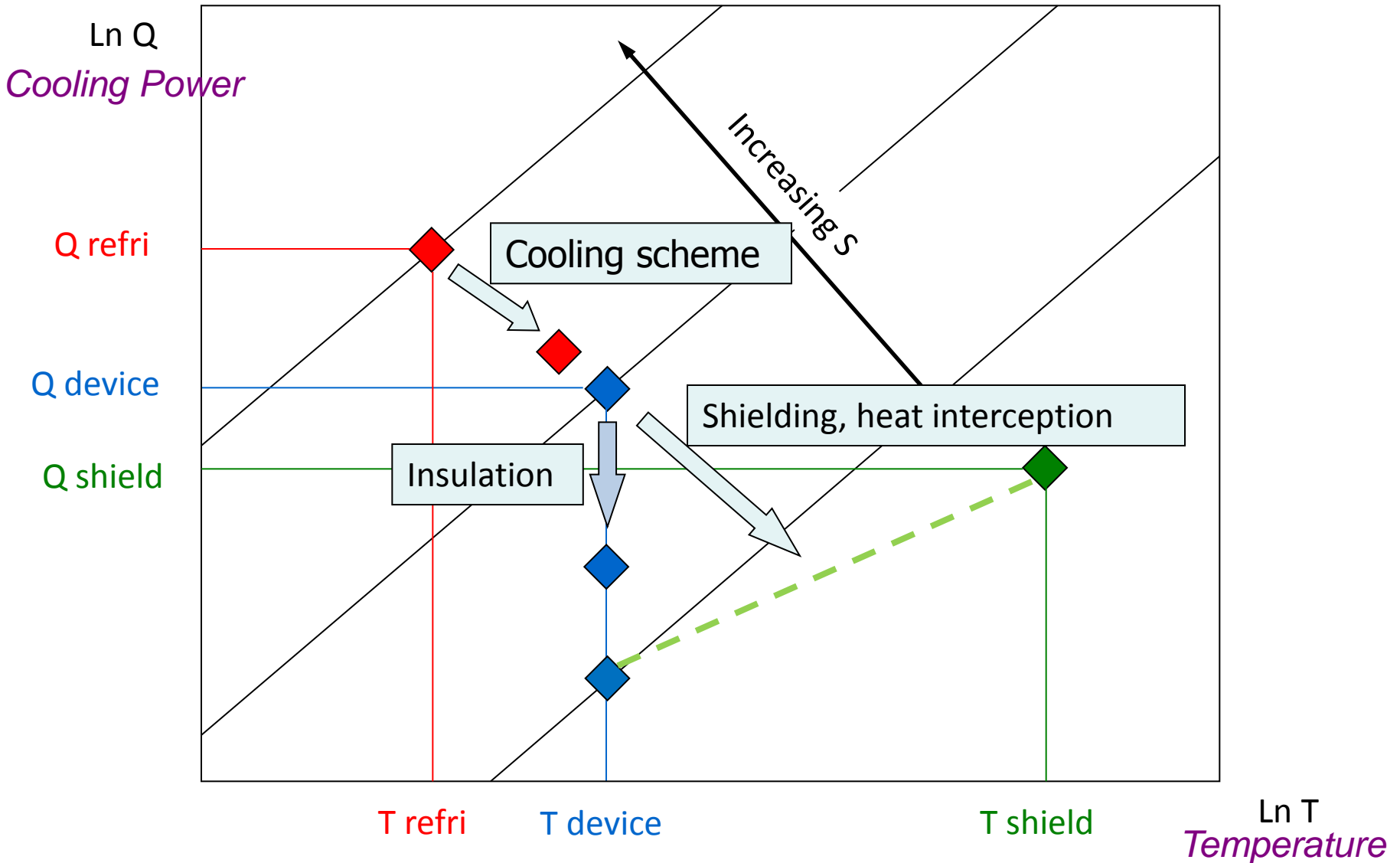
$$W_{\min} = Q (T_a/T - 1) = T_a \Delta S - Q$$

