

DE LA RECHERCHE À L'INDUSTRIE



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# QUANTIFICATION OF HEAT FLUX IN SUPERCRITICAL HELIUM

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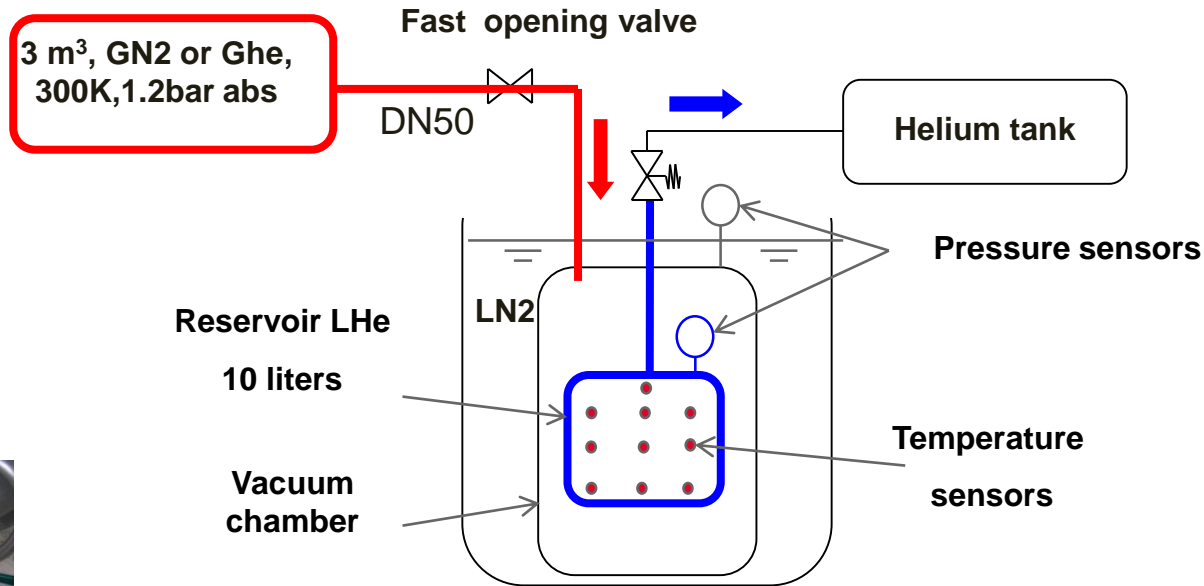


Reservoir LHe  
without MLI



Reservoir LHe  
with MLI

## Super critical discharge pressure



### Test parameters:

- Initial mass inventory of the reservoir
- Nature of the gas responsible (GN<sub>2</sub>, GHe, Air) for the loss of vacuum
- Number of layers of MLI

Poster presented at Aussois  
conference 2012

## Isochoric pressure rise

First thermodynamic law:  $\Delta U = \Delta Q + \Delta W$

$$\varphi = \rho_i \times \frac{V}{S} \times \frac{\Delta U}{\Delta t} \quad \Delta U = U(P_f, \rho_i) - U(P_i, \rho_i)$$

