



# Operational experience from the use of a 90 metre thermosiphon cooling plant for C<sub>3</sub>F<sub>8</sub> evaporative cooling of the ATLAS silicon tracker

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# Outline

Cooling of ATLAS detector

The thermosiphon evaporative cooling system

60 kW dummy load commissioning

Swap tests

Conclusion and what's next

# Cooling of the ATLAS detectors

## Thermal requirements:

- Detector temp  $-15^{\circ}\text{C}$ , corresponding to target evap temp of  $-25^{\circ}\text{C}$  to cope with radiation exposure over 10 years
- Temperature uniformity better than  $2^{\circ}\text{C}$  along the evaporators
- Total power to be removed 62.4 kW (204 parallel cooling loops)

*Attree et al. "The evaporative cooling system for the ATLAS inner detector" JINST 3.07 (2008): P07003*

## Advantages of the evaporative cooling system:

- Min extra material into Si trackers = min background particles
- Wide range of operating temperature
- Good thermal uniformity
- Mass flow 10-20 times less than in mono-phase liquid cooling system (smaller pipes)

# Cooling of the ATLAS detectors

Cooling of ATLAS detector is done by mean of a fluorocarbon evaporative cooling system

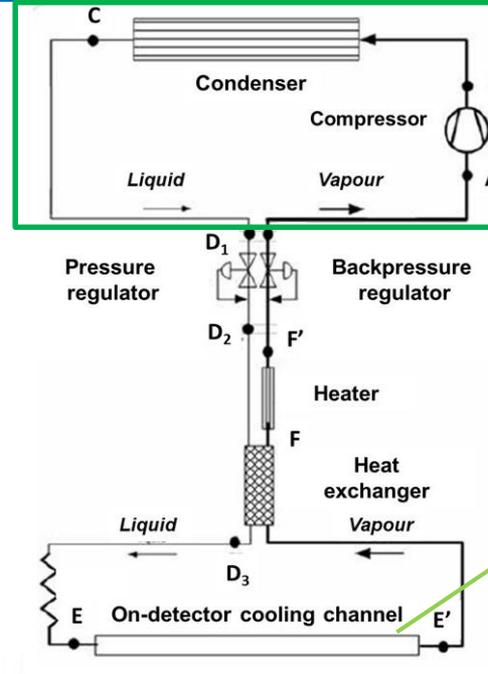
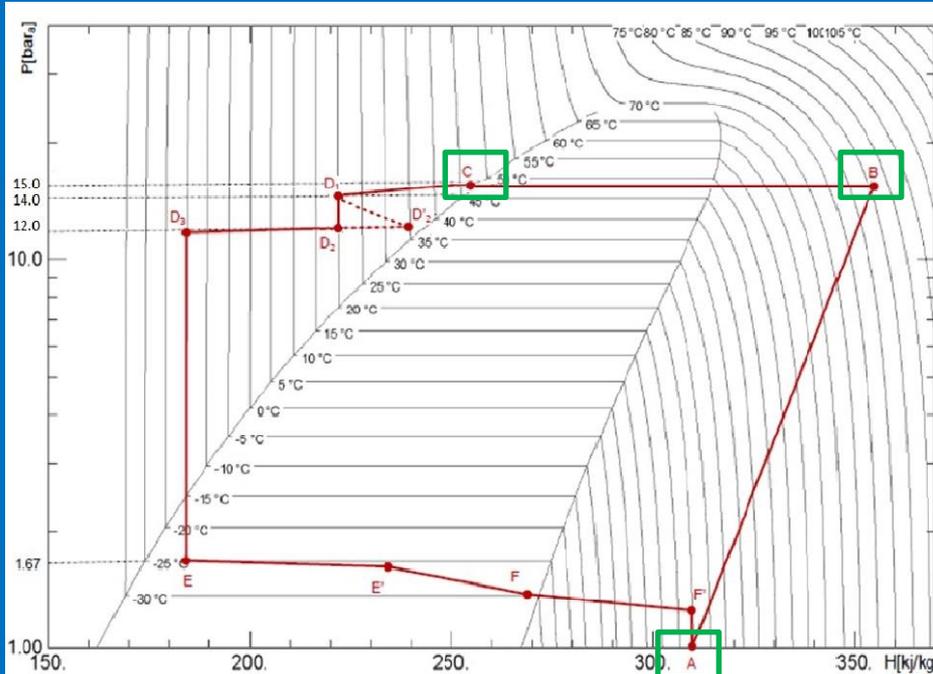
System based on a compression-condensation cycle similar to standard industrial direct expansion cooling plant.

Actually the external part of the evaporative cooling system is made of 7 oil free compressors working in parallel



# Cooling of the ATLAS detectors

Evaporative cooling system divided into two main parts separated by distribution /collection racks equipped with PRs and BPRs



EXTERNAL PART  
7 compressors working in parallel and a condenser

Target evaporation temperature in the on-detector cooling pipes  $-25^{\circ}\text{C}$  (corresponding to a saturation pressure of  $1.67 \text{ bar}_{\text{abs}}$  with  $\text{C}_3\text{F}_8$  coolant)

High radiation environment



Oil free compressor to prevent accidental mixing of activated coolant and lubricating oil

Especially modified to satisfy the very demanding compression ratio  
( $\max p_{\text{out}} = 15 \text{ bar}_{\text{abs}}$ ;  $\min p_{\text{aspirating}} = 1 \text{ bar}_{\text{abs}}$ ) Haug model QTOGX-160/80 ( $P_{\max} = 17 \text{ bar}_{\text{abs}}$ ;  $P_{\min} = 0.8 \text{ bar}_{\text{abs}}$ )

Compressors were improved and are presently working satisfactorily but still represent the weakest component of the system and need frequent preventive and corrective maintenance (frequent filter change because of carbon dust from piston segments)



Need of a more reliable plant

Increase of fluid activation due to increase of beam luminosity. RP risk related to the development of leaks on alternative vibrating machines



Need of a more leak-tight circuit



**Thermosiphon plant (TS)**

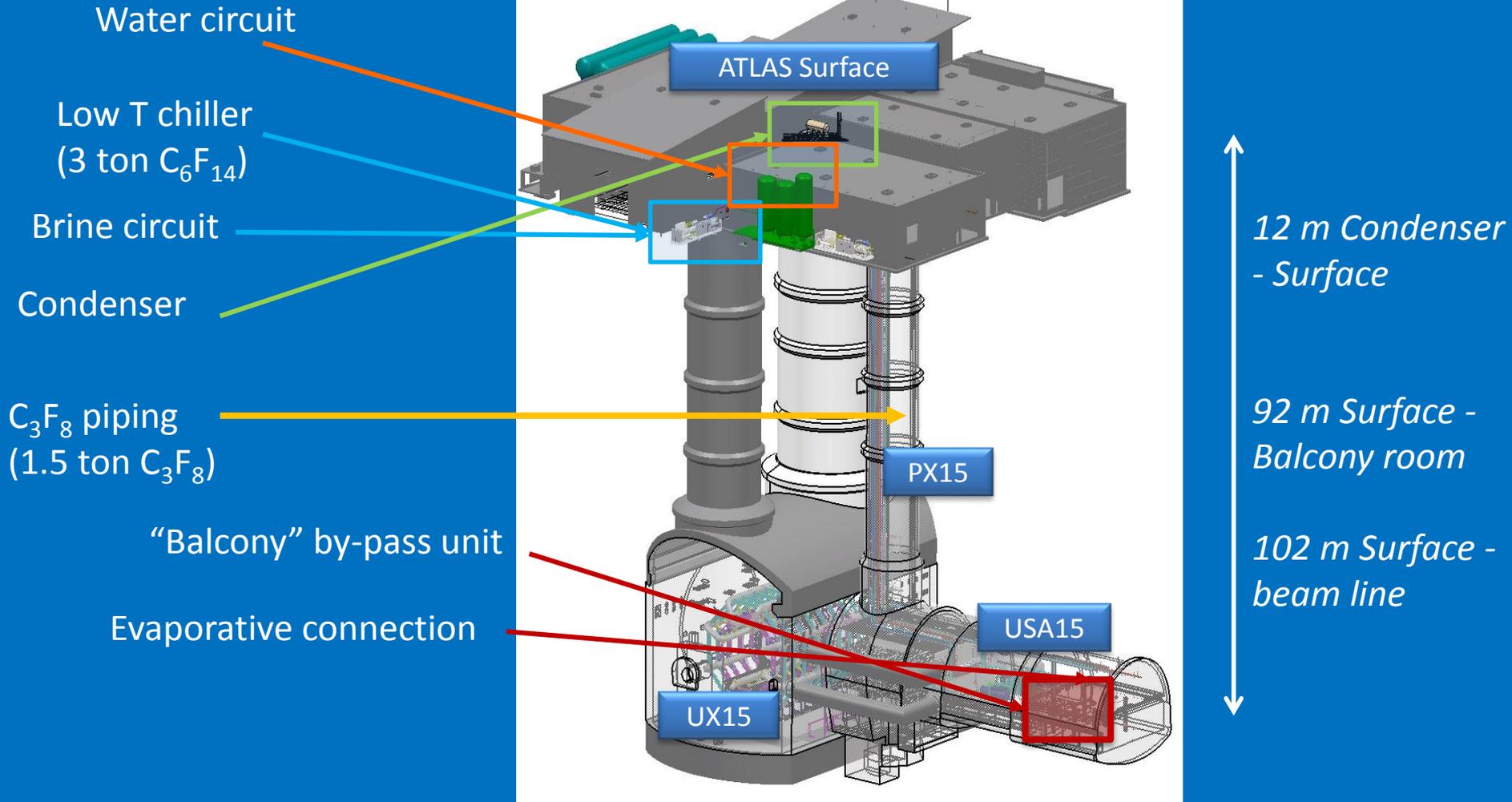
Any active component is eliminated from the primary loop.  
The plant takes advantage of the great height difference (~100 m) between the underground cavern housing the experiment and the surface



natural circulation of the coolant

# Description of the TS

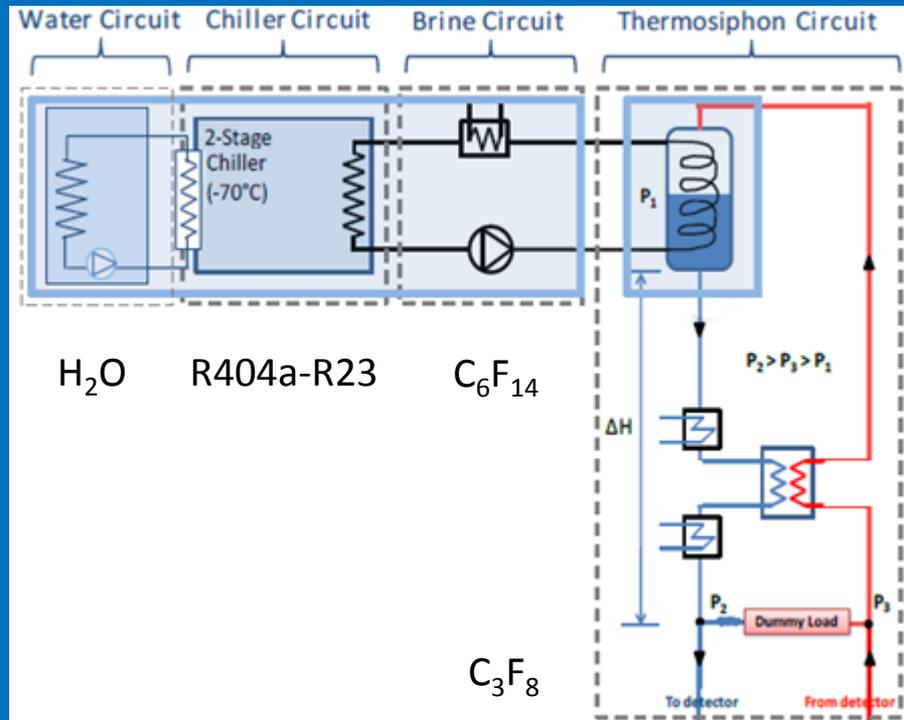
## Overview of the TS lay-out:



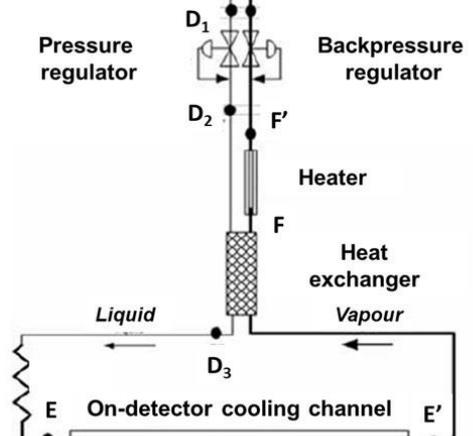
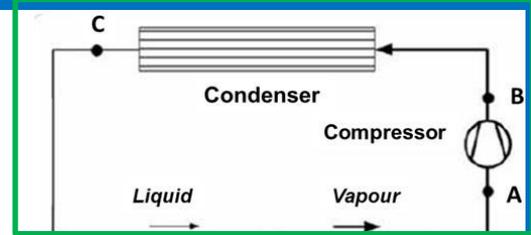
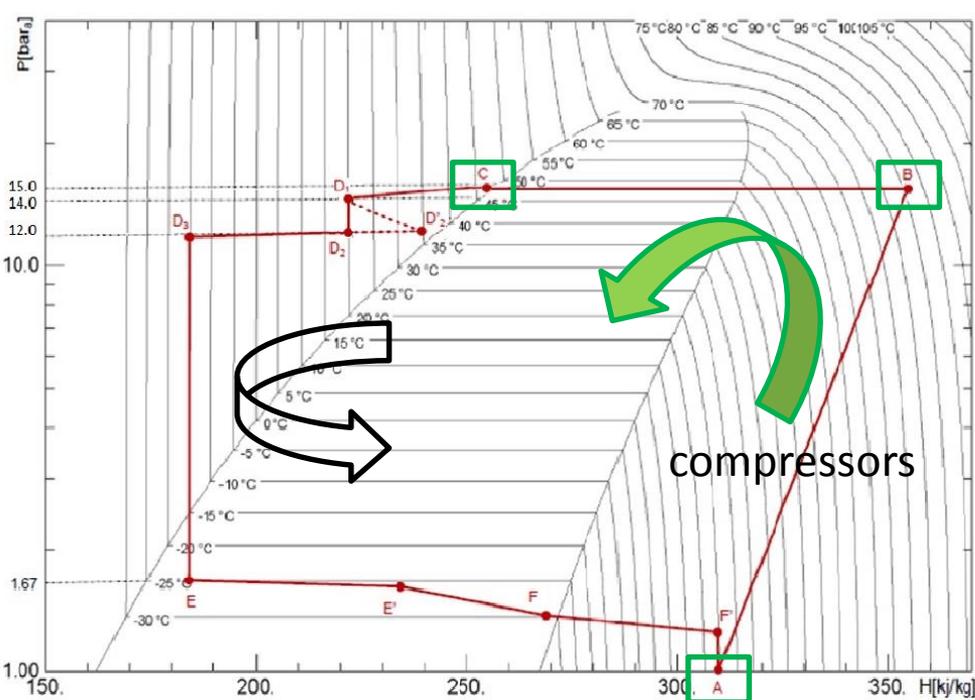
Let's see how the system works.....

# Description of the TS

The thermosiphon is composed of 4 separated circuits:



- 1. Water circuit:** cooling the first stage of the chiller circuit: water from cooling towers at  $\sim 25^\circ C$ :
- 2. Chiller circuit:** two stage compression cycle to cool down perfluorohexane ( $C_6F_{14}$ ) "brine" heat transfer liquid to  $-70^\circ C$ . The chiller operates in cascade: the first stage using R404a and the second stage R23;
- 3. Brine circuit:**  $C_6F_{14}$  closed loop used to condense the  $C_3F_8$  through heat exchange across the tubes in the condenser.  $C_6F_{14}$  is used as a transfer fluid mainly for its chemical similarity to  $C_3F_8$ ;
- 4. Thermosiphon primary circuit:** condensing  $C_3F_8$  at surface to produce a liquid column from surface to cavern (exit pressure  $\rightarrow$  hydrostatic column of fluid). Liquid evaporates in the unchanged on-detector cooling channels and returns to surface as vapour by differential pressure. System must supply high pressure liquid to on-detector components, while guaranteeing the required evaporation pressure.

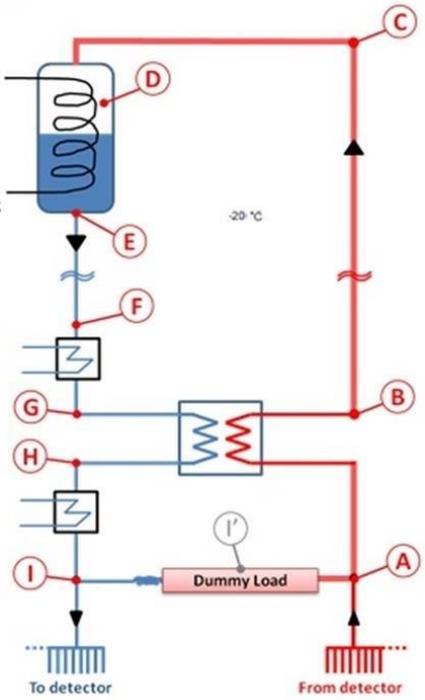
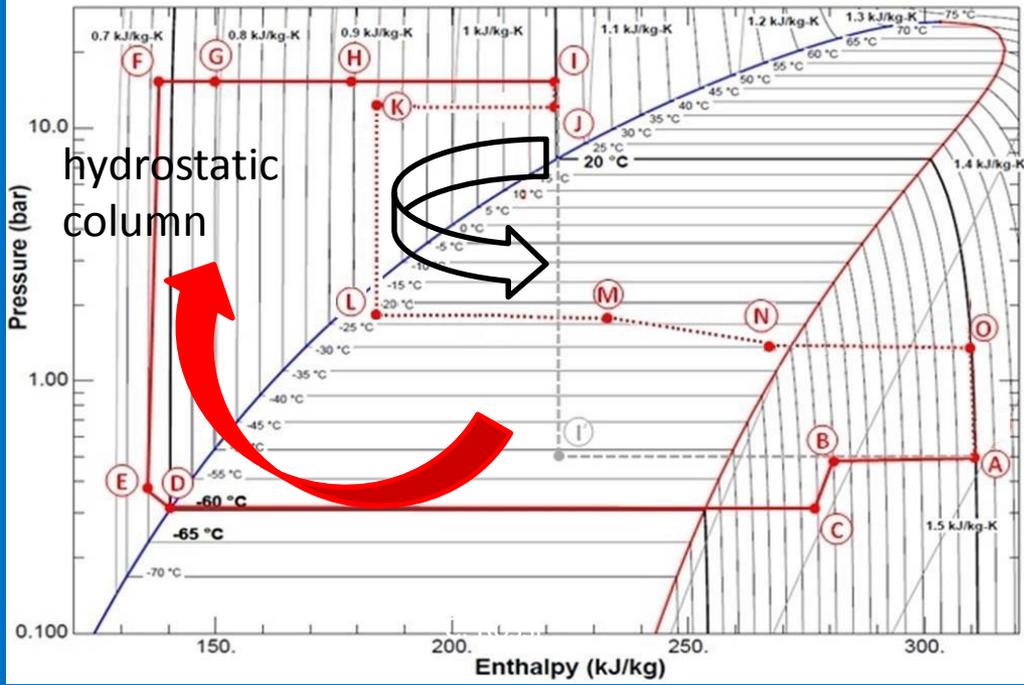


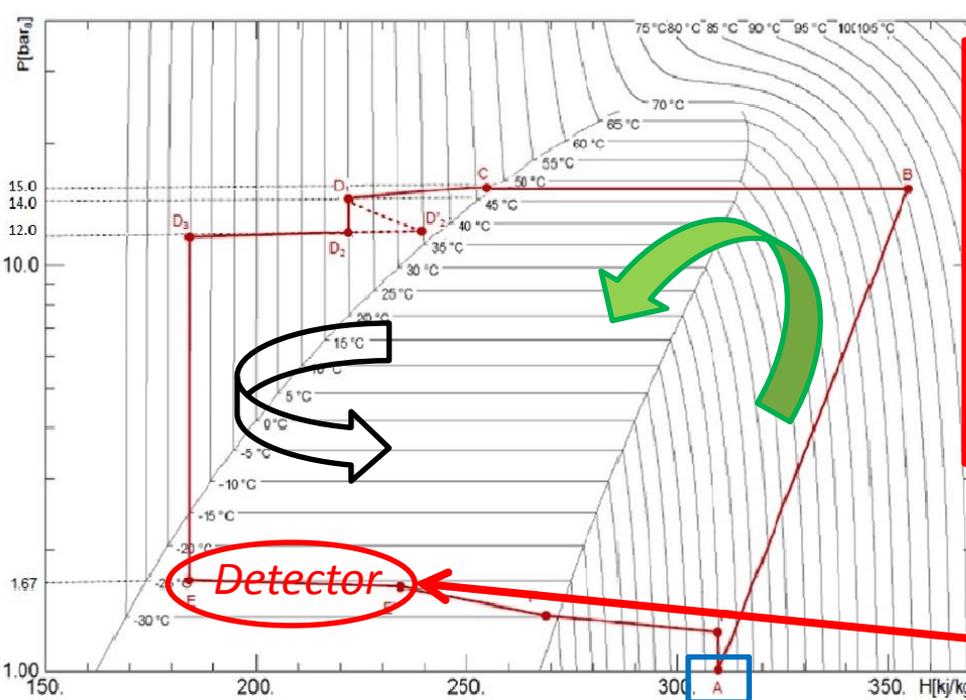
*Compressor driven evaporative system (A-C)*  
*Internal circuit (D1 – F')*

