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## **Using the HELIOS facility for assessment of bundle-jacket thermal coupling in a CICC**

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***The authors would like to thank***

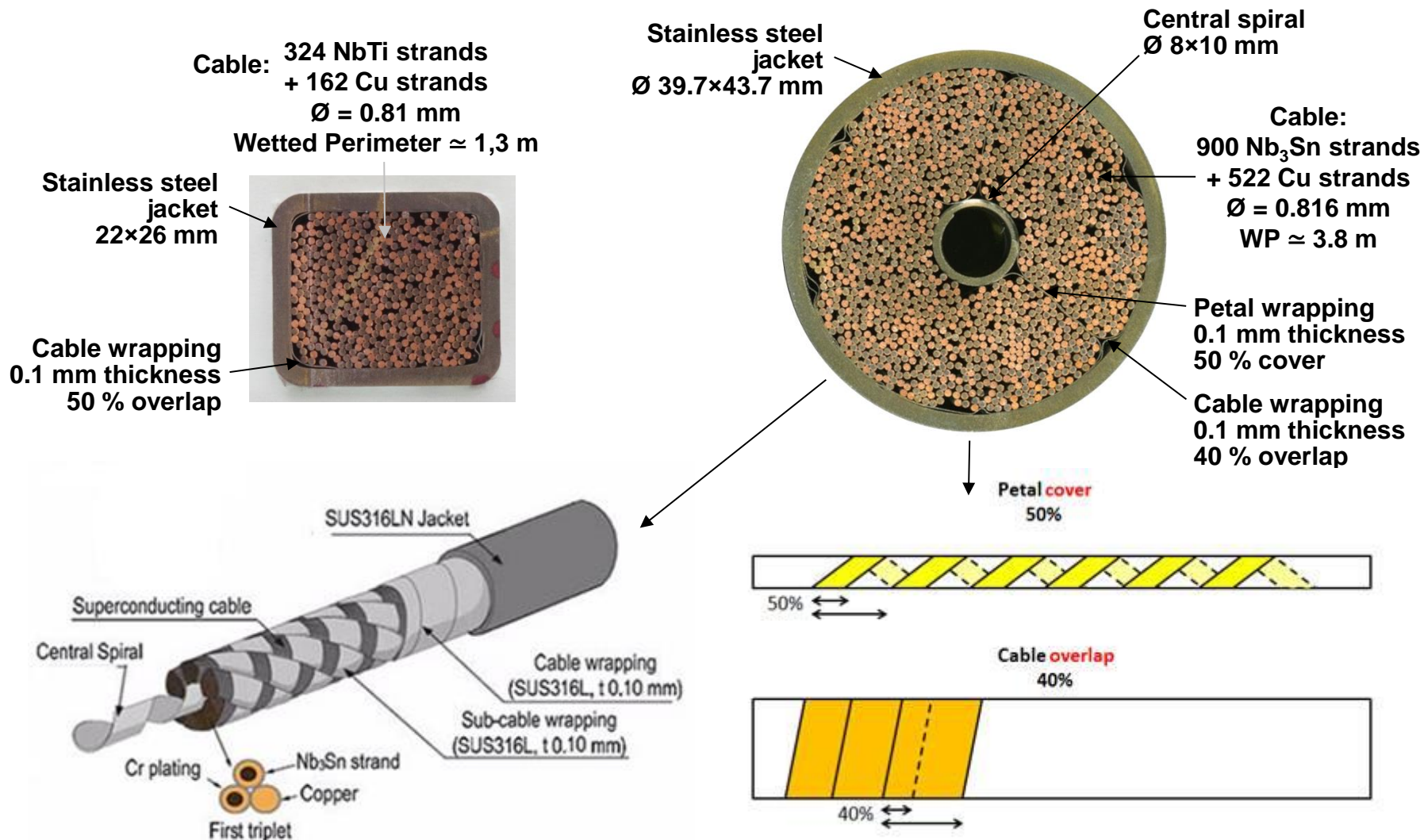
***D. Bessette and F. Gauthier***

***(ITER Organization)***

***for their scientific and material support***

- 1 – Impact of Heat Transfer Coefficient in CICC thermo-hydraulics**
- 2 – Measurement method and mock-up design**
- 3 – Manufacturing and integration in HELIOS facility**
- 4 – Experimental results analysis**
- 5 – Conclusion**

## 2 typical Cable In Conduit Conductors (CICC) for fusion magnets



➤ 2 Heat Transfer Coefficients (HTC) to assess in strands channel:

- h He/strands ( $h_{\text{bundle}}$ )
- h He/jacket ( $h_{\text{jacket}}$ )

➤ 2 correlations are usually applied:

- Dittus-Boelter  $Nu = 0,023 Re^{0.8} Pr^{0.4}$
- Colburn-Reynolds (Chilton-Colburn) analogy between heat transfer and friction

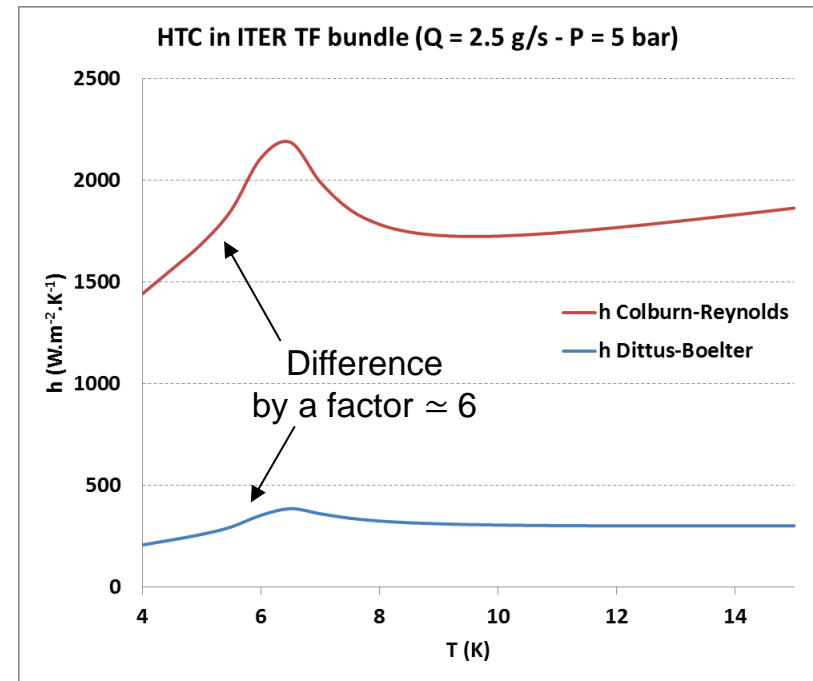
$$Nu = f_{EU}/8 Re Pr^{1/3}$$

➤ He/bundle and He/jacket HTC may impact CICC thermo-hydraulic behaviour and thus CICC design:

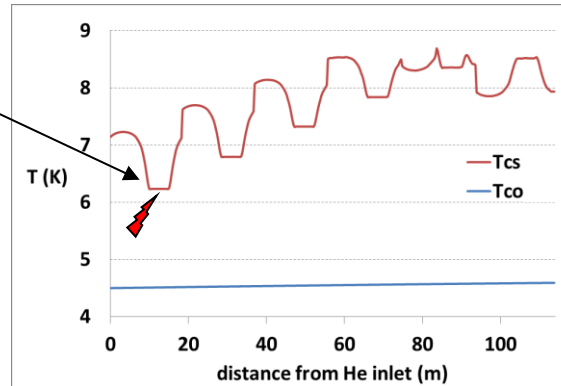
- conductor **thermal stability**
- **quench propagation** velocity
- **hot spot temperature** (maximum conductor temperature reached during Fast Safety Discharge of current in case of quench detection) – Usual criterion:  $T_{\text{hot spot}} < 150 \text{ K}$

➔ These effects were assessed by **Gandalf** calculations on **JT-60SA TF conductor** (easier interpretation in the **absence of central channel**)

*Remark : Operating temperature  $T_{op}$  and thus  $\Delta T_{ma} = T_{cs} - T_{op}$  are not affected by  $h$  value, because  $T_{He} - T_{strands} \simeq 0$  due to the large He/strands wetted perimeter*



- Simulations on JT-60SA TF conductor with  $Q = 3.5 \text{ g/s}$ ,  $P_{\text{inlet}} = 5 \text{ bar}$ ,  $T_{\text{inlet}} = 4.5 \text{ K}$  and without thermal load
- Disturbance of 100 ms and 1 m applied at middle of high field region (between 12 and 13 m from He inlet)



- By default,  $h_{\text{jacket}}$  integrates **thermal resistance  $R_{\text{th wraps}}$  due to He layer** (estimated average thickness  $e = 26 \mu\text{m}$ ) trapped between wrappings and jacket (conduction through SS wrappings integrated in jacket thickness)

$$h_{\text{jacket}} = \frac{1}{\frac{1}{h_{\text{conv}}} + R_{\text{th wraps}}} \quad \text{with} \quad R_{\text{th wraps}} = \frac{e_{\text{He layer}}}{\lambda_{\text{He layer}}}$$