$\varphi$  heat flux in W/m<sup>2</sup>

$\rho_i$  initial density

$V$  volume of the tank

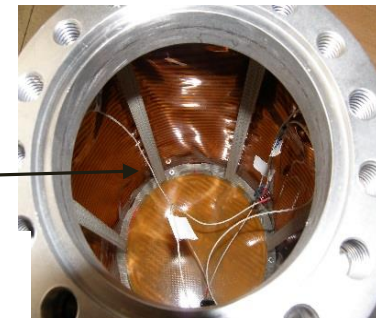
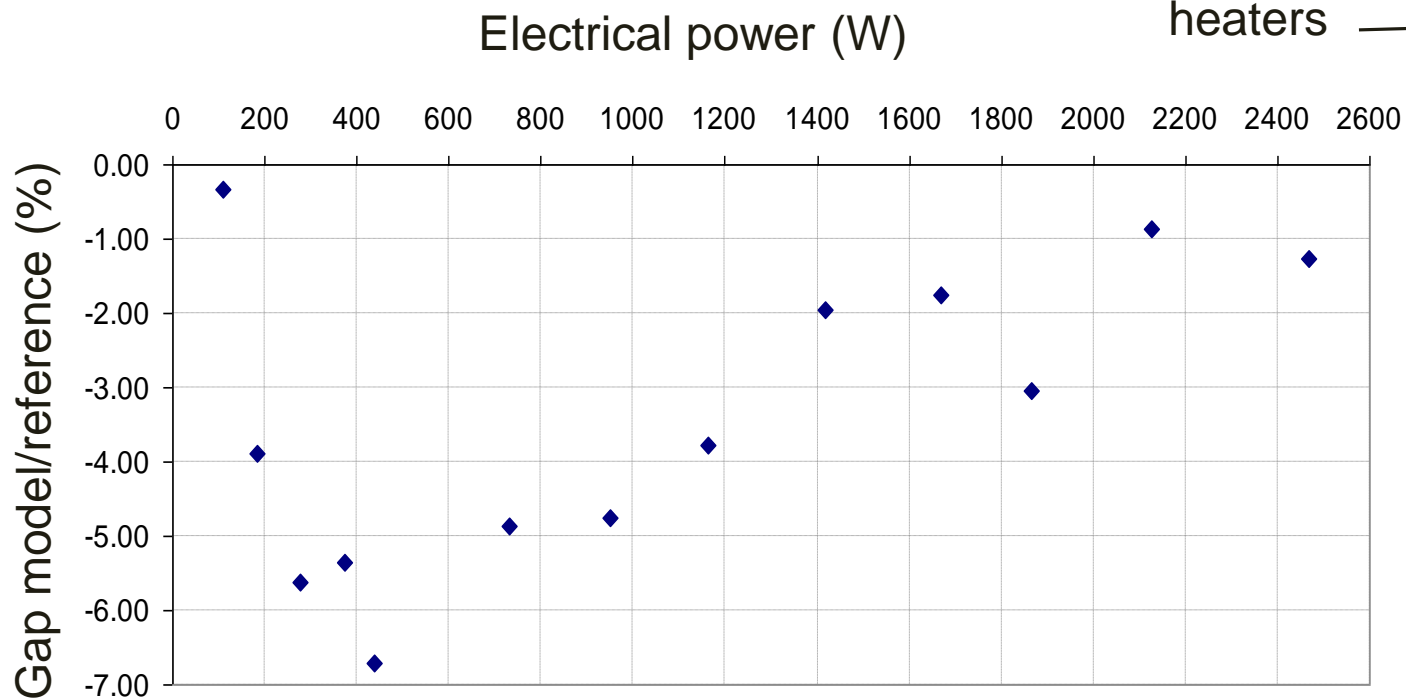
$S$  surface of the tank

