



Cryogenics for particle accelerators

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Contents

- Low temperatures and liquefied gases
- Cryogenics in accelerators
- Properties of fluids
- Heat transfer & thermal insulation
- Cryogenic distribution & cooling schemes
- Refrigeration & liquefaction



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- **cryogenics**, that branch of physics which deals with the production of very low temperatures and their effects on matter

Oxford English Dictionary

2nd edition, Oxford University Press (1989)

- **cryogenics**, the science and technology of temperatures below 120 K

New International Dictionary of Refrigeration

3rd edition, IIF-IIR Paris (1975)



Characteristic temperatures of cryogenes

Cryogen	Triple point [K]	Normal boiling point [K]	Critical point [K]
Methane	90.7	111.6	190.5
Oxygen	54.4	90.2	154.6
Argon	83.8	87.3	150.9
Nitrogen	63.1	77.3	126.2
Neon	24.6	27.1	44.4
Hydrogen	13.8	20.4	33.2
Helium	2.2 (*)	4.2	5.2

(*): λ Point



Densification, liquefaction & separation of gases

LNG



130 000 m³ LNG carrier
with double hull

Air separation by cryogenic
distillation

Up to 4500 t/day LOX

LIN & LOX



Rocket fuels



Ariane 5

25 t LHY, 130 t LOX

What is a low temperature?

- The entropy of a thermodynamical system in a macrostate corresponding to a multiplicity W of microstates is

$$S = k_B \ln W$$

- Adding reversibly heat dQ to the system results in a change of its entropy dS with a proportionality factor T

$$T = dQ/dS$$

⇒ *high temperature: heating produces small entropy change*

⇒ *low temperature: heating produces large entropy change*



L. Boltzmann's grave in the Zentralfriedhof, Vienna, bearing the entropy formula



Temperature and energy

- The average thermal energy of a particle in a system in thermodynamic equilibrium at temperature T is

$$E \sim k_B T$$
$$k_B = 1.3806 \times 10^{-23} \text{ J.K}^{-1}$$

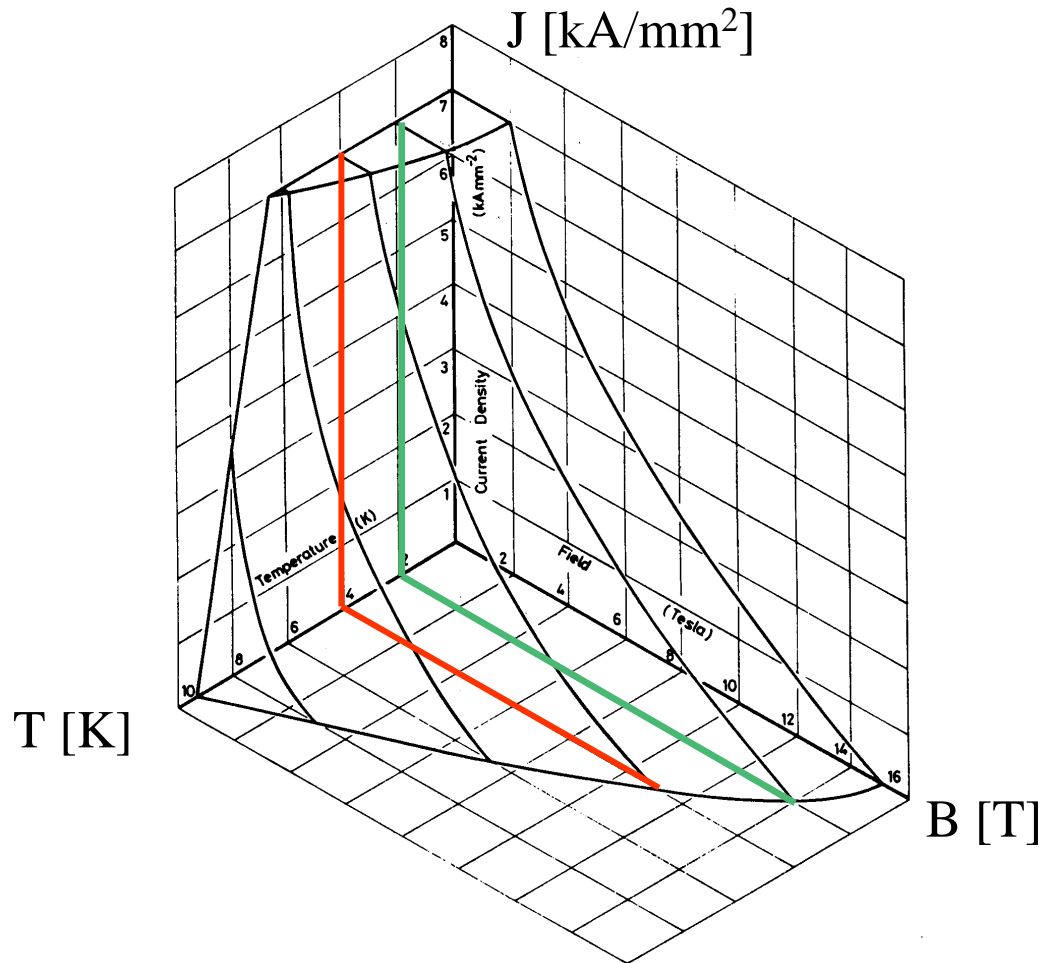
- 1 K is equivalent to 10^{-4} eV or 10^{-23} J thermal energy
 - a temperature is « low » for a given physical process when $k_B T$ is small compared with the characteristic energy of the process considered
 - cryogenic temperatures reveal phenomena with low characteristic energy and enable their application



Characteristic temperatures of low-energy phenomena

Phenomenon	Temperature
Debye temperature of metals	few 100 K
High-temperature superconductors	~ 100 K
Low-temperature superconductors	~ 10 K
Intrinsic transport properties of metals	< 10 K
Cryopumping	few K
Cosmic microwave background	2.7 K
Superfluid helium 4	2.2 K
Bolometers for cosmic radiation	< 1 K
Low-density atomic Bose-Einstein condensates	$\sim \mu\text{K}$

Operating temperature & performance of superconductors



- Superconductivity only exists in a limited domain of temperature, magnetic field and current density
- Electrotechnical applications require transport current and magnetic field
- Operating temperature of the device must therefore be significantly lower than the critical temperature of the superconductor



Optimization of operating temperature for superconducting RF cavity

- Power per unit length
- BCS theory
- For practical materials
- Refrigeration (Carnot)

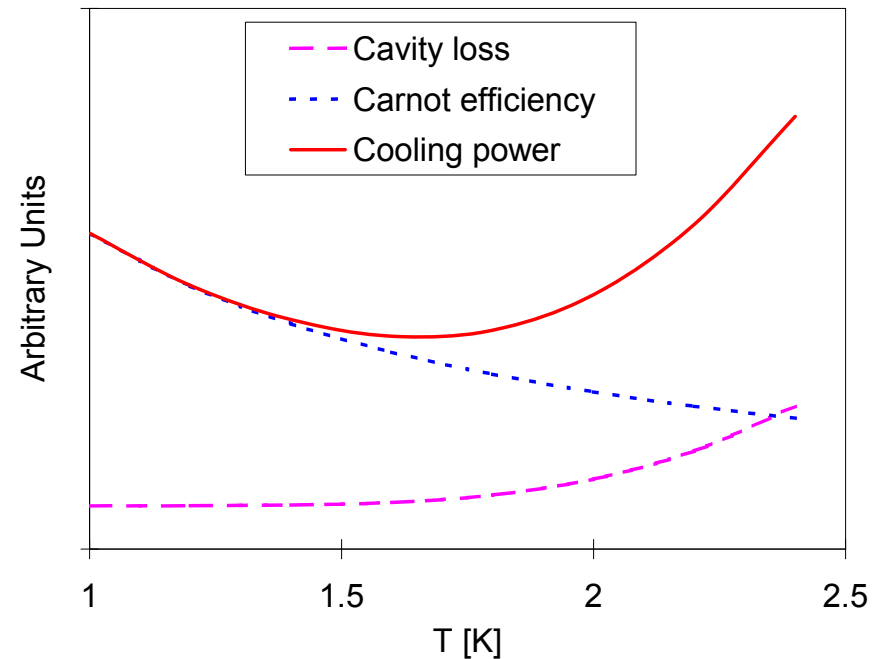
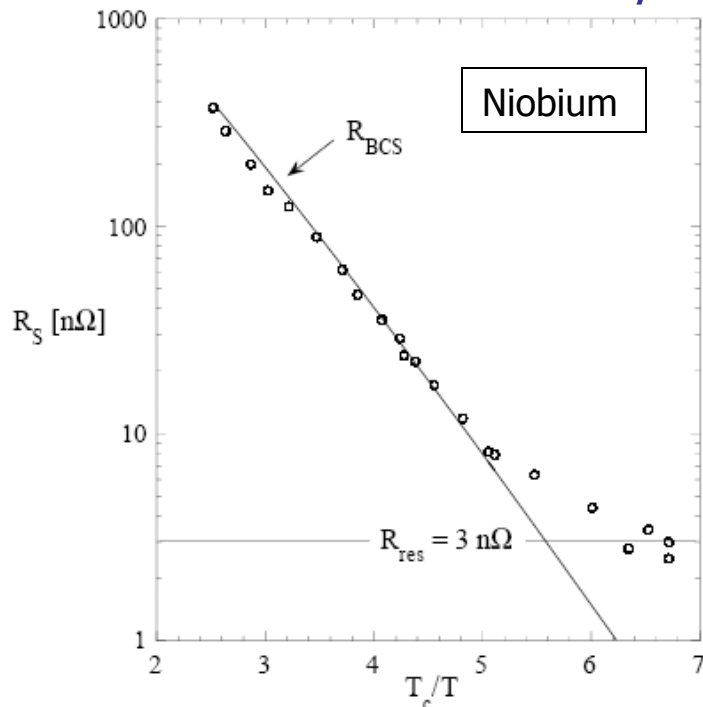
$$P/L \sim R_S E^2 / \omega$$

$$R_{\text{BCS}} = (A \omega^2 / T) \exp(-B T_c / T)$$

$$R_S = R_{\text{BCS}} + R_0$$

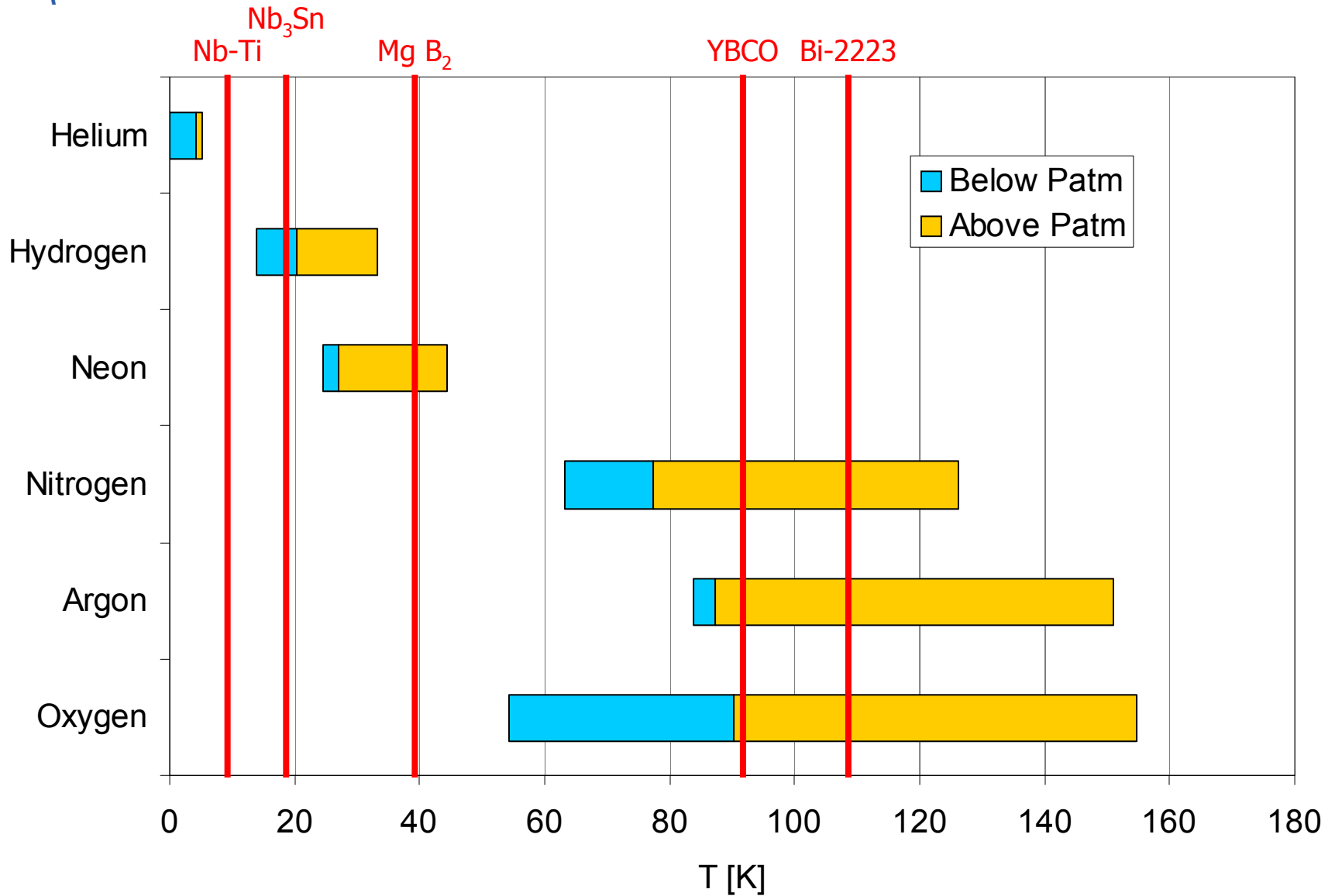
$$P_a = P (T_a / T - 1)$$

⇒ *optimum operating temperature for superconducting cavities is well below critical temperature of superconductor*





Useful range of cryogenes & critical temperature of superconductors





Cryogenics for superconducting devices

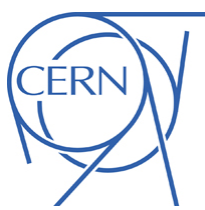
- Helium is the only practical cryogen for LTS devices
- Subcooled nitrogen is applicable to HTS devices at low and moderate current density
- Thanks to its general availability and low cost, liquid nitrogen is very often used for precooling and thermal shielding of helium-cooled devices
- In spite of its cost, neon can constitute an interesting alternative to subcooled nitrogen for operating HTS at high current density, and to helium for MgB₂ devices

⇒ *in the following, focus on helium and nitrogen*



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Superconductivity and circular accelerators

- Beam energy, field in bending magnets and machine radius are related by:

$$E_{\text{beam}} = 0.3 \mathbf{B} r$$

[GeV] [T] [m]

At the LHC ($r = 2.8 \text{ km}$), $\mathbf{B} = 8.33 \text{ T}$ to reach $E_{\text{beam}} = 7 \text{ TeV}$

- Superconductivity permits to produce high field and thus to limit size and electrical consumption of the accelerators

	Normal conducting	Superconducting (LHC)
Magnetic field	1.8 T (iron saturation)	8.3 T (NbTi critical surface)
Field geometry	Defined by magnetic circuit	Defined by coils
Current density in windings	10 A/mm ²	400 A/mm ²
Electromagnetic forces	20 kN/m	3400 kN/m
Electrical consumption	10 kW/m	2 kW/m



Limiting energy stored in beam

- Energy W stored in the beams of circular accelerators and colliders

$$W \text{ [kJ]} = 3.34 E_{\text{beam}} \text{ [GeV]} I_{\text{beam}} \text{ [A]} C \text{ [km]}$$

C circumference of accelerator/collider

⇒ building compact machines, i.e. producing higher bending field B limits beam stored energy

- Example: the LHC

$$E_{\text{beam}} = 7000 \text{ GeV}$$

$$I_{\text{beam}} = 0.56 \text{ A}$$

$$C = 26.7 \text{ km}$$

$$\Rightarrow W = 350 \text{ MJ!}$$



Low impedance for beam stability

- Transverse impedance

$$Z_T(\omega) \sim \rho r / \omega b^3$$

ρ wall electrical resistivity

r average machine radius

b half-aperture of beam pipe

- Transverse resistive-wall instability

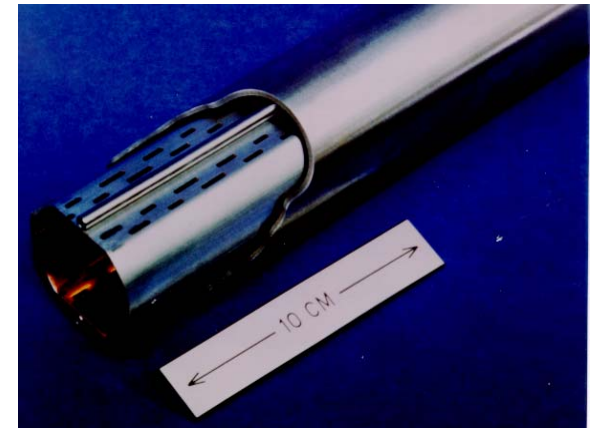
- dominant in large machines

- must be compensated by beam feedback, provided growth of instability is slow enough

- maximize growth time $\tau \sim 1 / Z_T(\omega)$ i.e. reduce $Z_T(\omega)$

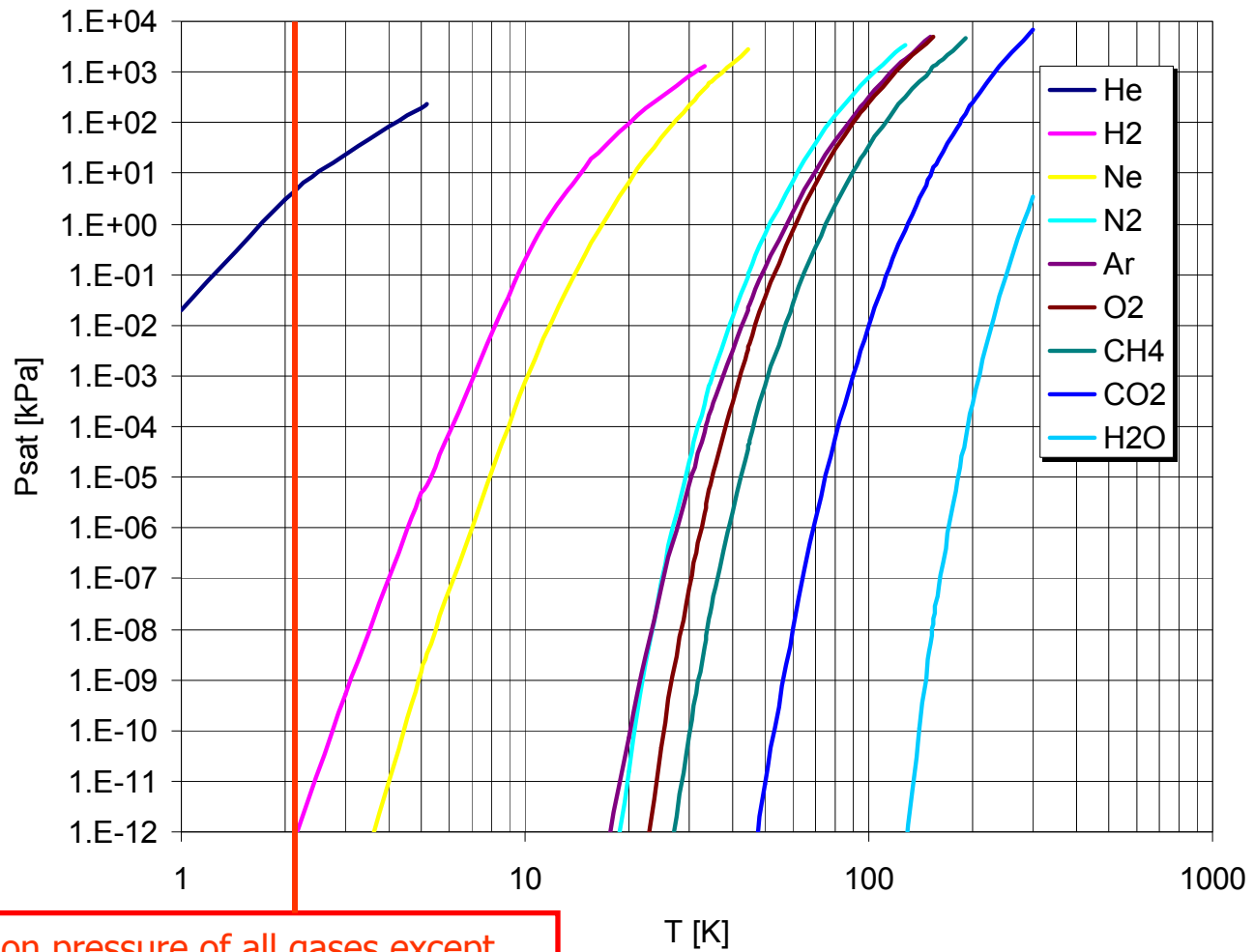
⇒ for a large machine with small aperture, low transverse impedance is achieved through low ρ , i.e. low-temperature wall