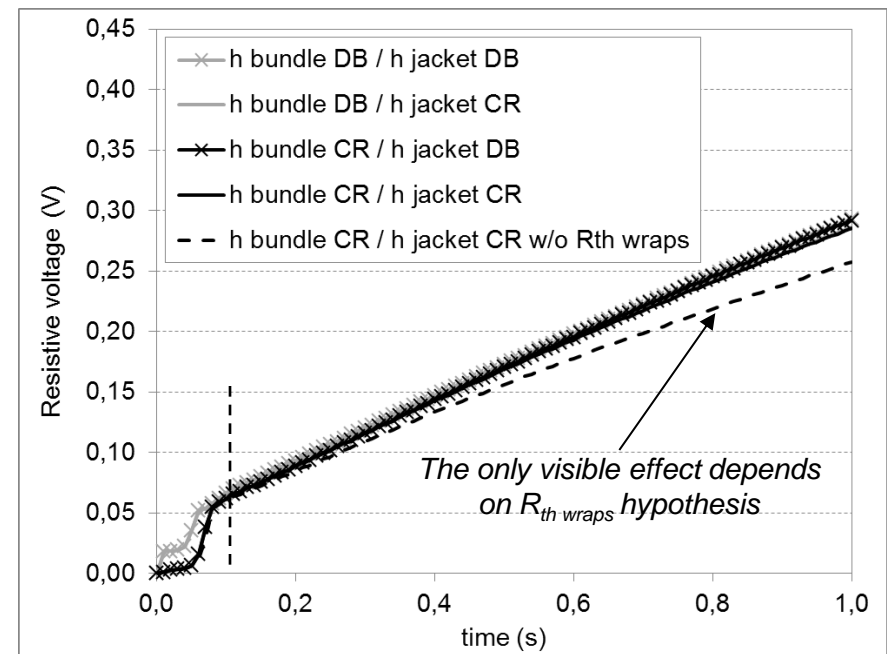
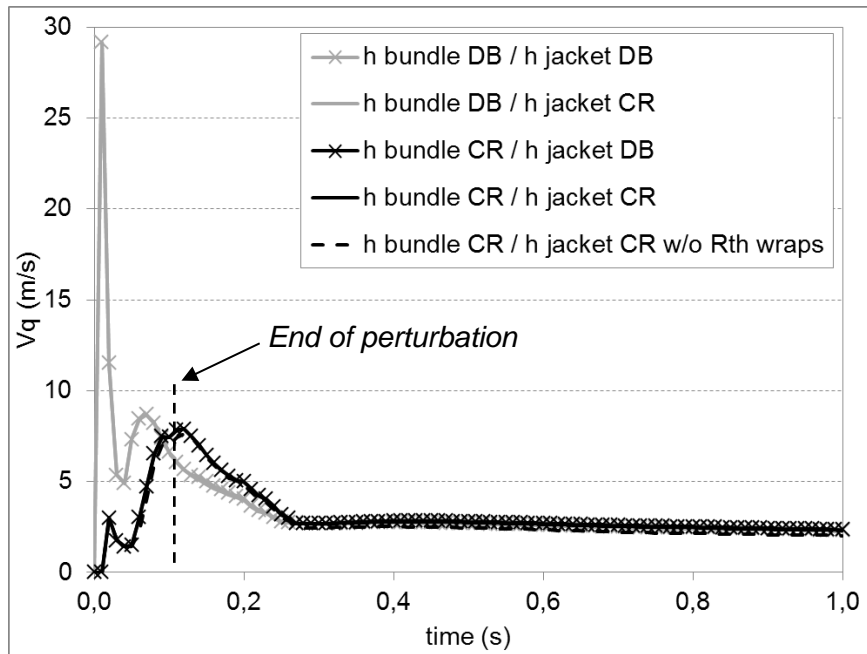
- ✓ Impact of HTC correlations on **thermal stability** (Minimum Quench Energy) and on  $T_{\text{hot spot}}$  :

$h_{\text{bundle}}$	$h_{\text{jacket}}$	MQE (W/m)	$T_{\text{hot spot}}$ (K)
DB	DB with $R_{\text{th wraps}}$	460	187
DB	CR with $R_{\text{th wraps}}$	460	156.5
CR	DB with $R_{\text{th wraps}}$	850	183
CR	CR with $R_{\text{th wraps}}$	850	152.5
CR	CR w/o $R_{\text{th wraps}}$	870	134

- ➔
- ✓ **MQE** is mainly sensitive to  $h_{\text{bundle}}$
  - ✓  **$T_{\text{hot spot}}$**  is mainly sensitive to  $h_{\text{jacket}}$



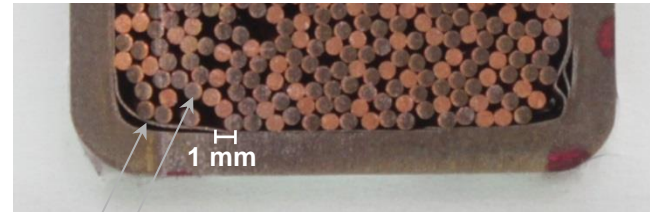
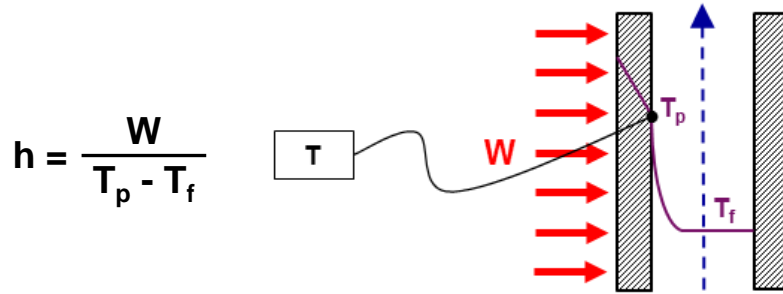
- ✓ Limited impact of HTC correlations on early **quench propagation**



- 
- ✓  $h_{bundle}$  may impact **thermal stability**
  - ✓  $h_{jacket}$  impact  $T_{hot\ spot}$  calculation, and to a lesser extent early quench propagation, so  $h_{jacket}$  may impact the parameterization of the **quench detection system**

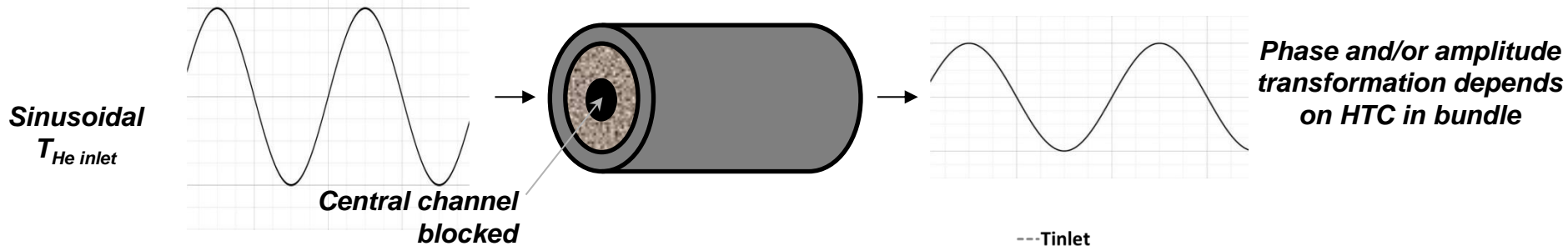
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- Usual method for measuring a Heat Transfer Coefficient requires  $T_p$  measurement at inner wall