$\Delta U$  internal energy variation between a final and an initial time

$\Delta t$  variation of time

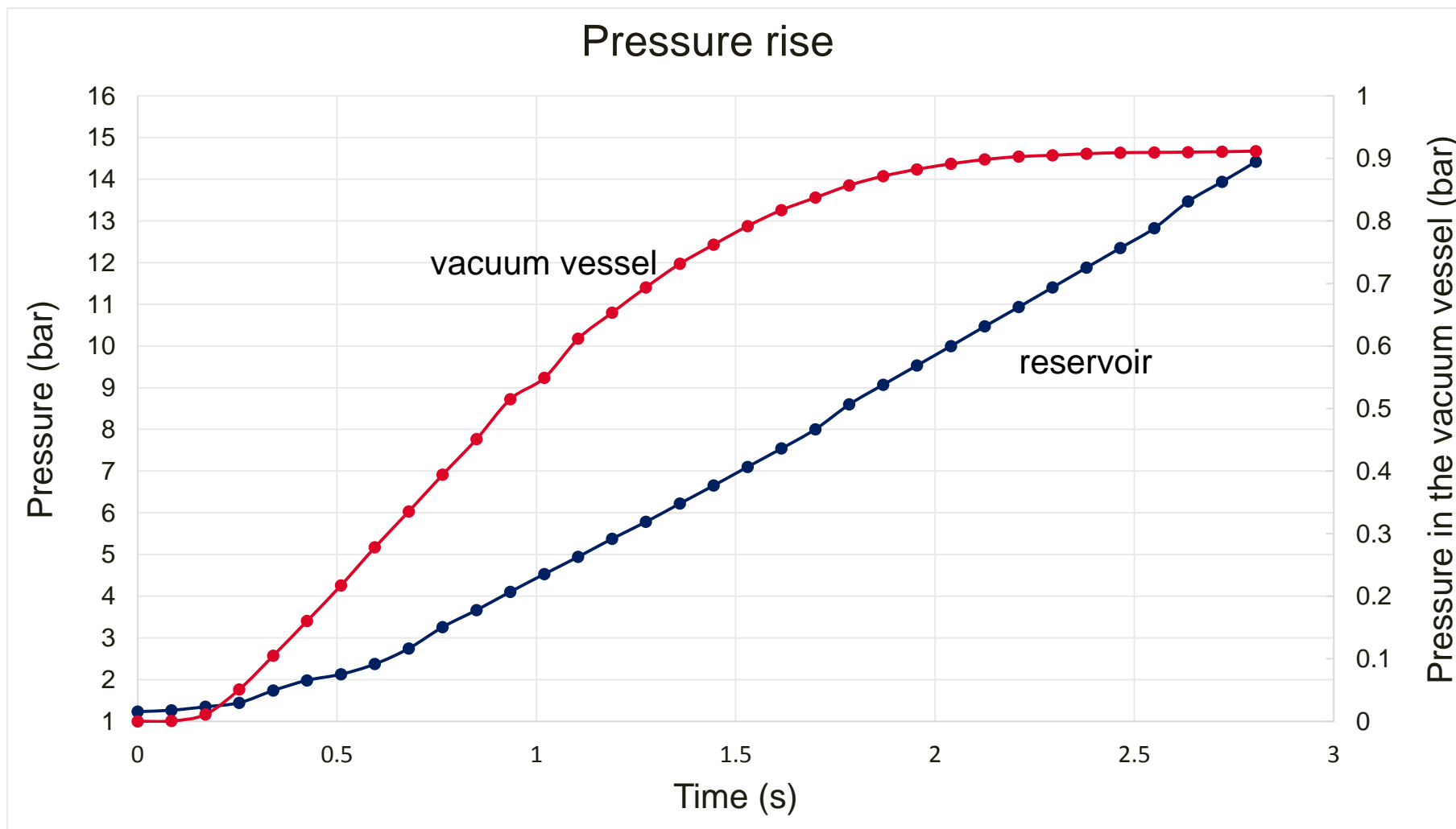
$P_f, P_i$  pressure at final and initial time

A first tank with electrical heaters has been used to qualify the instrumentation and the analysis method