LHC beam pipe





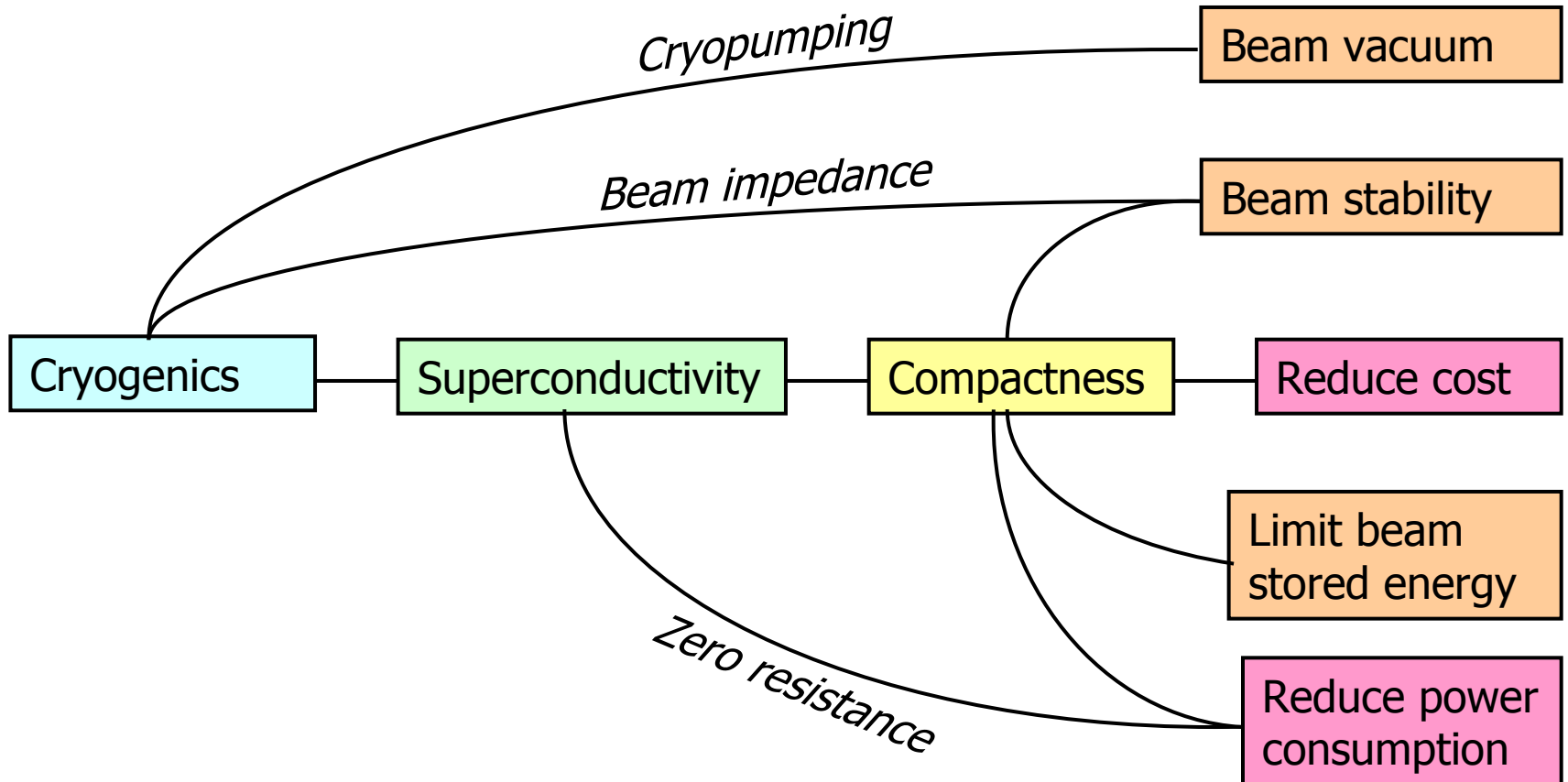
Cryopumping maintains good vacuum



Saturation pressure of all gases except helium vanish at cryogenic temperature



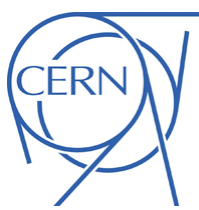
Rationale for superconductivity & cryogenics in particle accelerators





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Properties of cryogenes compared to water

Property		He	N ₂	H ₂ O
Normal boiling point	[K]	4.2	77	373
Critical temperature	[K]	5.2	126	647
Critical pressure	[bar]	2.3	34	221
Liq./Vap. density (*)		7.4	175	1600
Heat of vaporization (*)	[J.g ⁻¹]	20.4	199	2260
Liquid viscosity (*)	[μPI]	3.3	152	278

(*) at normal boiling point



Vaporization of normal boiling cryogenes under 1 W applied heat load

Cryogen	[mg.s ⁻¹]	[l.h ⁻¹] (liquid)	[l.min ⁻¹] (gas NTP)
Helium	48	1.38	16.4
Nitrogen	5	0.02	0.24

These numbers may be used for measuring heat load to a cryogen bath from boil-off flow measurements **at constant liquid level**

At decreasing level, the escaping flow is lower than the vaporization rate and a correction must be applied

$$\dot{m}_{out} = \dot{m}_{vap} \left(1 - \frac{\rho_v}{\rho_l} \right) < \dot{m}_{vap}$$



Amount of cryogenics required to cool down 1 kg iron

Using	Latent heat only	Latent heat and enthalpy of gas
LHe from 290 to 4.2 K	29.5 litre	0.75 liter
LHe from 77 to 4.2 K	1.46 litre	0.12 litre
LN2 from 290 to 77 K	0.45 litre	0.29 litre

⇒ recover enthalpy from cold gas (i.e. moderate flow of cryogen)

⇒ pre-cool with liquid nitrogen to save liquid helium



Cooldown of LHC sector (4625 t over 3.3 km)



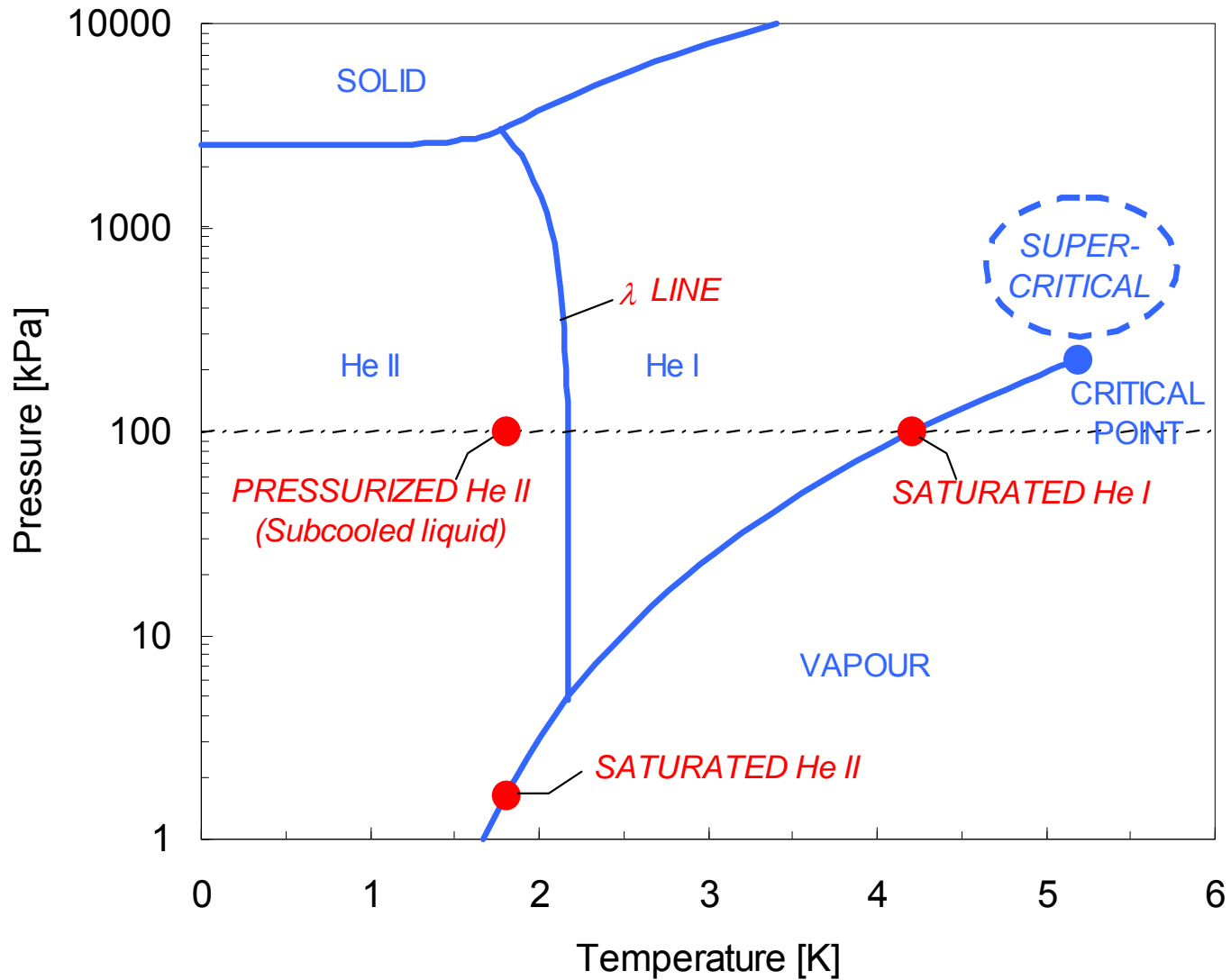
1260 tons LIN unloaded

600 kW precooling to 80 K with
LIN (up to ~5 tons/h)





Phase diagram of helium



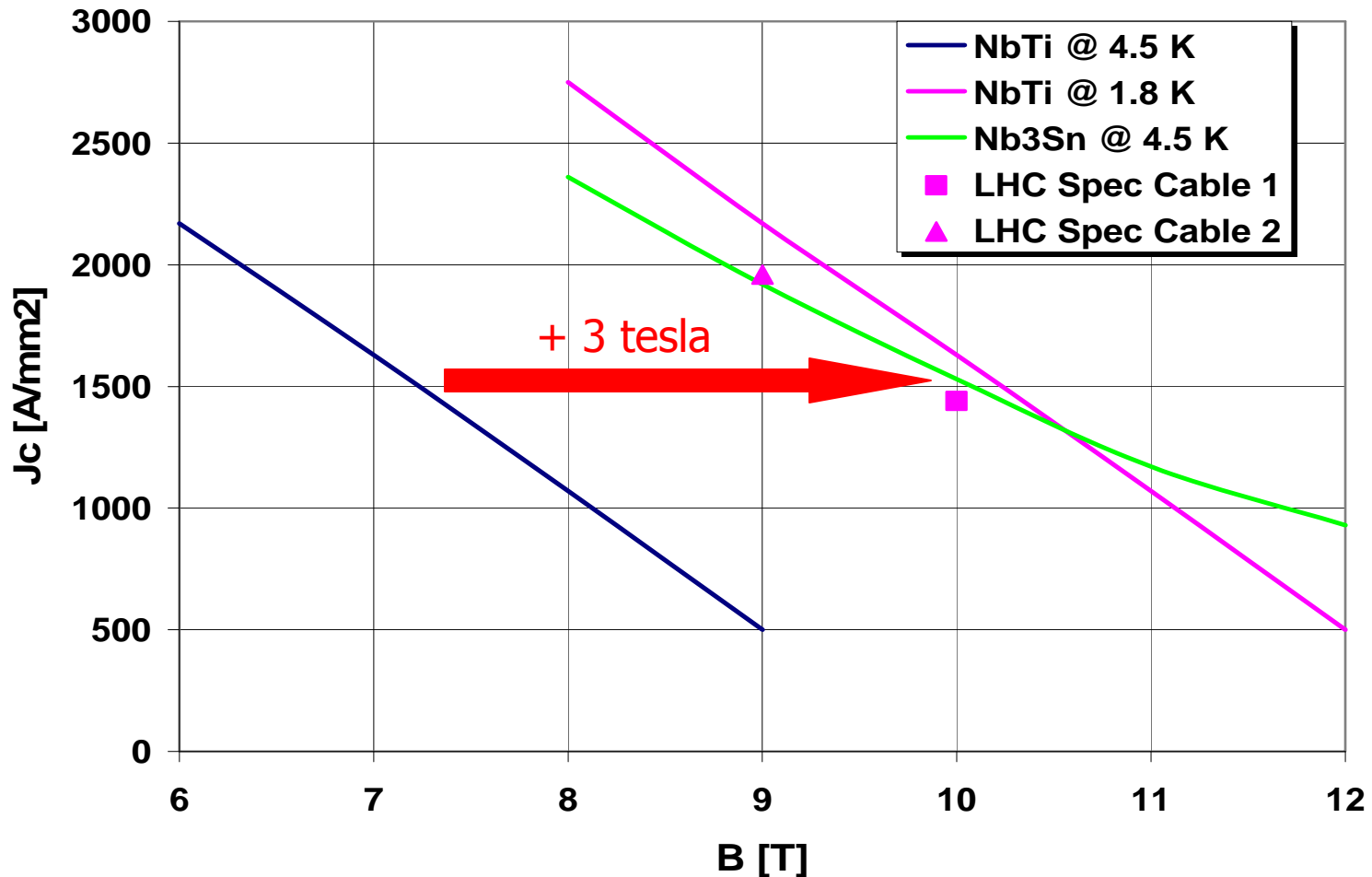


Helium as a cooling fluid

Phase domain	Advantages	Drawbacks
Saturated He I	Fixed temperature High heat transfer	Two-phase flow Boiling crisis
Supercritical	Monophase Negative J-T effect	Non-isothermal Density wave instability
He II	Low temperature High conductivity Low viscosity	Second-law cost Subatmospheric



He II cooling of LHC magnets allows to reach the 8 -10 T range using Nb-Ti superconductor





Enhancement of heat transfer

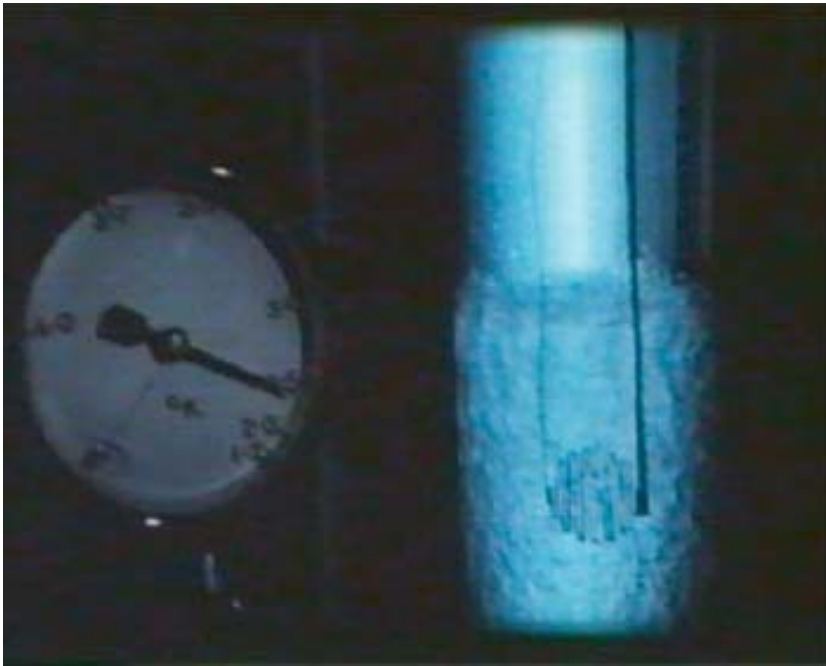
- Low viscosity \Rightarrow *permeation*
- Very high specific heat \Rightarrow *stabilization*
 - 10^5 times that of the conductor per unit mass
 - 2×10^3 times that of the conductor per unit volume
- Very high thermal conductivity \Rightarrow *heat transport*
 - 10^3 times that of cryogenic-grade OFHC copper
 - peaking at 1.9 K

Full benefit of these transport properties can only be reaped by appropriate design providing good wetting of the superconductors and percolation paths in the insulation, often in conflict with other technical requirements

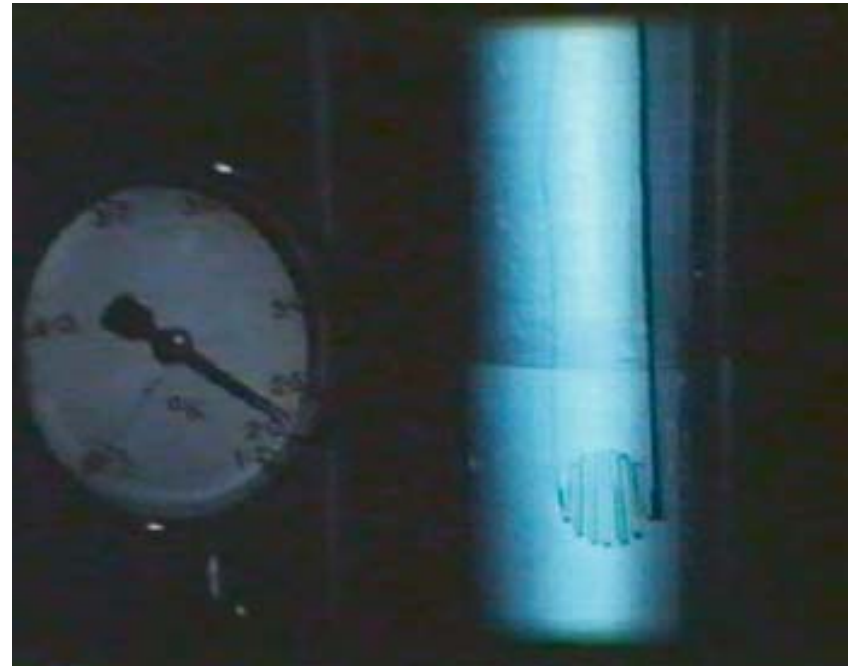


High thermal conductivity of the liquid suppresses boiling

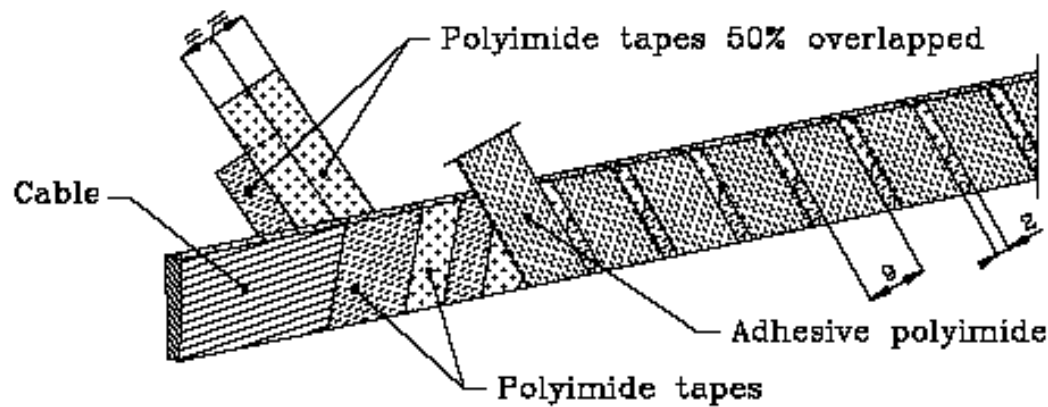
Electrical heater in saturated liquid helium