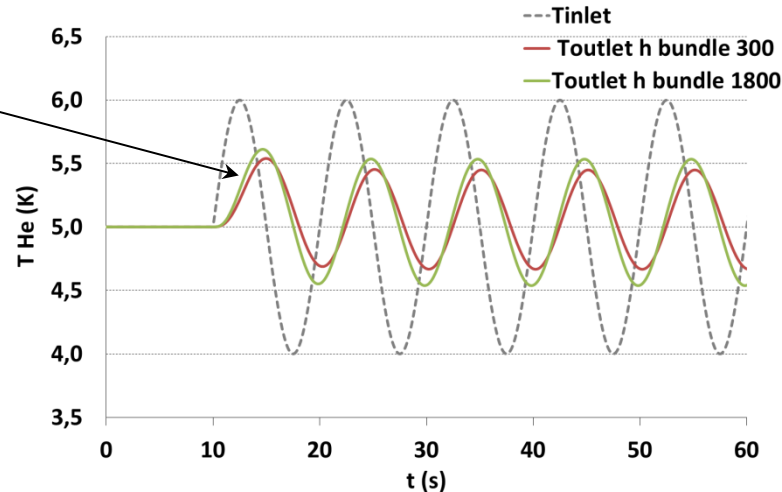


**But  $T_p$ ?** Wall temperature measurement is not possible for inner jacket nor for strands

- Possible alternative = technique used for measuring HTC in porous media



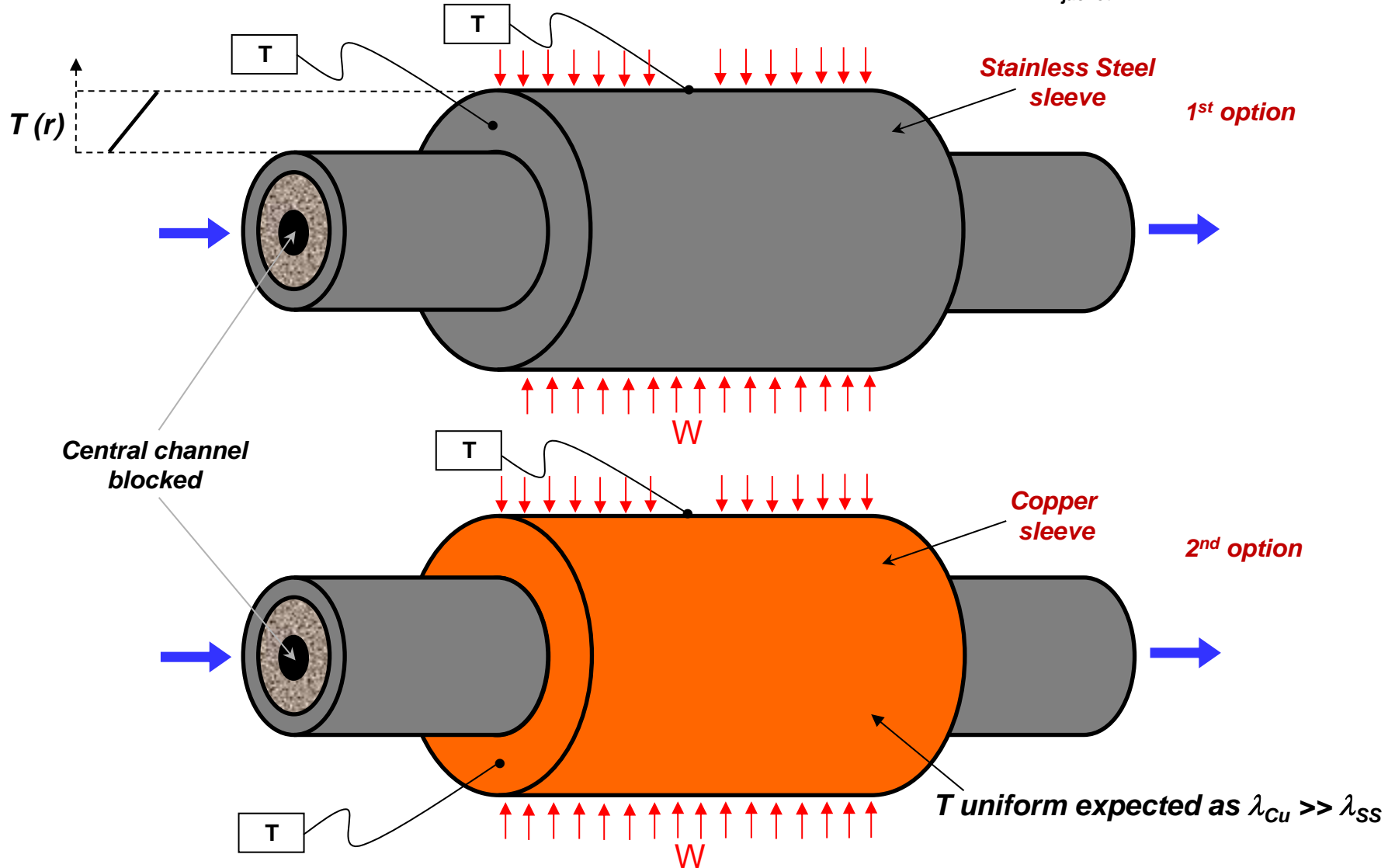
- But** • simulations showed little impact of  $h_{bundle}$  on  $T_{outlet}$  shape
- Method seems inadequate at cryogenic operating conditions probably due to ratio of materials / He enthalpies



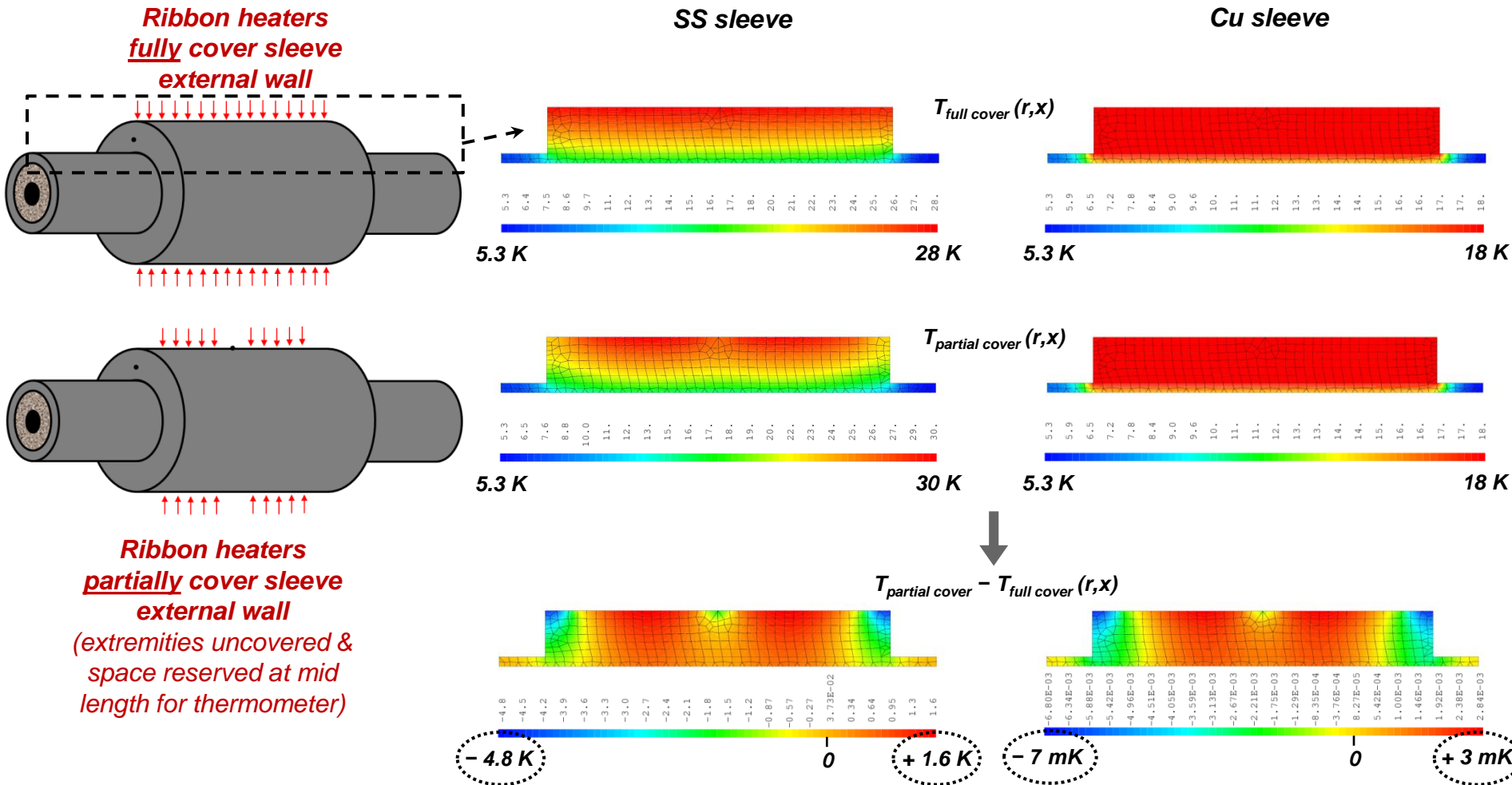
*Gandalf simulation of response to sinusoidal  $T_{inlet}$  (ITER TF conductor sample of 10 cm with  $Q = 1\ g/s$ )*



➤ Possible solution : externalize wall temperature measurement for assessing  $h_{jacket}$



➤ First reason why Cu sleeve option is more adequate



✓ With **Cu sleeve**, external wall  $T^e$  do not depend on sensor location, allowing an easier manufacturing, whereas **analysis of SS sleeve mock-up** would require taking into account **detailed geometry**

➤ Second reason why Cu sleeve option is more adequate

Radial T<sup>e</sup> gradient:  $T_{\text{outer sleeve}} - T_{\text{fluid}} = (T_{\text{inner jacket}} - T_{\text{fluid}}) + (T_{\text{outer jacket}} - T_{\text{inner jacket}}) + (T_{\text{outer sleeve}} - T_{\text{outer jacket}})$

$= \Delta T_{\text{conv}} + \Delta T_{\text{jacket}} + \Delta T_{\text{sleeve}} \quad (1)$