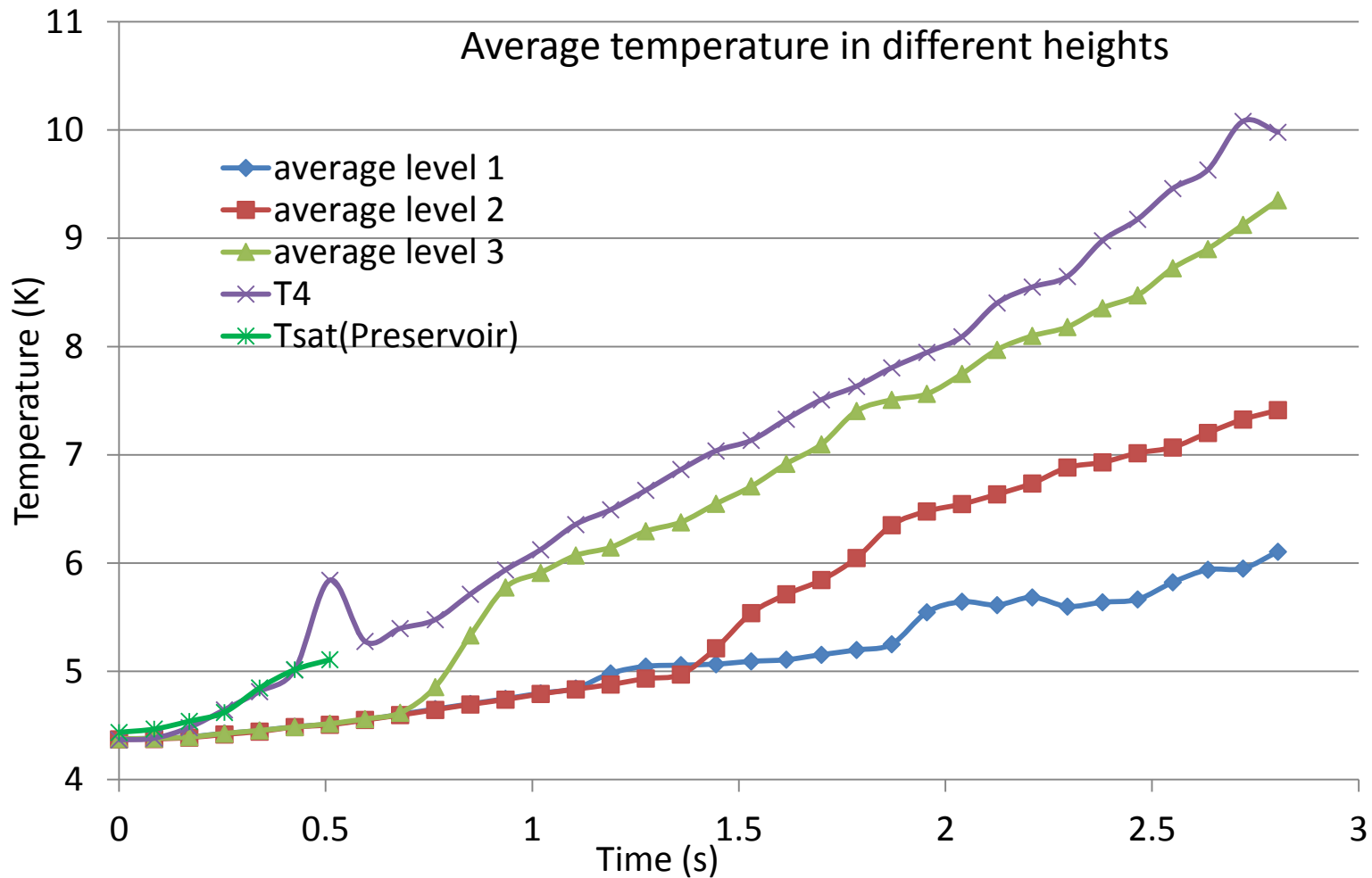


- Gap:
- a part of the initial mass goes to the dead volumes (0.5l)
  - heat accumulation on the wall tank can not be determined precisely (response time for the temperature sensors)