*EDMS 1083852*

*Thermosiphon circuit (A-I)*  
*Internal circuit (J – O)*

Evap	TS
D1	I
D2	J
D3	K
E	L
E'	M
F	N
F'	O



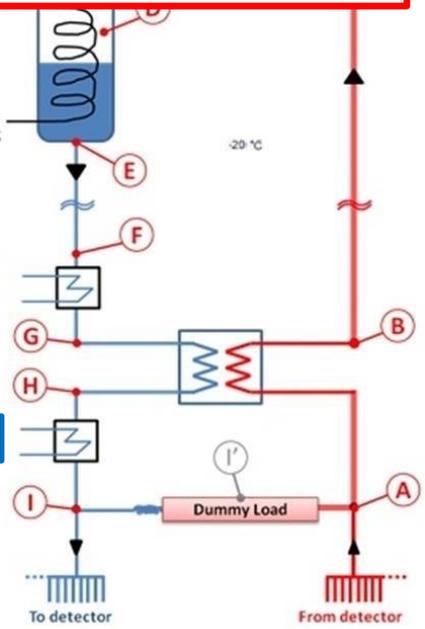
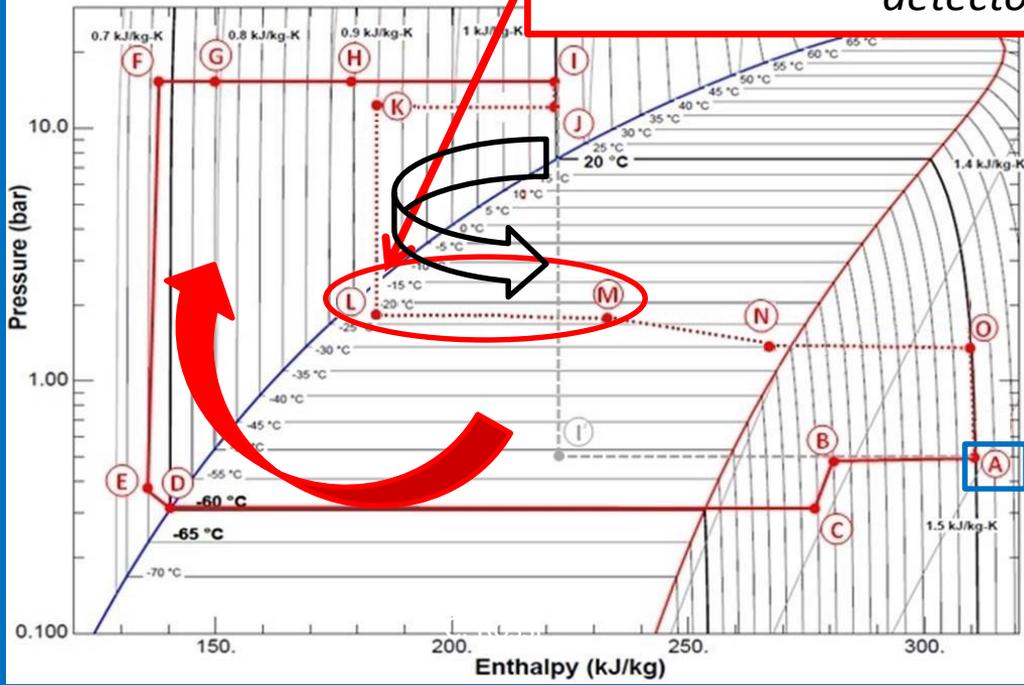


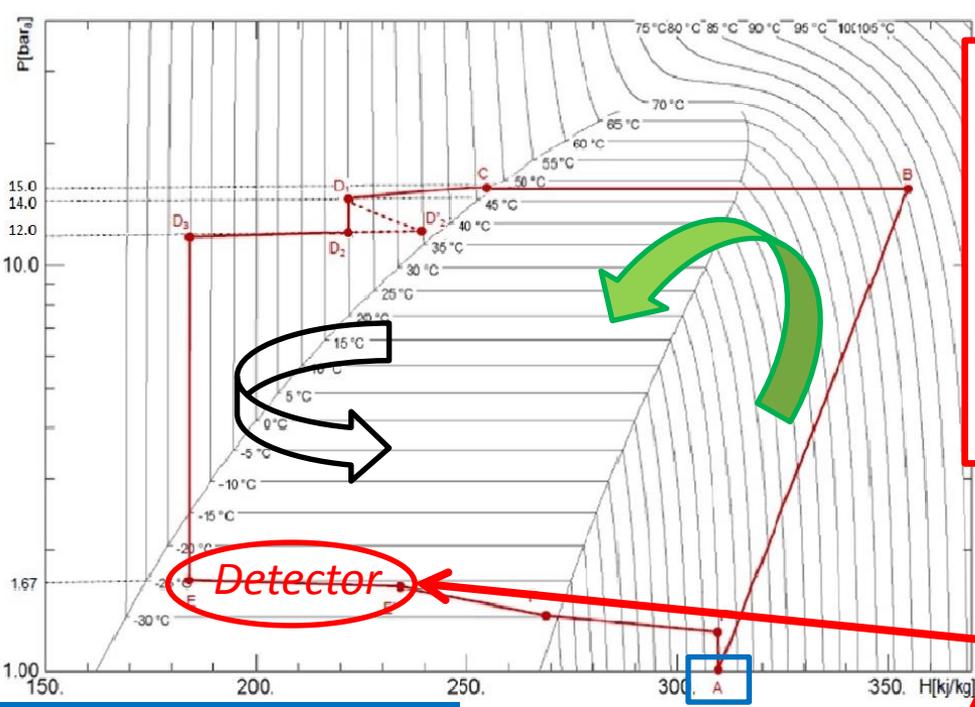
Compressors reliability 1<sup>st</sup> reason for TS  
 → but also higher margin on required  $p/T@detector$ .  
Baseline pressures:  
 Compressor-driven → = 1 bar<sub>abs</sub> ;  
 TS → = 500 mbar<sub>abs</sub>  
 → Required evaporation p easier to achieve

Target pressure specified at end of on-detector cooling channels → Pressure drop in return line increases operating T of Si detectors.

Thermosiphon circuit  
 (A-I)  
 Internal circuit (J-O)

Evap	TS
D1	I
D2	J
D3	K
E	L
E'	M
F	N
F'	O



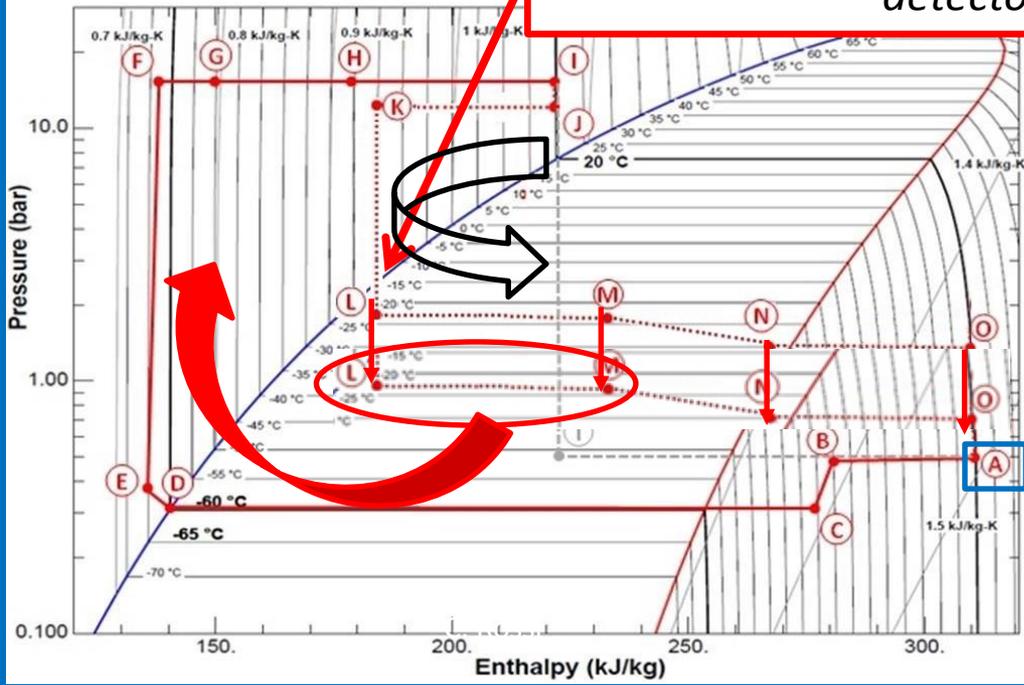


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Thermosiphon circuit (A-I)  
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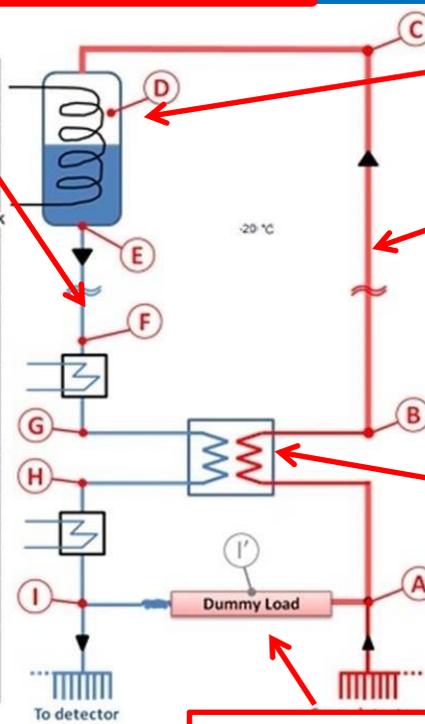
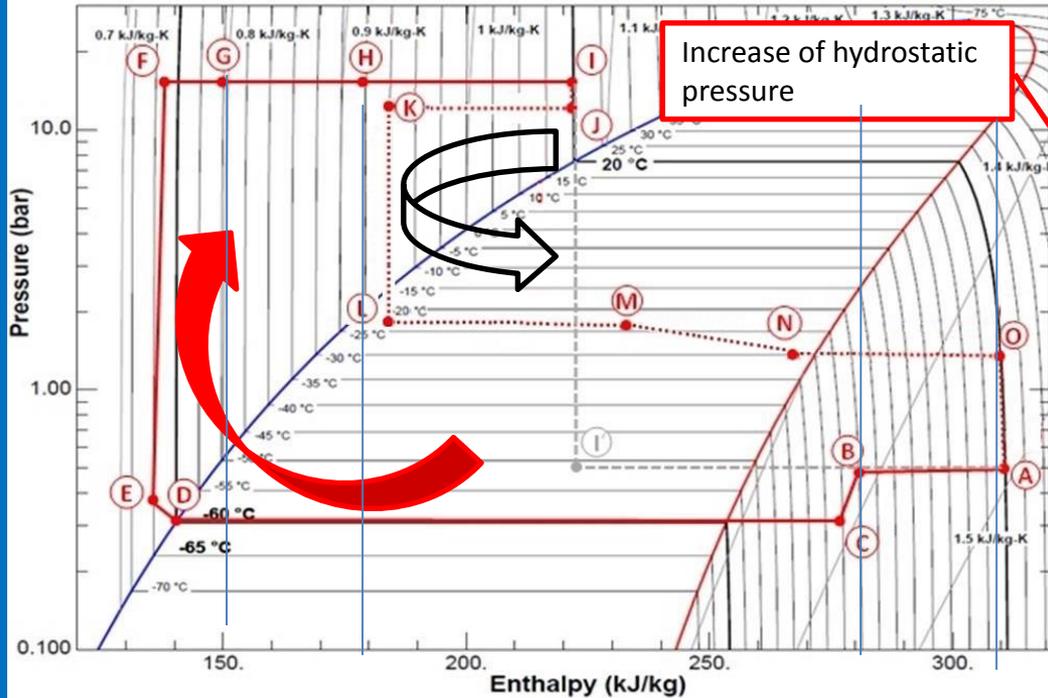
Evap	TS
D1	I
D2	J
D3	K
E	L
E'	M
F	N
F'	O



In TS baseline pressure (A) is lower → by regulating BPR we can lower O and therefore have a lower  $p/T@detector$



# Description of the TS



condenser and subcooling. storage when system is stopped.

pressure drop along vapour return line (vapour column weight and frictional pressure drop)

counter flow heat exchanger

I-A: by-pass to rapidly ramp down at start-up. Stable performance even when SCT and Pixel trackers are off (minimum thermal load).