He I ($T=2.4$ K)

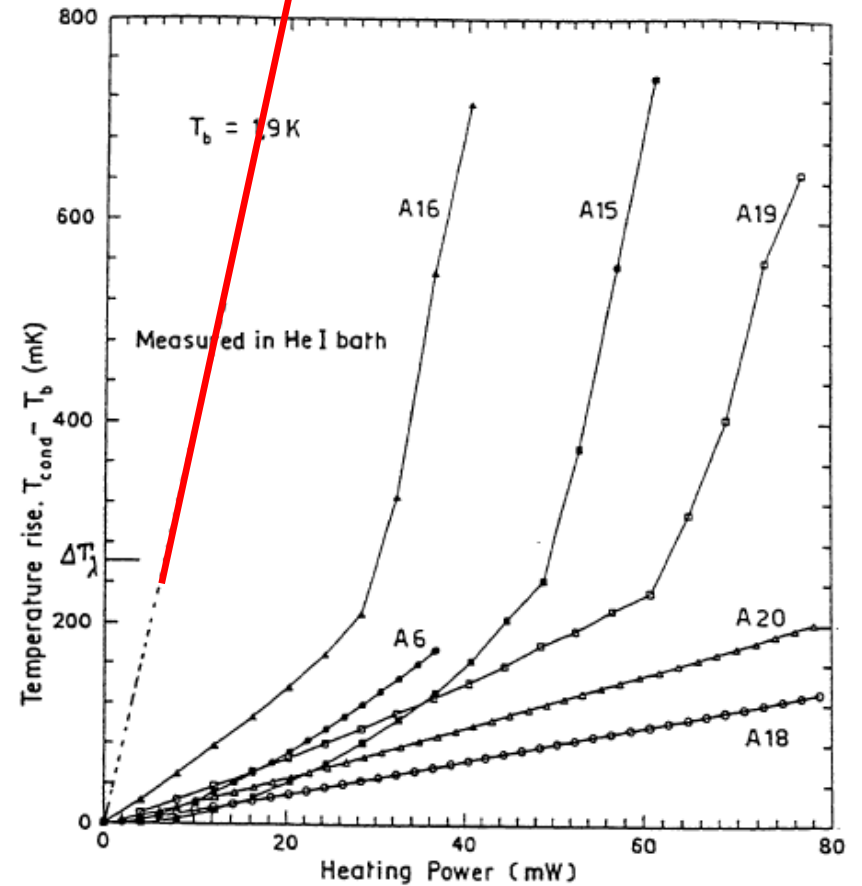


He II ($T=2.1$ K)

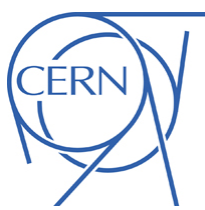


Conduction in polyimide

Heat transfer across electrical insulation of LHC superconducting cable



C. Meuris *et al.*



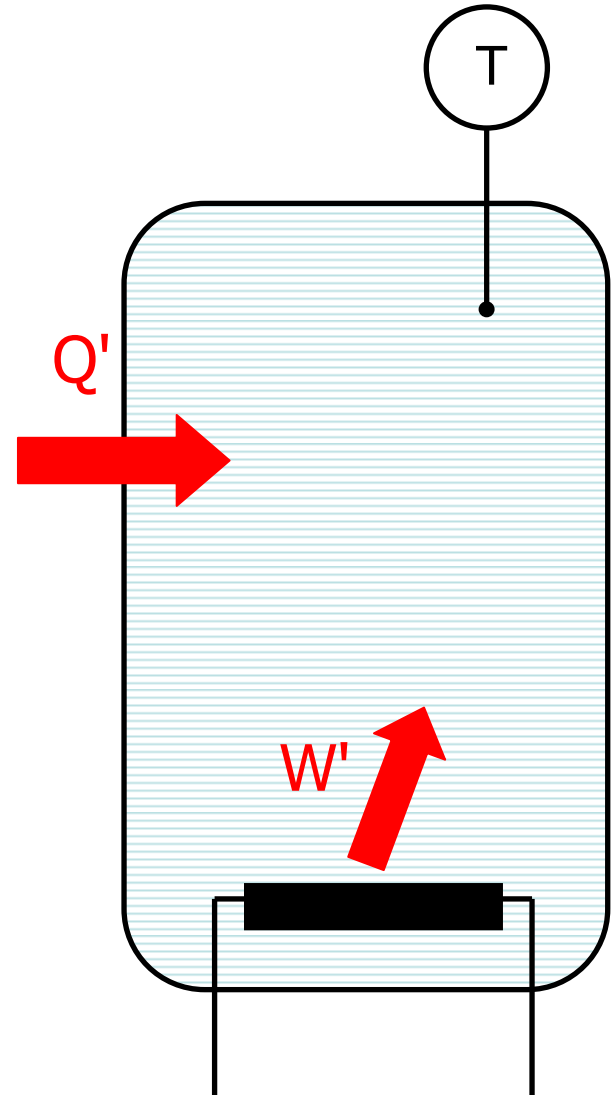
Calorimetry in isothermal He II bath

- For slow thermal transients, the He II bath is quasi-isothermal: a single temperature measurement allows to estimate heat deposition/generation Q'

$$Q' = M_{\text{bath}} dH/dt|_1$$

- M_{bath} can be estimated by *in situ* calibration, using applied heating power W'

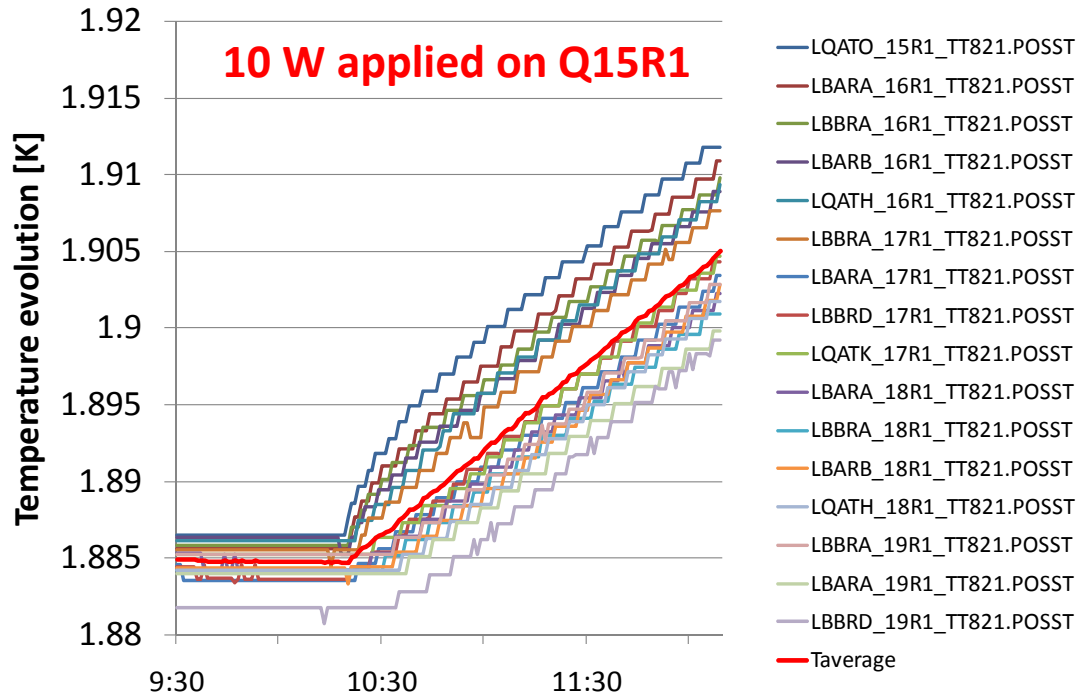
$$W' = M_{\text{bath}} dH/dt|_2$$





Measurement of electrical dissipation in LHC magnet subsector by He II calorimetry

10 W applied on Q15R1



	Before heating	With heating
ΔU [J/kg]	-1.1	78
M [kg]	823	
ΔU [kJ]	-0.92	64.2
t [s]	2880	6600
W [W]	-0.3	9.7
ΔW [W]	10.0	

- The additional power measured by He II calorimetry is 10.0 W, corresponding to the applied electrical power
- The method is validated and able to resolve $< W$



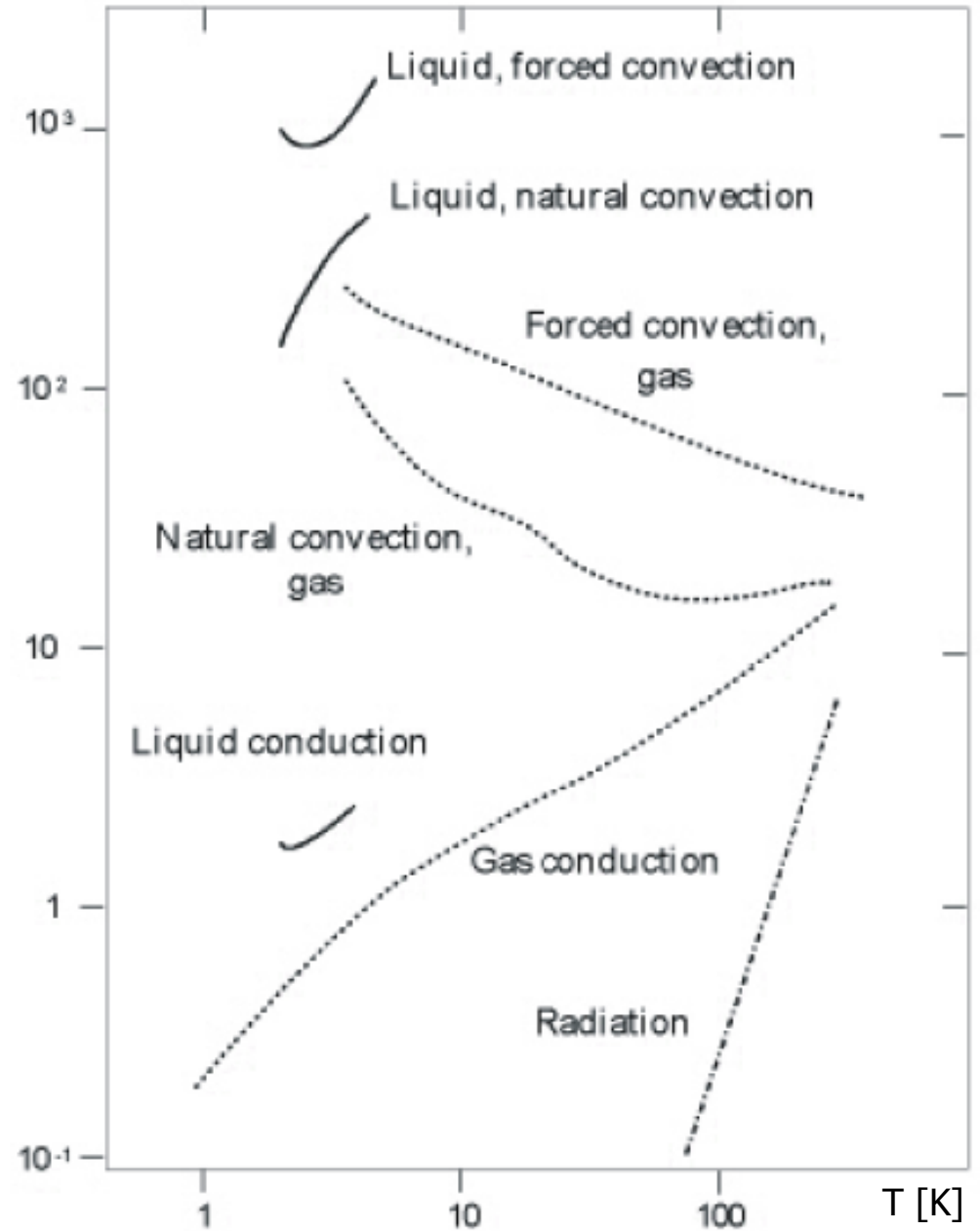
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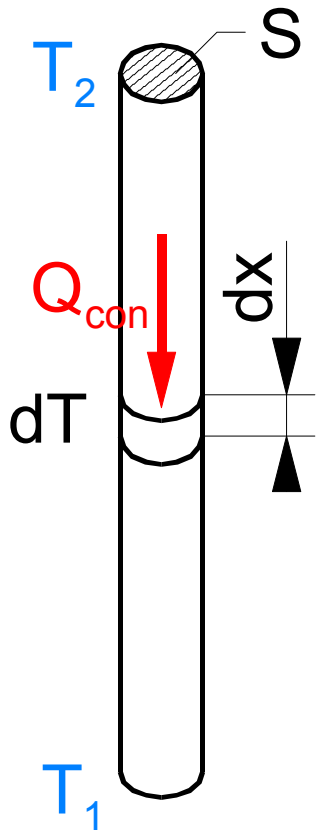
Typical heat transfer coefficients at cryogenic temperatures

$Q/(\Delta T.A)$ [W/ (m².K)]





Heat conduction in solids



Fourier's law: $Q_{\text{con}} = k(T) \cdot S \cdot \frac{dT}{dx}$

$k(T)$: thermal conductivity [W/m.K]

Integral form: $Q_{\text{con}} = \frac{S}{L} \cdot \int_{T_1}^{T_2} k(T) \cdot dT$

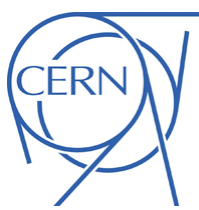
$\int k(T) \cdot dT$: thermal conductivity integral [W/m]

Thermal conductivity integrals for standard construction materials are tabulated

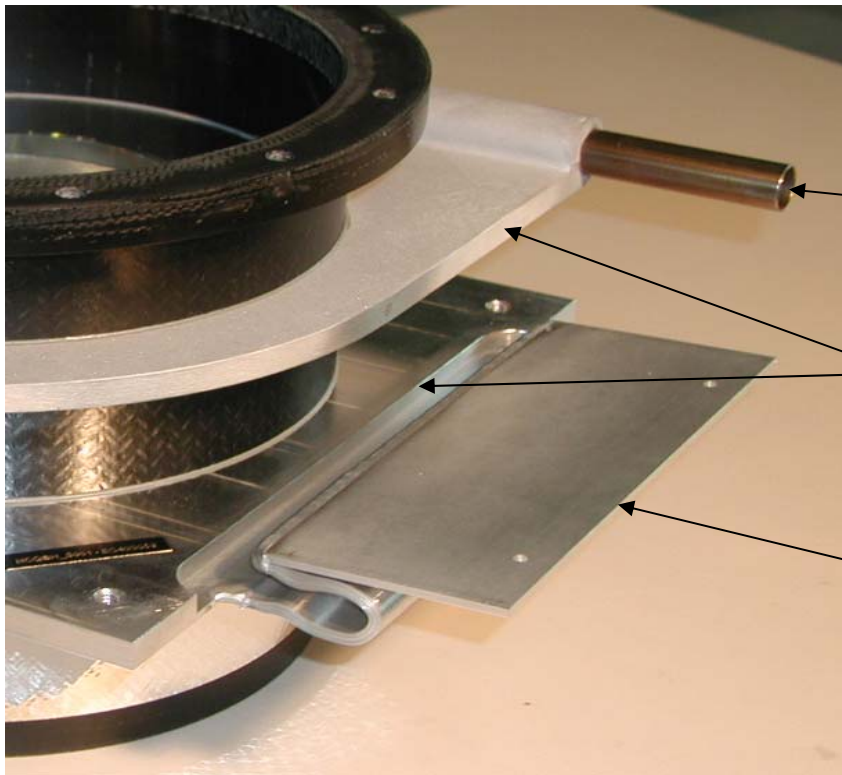
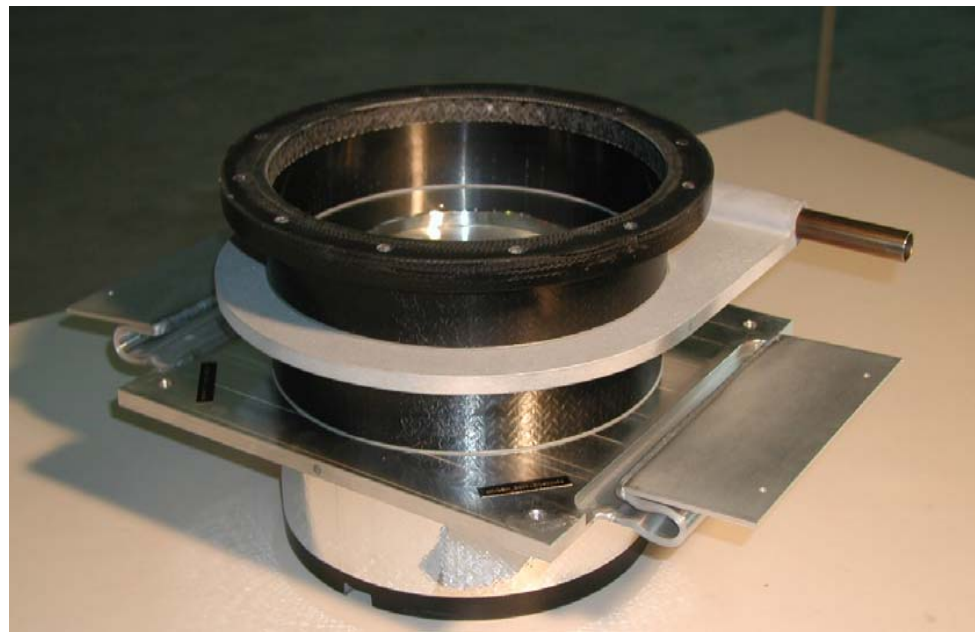


Thermal conductivity integrals of selected materials [W/m]

From vanishingly low temperature up to	20 K	80 K	290 K
OFHC copper	11000	60600	152000
DHP copper	395	5890	46100
1100 aluminium	2740	23300	72100
2024 aluminium alloy	160	2420	22900
AISI 304 stainless steel	16.3	349	3060
G-10 glass-epoxy composite	2	18	153



Non-metallic composite support post with heat intercepts



5 K cooling line (SC He)

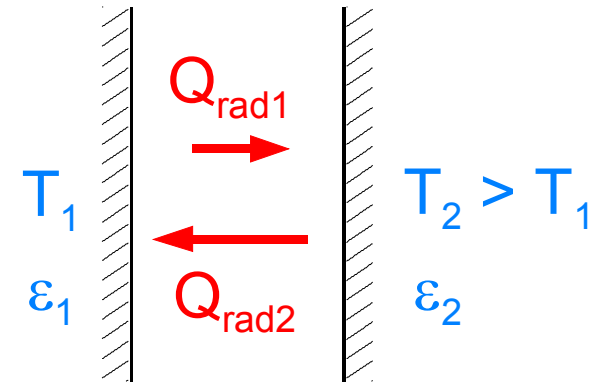
Aluminium intercept plates
glued to G-10 column