*measured* (points to  $T_{\text{outer sleeve}}$  and  $T_{\text{fluid}}$ )

*calculated* (points to  $\Delta T_{\text{jacket}}$  and  $\Delta T_{\text{sleeve}}$ )

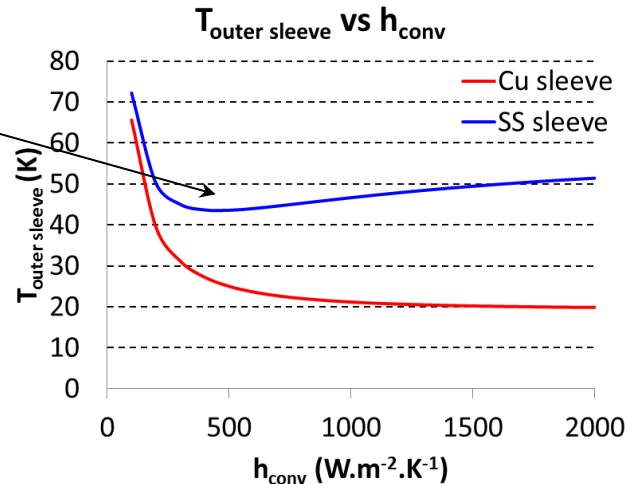
$= \frac{\phi}{h_{\text{conv}}}$  where  $\phi$  is imposed and  $h_{\text{conv}}$  is tuned for balancing the equality

✓ With Cu sleeve,  $\Delta T_{\text{sleeve}} \approx 0 \rightarrow$  lower uncertainty & better sensitivity to  $h_{\text{conv}}$  ( $\Delta T_{\text{conv}}$  has higher relative weight)

✓ If  $h_{\text{conv}} \nearrow \rightarrow$

- $\Delta T_{\text{conv}} \searrow$
- in case of SS sleeve, as  $\lambda_{\text{SS}} \searrow$  when  $T \searrow$ ,  $\Delta T_{\text{sleeve}} \nearrow$

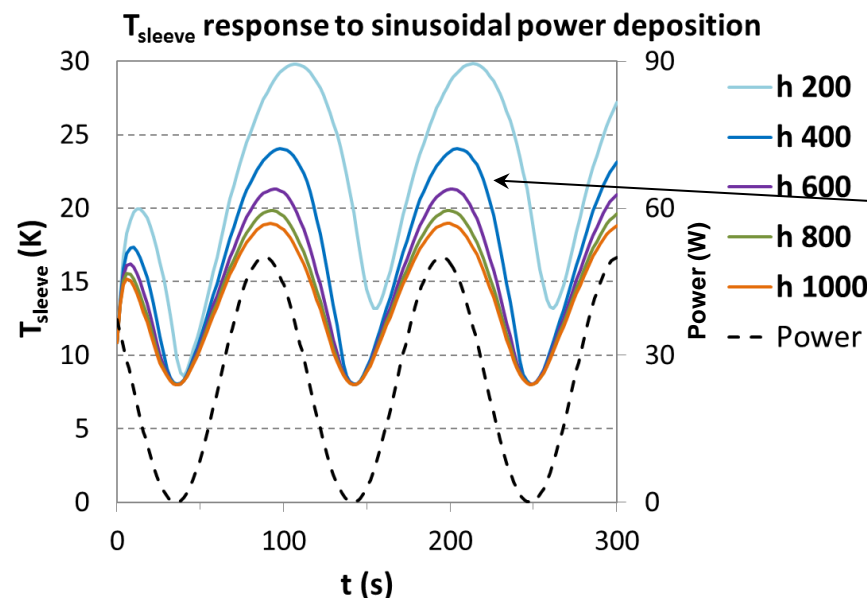
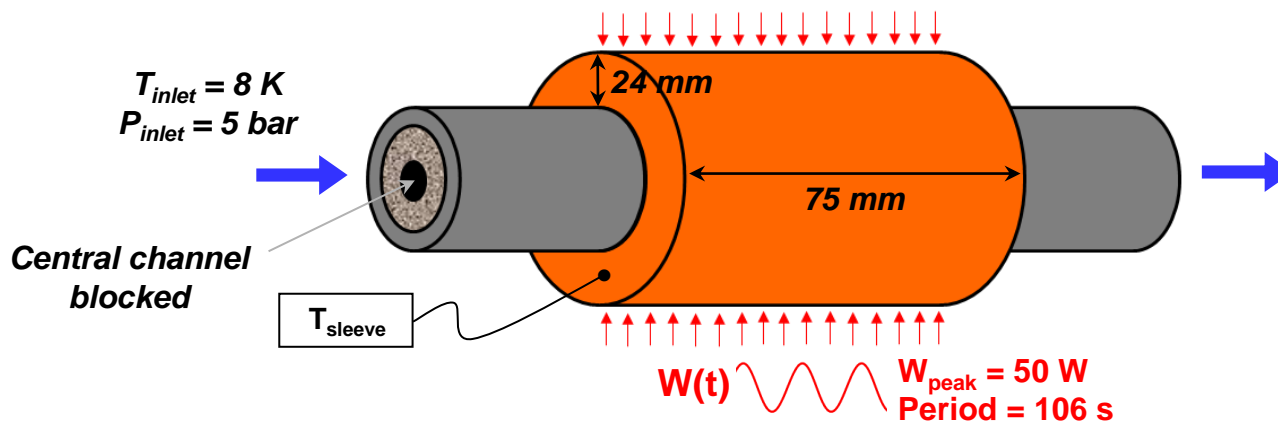
Thus, if SS sleeve thickness is large enough, equation (1) can have 2 solutions on  $h_{\text{conv}}$



Computation with:

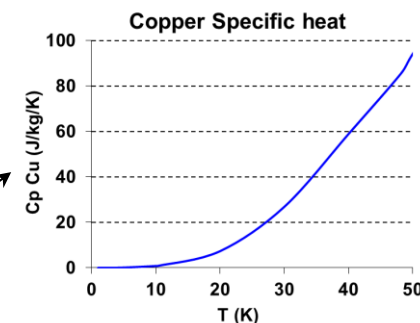
- $P = 50 \text{ W}$
- $T_{\text{fluid}} = 10 \text{ K}$
- Sleeve thickness = 10 mm
- length = 75 mm

- Retained mock-up could allow an alternative  $h_{jacket}$  measurement by applying **sinusoidal power deposition** instead of constant heating
- **Sensitivity of  $T_{sleeve}(t)$  to  $h_{jacket}$**  was assessed by simulating the following case:



✓ Sensitivity to  $h_{conv}$  seems **workable**

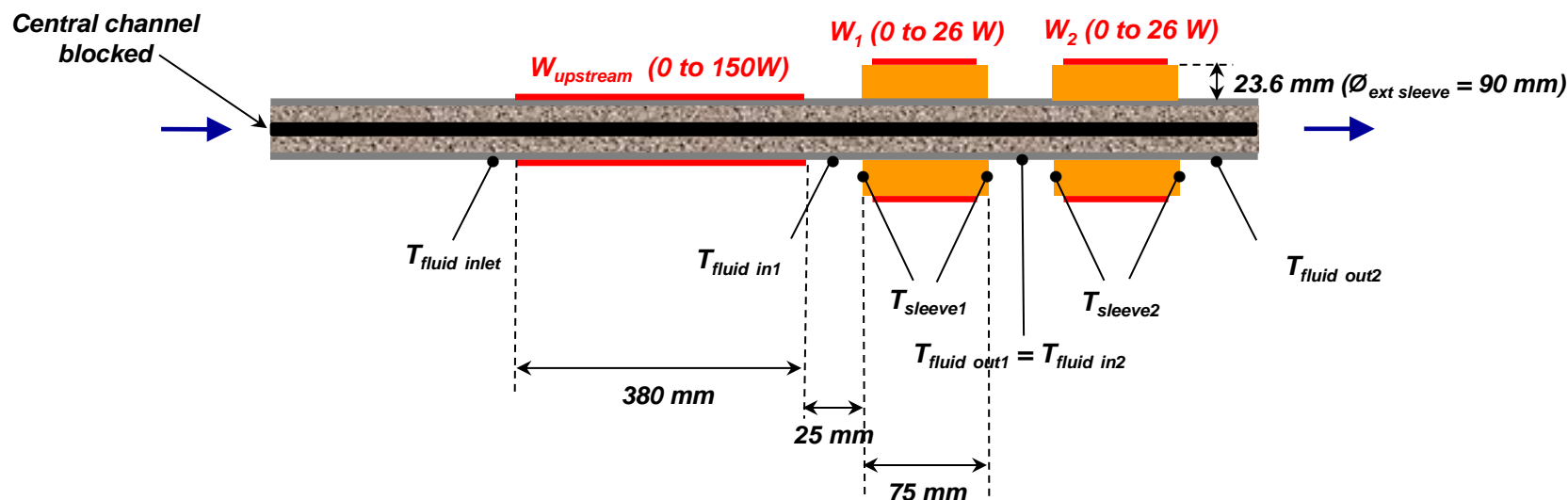
✓ The asymmetric shape of  $T_{sleeve}(t)$  is due to large dependence of Cu specific heat on T