- At cryogenic temperature  $T \ll T_a$

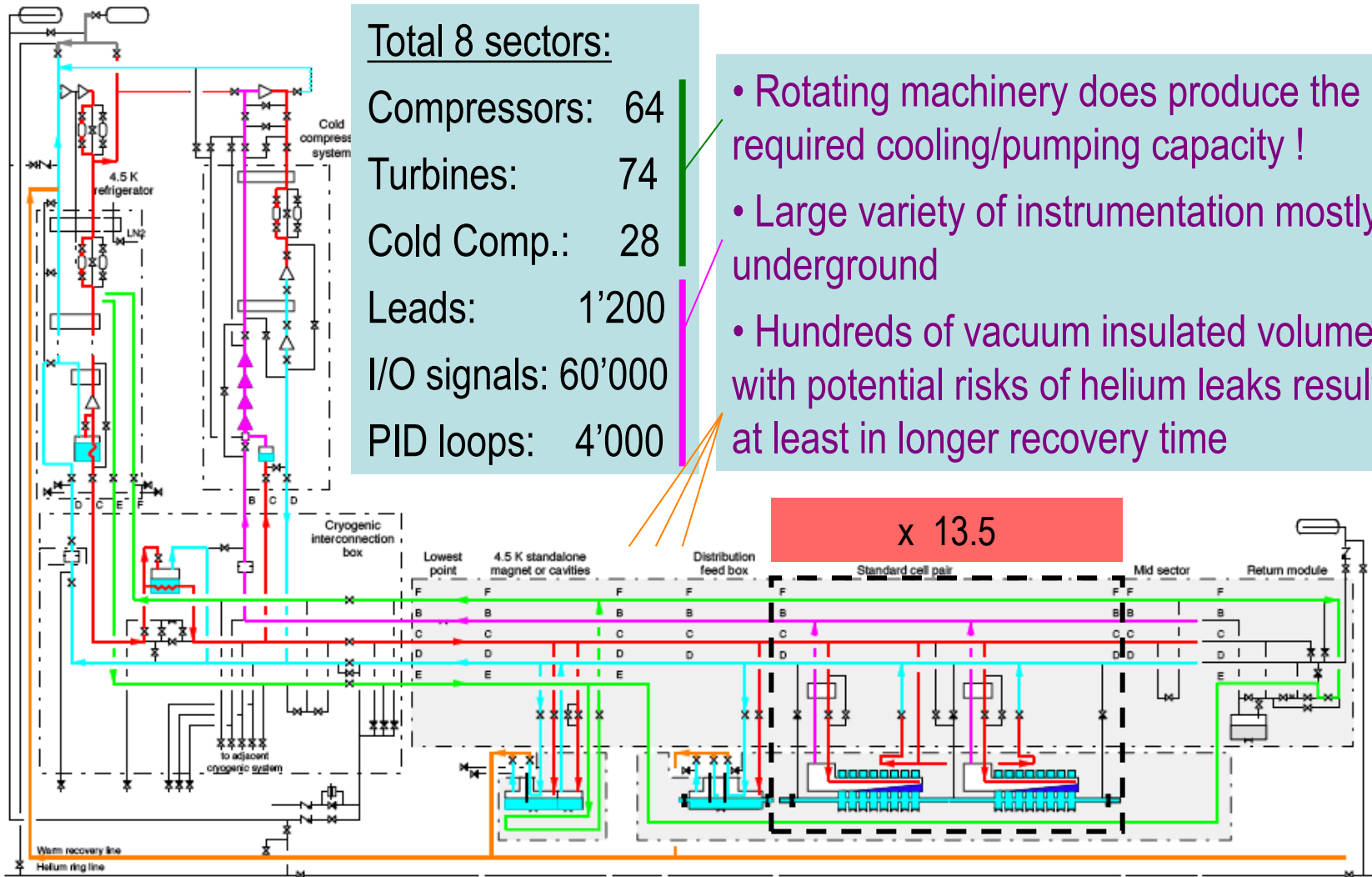
$$W_{\min} \approx Q T_a/T \approx T_a \Delta S$$