Aluminium strips to thermal
shield at 50-75 K



Thermal radiation

- Wien's law
 - Maximum of black body power spectrum
 $\lambda_{max} T = 2898 [\mu\text{m.K}]$
- Stefan-Boltzmann's law
 - Black body
 - "Gray"body
 - "Gray" surfaces at T_1 and T_2



$$Q_{rad} = \sigma A T^4$$

$$\sigma = 5.67 \times 10^{-8} \text{ W/m}^2\text{.K}^4$$

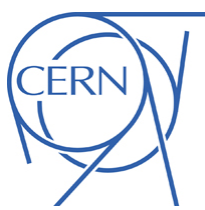
(Stefan Boltzmann's constant)

$$Q_{rad} = \epsilon \sigma A T^4$$

ϵ emissivity of surface

$$Q_{rad} = E \sigma A (T_1^4 - T_2^4)$$

E function of $\epsilon_1, \epsilon_2, \text{ geometry}$

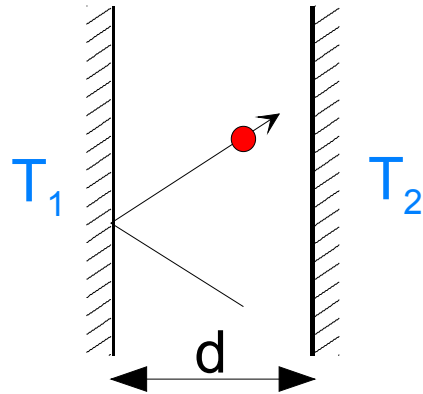


Emissivity of technical materials at low temperatures

	Radiation from 290 K Surface at 77 K	Radiation from 77 K Surface at 4.2 K
Stainless steel, as found	0.34	0.12
Stainless steel, mech. polished	0.12	0.07
Stainless steel, electropolished	0.10	0.07
Stainless steel + Al foil	0.05	0.01
Aluminium, as found	0.12	0.07
Aluminium, mech. polished	0.10	0.06
Aluminium, electropolished	0.08	0.04
Copper, as found	0.12	0.06
Copper, mech. Polished	0.06	0.02



Residual gas conduction



$\lambda_{molecule}$: mean free path of gas molecules

- Viscous regime

- At high gas pressure $\lambda_{molecule} \ll d$
- Classical conduction $Q_{res} = k(T) A dT/dx$
- Thermal conductivity $k(T)$ independent of pressure

- Molecular regime

- At low gas pressure $\lambda_{molecule} \gg d$
- Kennard's law $Q_{res} = A \alpha(T) \Omega P (T_2 - T_1)$
- Conduction heat transfer proportional to pressure, independent of spacing between surfaces
 Ω depends on gas species
- Accommodation coefficient $\alpha(T)$ depends on gas species, T_1 , T_2 , and geometry of facing surfaces



Multi-layer insulation (MLI)



- Complex system involving three heat transfer processes
 - $Q_{MLI} = Q_{rad} + Q_{sol} + Q_{res}$
 - With n reflective layers of equal emissivity, $Q_{rad} \sim 1/(n+1)$
 - Due to parasitic contacts between layers, Q_{sol} increases with layer density
 - Q_{res} due to residual gas trapped between layers, scales as $1/n$ in molecular regime
 - Non-linear behaviour requires layer-to-layer modeling
- In practice
 - Typical data available from (abundant) literature
 - Measure performance on test samples



Typical heat fluxes at vanishingly low temperature between flat plates [W/m²]

Black-body radiation from 290 K	401
Black-body radiation from 80 K	2.3
Gas conduction (100 mPa He) from 290 K	19
Gas conduction (1 mPa He) from 290 K	0.19
Gas conduction (100 mPa He) from 80 K	6.8
Gas conduction (1 mPa He) from 80 K	0.07
MLI (30 layers) from 290 K, pressure below 1 mPa	1-1.5
MLI (10 layers) from 80 K, pressure below 1 mPa	0.05
MLI (10 layers) from 80 K, pressure 100 mPa	1-2

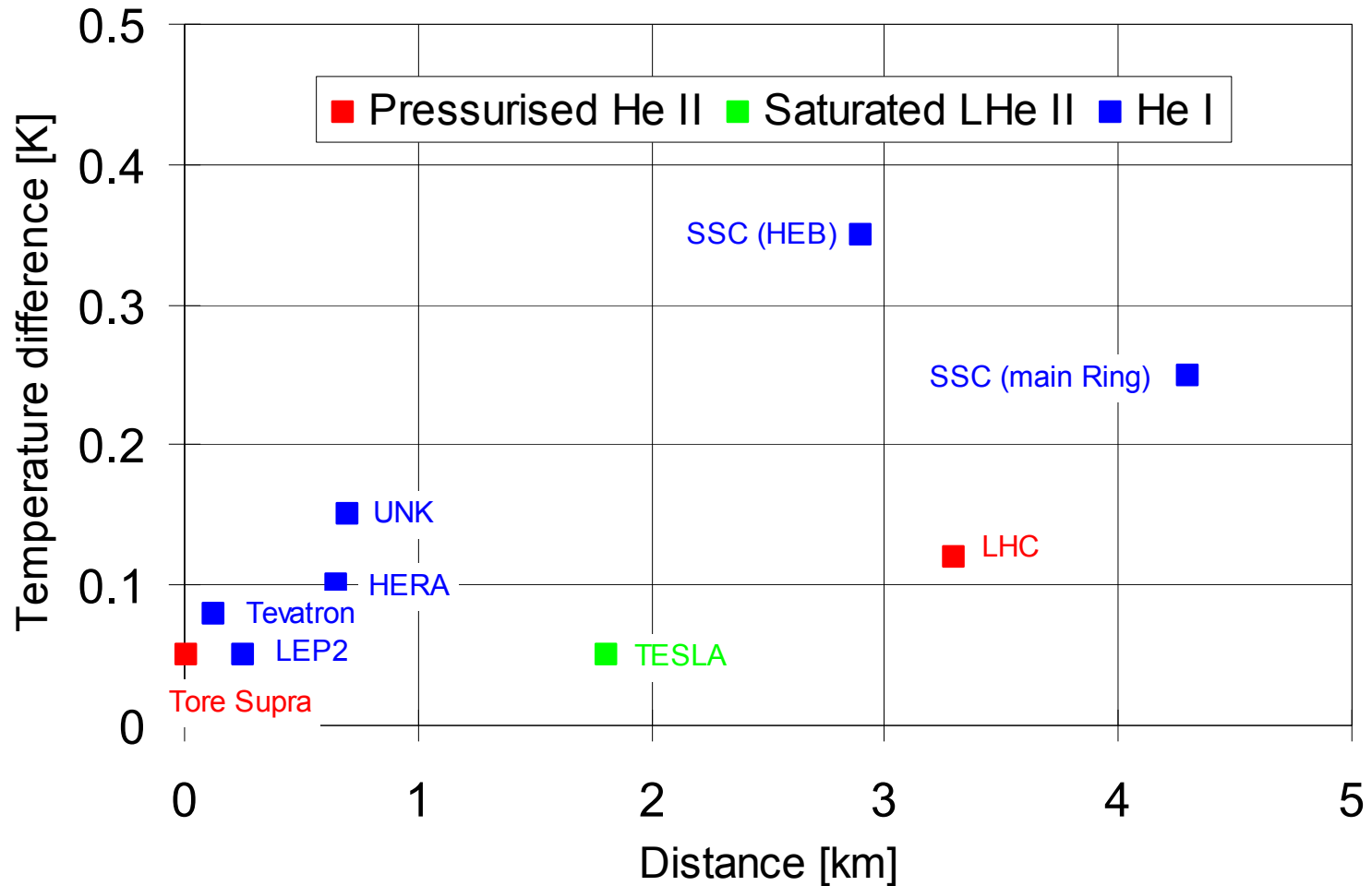


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Transport of refrigeration in large distributed cryogenic systems





Cryogenic distribution scheme: design issues

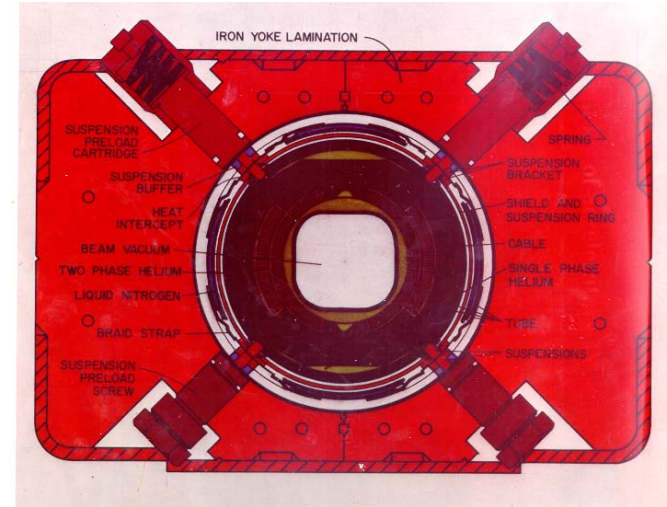
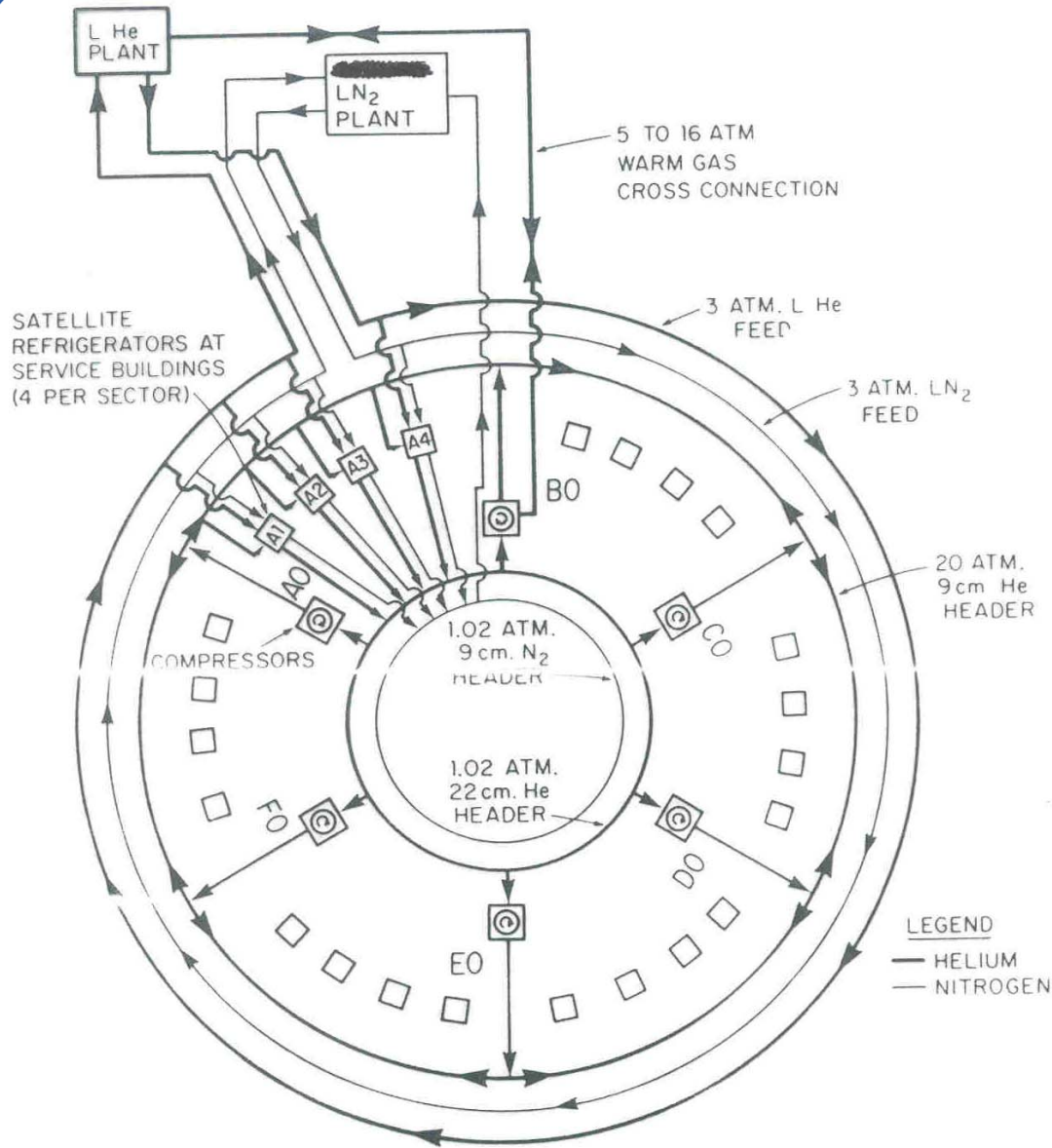
- Monophase vs. two-phase
 - temperature control
 - hydrostatic head & flow instabilities
- Pumps vs. no pumps
 - efficiency & cost
 - reliability & safety
- Use of liquid nitrogen
 - cooldown and/or normal operation
 - capital & operating costs of additional fluid
 - safety in underground areas (ODH)
- Lumped vs. distributed cryoplants
- Separate cryoline vs. integrated piping
- Number of active components (valves, actuators)
- Redundancy of configuration



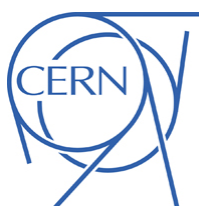
The Tevatron at Fermilab, USA



Tevatron distribution scheme



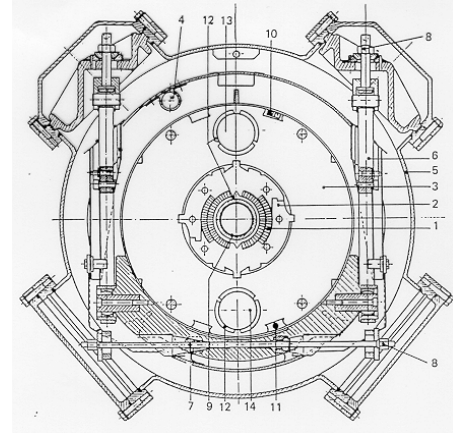
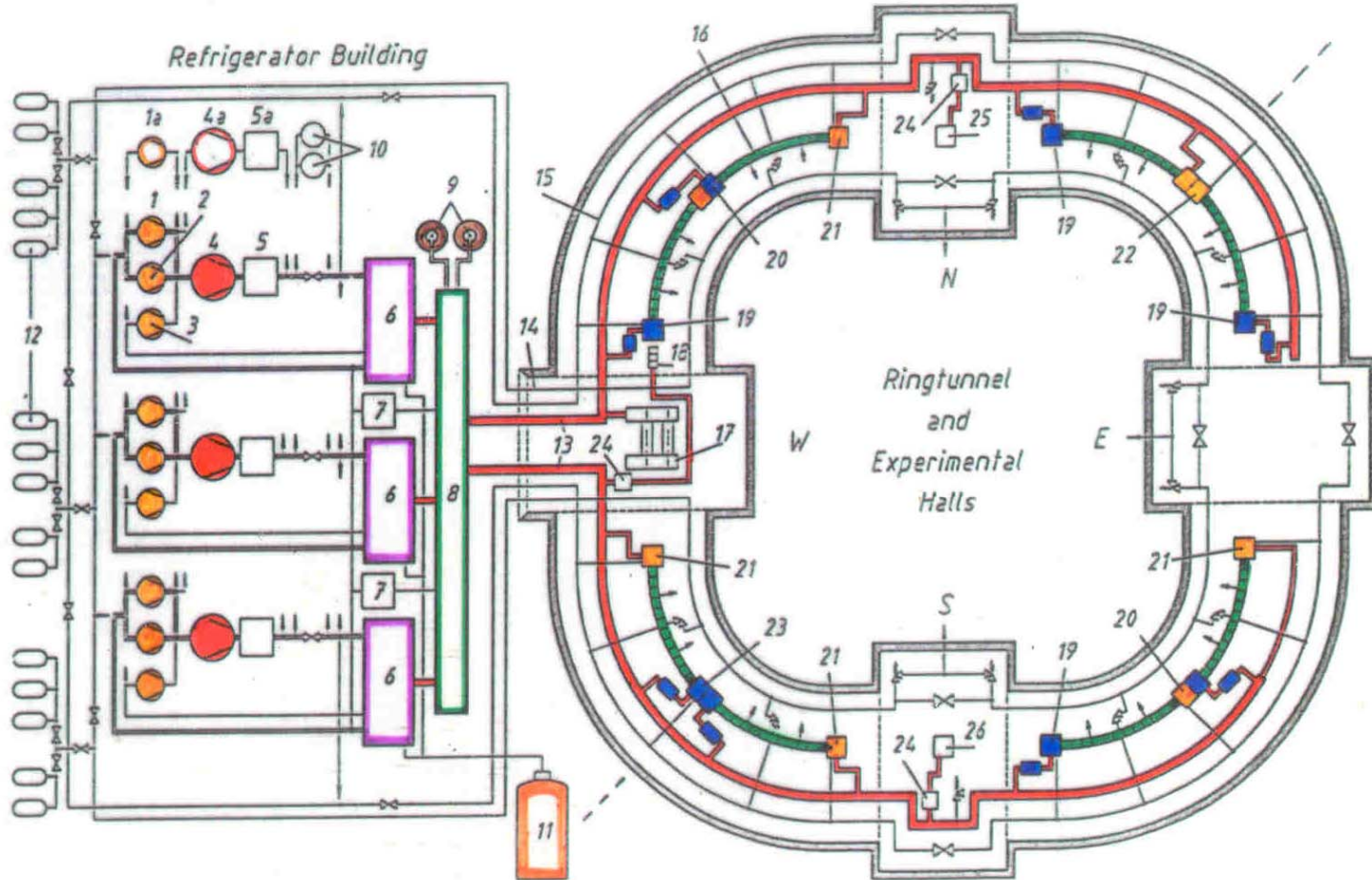
Central helium liquefier,
separate ring cryoline and
24 satellite refrigerators



HERA proton ring at DESY, Germany

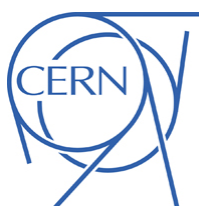


HERA distribution scheme



Central cryoplat and separate ring cryoline

Refrigeration 4.3 K	6775 W	total mass flow	0.871 kg/s
Refrigeration 40/80 K	20000 W	Primary power	2845 kW
Current lead flow	20.5×10^{-3} kg/s	Specif. power consumption	281 W (300 K)/W (4.3 K)

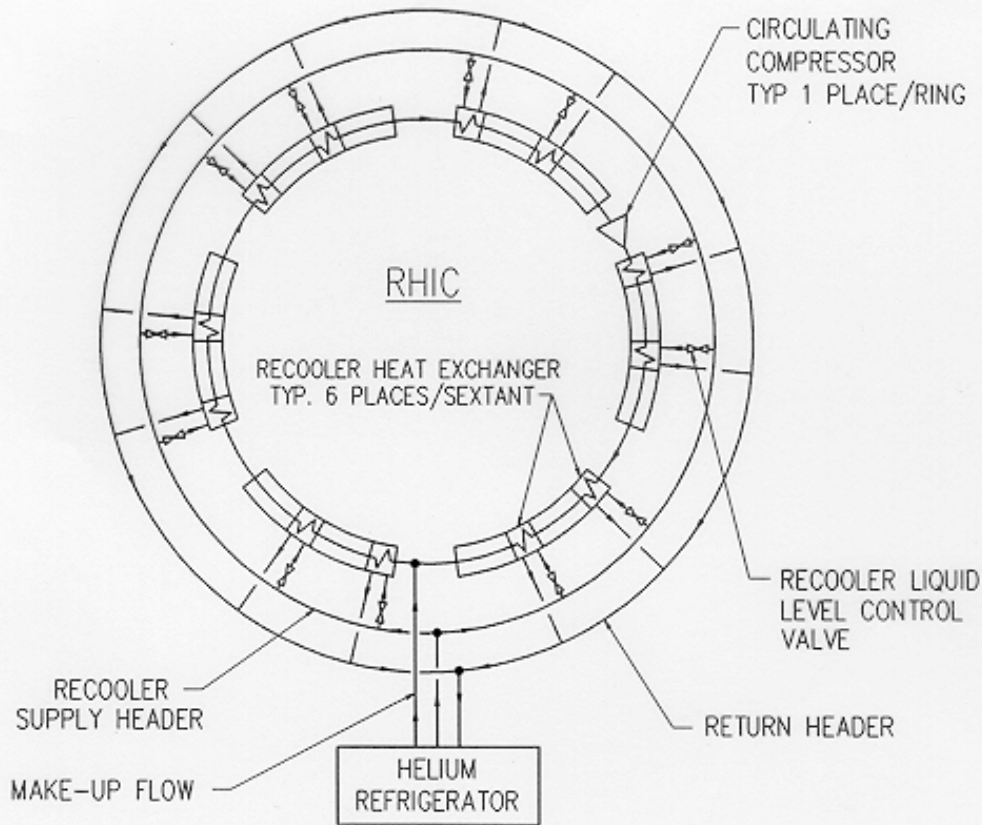


RHIC at Brookhaven National Lab, USA

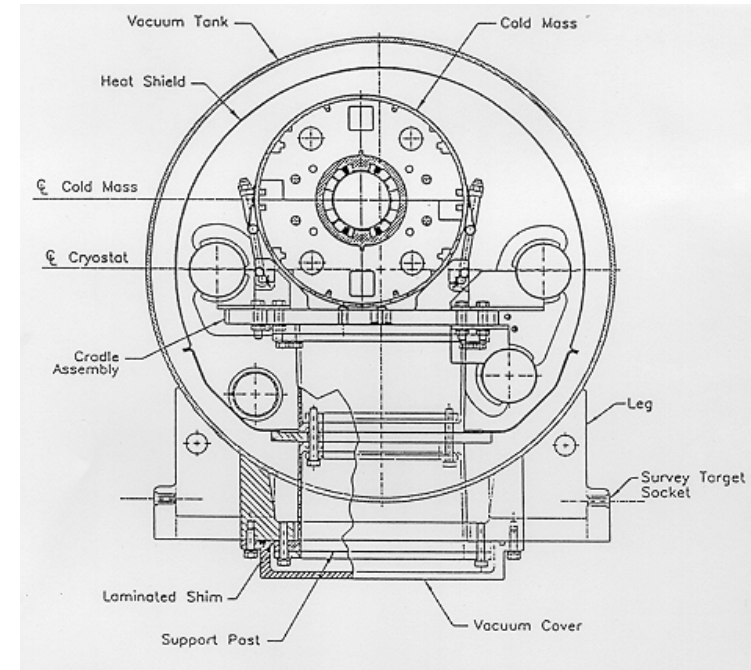




RHIC distribution scheme



HELIUM PRIMARY FLOW CIRCUIT FOR STEADY-STATE OPERATION.
ONLY ONE OF THE RINGS IS SHOWN.