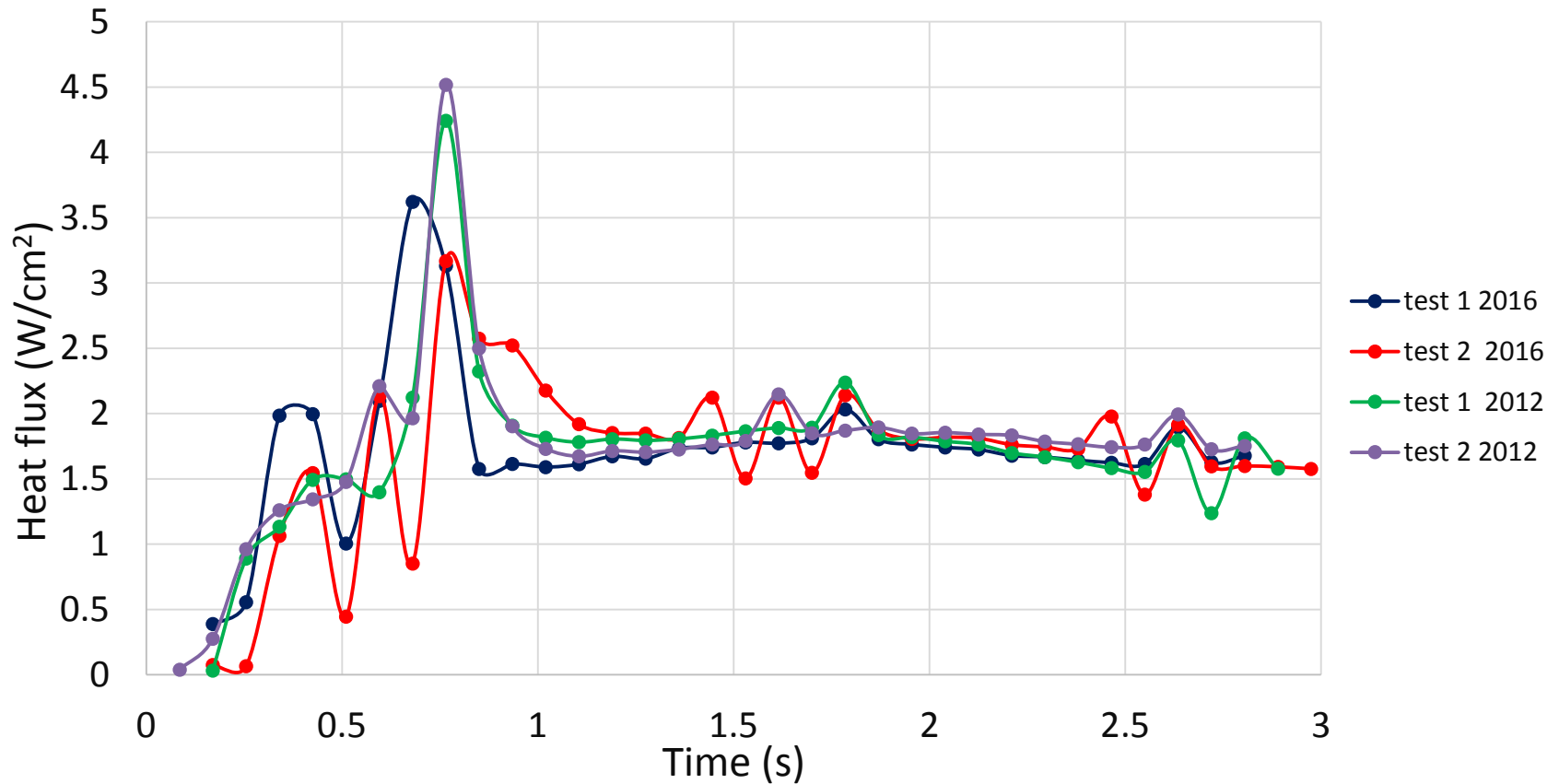
# PRESSURE RISE OF THE RESERVOIR AND VACUUM VESSEL: LOSS OF VACUUM VESSEL WITH GN<sub>2</sub>