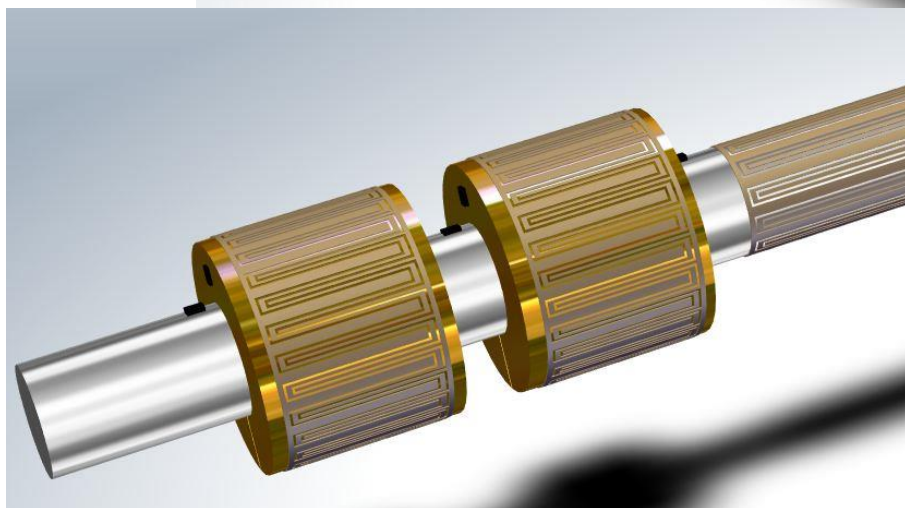
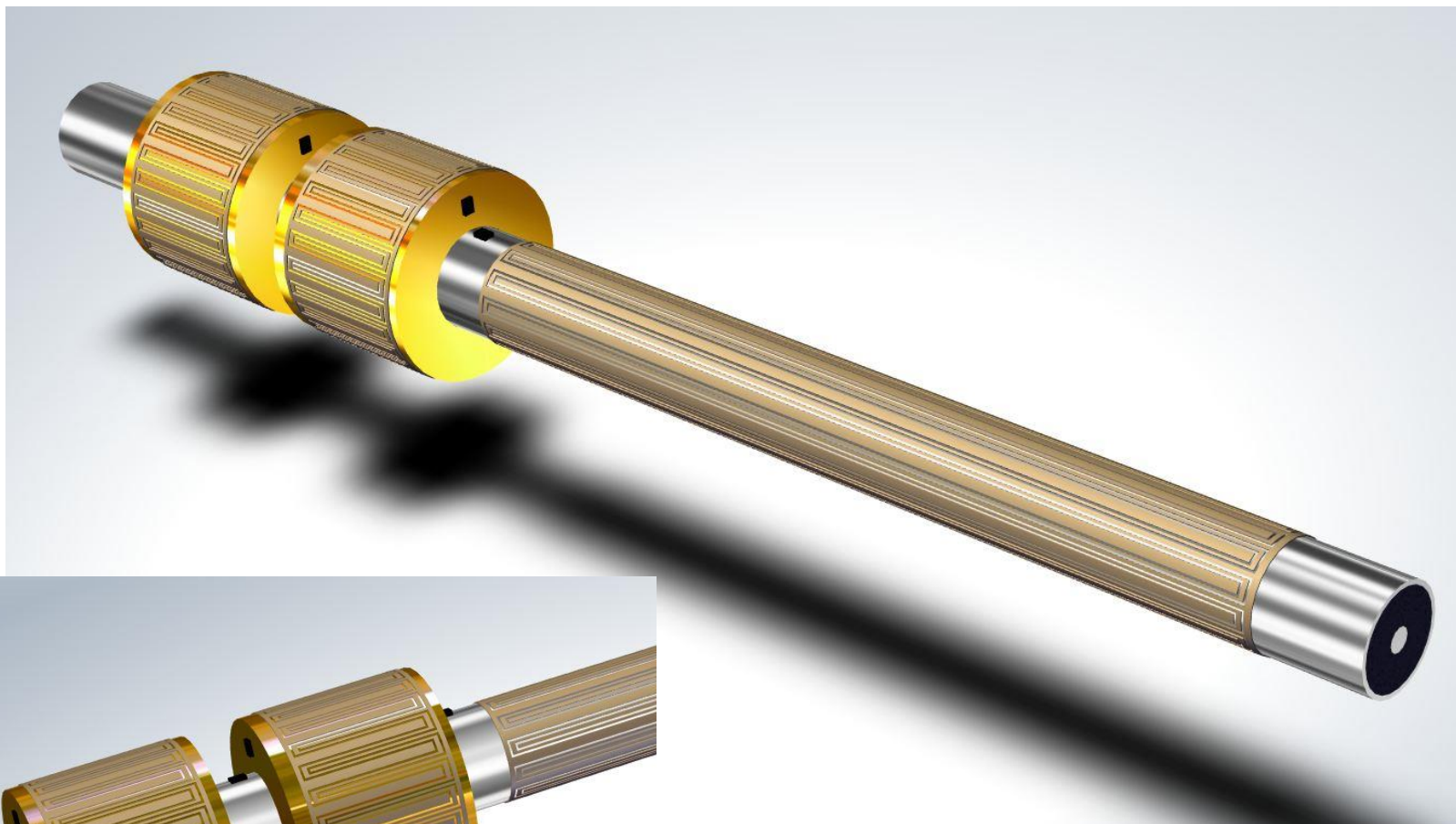


- **Cu sleeve option is chosen**
- Mock-up allows  $h_{jacket}$  **assessment only**, but **by 2 methods**: with **stationary** or **sinusoidal** power deposition

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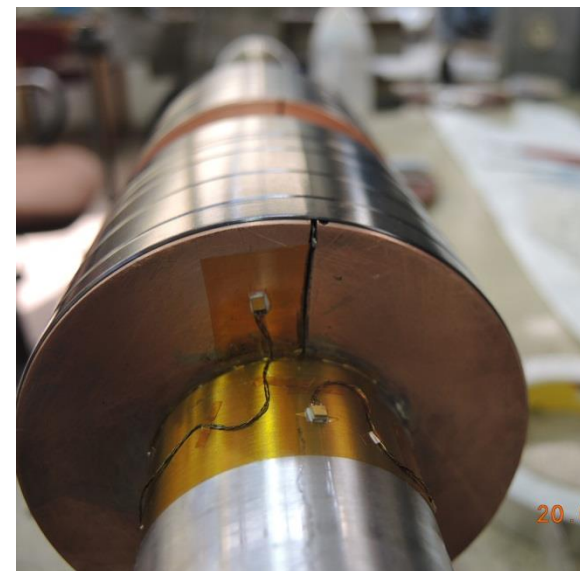
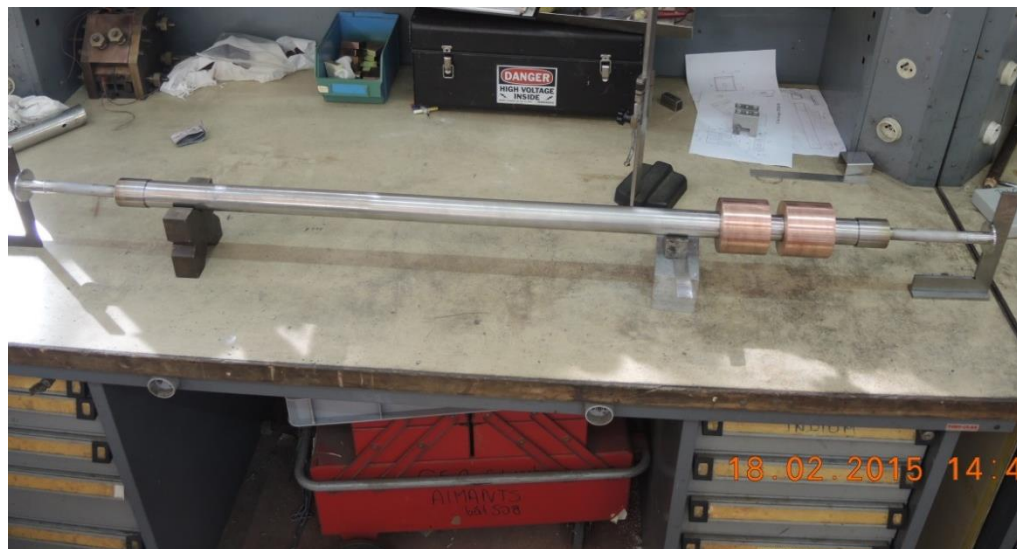
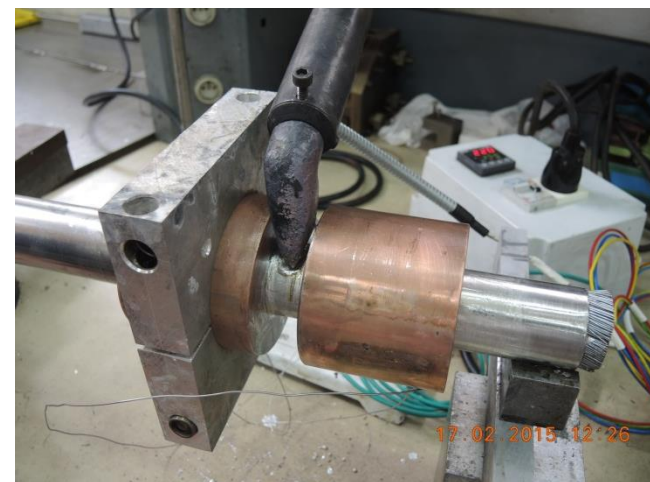
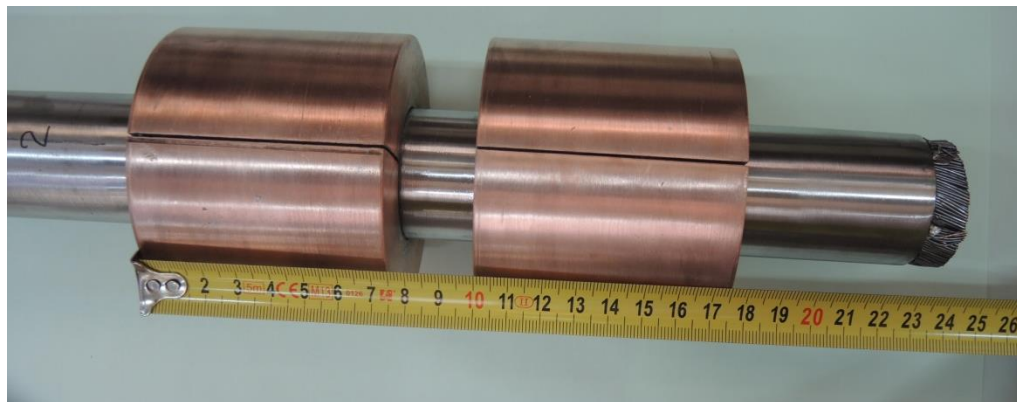
- The mock-up was manufactured from a **1.2 m sample of ITER TF dummy conductor (SC strands replaced by Cu strands)**
- **2 sleeves of OFHC Cu** (for a high thermal conductivity) were **soldered** on SS jacket (SnAg brazing) for the **best thermal coupling jacket/sleeve**
- **3 ribbon heaters** were installed, **2 on both sleeves** outer face and **one upstream** of sleeves for accessing a wider range of temperature
- **7 Cernox T<sup>re</sup> sensors** were installed on sleeves zone, **3 on jacket around sleeves** for measuring fluid temperature and **4 on sleeves lateral sides** for measuring Cu temperature (2 sensors per sleeve for checking T<sup>re</sup> uniformity)