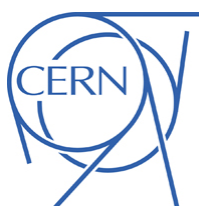


Central cryoplat and
piping integrated in
magnet cryostat

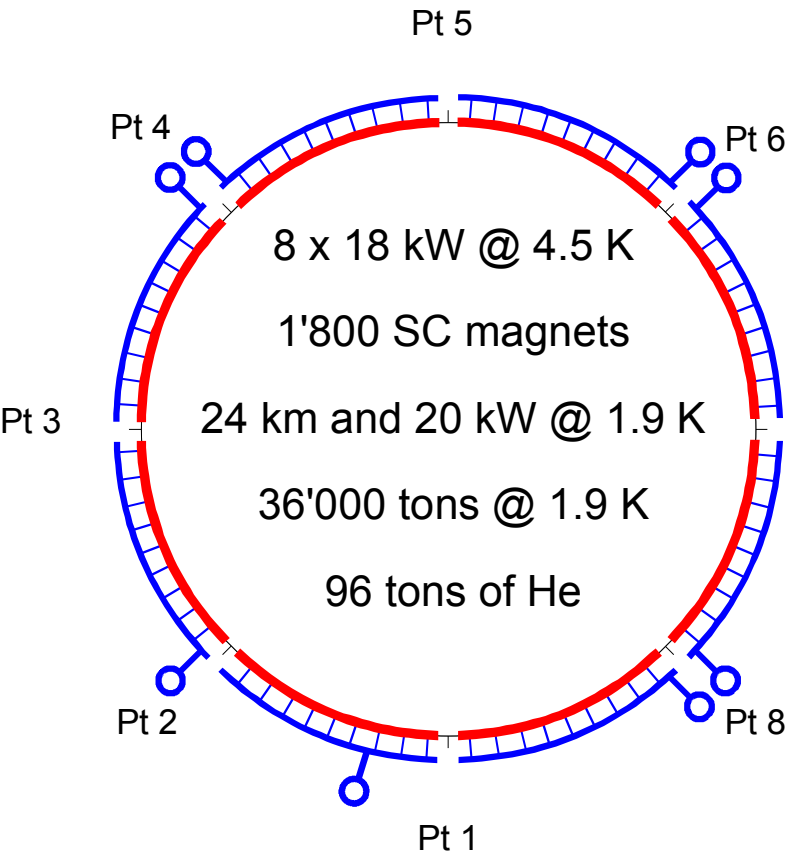


The LHC at CERN

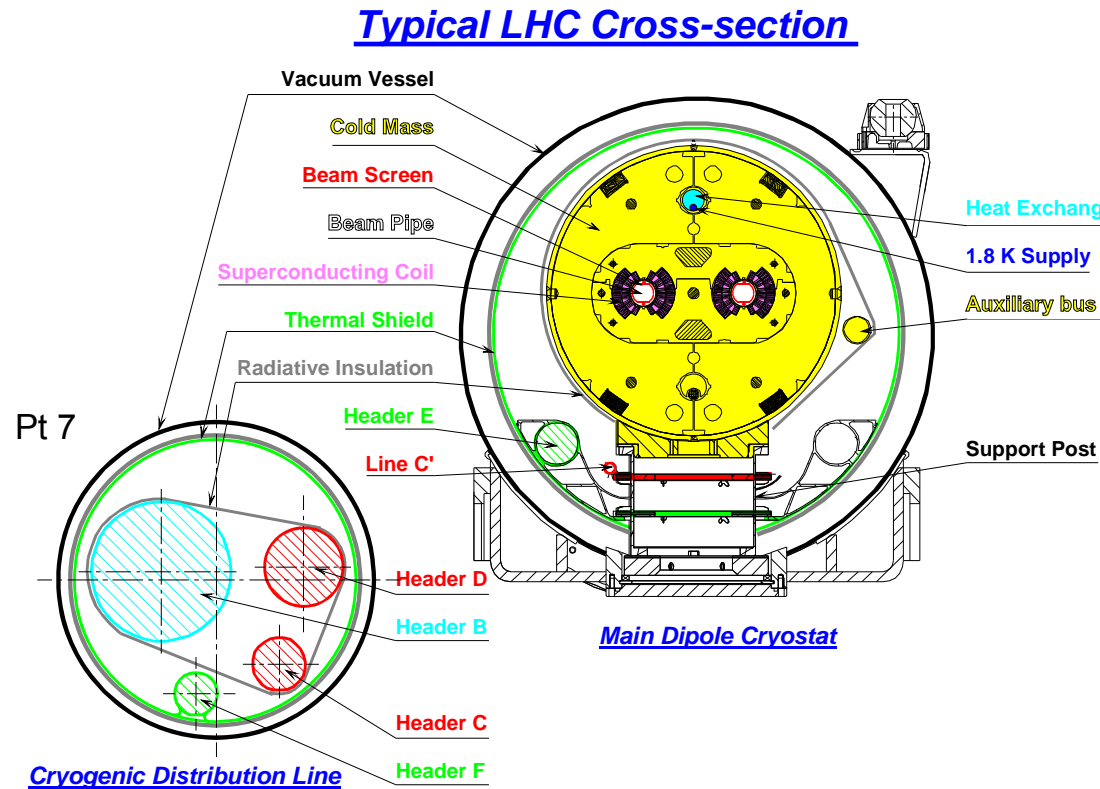




LHC distribution scheme

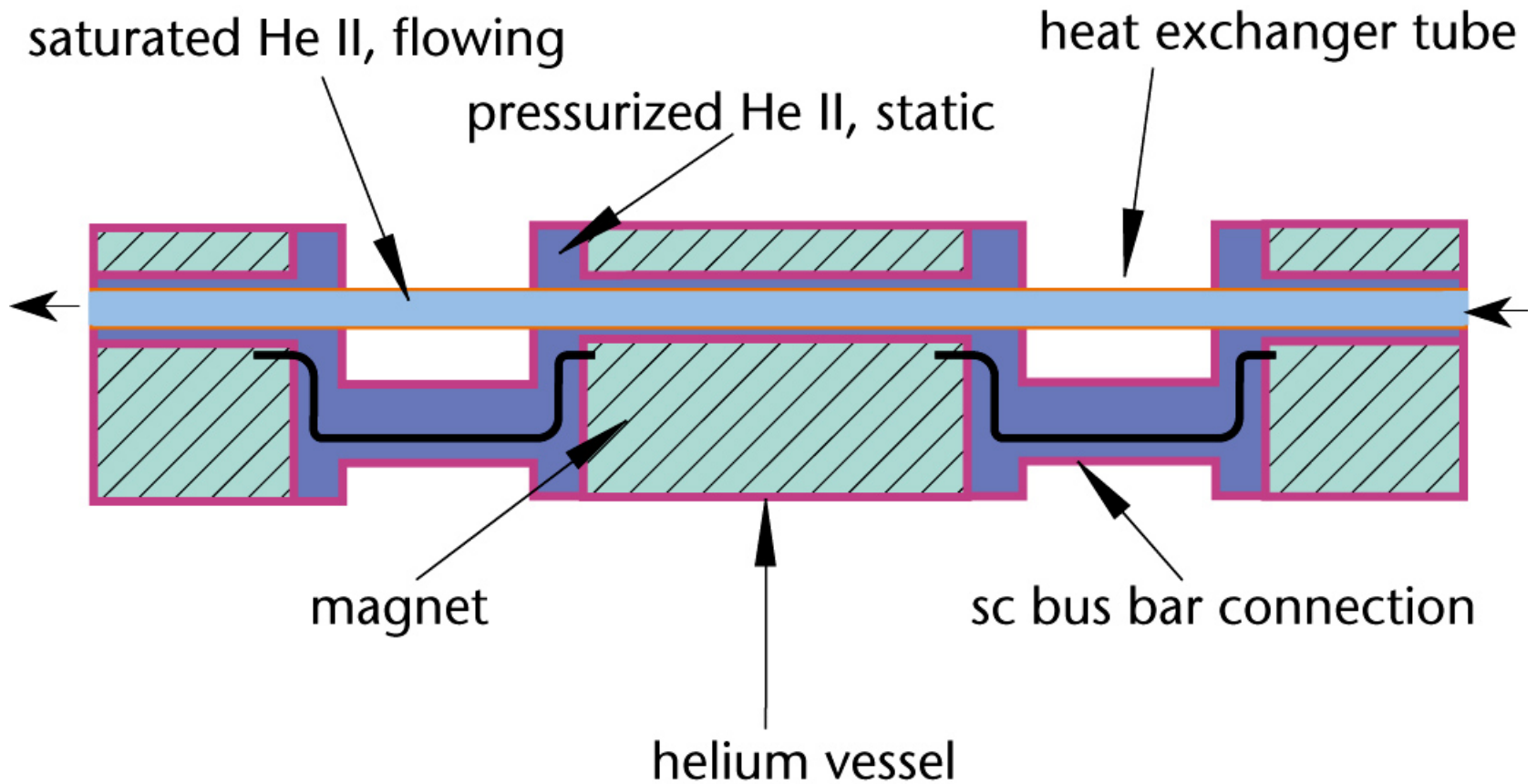


○ Cryogenic plant



Cryoplants at five points,
separate ring cryoline,
107 m long strings

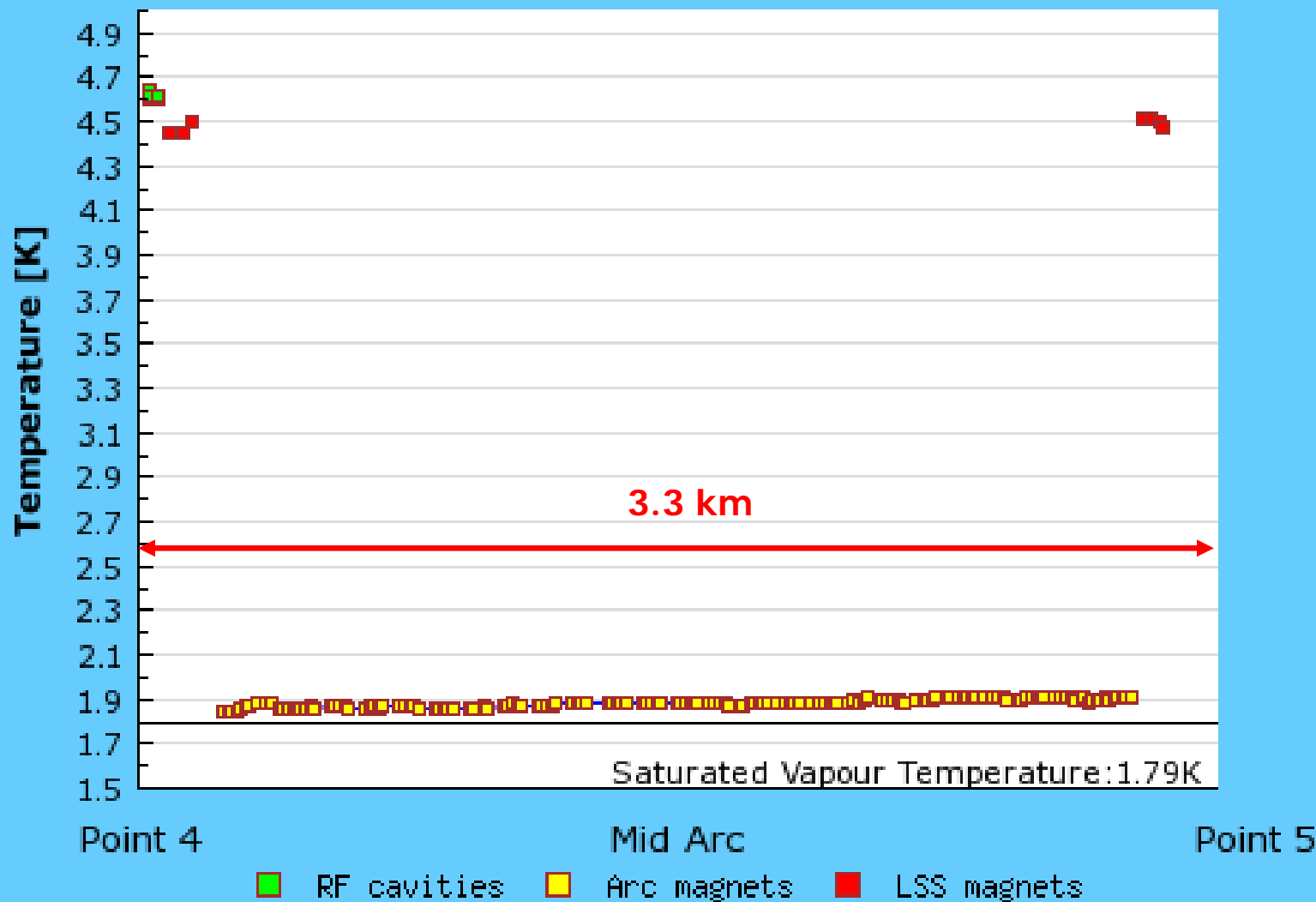
Principle of He II cooling of LHC magnets





Cryogenic operation of LHC sector

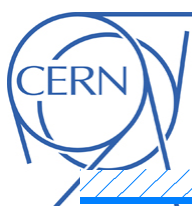
Sector temperature profile at 19 Feb 14:28



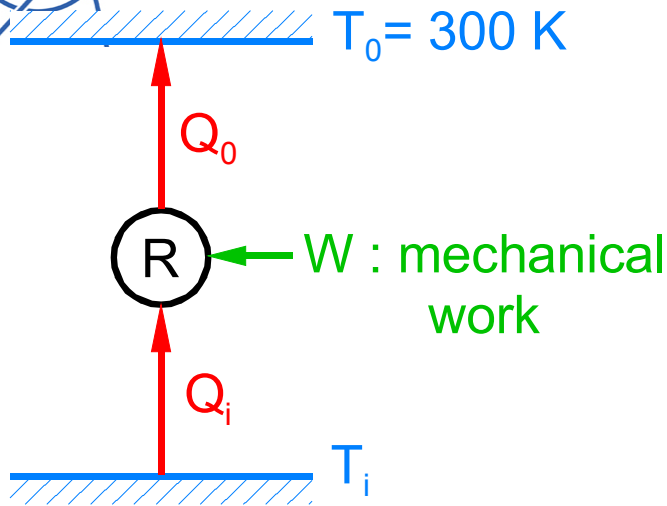


Contents

- Low temperatures and liquefied gases
- Cryogenics in accelerators
- Properties of fluids
- Heat transfer & thermal insulation
- Cryogenic distribution & cooling schemes
- **Refrigeration & liquefaction**



Thermodynamics of cryogenic refrigeration



First principle [Joule]

$$Q_0 = Q_i + W$$

Second principle [Clausius]

$$\frac{Q_0}{T_0} \geq \frac{Q_i}{T_i}$$

(= for reversible process)

Hence, $W \geq T_0 \cdot \frac{Q_i}{T_i} - Q_i$ which can be written in three different ways:

① $W \geq T_0 \cdot \Delta S_i - Q_i$ introducing **entropy S** as

$$\Delta S_i = \frac{Q_i}{T_i}$$

② $W \geq Q_i \cdot \left(\frac{T_0}{T_i} - 1 \right)$ ← **Carnot factor**

③ $W \geq \Delta E_i$ introducing **exergy E** as

$$\Delta E_i = Q_i \cdot \left(\frac{T_0}{T_i} - 1 \right)$$



Minimum refrigeration work

Consider the extraction of 1 W at 4.5 K, rejected at 300 K
The minimum refrigeration work (equation 2) is:

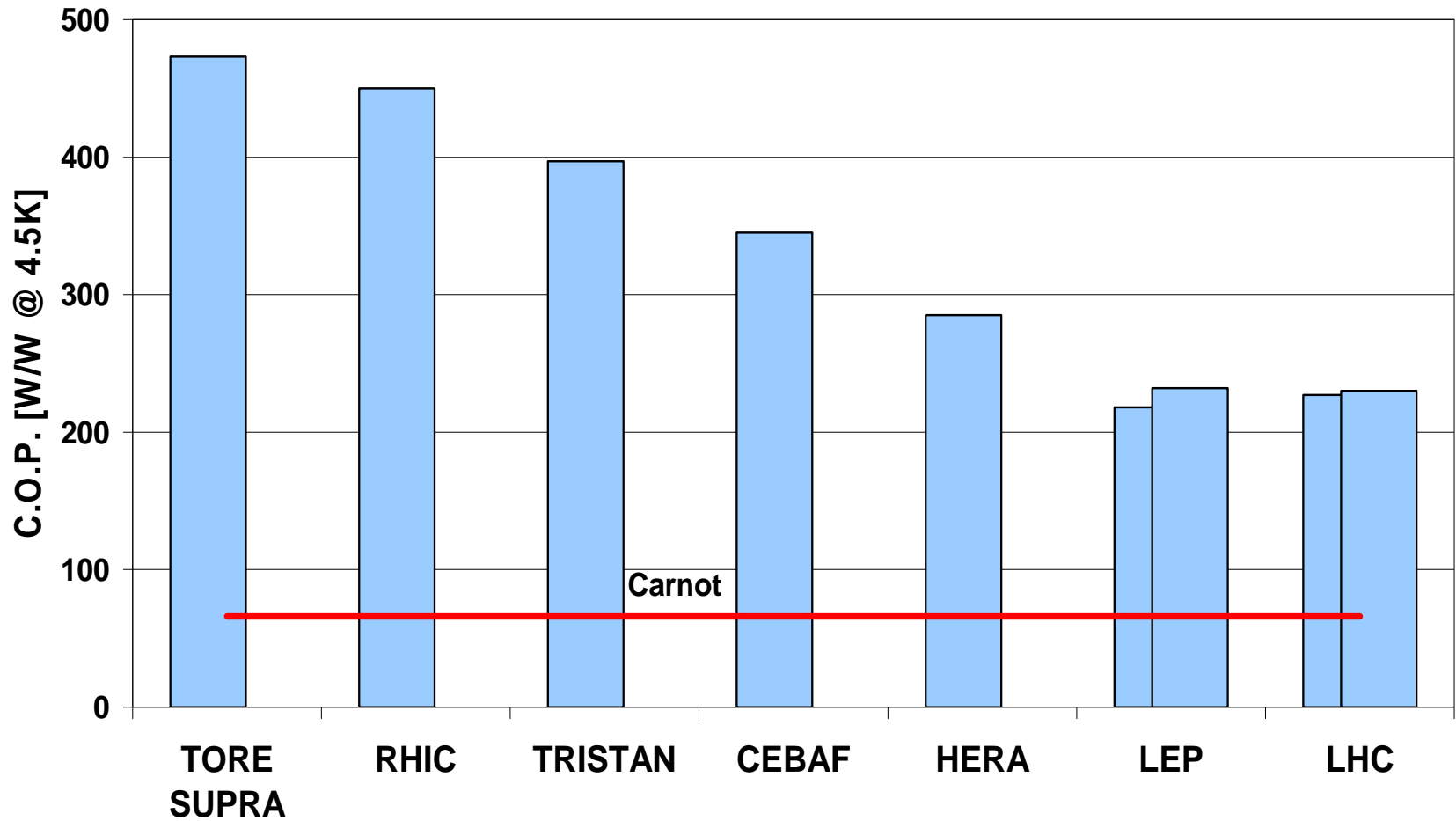
$$W_{\min} = Q_i \cdot \left(\frac{T_0}{T_i} - 1 \right) = 1 \cdot \left(\frac{300}{4.5} - 1 \right) = 65.7 \text{ W}$$