Thermodynamic cycle of the thermosiphon circuit and corresponding schematic. Thermosiphon circuit (A-I). Beyond these points  $C_3F_8$  enters the internal cooling circuits. Fluid exits the detectors at point M point (E' in the previous compressor evaporative cycle)

Operating point	Pressure [bar <sub>abs</sub> ]	Temperature [°C]	Physical State
A	0.5	20	Superheated vapour
B	0.495	-20	Superheated vapour
C	0.309	-25	Superheated vapour
D	0.309	-60	Saturated liquid
E	0.4	-65	Sub-cooled liquid
F	16.1	-51	Sub-cooled liquid
G	16.1	-20	Sub-cooled liquid
H	16	20	Sub-cooled liquid
I	16	20	Sub-cooled liquid
I'	0.5	-51	Two-phase x=0.6

Designed parameter  
EDMS 1083852

# Description of the TS



TS Condenser: 12m above ground level



Brine and Chiller circuit: Ground level



Connection to existing system: 92m underground



Water circuit: Ground level

## Tests with dummy load

Several preliminary tests were done running the TS on the 60kW dummy load from February 2016.

### Aim:

- Tune set points of the system
- Improve reliability and performance
- Define an automatic procedure for the TS start and pull down
- Verify TS stability and possibility of swap between the two systems

### Tests:

Start-up of the system

run at warm conditions

run at normal conditions

#### Warm conditions:

Temperature in condenser -20 °C

Vapour pressure 2 bar<sub>a</sub>

C<sub>3</sub>F<sub>8</sub> mass flow 0.3 kg/s

#### Normal conditions:

Temperature in condenser -40 °C

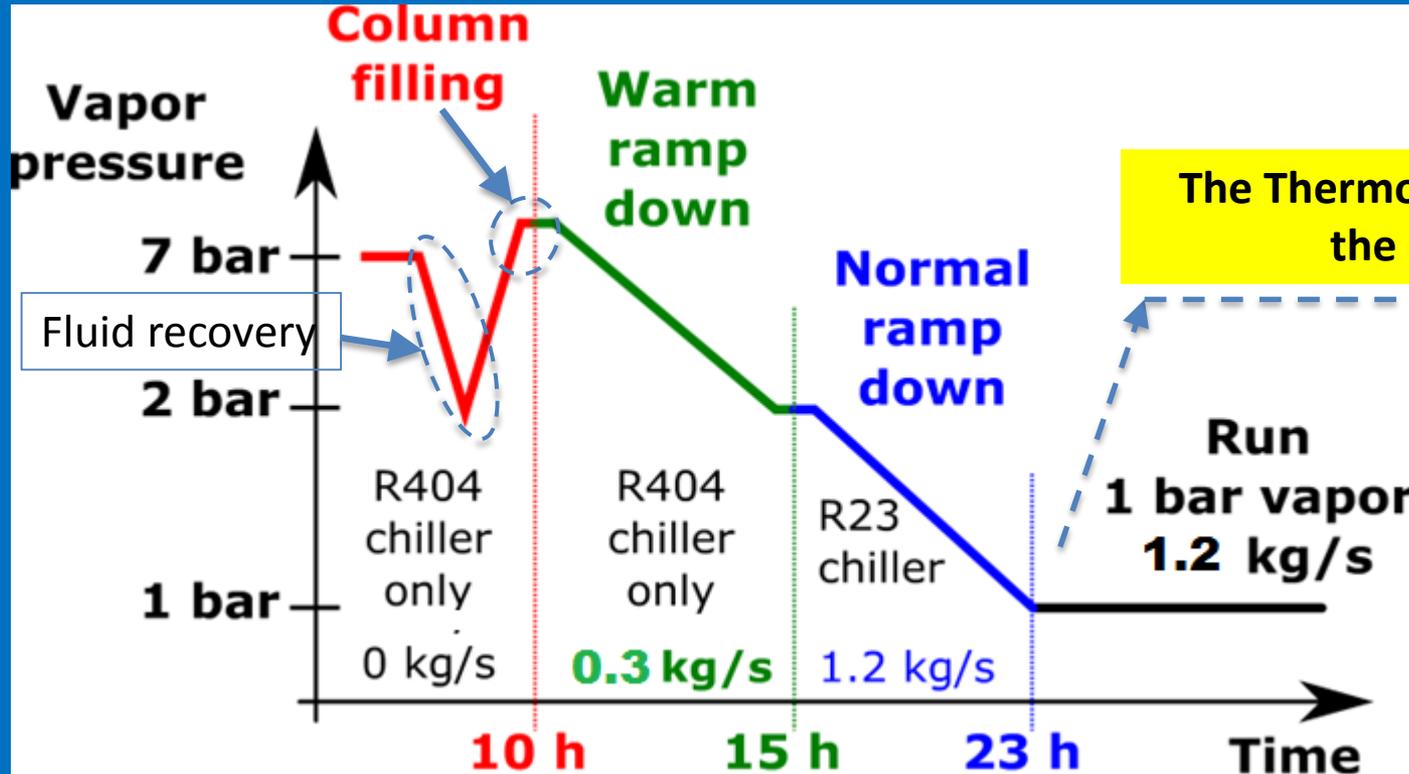
Vapour pressure 1.3 bar<sub>a</sub>

C<sub>3</sub>F<sub>8</sub> mass flow 1.2 kg/s

# Tests with dummy load

## Start-up of the system:

1. Circulation starts after liquid column is filled at condenser temp =  $-15\text{ }^{\circ}\text{C}$
2. Slow temperature ( $0.2\text{ }^{\circ}\text{C}/\text{min}$ ) ramp-down to warm mode
3. Warm mode circulation through dummy load (only R404a chiller)
4. Slow temperature ( $0.2\text{ }^{\circ}\text{C}/\text{min}$ ) ramp-down to normal mode
5. Set points are achieved

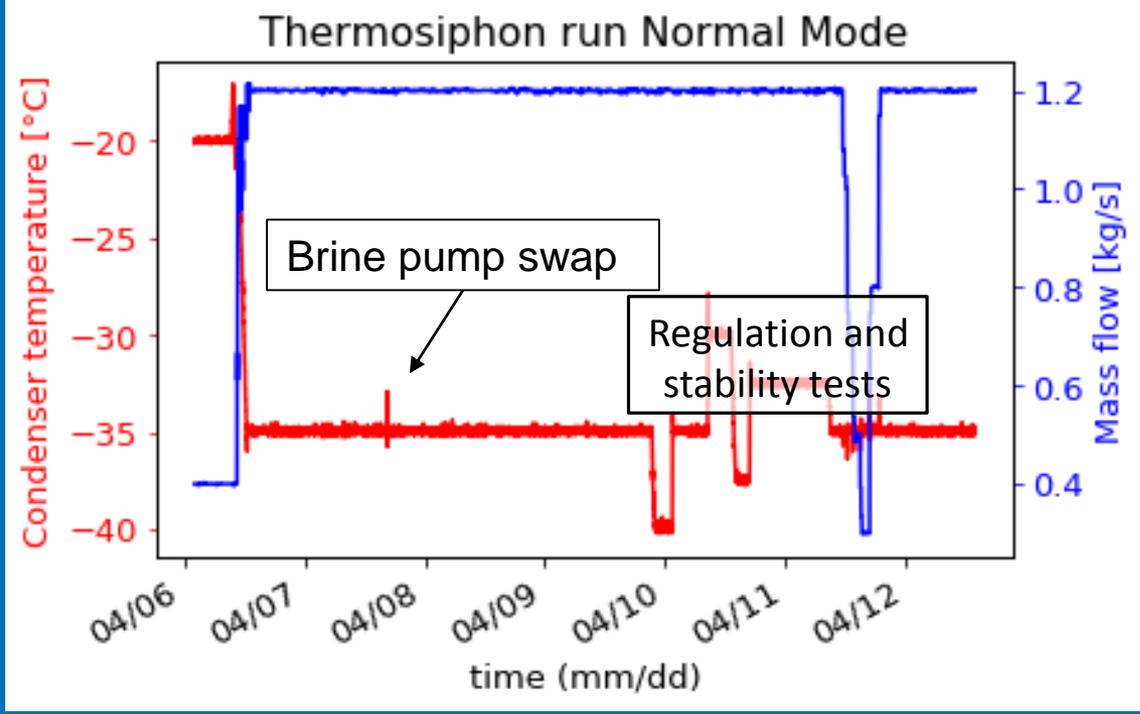
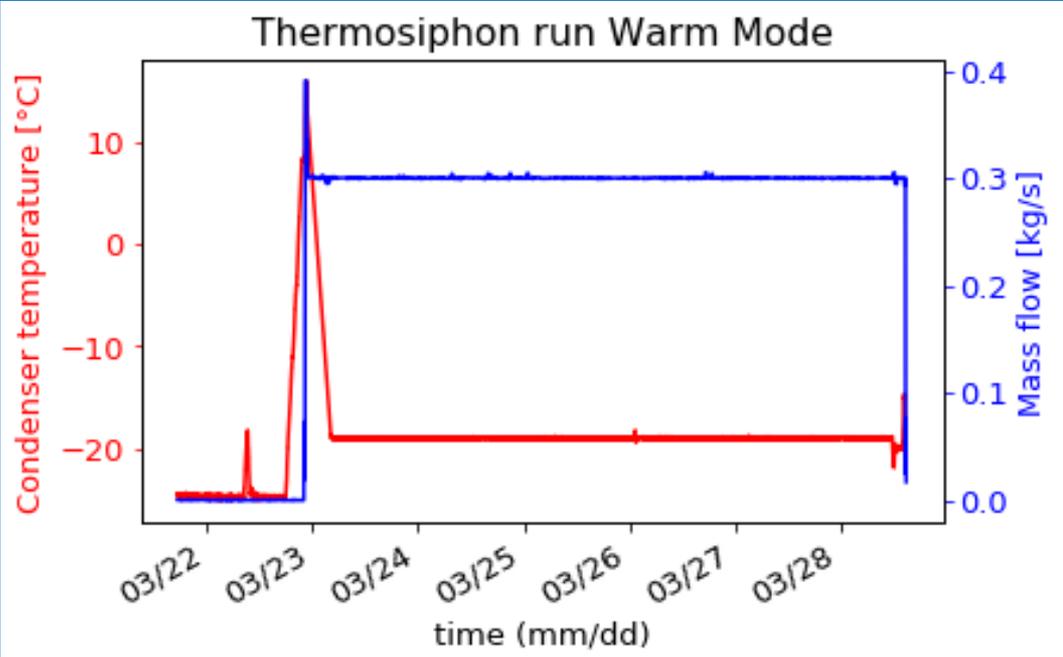


From Martin Doubek

On dummy load - Connection valves closed

Run at warm and normal mode:

The stability of the system is verified



EDMS 1791134

## Tests with dummy load

### Results:

- It takes approx. 24 hours to start the Thermosiphon from stand still (empty liquid pipes)
- The thermosiphon can match the parameters of the current compressor plant ( $C_3F_8$  mass flow 1.2 kg/s, vapor pressure  $\sim 1.3$  bar<sub>a</sub> and liquid pressure  $\sim 15$  bar<sub>a</sub> at compressor room level)
- Up to 20-day long run have been carried out, proving that stable circulation and pressure can be maintained through the dummy load
- During commissioning it was also proven that TS can run as low as 0.4 bar<sub>a</sub> in the condenser at full mass flow of 1.2 kg/s

Satisfying results of the dummy load tests  
(stable operation, comparative cooling performance of  
compressor system)



Swap tests

During the swap tests (18.04.17 – 24.04.17) the external part  
of the evaporative cooling system (7 // compressors) was  
replaced by the thermosiphon



Thermosiphon was the primary cooling system for ID



Several swap tests between the two systems

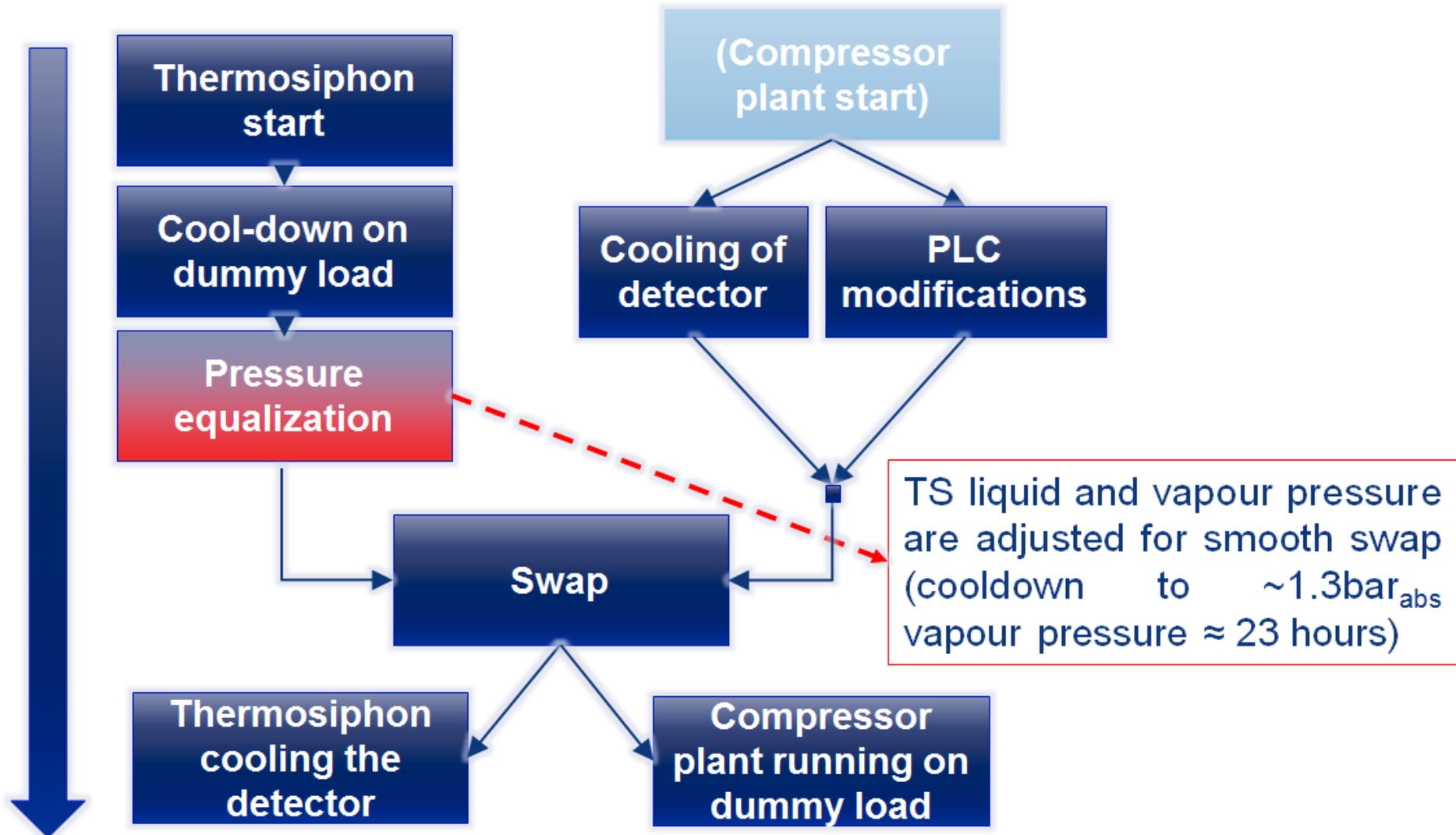
# Swap tests

## Aim:

- Validate swap between compressor plant and Thermosiphon (back and forth)
- Optimize some Thermosiphon set points for the detector cooling
- Evaluate various pressures (delivered liquid...) and pressure drops (vapor return, liquid line...)
- Maintain stable cooling of the detector for few days.