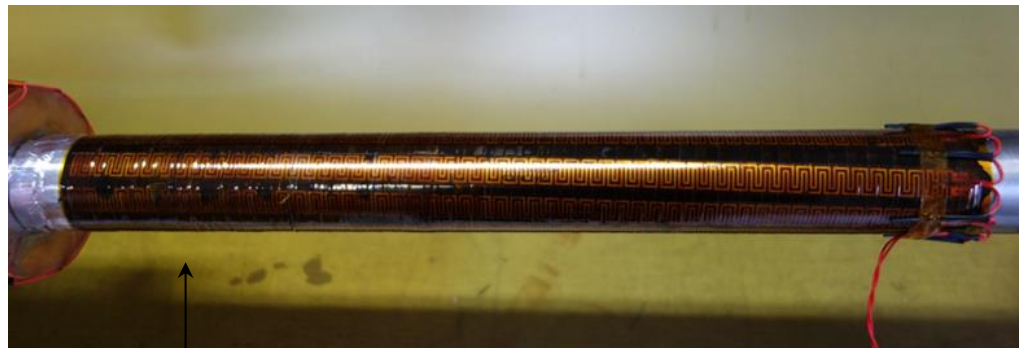
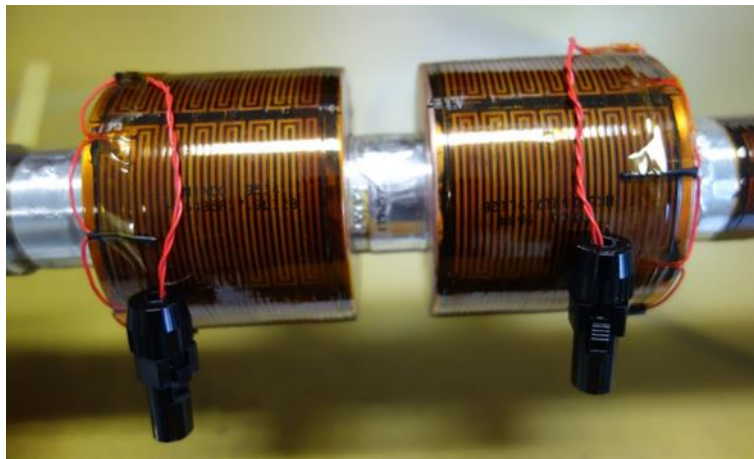
*CAD view of sleeves, heaters  
and instrumented zone*

## First manufacturing stage at IRFM Cadarache





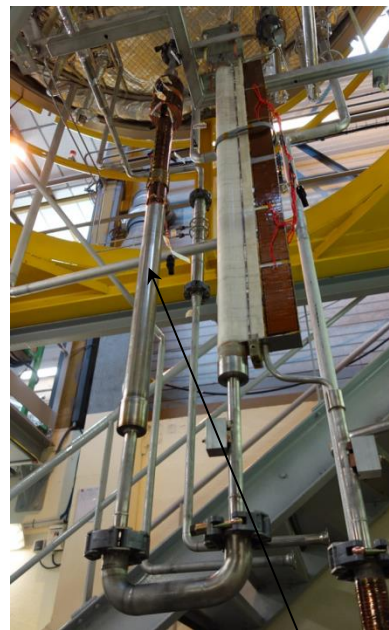
## 2nd manufacturing stage at INAC/SBT Grenoble



← MINCO heaters glued with Stycast



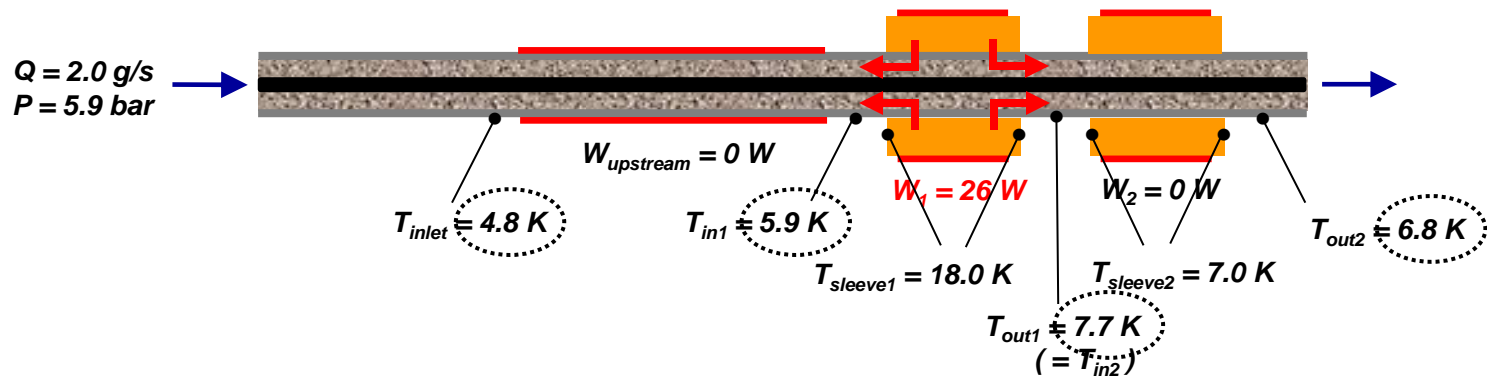
INAC/SBT refrigerator – 400 W at 4 K



Installing in HELIOS facility

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- Steady state power runs allowed exploring the following ranges:
  - $T_{\text{fluid}}$  from **6.0** to **38.4 K**
  - **Pressure** from **4.9** to **8.8 bar**
  - $Q_{\text{He bundle}}$  from **1.0** to **6.1 g/s**
  - $Re_{\text{bundle}}$  from **180** to **2350**
  
- **Unexpected thermohydraulic behaviour** was systematically observed. One case is reported hereafter:

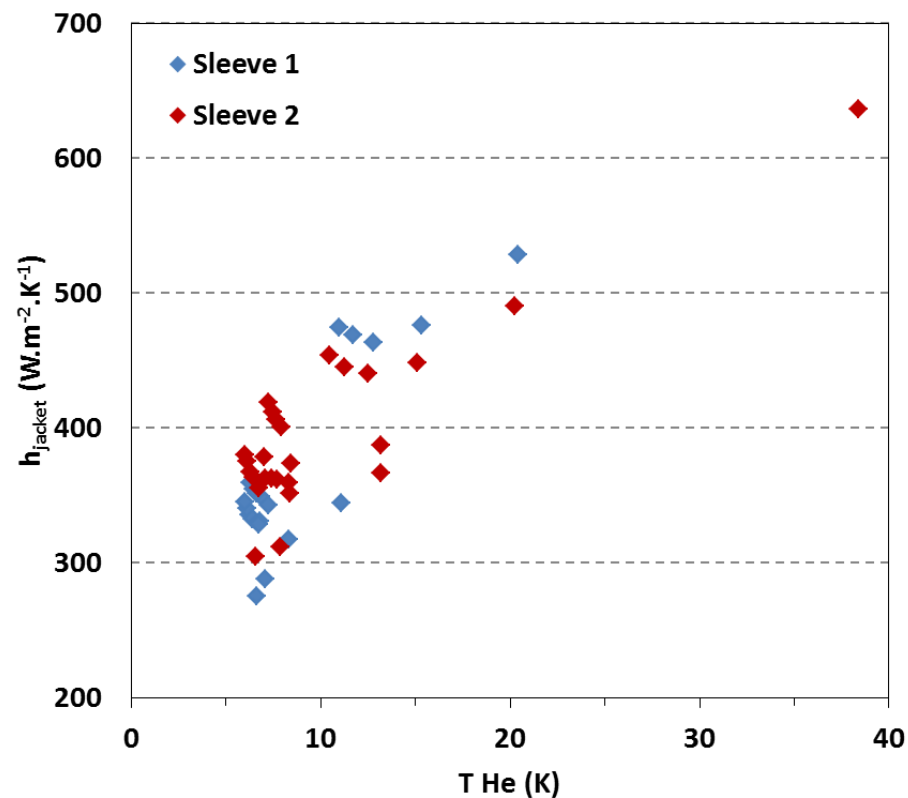
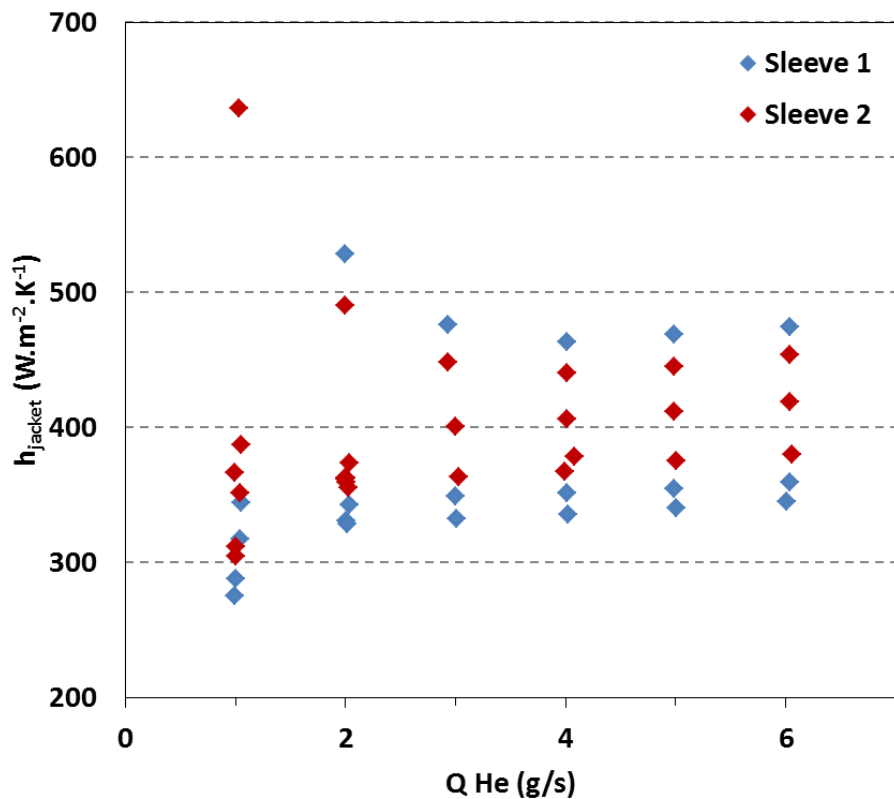


- ✓  $T_{\text{in1}} > T_{\text{inlet}}$  : **upstream  $T^{\text{re}}$  is affected by heat applied downstream** → heat is « **backflowing** », certainly due to **conduction in strands** (cooling fin effect), this phenomenon being emphasized by the fact that all strands are in Cu (sample was made from dummy Cu conductor)
  
- ✓  $T_{\text{out1}} > T_{\text{out2}}$  : downstream the heated zone,  $T^{\text{re}}$  should remain constant (no heat load, no significant P decrease). As **cooling without cold source is impossible**, one explanation can be a mixing between a **cold** (not heated) **central flow** and a **warm flow in the vicinity of inner jacket**



As heat exchange process takes place close to the wall, all runs were analyzed considering  $T_{\text{fluid } i} = (T_{\text{in } i} + T_{\text{out } i}) / 2$ , with  $i = 1$  or  $2$  for sleeve 1 or 2

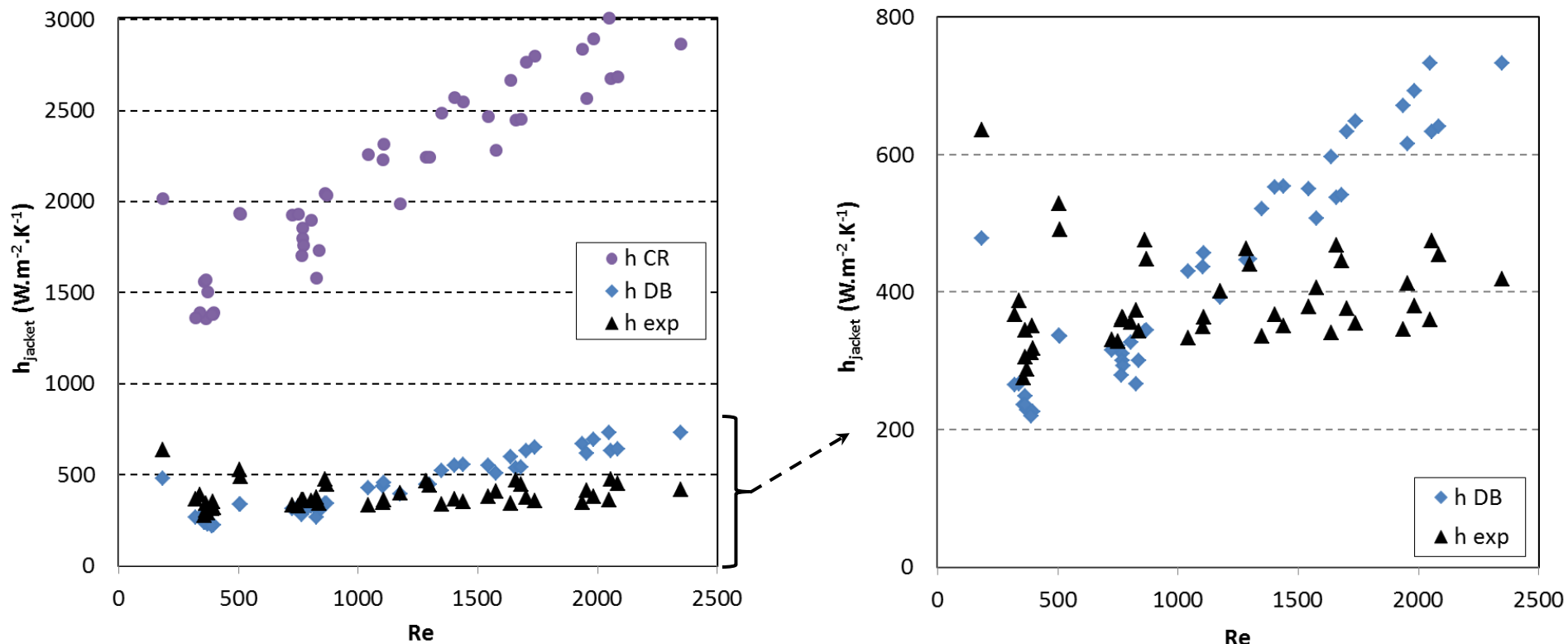
## Analysis of steady state runs



➤ **Good agreement** between experimental  $h_{jacket}$  values assessed with **both sleeves**

## Analysis of steady state runs

Comparison with Dittus-Boelter and Colburn-Reynolds correlations



- $h_{jacket}$  order of magnitude is **closer to Dittus-Boelter** than to Colburn-Reynolds
- But a **discrepancy** exists between experimental and computed Dittus-Boelter values