In practice, the most efficient helium refrigerators have an efficiency of about 30% w.r. to the Carnot limit.

$$\Rightarrow W_{\text{real}} = \frac{W_{\min}}{\eta} = \frac{65.7}{0.3} = 220 \text{ W}$$



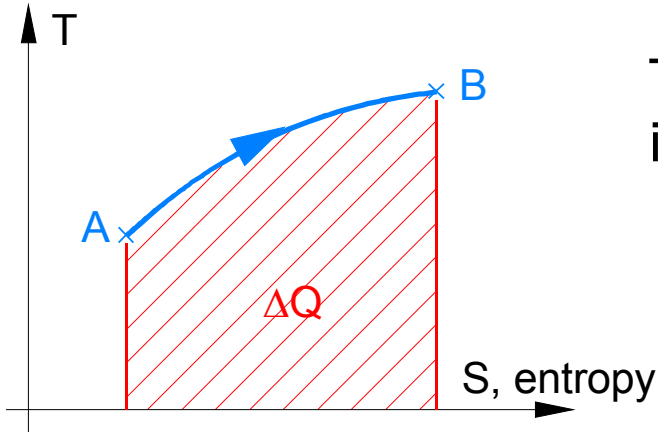
C.O.P. of large cryogenic helium refrigerators





Refrigeration cycles and duties

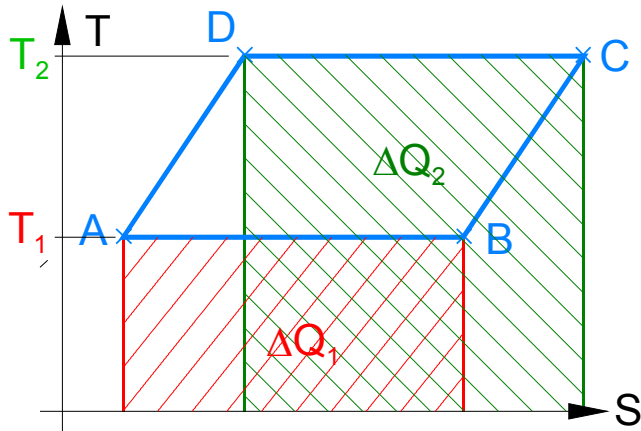
Introduction to the T-S diagram



Thermodynamic transformation from A to B,
if reversible:

$$\Delta Q = \int_A^B T \cdot dS$$

To make a refrigeration cycle, need a substance, the entropy of which depends on some other **variable** than temperature

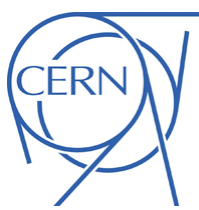


Pressure of gas: Compression/expansion cycle
Magnetization of solid: magnetic refr. cycle

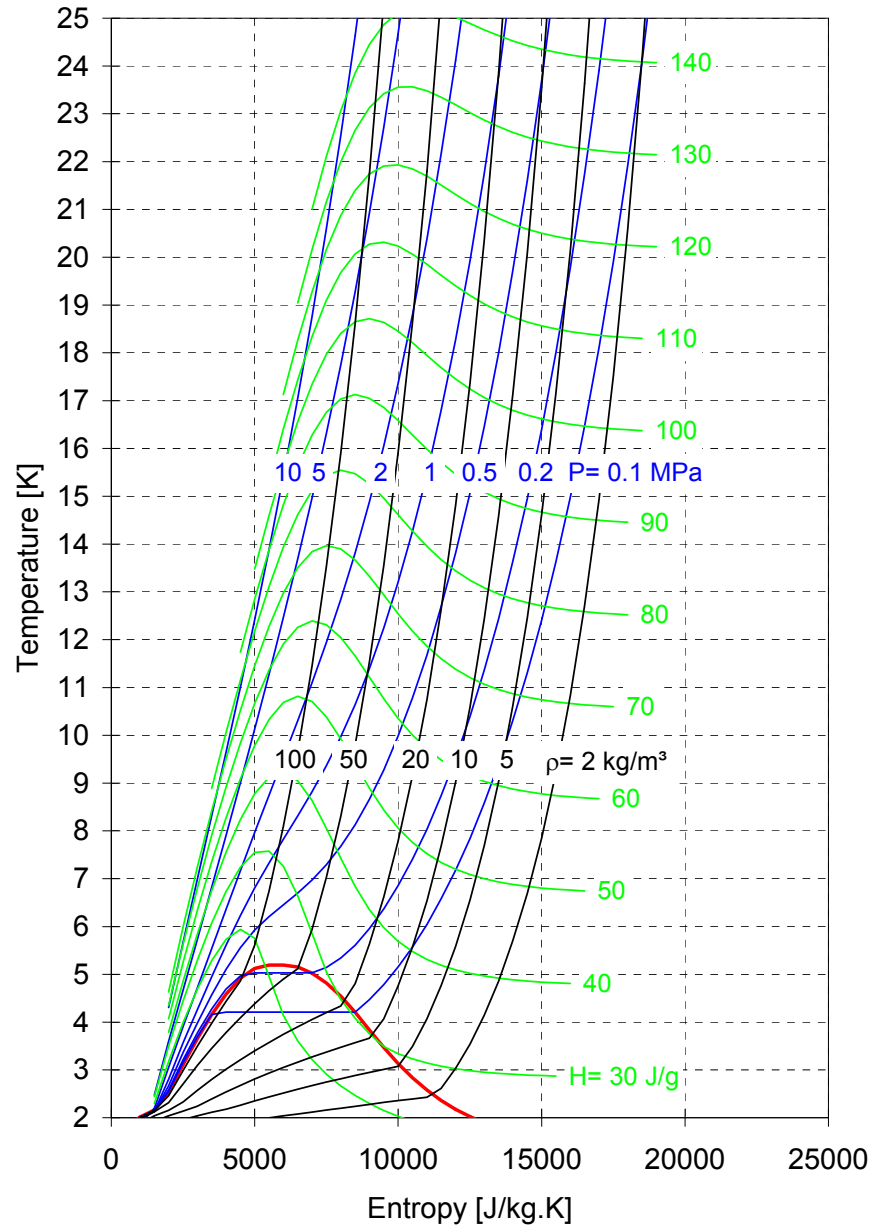
ΔQ_1 : heat absorbed at T_1

ΔQ_2 : heat rejected at T_2

→ Refrigeration cycle A B C D

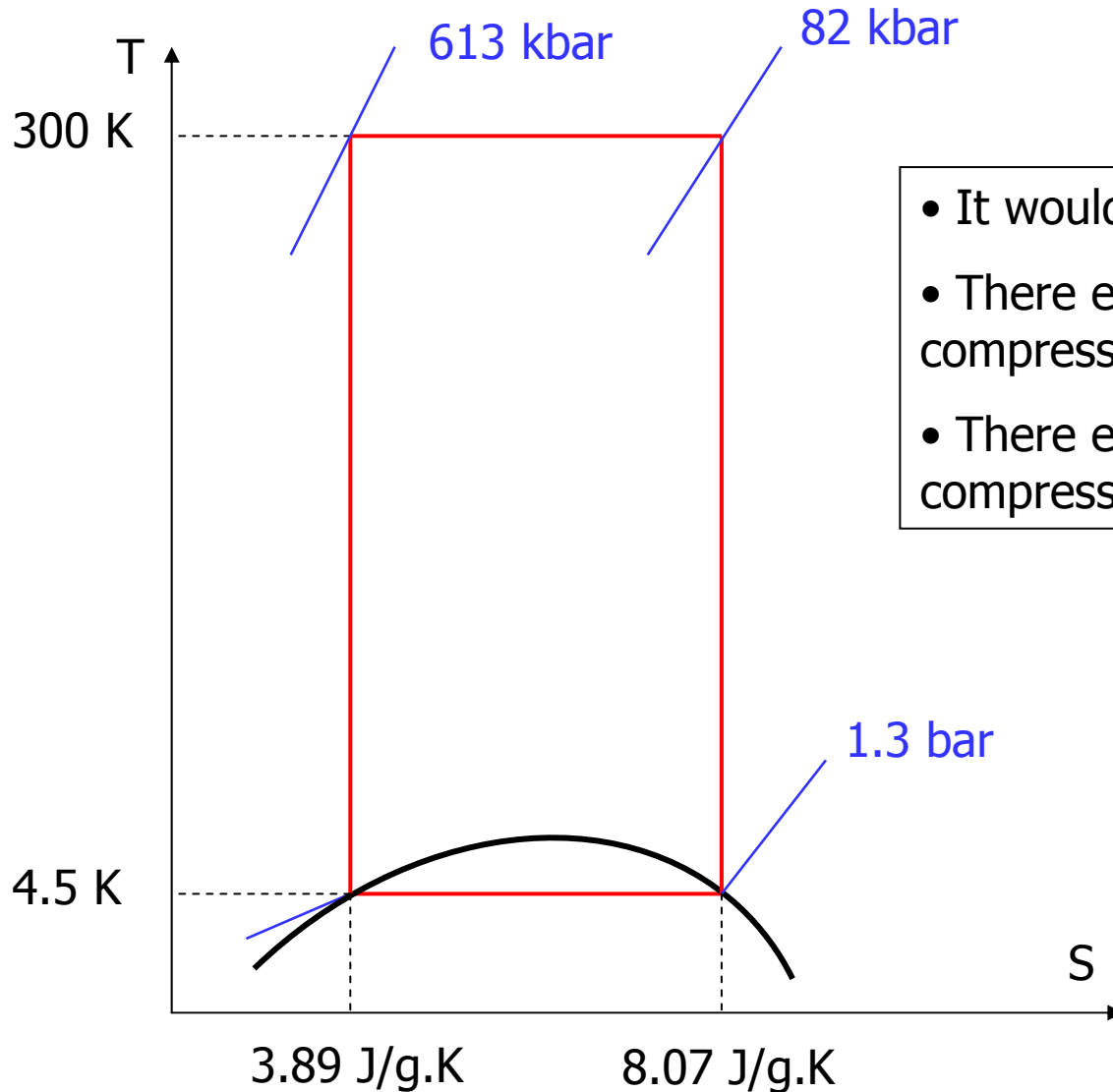


T-S diagram for helium





A Carnot cycle is not feasible for helium liquefaction

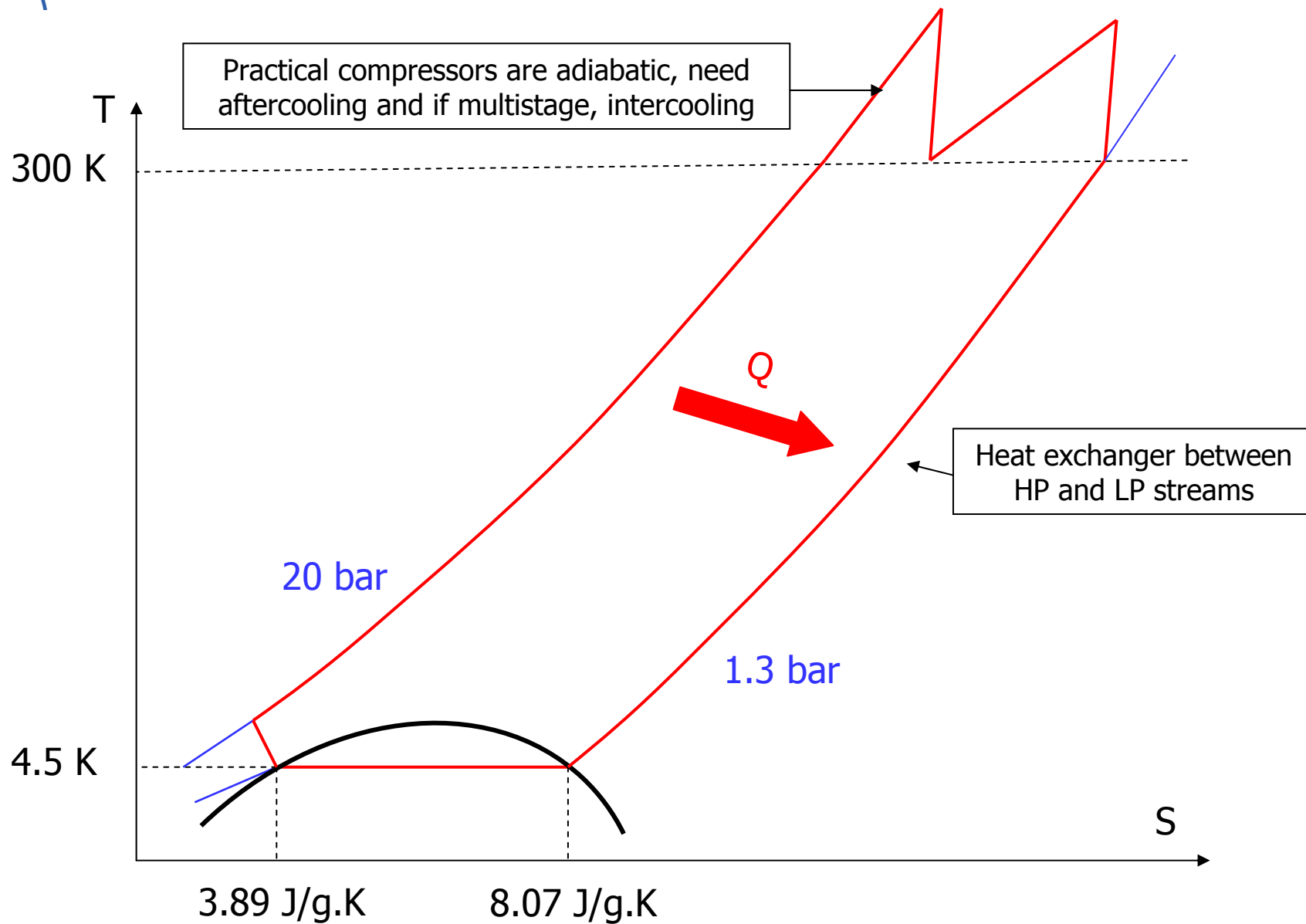


- It would need a HP of 613 kbar!
- There exists no true isothermal compressor
- There exists no true isentropic compressor or expander