# TEMPERATURE RISE INSIDE THE TANK

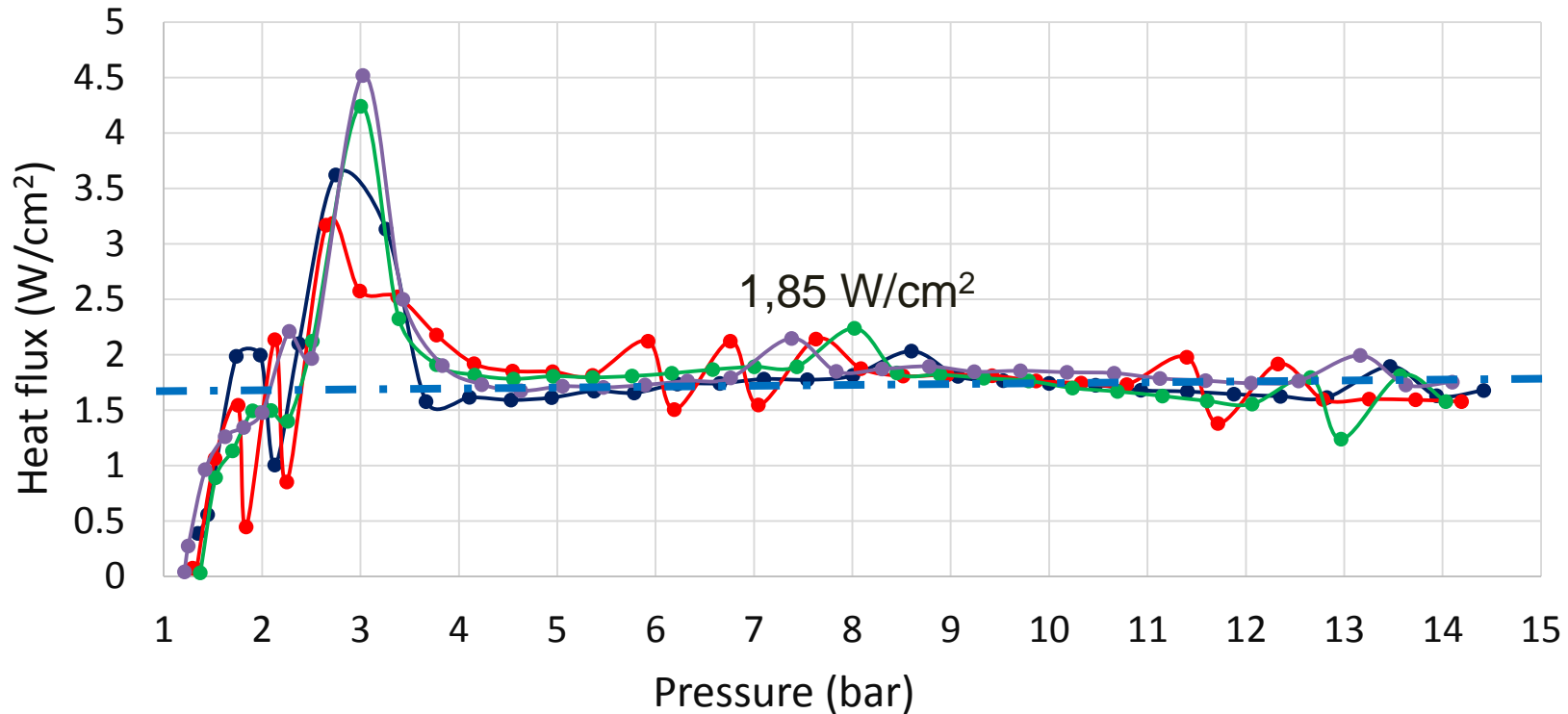


# HEAT FLUX RECEIVED BY THE LIQUID



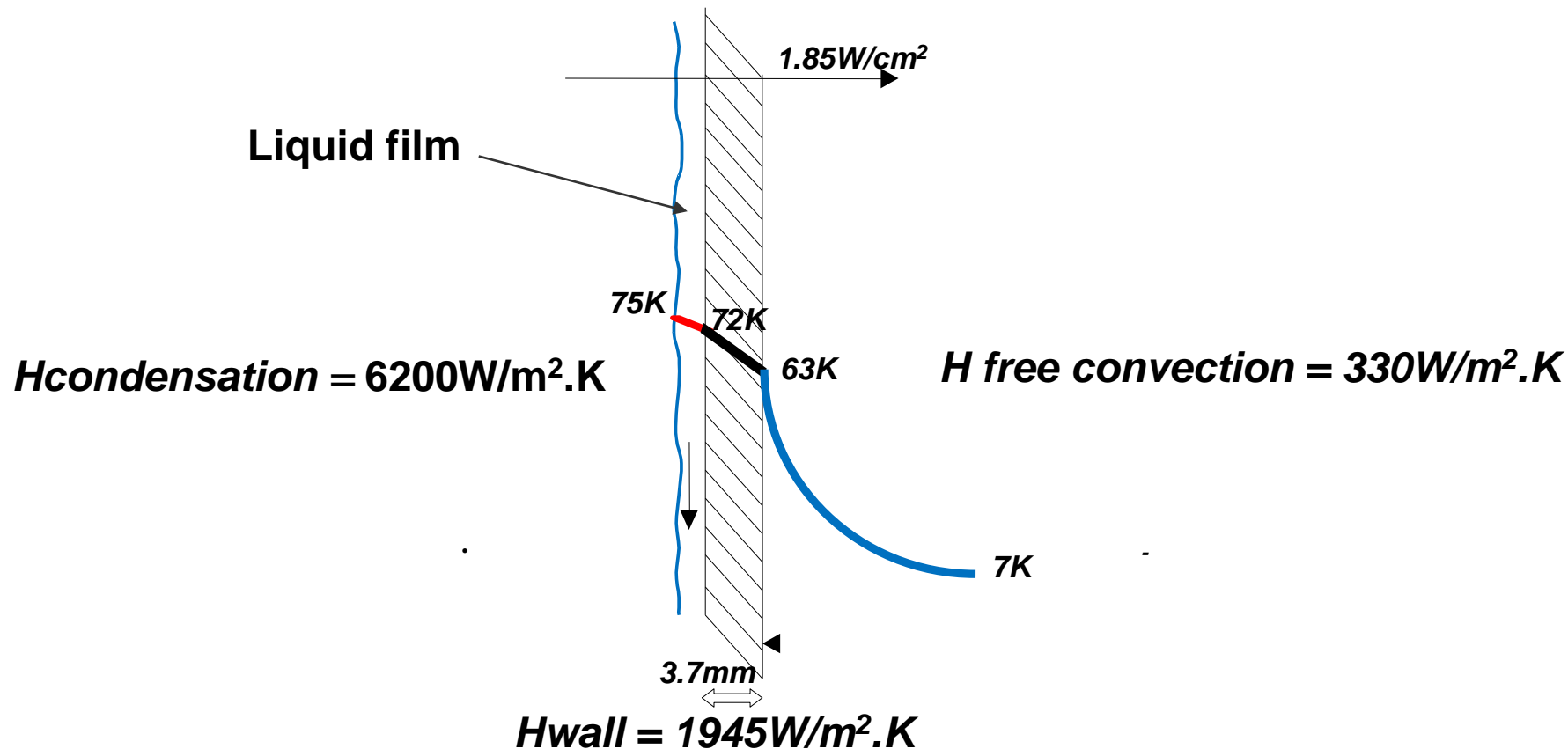
- Peak of heat flux at the first moments < 1s: nucleate and film boiling inside the tank
- After the heat flux remains constant: free convection inside the tank