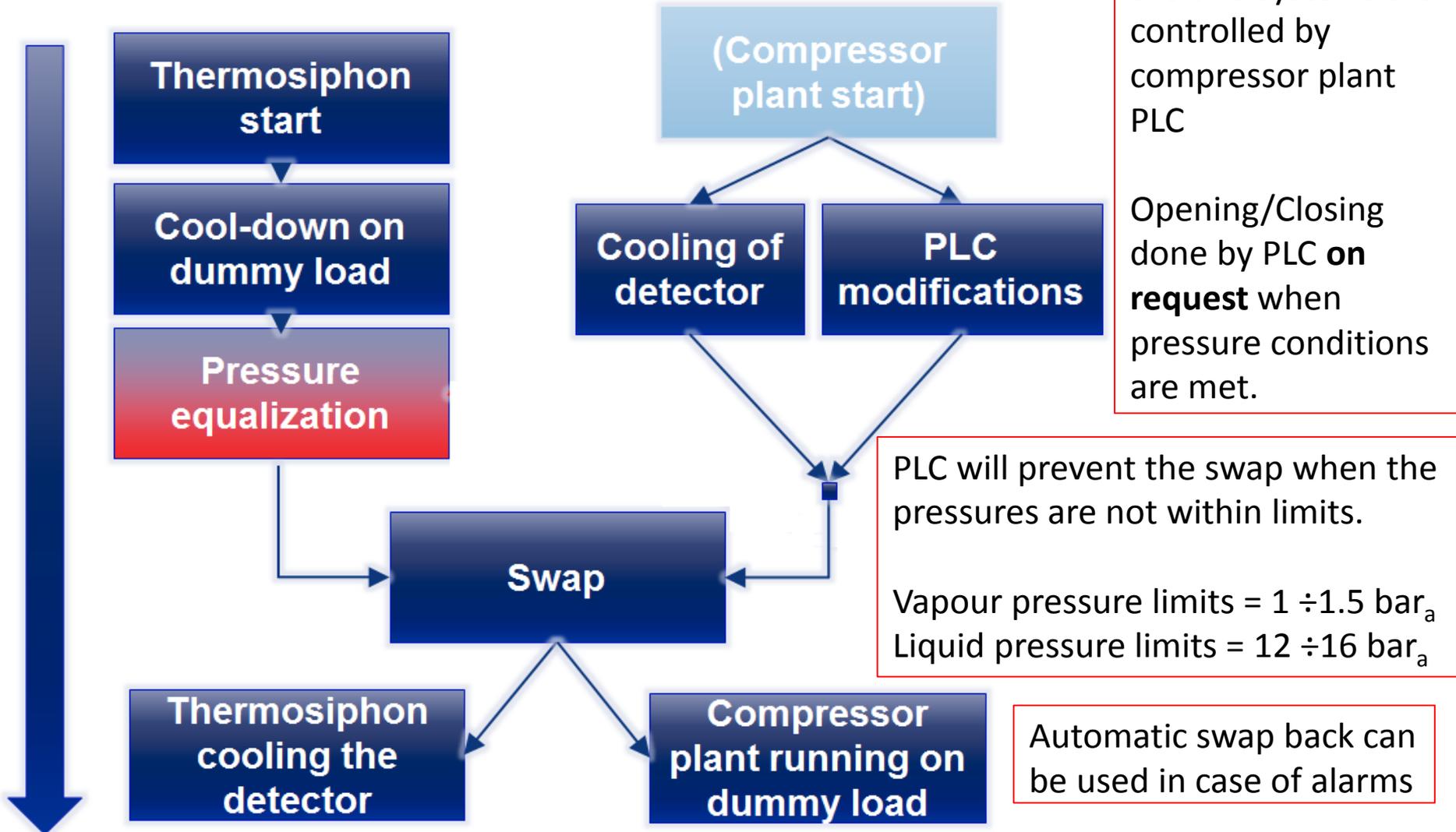
# Swap tests

## Swap procedure flow chart



# Swap tests

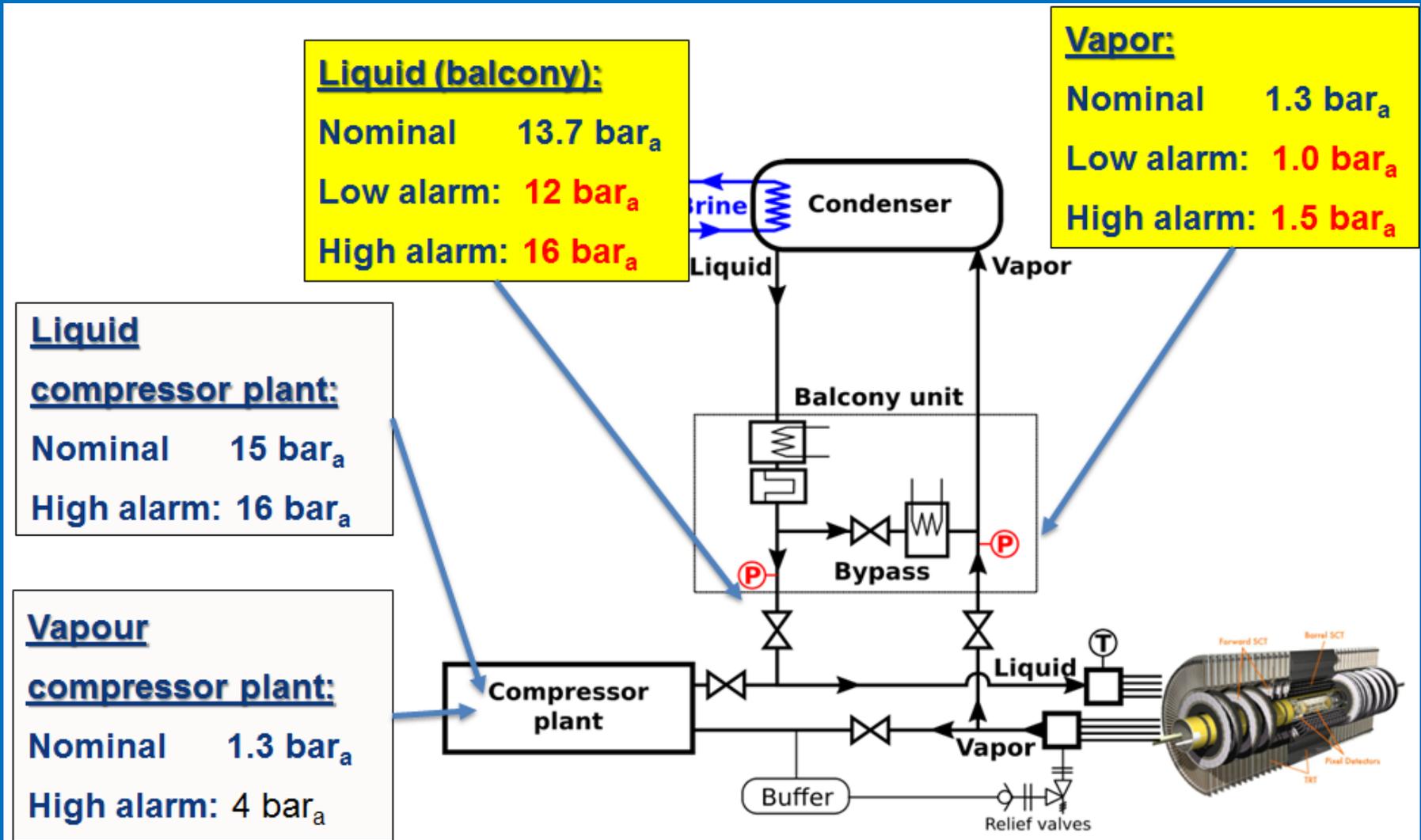
## Swap procedure flow chart



# Swap tests

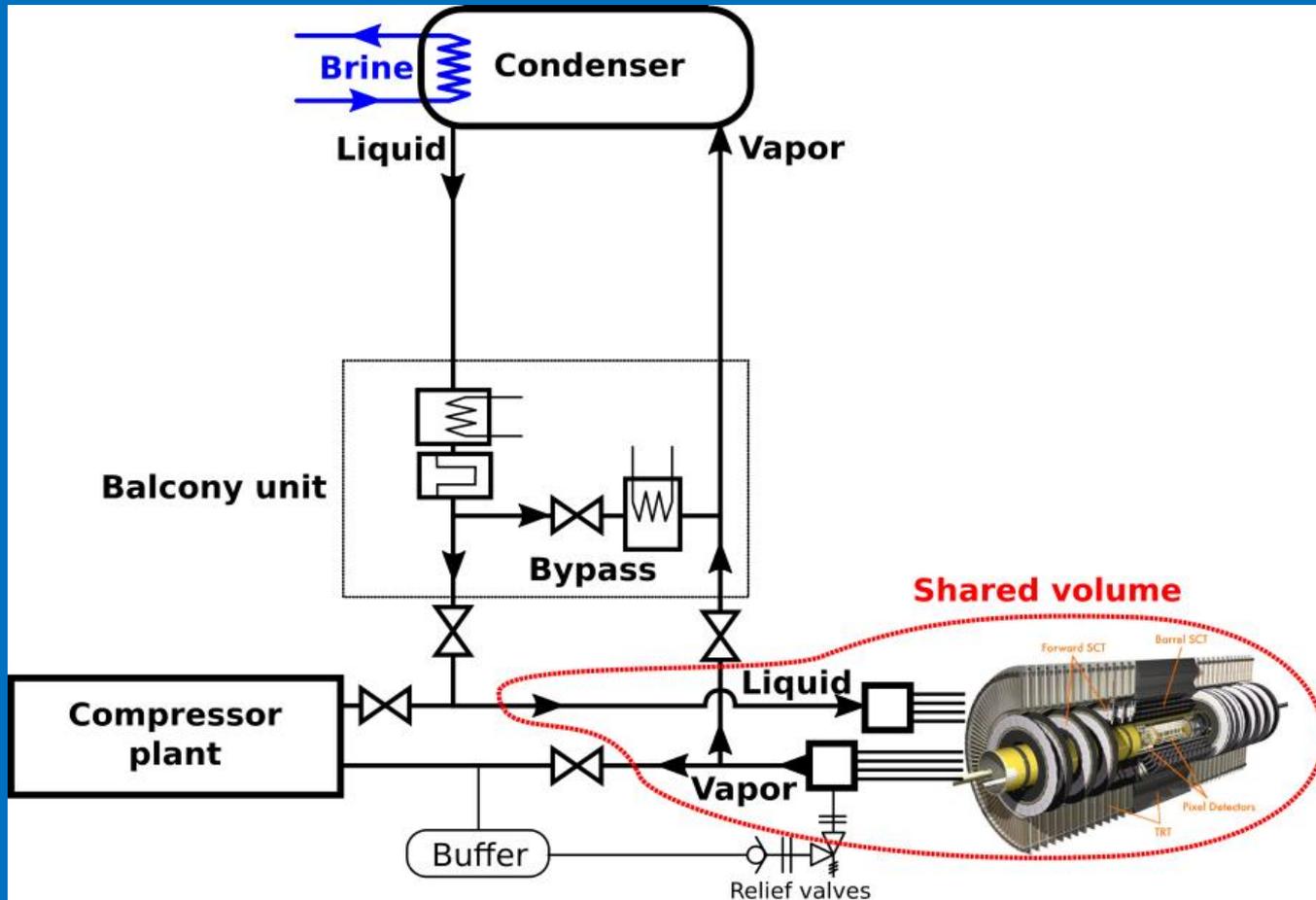
## Alarms:

Dedicated pressure alarms are installed in the balcony unit and connected to the compressor plant PLC which controls all the valves involved in the swap.



# Swap tests

Buffer:



The 8 m<sup>3</sup> vapour expansion tank will be permanently connected to compressor plant only, ready at 1.3 bar<sub>a</sub> to take care of the vapour in case of problems. (TS vapour volume = 7 m<sup>3</sup>)

# Swap tests

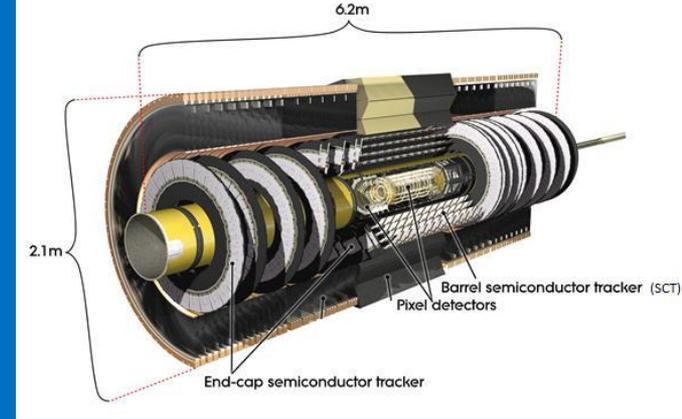
Tests:

## Cooling steps:

1) “Dry” swaps	- all detector loops closed	0.00 kg/s
2) “33%” swaps	- SCT END-CAPS only	0.34 kg/s
3) “70%” swaps	- SCT (END-CAPS + BARREL)	0.74 kg/s
4) “100%” swaps	- SCT + PIXEL	1.03 kg/s

Mass flow increased while involving different cooling loops.

Nominal pressure kept in all the tests



## Normal conditions:

Compressor room level:

Vapour pressure 1.3 bar<sub>a</sub>

Liquid pressure 13.7 – 15.7 bar<sub>a</sub>

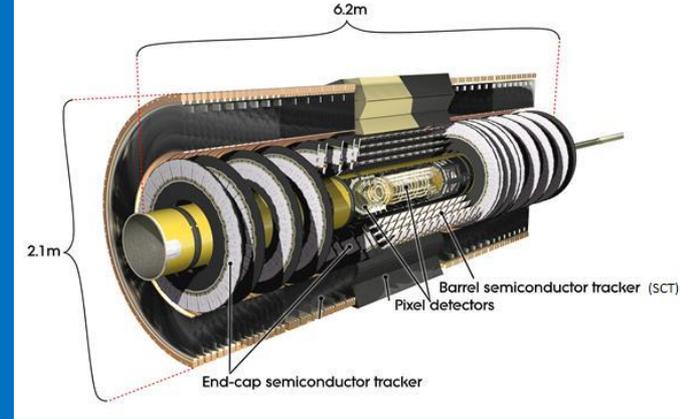
Liquid temperature 20 °C

C<sub>3</sub>F<sub>8</sub> mass flow 1.15 kg/s

Condenser Temperature ≈ -40 °C

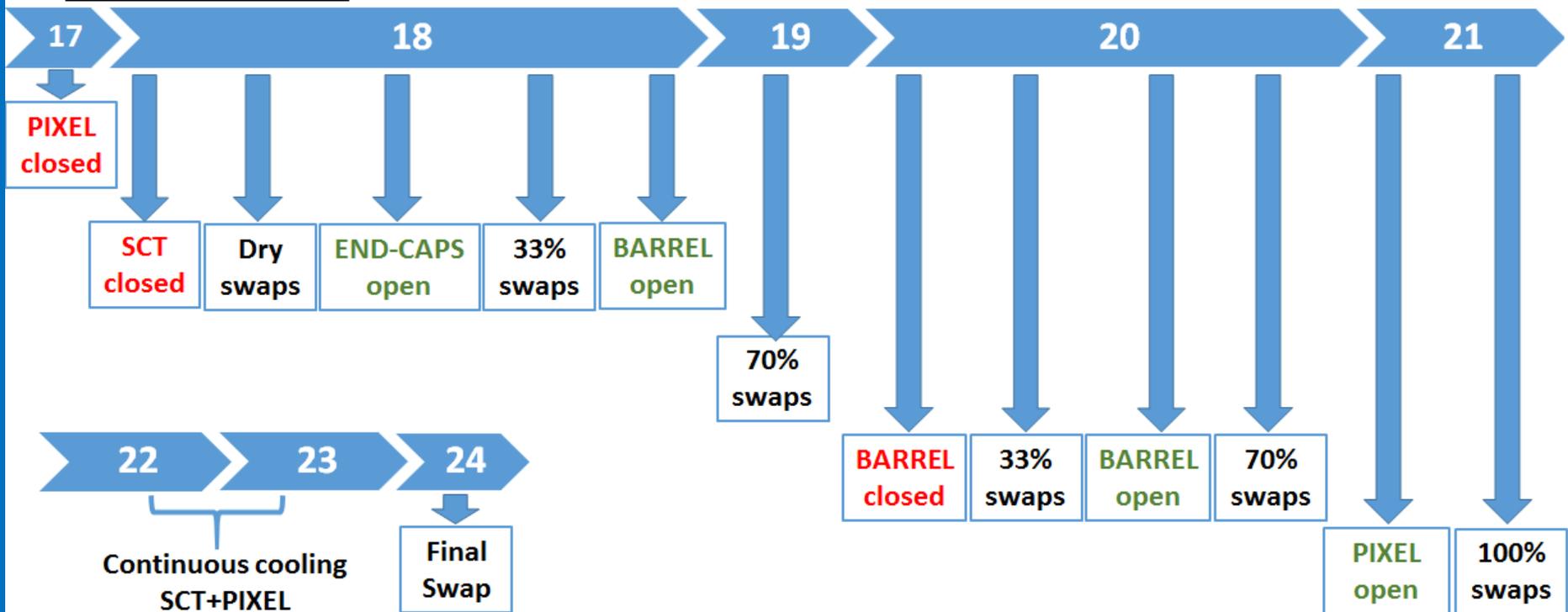
# Swap tests

DRY	3 swaps
SCT END CAPS	3 swaps
SCT (EC + Barrel)	6 swaps
SCT+ PIXEL	3 swaps



From EDMS N. 1801926

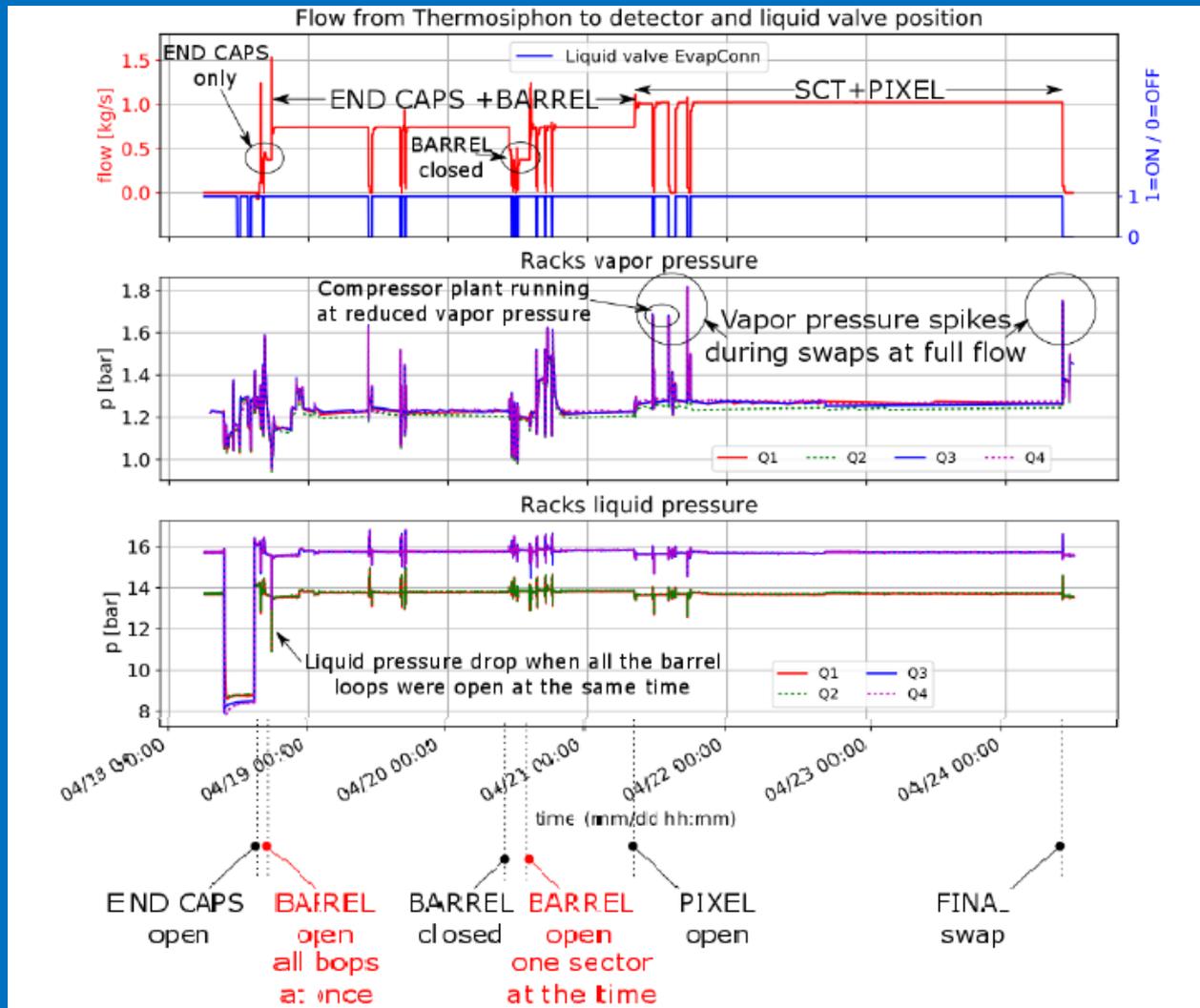
## Tests execution



# Swap tests

## Results:

- ✓ Liquid and vapour pressure measured at balcony level were stable



# Swap tests

## Results:

- ✓ Vapour and liquid pressure in the distribution rack delivered by TS very close to the nominal pressure of the compressor plant

Table 4 - Distribution racks pressures				
	Q1	Q2	Q3	Q4
Compressor plant (SCT+PIXEL)				
Liquid pressures [bar <sub>a</sub> ]	13.55	13.57	15.56	15.56
Vapour pressures [bar <sub>a</sub> ]	1.44	1.43	1.44	1.44
Thermosiphon (SCT+PIXEL)				
Liquid pressures [bar <sub>a</sub> ]	13.72	13.75	15.71	15.71
Vapour pressures [bar <sub>a</sub> ]	1.26	1.25	1.26	1.28

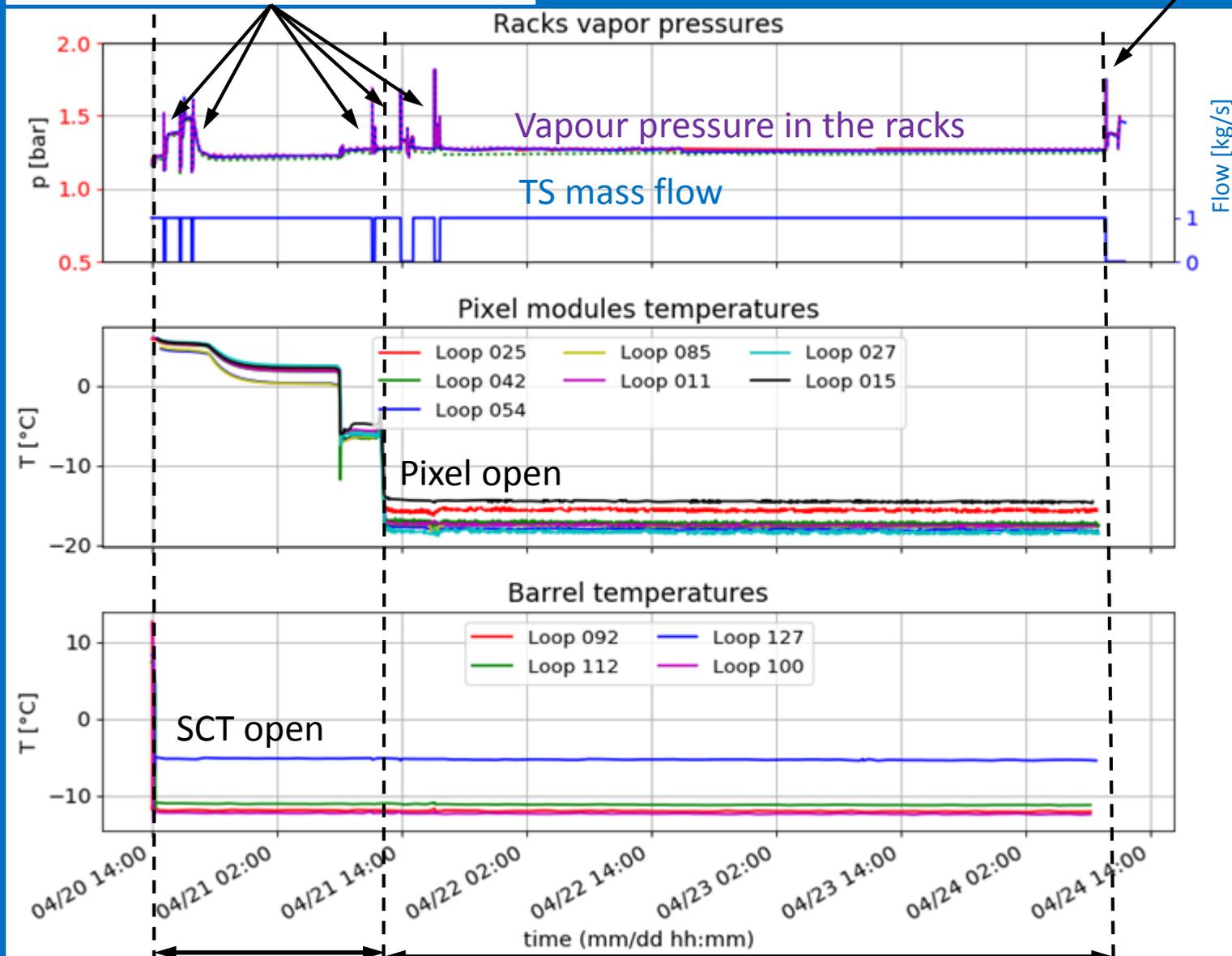
## Swap tests

### Results:

- ✓ Detector module temperature remained stable during the swaps (max fluctuation of temperature approximately 2-3 °C with the lowest back pressure settings)

Test swaps between TS and compressor plant

Final swap back to compressor plant



Stable cooling of SCT

Stable cooling of SCT+Pixel

## Swap tests

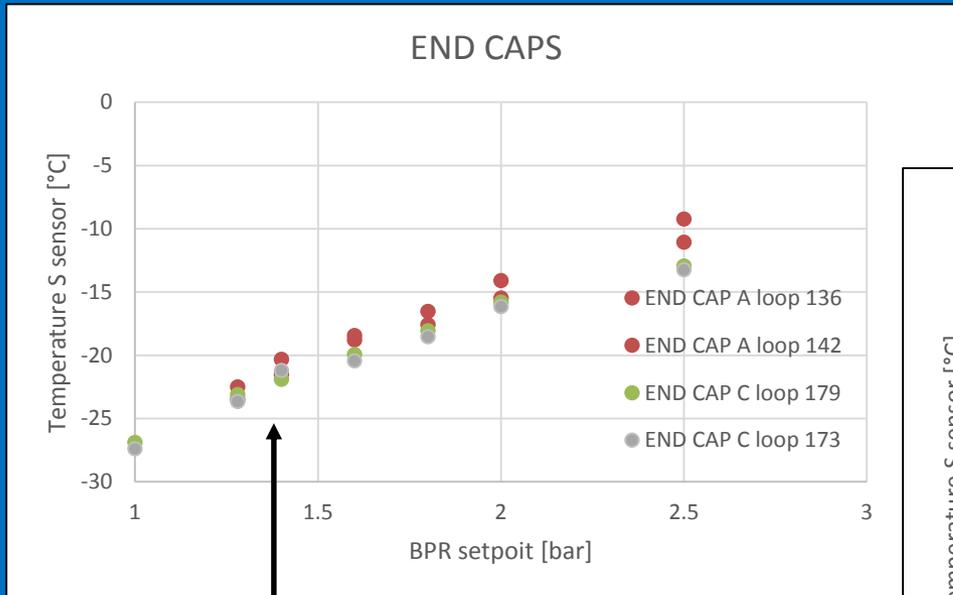
### Results:

- ✓ Liquid and vapour pressure measured at the balcony level were stable
- ✓ Vapour and liquid pressure in the distribution rack delivered by TS very close to nominal pressure of compressor plant
- ✓ Detector module temperature remained stable during the swaps (max fluctuation of temperature approximately 2-3 °C)
- ✓ TS had been continuously cooling the Inner Detector
- ✓ The Inner Detector temperature was stable