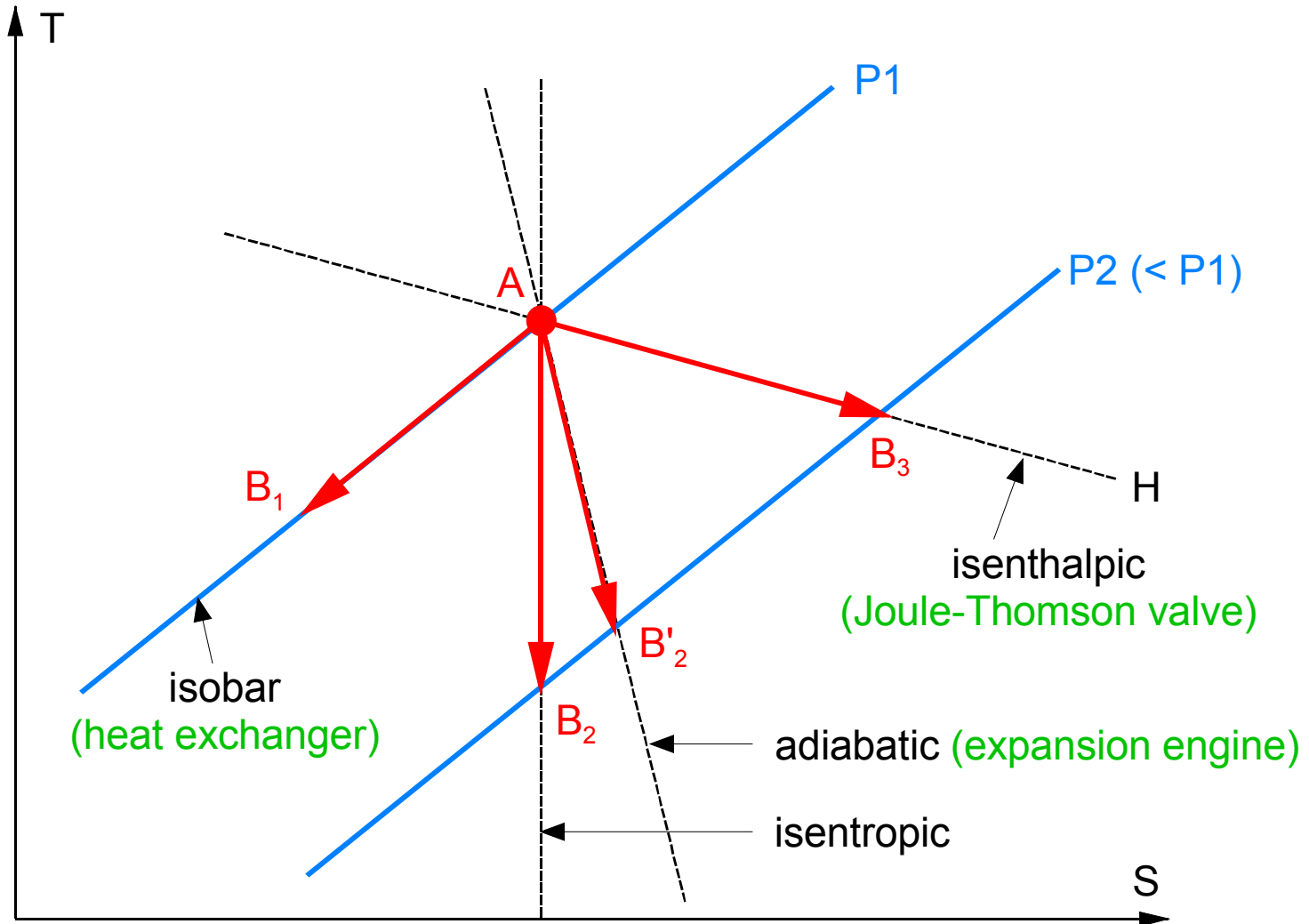
A real cycle

internal heat exchange and para-isothermal compression



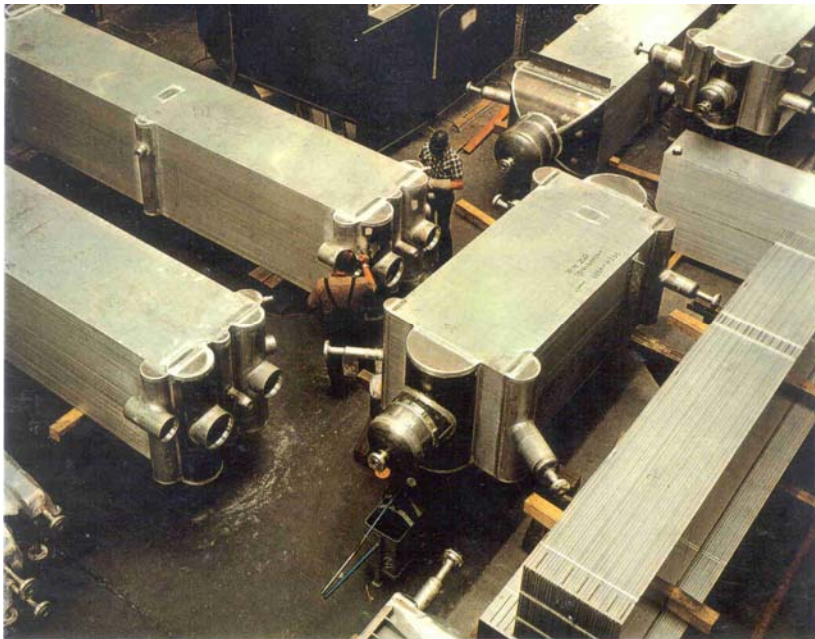
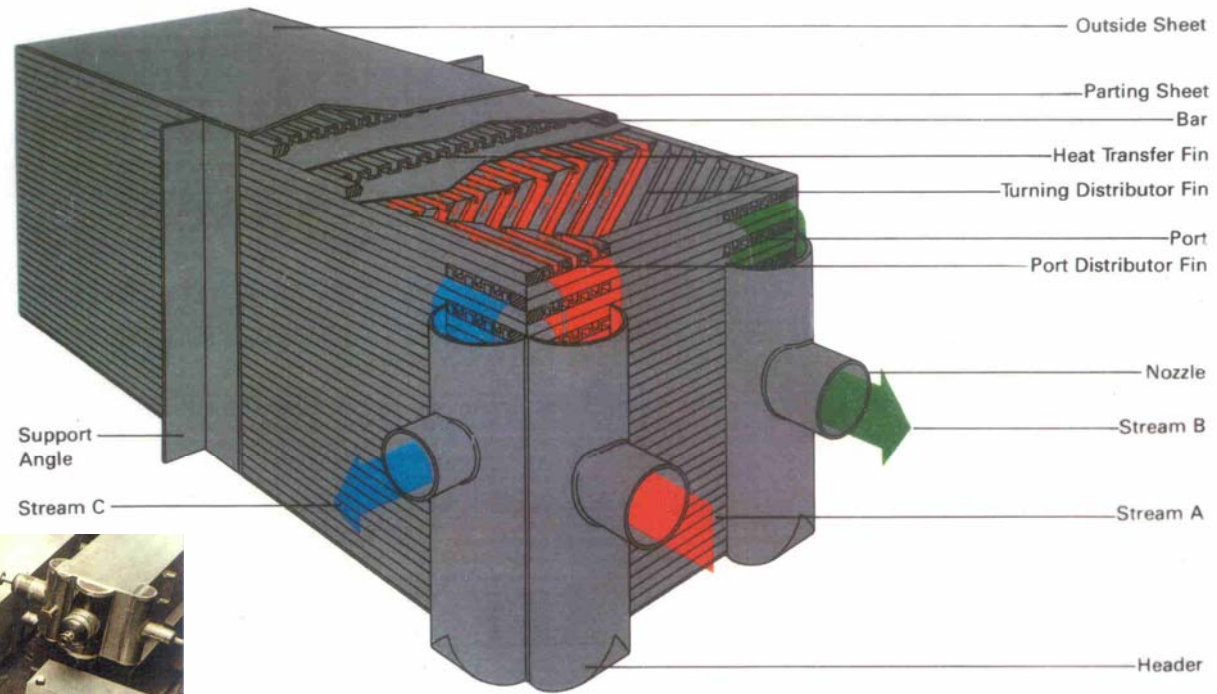


Elementary cooling processes on T-S diagram



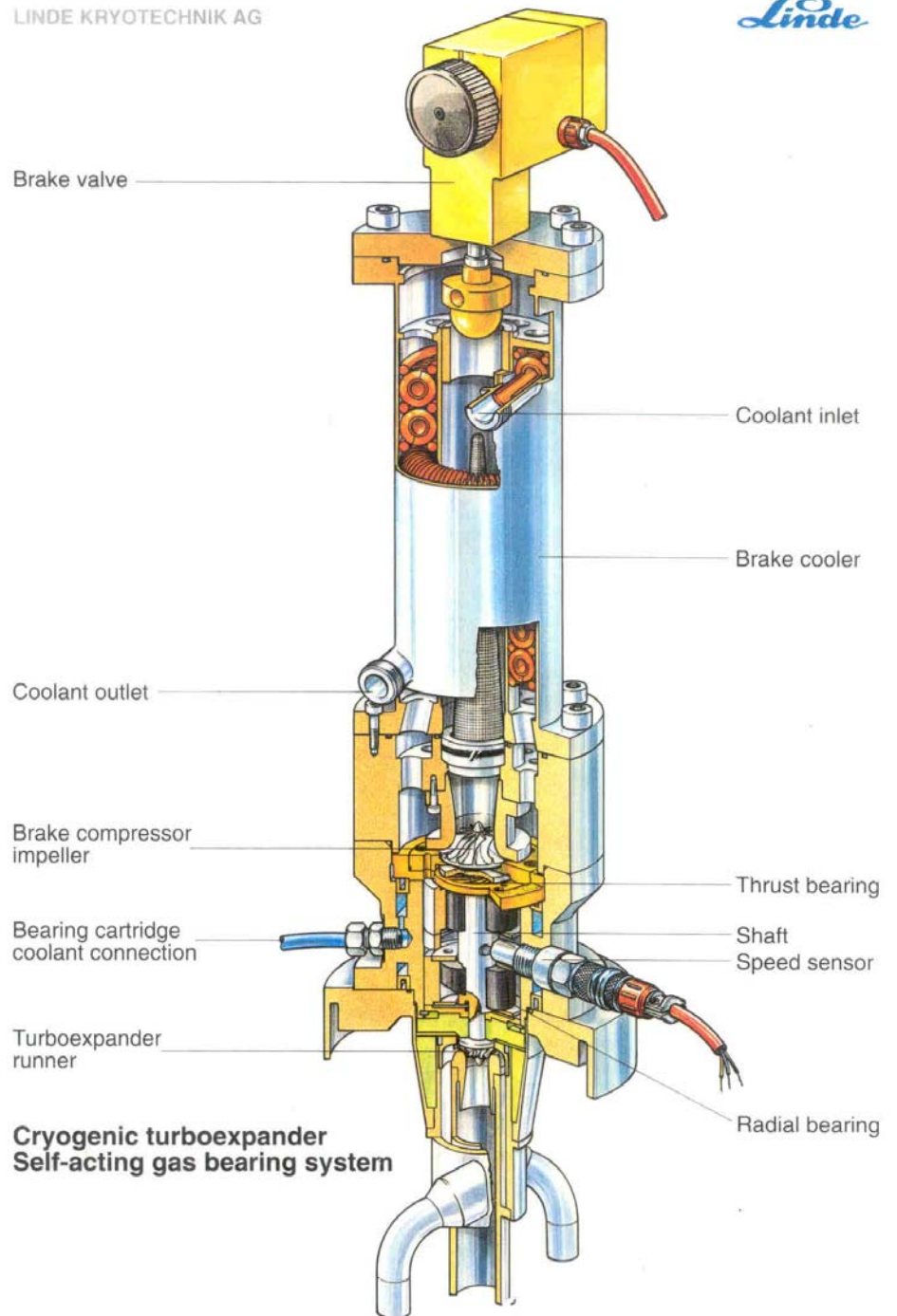


Brazed aluminium plate heat exchanger





Cryogenic turbo-expander



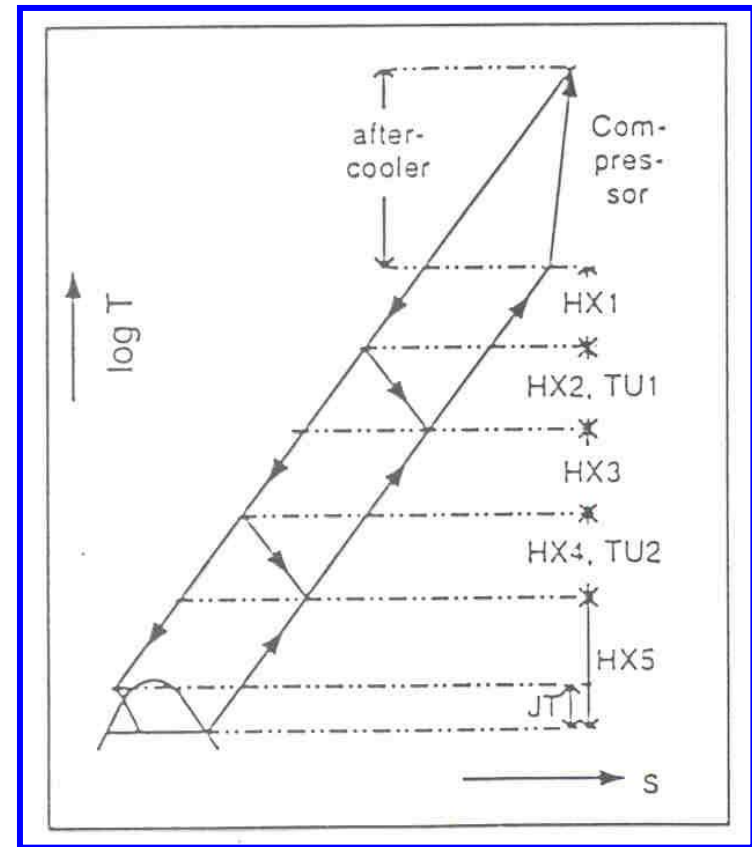
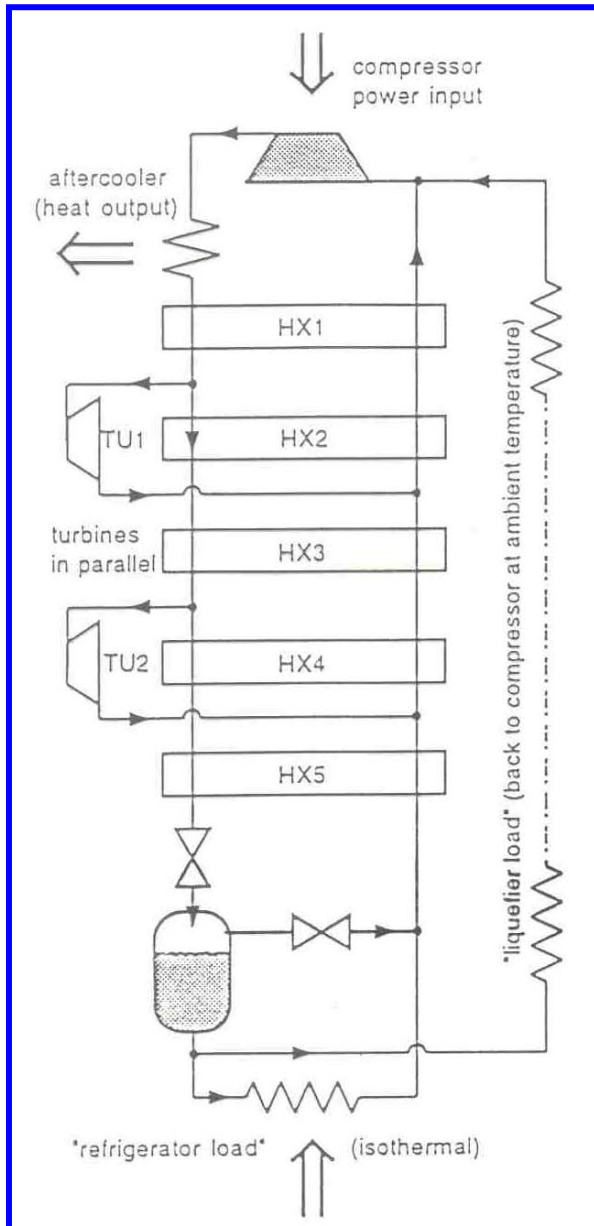


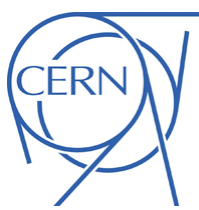
Maximum Joule-Thomson inversion temperatures

Cryogen	Maximum inversion temperature [K]
Helium	43
Hydrogen	202
Neon	260
Air	603
Nitrogen	623
Oxygen	761

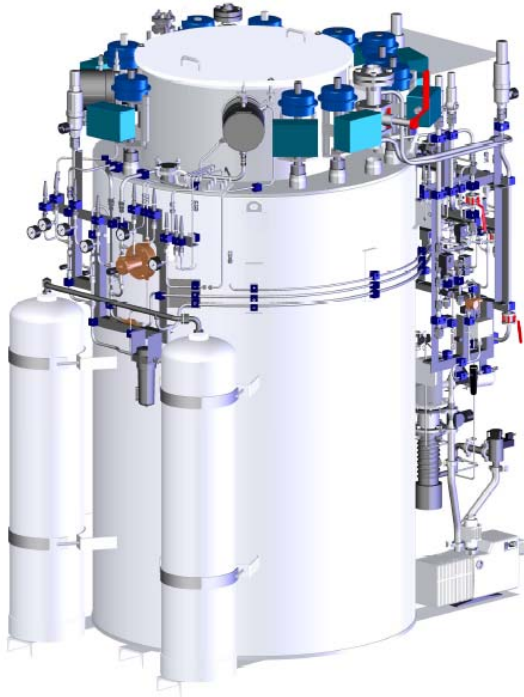
While air can be cooled down and liquefied by JT expansion from room temperature, helium and hydrogen need precooling down to below inversion temperature by heat exchange or work-extracting expansion (e.g. in turbines)

Two-stage Claude cycle





Claude-cycle helium refrigerators/liquefiers (Air Liquide & Linde)



	<i>HELIAL SL</i>	<i>HELIAL ML</i>	<i>HELIAL LL</i>
Max. Liquefaction capacity without LN2	25 L/h	70 L/h	145 L/h
Max. Liquefaction capacity with LN2	50 L/h	150 L/h	330 L/h
Compressor electrical motor	55 kW	132 kW	250 kW
Specific consumption for liquefaction w/o LN2	645 W/W	552 W/W	505 W/W
% Carnot	10%	12%	13%



	Without LN ₂ precooling	With LN ₂ precooling
L70	20 – 35 l/h	40 – 70 l/h
L140	45 – 70 l/h	90 – 140 l/h
L280	100 – 145 l/h	200 – 290 l/h
LR70	100 – 145 Watt	130 – 190 Watt
LR140	210 – 290 Watt	255 – 400 Watt
LR280	445 – 640 Watt	560 – 900 Watt

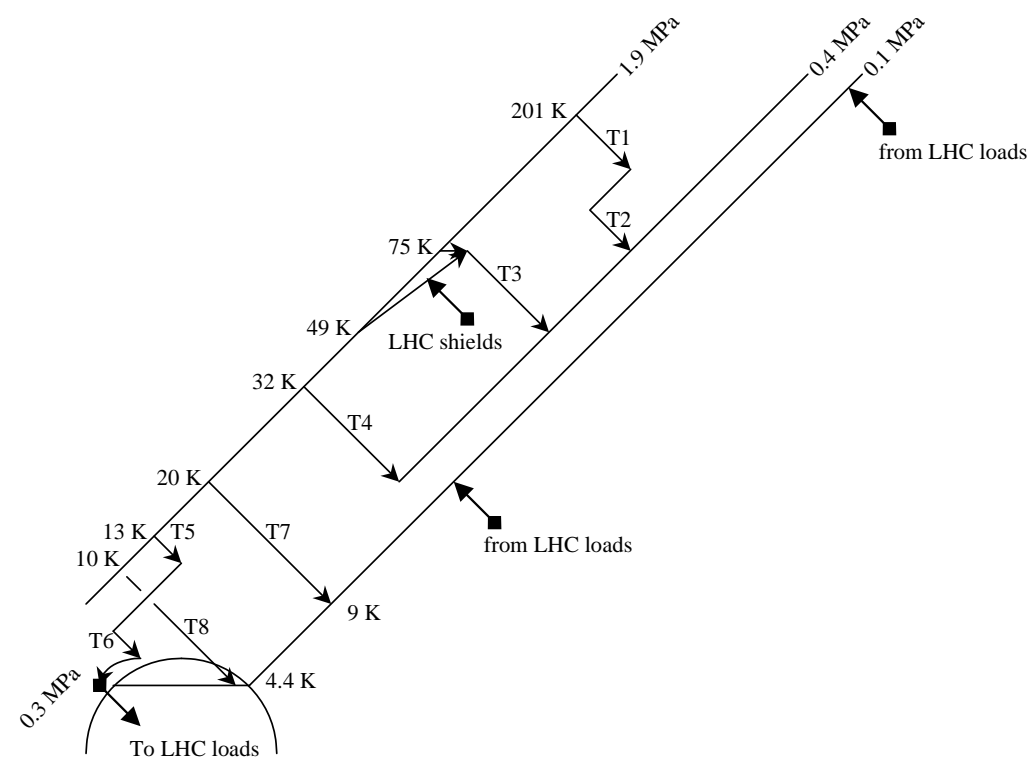
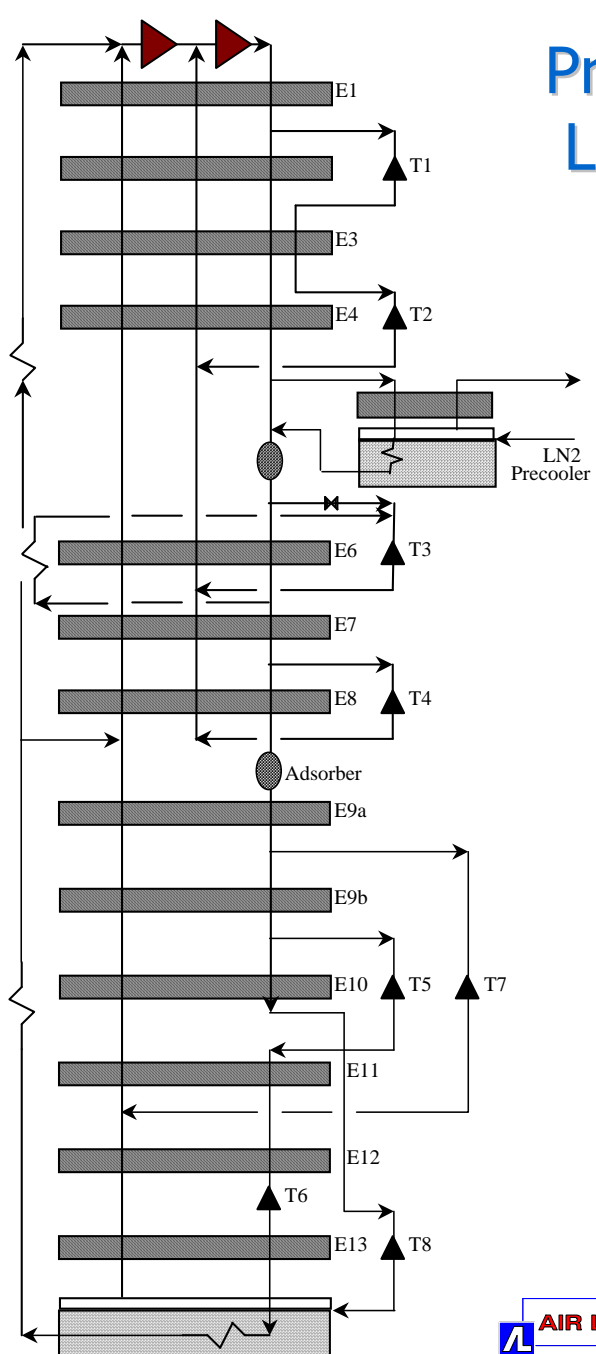