# HEAT FLUX RECEIVED BY THE LIQUID



- Delay of peak nucleate/film boiling in comparison with the pressure at the first moments (Be careful with a safety device calculated at pressure close to 3 bars...)
- Constant heat flux  $1.85 \text{ W/cm}^2$  , steady state outside the tank?  $\Rightarrow$  no variation of the thickness film condensation, free convection inside the tank.





- Heat flux limited by free convection inside the tank
- High condensation coefficient because super heated gas, strong interfacial friction between the vapor and the liquid film, turbulent flow  $\Rightarrow$  very low film thickness ( $0.025\text{mm}$ )

## □ GHe

heat flux:  $0.15 \text{ W/cm}^2$ , the heat flux is limited by free convection inside the vacuum vessel ( $h = 30 \text{ W/m}^2\cdot\text{K}$  to compare to  $6200 \text{ W/m}^2\cdot\text{K}$  by condensation)

## □ AIR (one test)

heat flux:  $2 \text{ W/cm}^2$ , close to the value obtained with  $\text{GN}_2$

# HEAT FLUX WITH MUTI LAYER INSULATION

- ❑ Currently, no reproducible values have been obtained, we have to continue to work on this point...
- ❑ The value depends strongly on the way to install MLI on the reservoir !
- ❑ Question: is it relevant to measure /give some values.....?  
(way to install the MLI, types of MLI....)

Reservoir LHe  
with MLI



Experimentators	Intial conditions		Final conditions		Geometry tank	Filling rate	Heat Flux
Lehman 1980	1bar	4.2K	1bar	4.2K	Ø=0.3m L=1m 70 liters	50%	3.8 W/cm <sup>2</sup>
Harrison 2001	23mbar	1.9K	11bar	6K	Ø=0.2m L=0.4m 12 liters	90%	3W/cm <sup>2</sup>
Van Sciver 2015	1bar	4.2K	1bar	4.2K	Not mentioned	Not mentioned	2.5W/cm <sup>2</sup>

- Difference between Lehman and Van Sciver in sub-critical condition
- Difference between Harrison and CEA in super-critical condition



Different designs cryostat, different geometry of reservoirs and different analysis methods may lead to different results... **BE CAREFUL**

- ❑ A heat flux of  $1.85 \text{ W/cm}^2$  has been measured with our facility in super critical condition with a brutal loss of vacuum ( $\text{GN}_2$ ).  
Value to compare with Harrison ( $3\text{W/cm}^2$ ).....
  
- ❑ Heat flux is limited by the free convection coefficient inside the tank (except for GHe break of vacuum)
  
  
- ❑ Future work:
  - Heat flux with MLI.....
  - It will be interesting to compare the heat transfer condensation coefficient with bibliographic correlations.