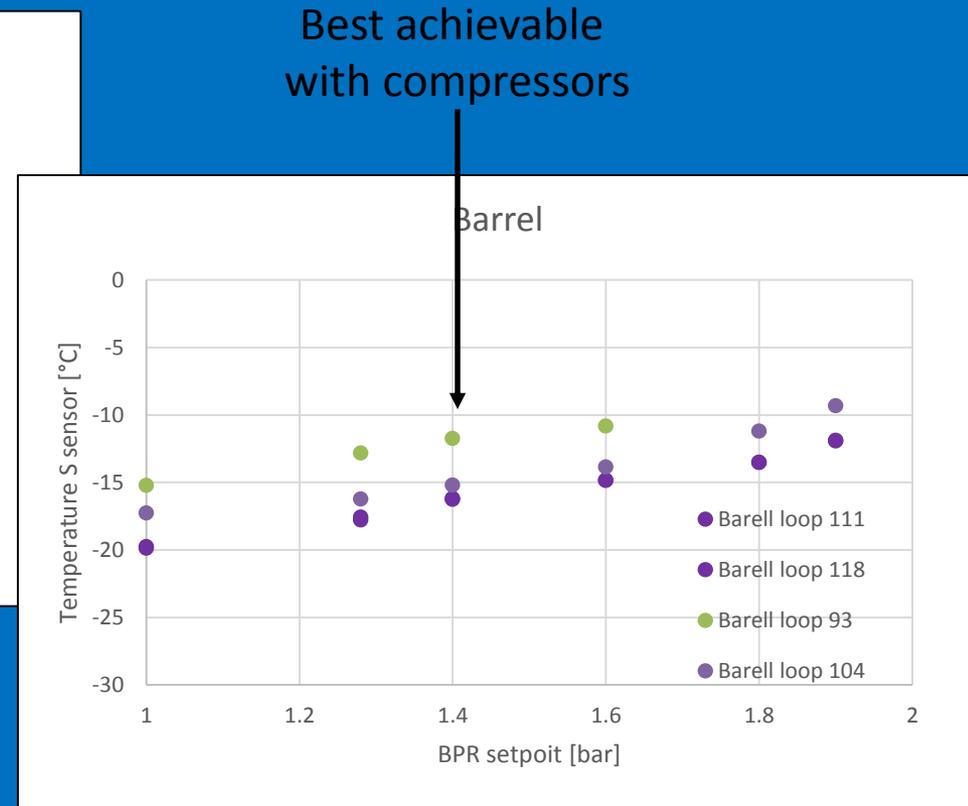
## Conclusion and What's next

- Transient occurring during the swaps are safely within alarm limits → automatic swap can be implemented
- New condenser is approved and will be produce by the December 2017 → new more reliable design, subcooling power doubled to shorten the ramp down, levelmeter added

# Latest TS runs (July 3 2017: exploiting thermosiphon « headroom » by further reducing pressure (in SCT endcap and barrel cooling circuits: preliminary)



Best achievable with compressors



Best achievable with compressors

BPR at 1 bar<sub>a</sub> - 27 °C in SCT end-cap, -20 °C in SCT barrel

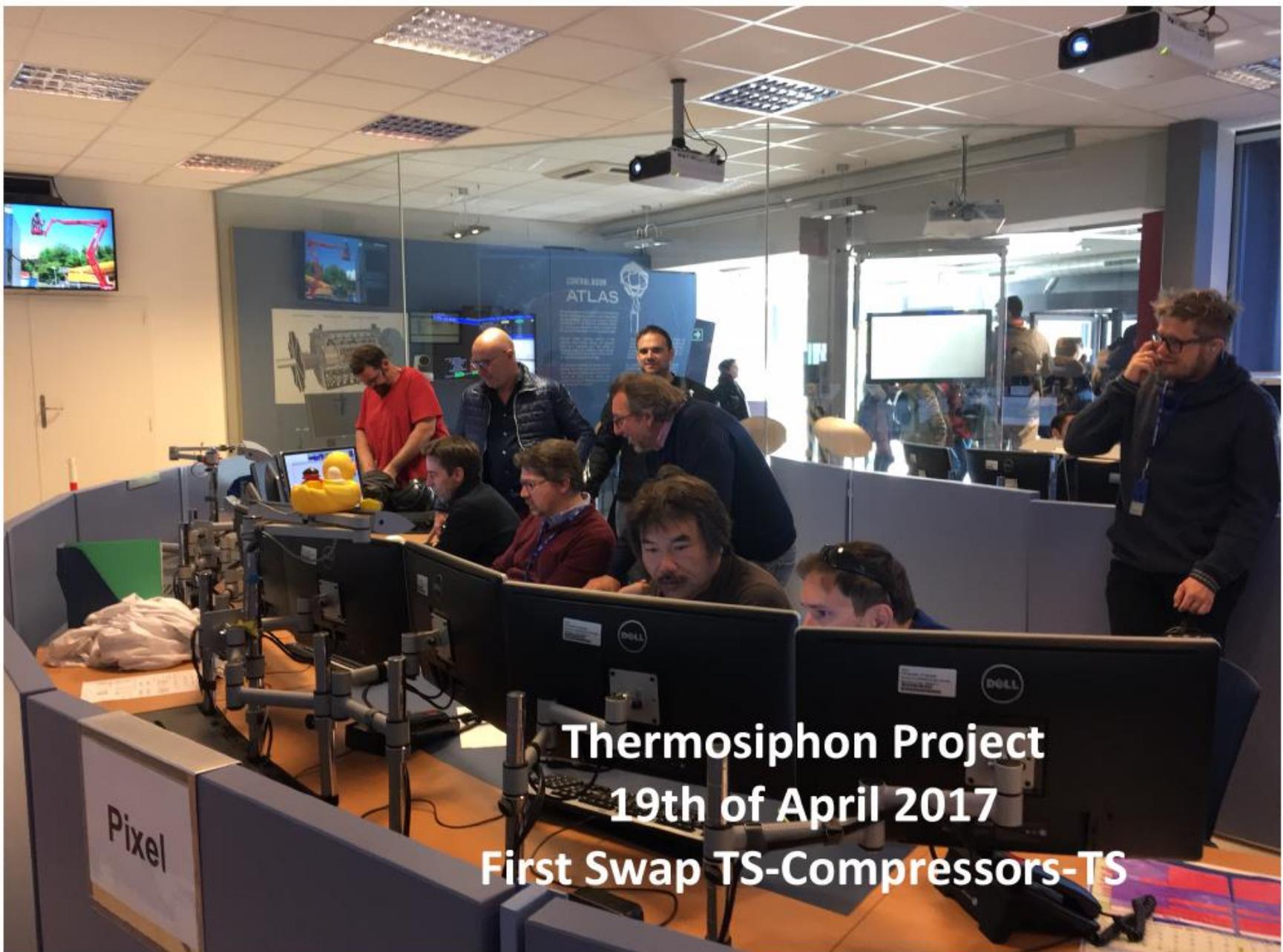
Present limitation is the minimal back pressure setting on the dome-loaded back pressure regulators: will need a sub-atmospheric dome pressure system to run lower with C<sub>3</sub>F<sub>8</sub>, but C<sub>2</sub>F<sub>6</sub>/ C<sub>3</sub>F<sub>8</sub> blends would not require this

## Conclusion and What's next

- 3/7/17 low vapour pressure tests (below 1 bar) to verify the minimum temperature reachable with TS. The first results highlight that we can gain 8 °C on Barrel modules and 13 °C on End-caps ones.
- C<sub>3</sub>F<sub>8</sub> / C<sub>2</sub>F<sub>6</sub> blends can offer further temperature reductions (~9° C) in the present through-detector and on-detector services – see talk by G. Hallewell

Thank you for you attention

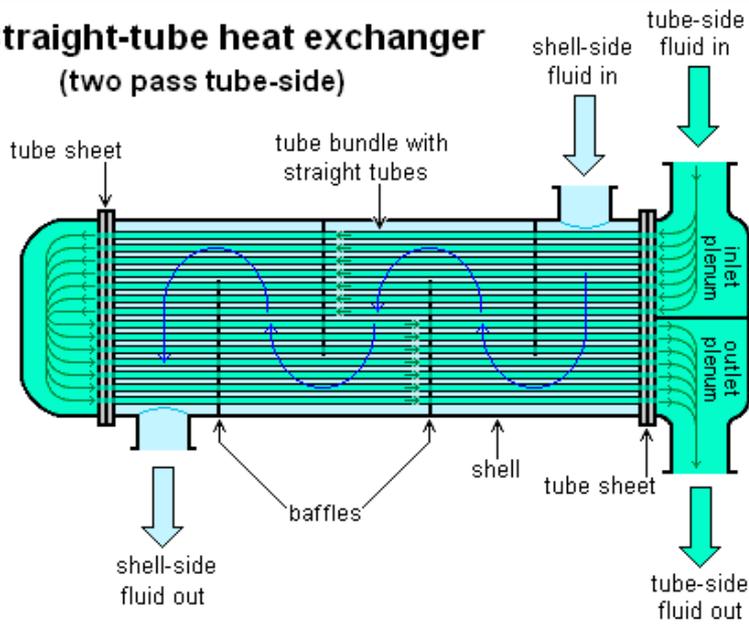
[cecilia.rossi@cern.ch](mailto:cecilia.rossi@cern.ch)



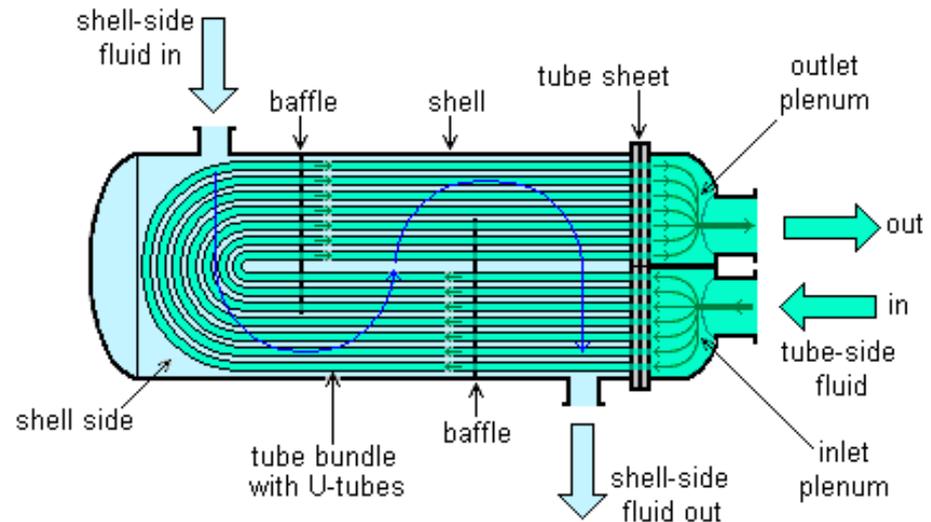
**Thermosiphon Project**  
**19th of April 2017**  
**First Swap TS-Compressors-TS**

# New condenser: modification of the mechanical design

**Straight-tube heat exchanger  
(two pass tube-side)**



**U-tube heat exchanger**



- Reduction of number of welds (1110 -> 370)
- Reduction of thermal stress

# Swap tests

## Results:

- ✓ Liquid and vapour pressure measured at balcony level were stable