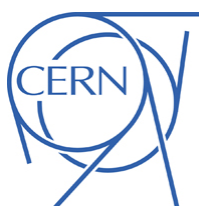
Process cycle & T-S diagram of LHC 18 kW @ 4.5 K cryoplant

20 K - 280 K loads
(LHC current leads)

50 K - 75 K loads
(LHC shields)

4.5 K - 20 K loads
(magnets + leads + cavities)






LHC 18 kW @ 4.5 K helium cryoplants



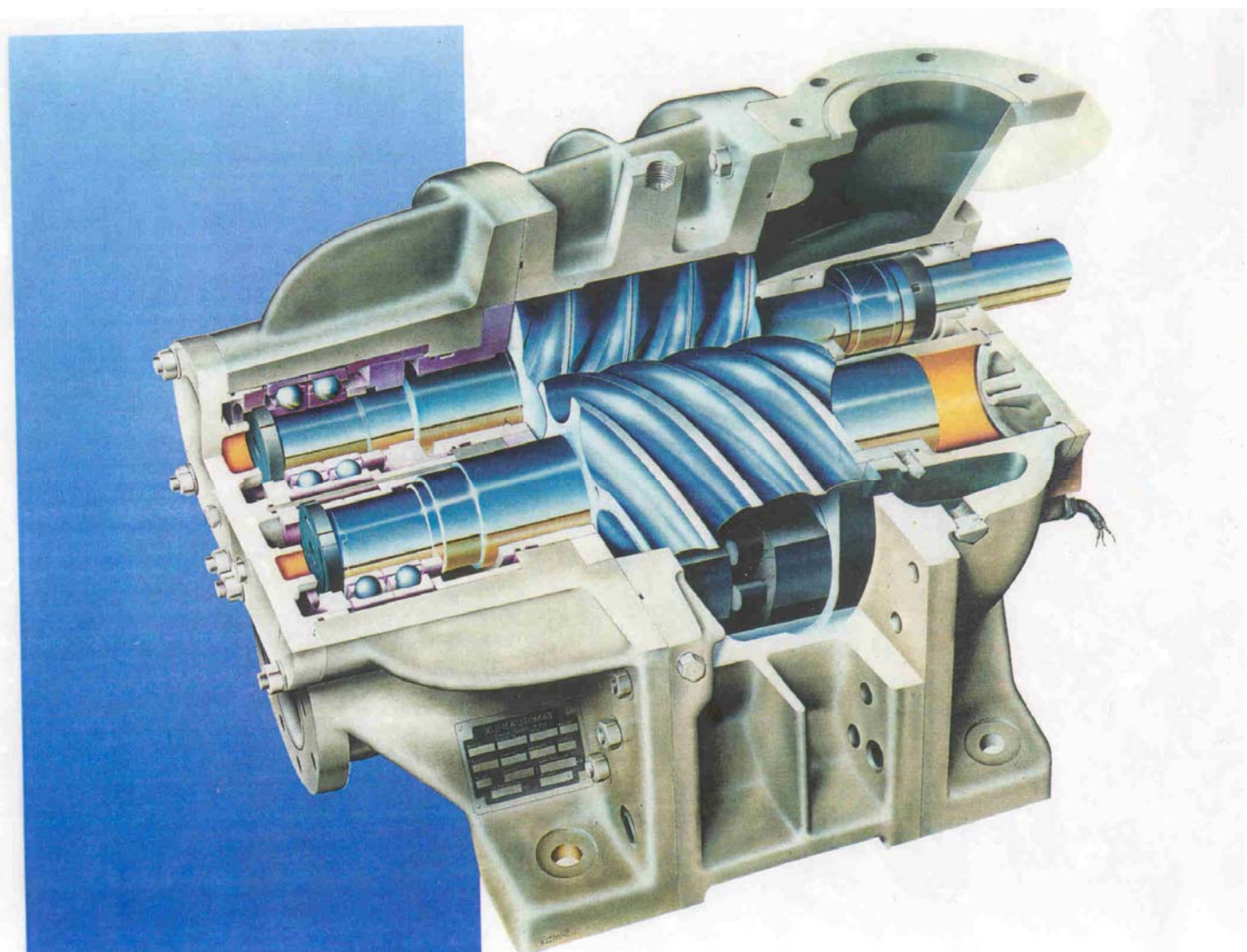
33 kW @ 50 K to 75 K
23 kW @ 4.6 K to 20 K
41 g/s liquefaction
4 MW compressor power
C.O.P. 220-230 W/W @ 4.5 K



Air Liquide 

Linde 

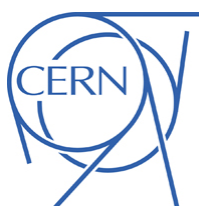
Oil-injected screw compressor



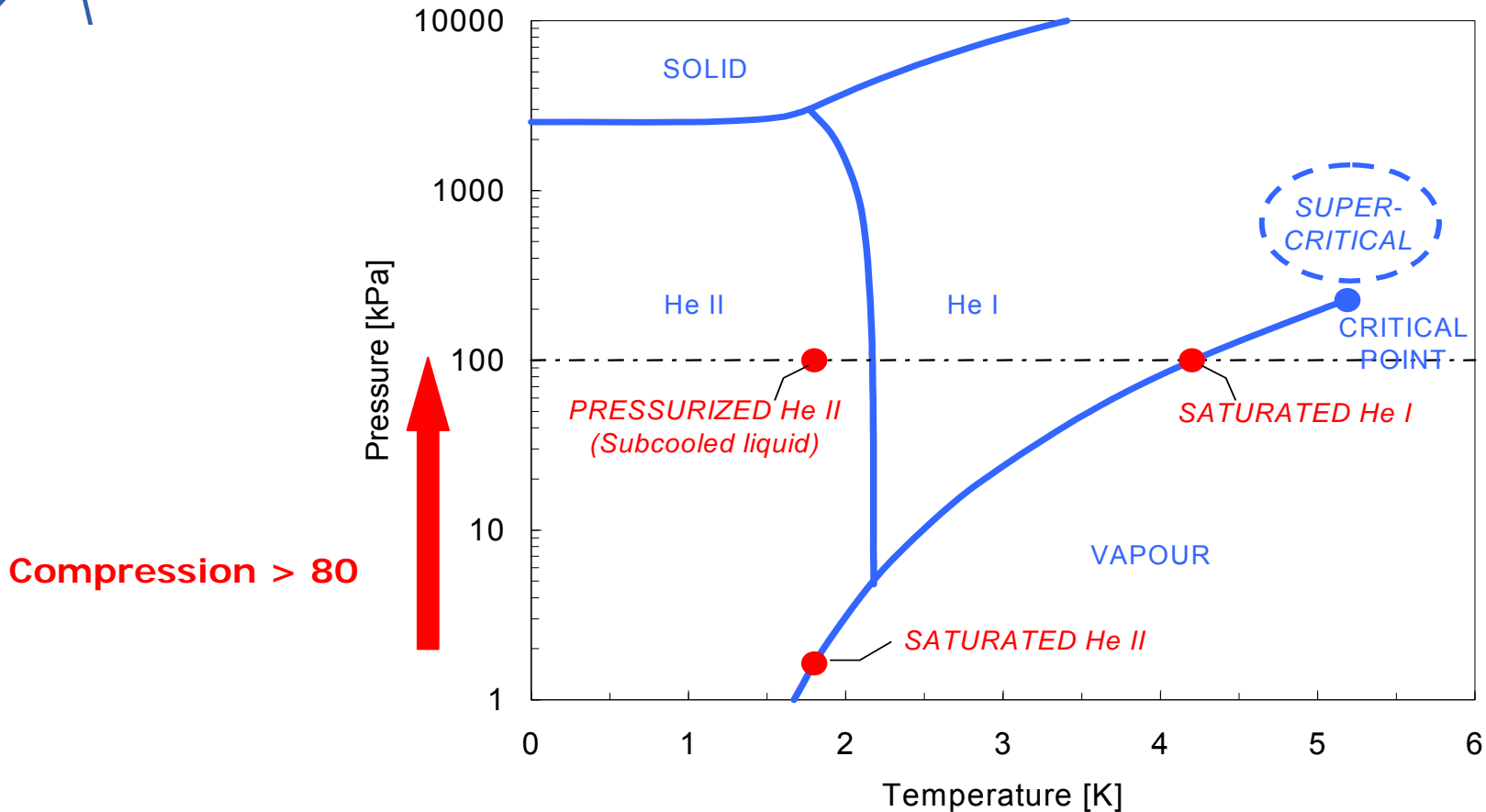


Compressor station of LHC 18 kW@ 4.5 K helium refrigerator





Challenges of power refrigeration at 1.8 K



- Compression of large mass flow-rate of He vapor across high pressure ratio
⇒ intake He at maximum density, i.e. cold
- Need contact-less, vane-less machine ⇒ hydrodynamic compressor
- Compression heat rejected at low temperature ⇒ thermodynamic efficiency

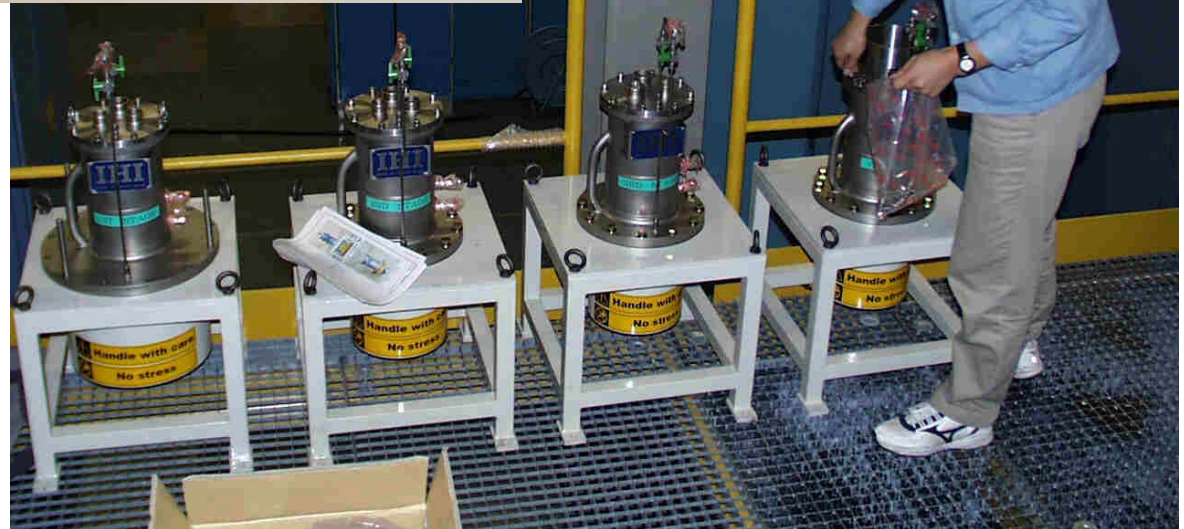


Cold compressors for 1.8 K refrigeration

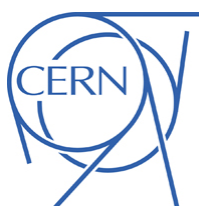
Axial-centrifugal impeller



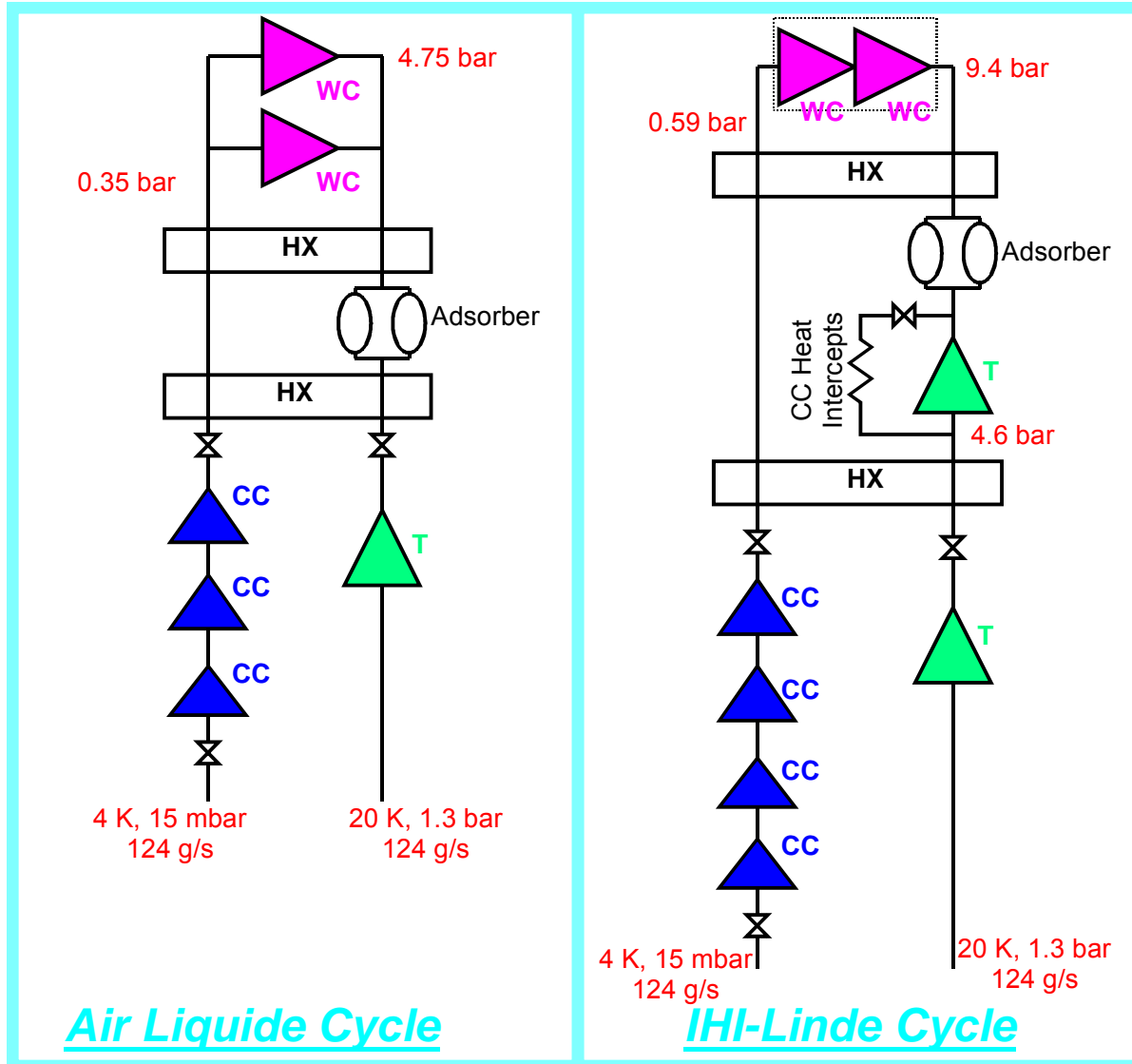
Cartridge 1st stage



4 cold compressor stages



Simplified flow-schemes of the 1.8 K refrigeration units of LHC

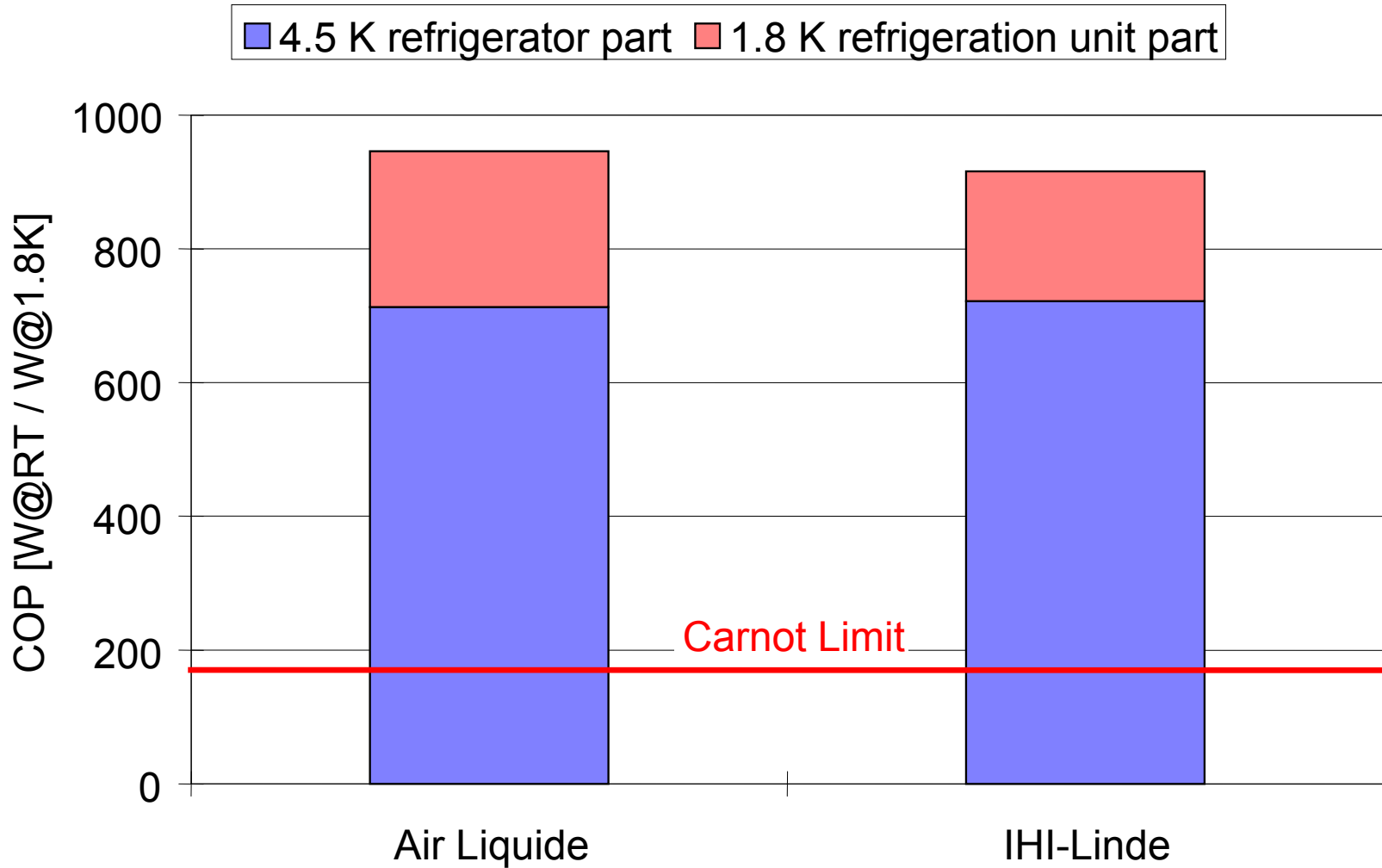


Air Liquide Cycle

IHI-Linde Cycle



C.O.P. of LHC 1.8 K units





Some references

- K. Mendelssohn, *The quest for absolute zero*, McGraw Hill (1966)
- R.B. Scott, *Cryogenic engineering*, Van Nostrand, Princeton (1959)
- G.G. Haselden, *Cryogenic fundamentals*, Academic Press, London (1971)
- R.A. Barron, *Cryogenic systems*, Oxford University Press, New York (1985)
- B.A. Hands, *Cryogenic engineering*, Academic Press, London (1986)
- S.W. van Sciver, *Helium cryogenics*, Plenum Press, New York (1986)
- K.D. Timmerhaus & T.M. Flynn, *Cryogenic process engineering*, Plenum Press, New York (1989)
- Ph. Lebrun, *An introduction to cryogenics*, CERN-AT-2007-01 (2007)
<http://cdsweb.cern.ch/record/1012032?ln=en>
- Proceedings of *CAS School on Superconductivity and Cryogenics for Particle Accelerators and Detectors*, Erice (2002)
 - U. Wagner, *Refrigeration*
 - G. Vandoni, *Heat transfer*
 - Ph. Lebrun, *Design of a cryostat for superconducting accelerator magnet*
 - Ph. Lebrun & L. Taviani, *The technology of superfluid helium*
<http://cdsweb.cern.ch/record/503603?ln=en>
- Proceedings of ICEC and CEC/ICMC conferences