- entropy is a good measure of the cost of cryogenic refrigeration
- strategies minimizing  $\Delta S$  improve cryogenic design

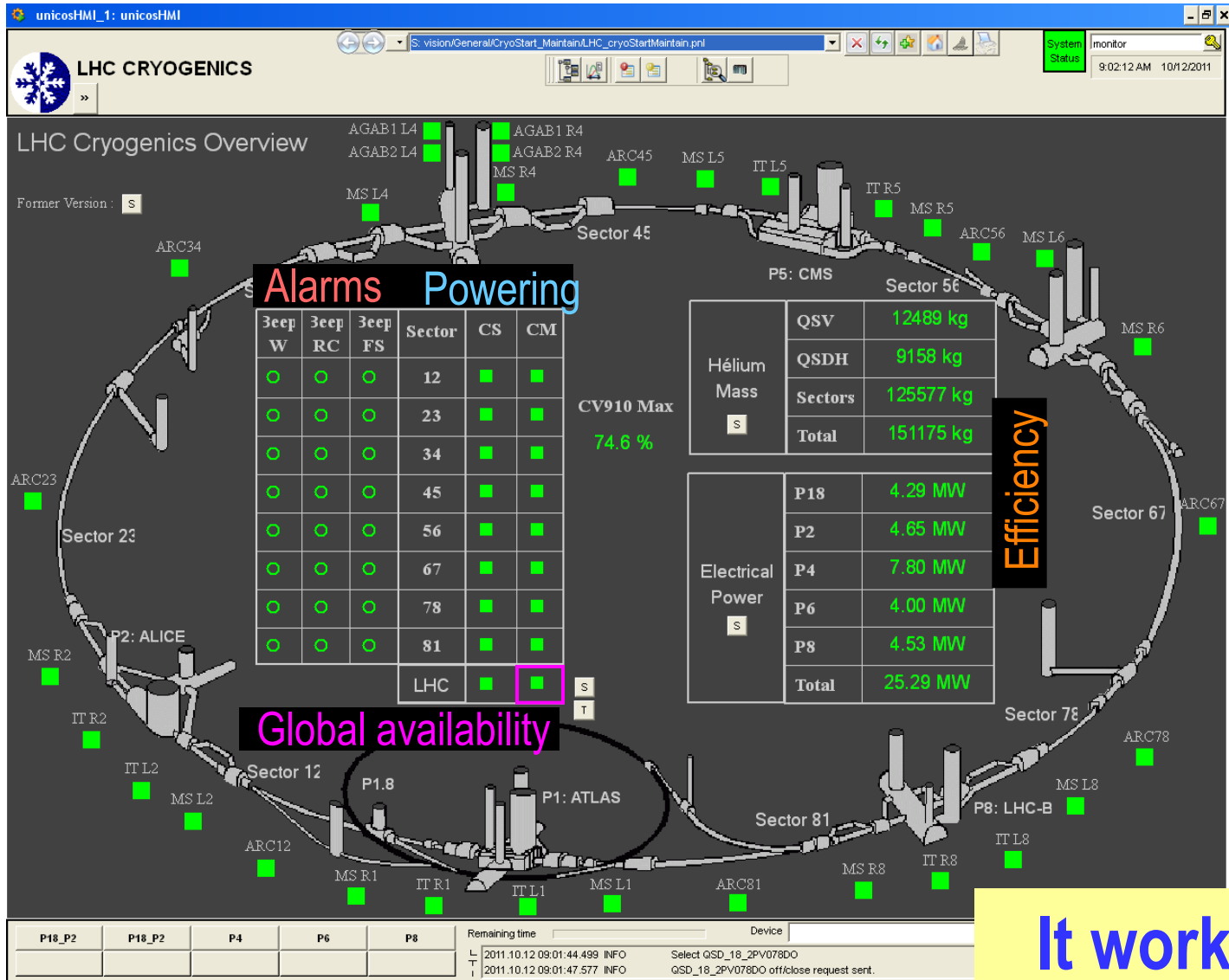
# Cryogenic design strategies



# 1/8e of LHC: production-distribution-magnets

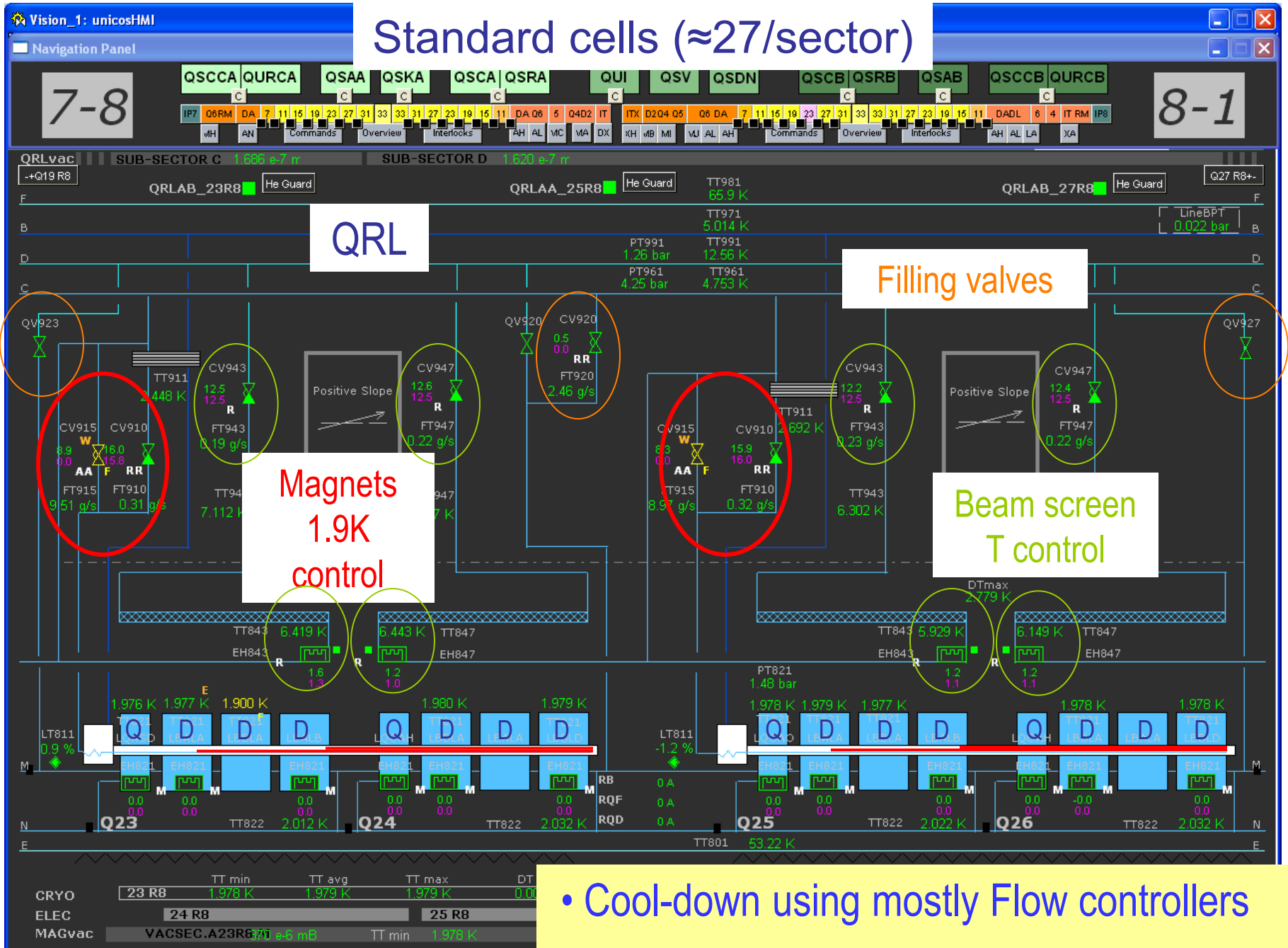


# Operation, indicators



**It works !!!**

# Standard cells ( $\approx 27$ /sector)



- Cool-down using mostly Flow controllers
- P, T, L controllers at operating conditions