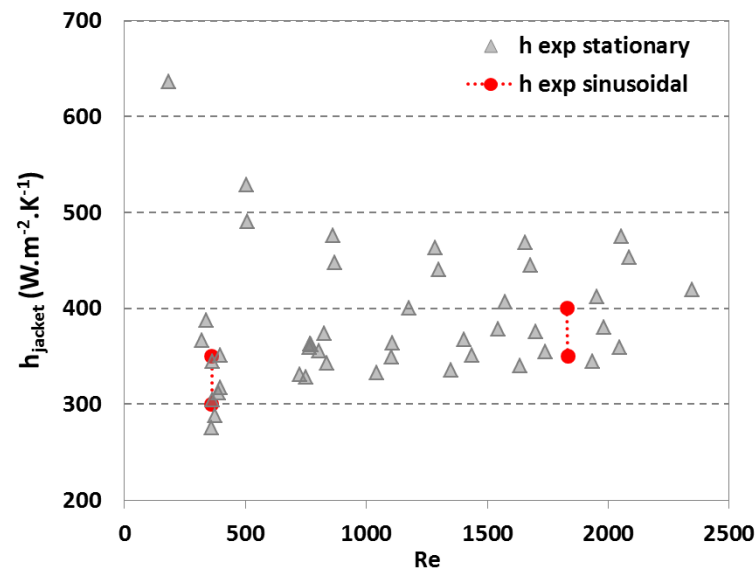
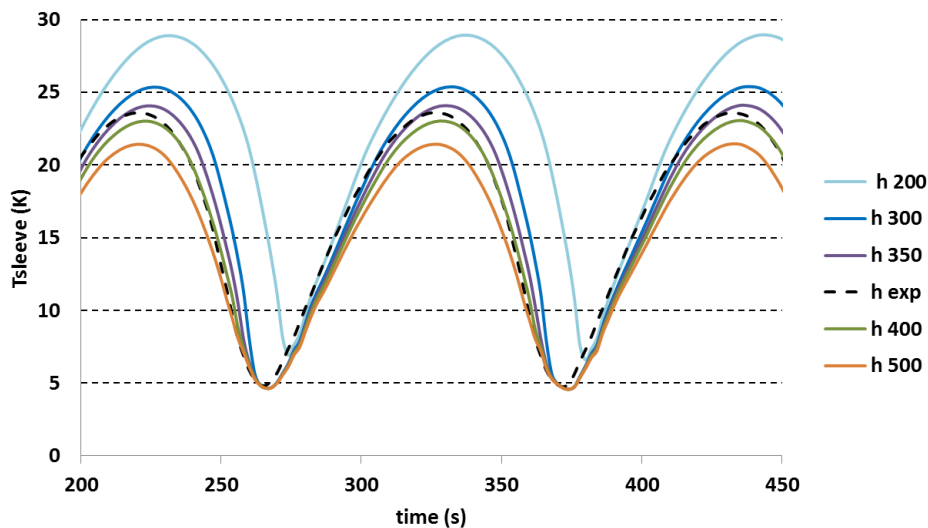
## Analysis of sinusoidal runs

- 4 sinusoidal power deposition runs were performed, varying QHe (1 g/s and 6 g/s) and at 2 frequencies (period = 38 s and 106 s)
- Experimental response of sleeve  $T^e$  had the expected asymmetric shape, but  $h_{jacket}$  assessment was less obvious than for stationary power runs

QHe	Frequency	Tfluid (average)	Re (average)	$h_{jacket}$ ( $W.m^{-2}.K^{-1}$ )
1 g/s	Low	8.86 K	360	300 – 350
1 g/s	High	8.05 K	360	Idem
6 g/s	Low	5.82 K	1833	350 – 400
6 g/s	High	5.82 K	1829	Idem

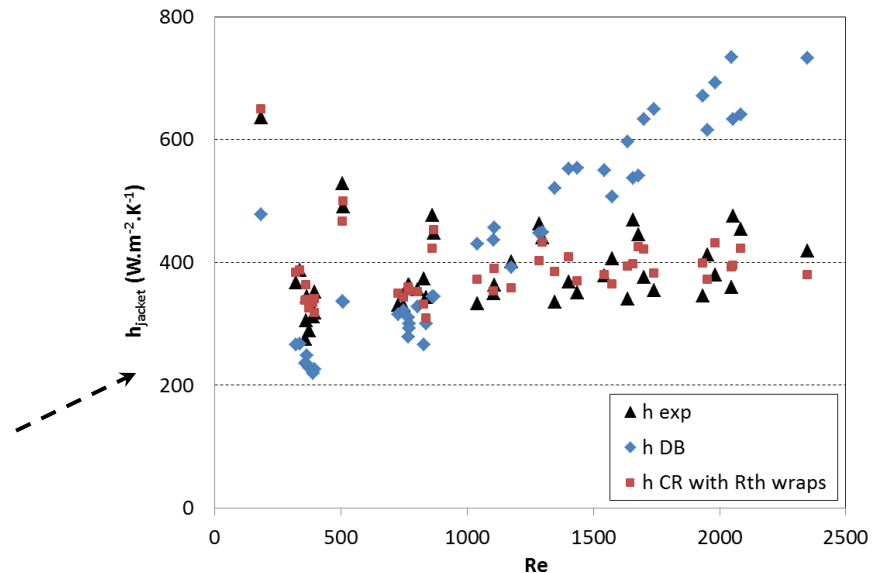
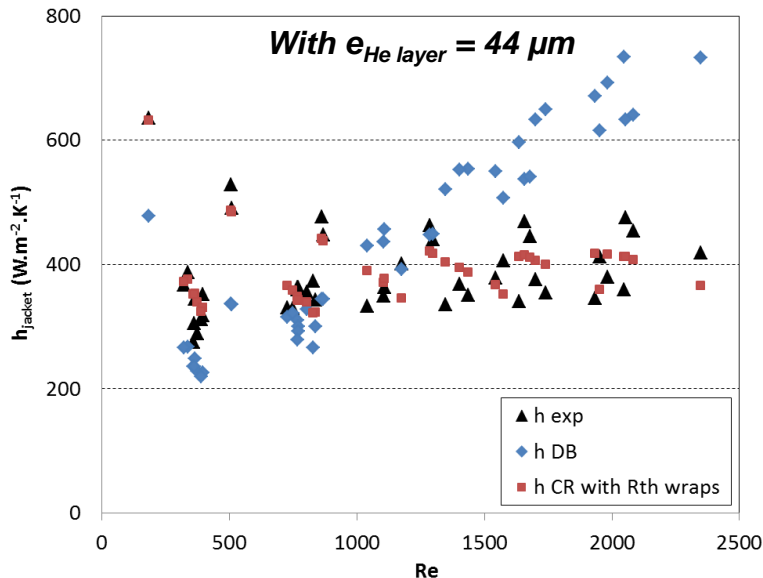
➔  $h_{jacket}$  assessed with sinusoidal heat deposition is in good agreement with stationary approach, bringing confidence in the analyses

Sinusoidal run with QHe = 6 g/s and at low frequency (period = 106 s)



## Attempt to fit experimental values

- Considering the He layer trapped between wraps and jacket, 
$$h_{jacket} = \frac{1}{\frac{1}{h_{conv}} + R_{th\ wraps}} \quad (1) \quad \text{with } R_{th\ wraps} = \frac{e_{He\ layer}}{\lambda_{He\ layer}}$$
- Even if  $h_{jacket}$  order of magnitude is close to Dittus-Boelter,  $h_{conv}$  cannot be approached by DB correlation since  $h_{DB} < h_{exp}$  at low Re values
- The model based on (1) was applied, considering **Colburn-Reynolds analogy for  $h_{conv}$**  and **tuning  $e_{He\ layer}$  in each sleeve** in order to fit experimental values of  $h_{jacket}$
- The best consistence was found with  $e_{He\ layer} = 47$  and  $43\ \mu\text{m}$  in sleeves 1 and 2 respectively
  - These orders of magnitude are consistent with the value of  $26\ \mu\text{m}$  estimated for JT-60SA TF conductor
  - This analysis suggests that **Colburn-Reynolds analogy** is applicable for **convective HTC** between He and wraps or thus between He and strands too ( $h_{bundle}$ )



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- Due to **complex geometry**, **Heat Transfer Coefficient** in a **CICC** is a **not well documented parameter**
- An **experiment** was designed and carried out in **HELIOS** facility (CEA Grenoble – spring 2015) for **estimating He/jacket thermal coupling** in a sample of **ITER TF conductor**
- Experimental results suggest that **Colburn-Reynolds** analogy could be applied for both **He/strands** and **He/wraps** Heat Transfer Coefficients
- Regarding the **overall He/jacket HTC**, the thermal resistance induced by **cable wraps can limit strongly the thermal coupling** between the He and the conduit.  
If this thermal resistance cannot be assessed, Dittus-Boelter correlation should give a good order of magnitude for He/jacket HTC.
- An **additional experiment** based on **HTC measurement method in porous media** could help **confirming these results**. But such an experiment seems incompatible with cryogenic operating conditions (to be confirmed) and could require similitude conditions.



***Thank you  
for your attention***

*Courtesy of ITER Organization*