

# Test of a Submersible Liquid Helium Transfer Pump [C1Po1A-08]

Steffen Klöppel<sup>1</sup>, Nico Steinert<sup>2</sup>, Niklas Faust<sup>1</sup>, Thomas Funke<sup>1</sup>, Christoph Haberstroh<sup>1</sup>

<sup>1</sup>Technische Universität Dresden, <sup>2</sup>maxon motor ag

<sup>1</sup>steffen.kloeppe@tu-dresden.de, <sup>2</sup>nico.steinert@maxonmotor.com

## Introduction

- Transfer by pressurization is inefficient and slow
- A transfer pump was developed and tested
- This poster shows the test setup and first results

## Advantages of the pump

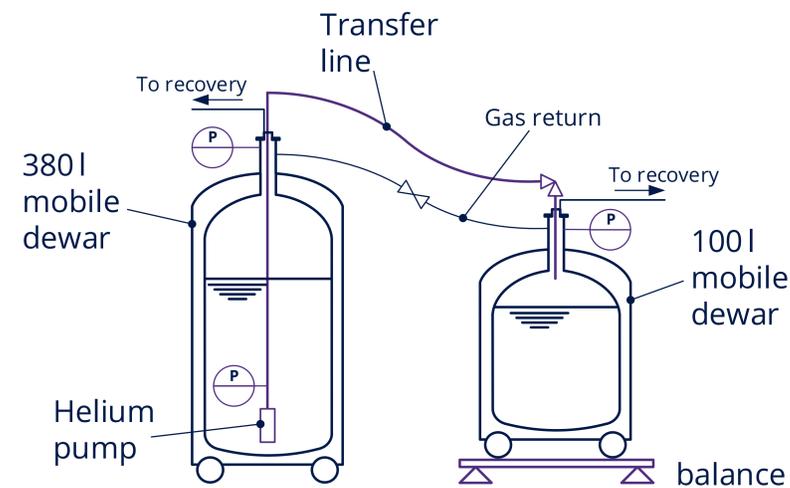
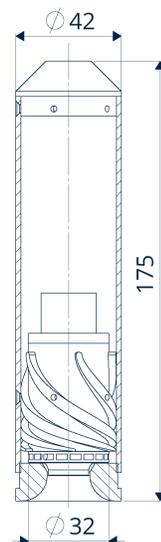
- Transfer losses by pressurization are up to 30% of transferred volume
  - With a pump, this value can be decreased below 2% [1]
- This presents the highest possible efficiency increase, more than optimization of compressor, turbines, HXs, etc.
- Considerably higher filling rates can be achieved

## Pump design

- Submersible design, short shaft, no rotating seal
- Centrifugal impeller, axial stator
- Design for 40g/s and 350mbar
- Design speed 16000rpm
- Shrouded impeller was additively manufactured
- Adjustment of axial clearance by threaded intake trumpet

## Electric motor

- Pump is driven by a maxon EC-4pole22 brushless DC-motor
- Special dry running bearings for operation without lubricants
- Originally designed for extended operation down to 77K
- Sensorless operation without any electronics in the cold environment



## Test set-up

To assess performance data, a transfer set-up between two mobile dewars was established.

The pump is mounted at the lower end of the riser of a purpose-built single-flow transfer line with ID 16mm (of flexible part).

Both dewars are connected to the recovery system on individual inlets.

A gas return ensures that the pressure of the starting dewar remains above atmospheric, while a valve prevents runaway of the pressure in the system.

Dewar pressures are measured at the top flanges with transducers with a total error of  $\pm 4$ mbar. Static pressure at pump outlet was measured via a capillary with a warm transducer with a total error of  $\pm 8$ mbar.

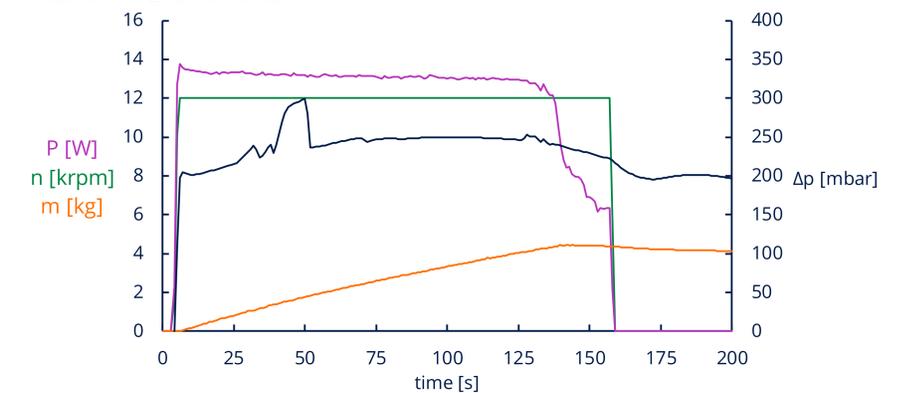
The transferred mass is recorded with a digital balance with a total error of  $\pm 15$ g

The temperature of the cold gas leaving the receiving dewar was estimated to 8K. This unknown parameter gives the highest uncertainty in the measurement.

## Lifetime test

The motor was run in LN<sub>2</sub> continuously for 14 days to verify the lifetime of the bearings under no-load conditions. No signs of degradation were found. This timespan equals transfer of 400,000l of LHe, or several years of filling operations.

Test run in LHe 19/06/03



## Results

Flow rates of 40g/s against a pressure of 200mbar were achieved. For this, the electric power of 13W was required. Consequently, less than 2% of the transferred helium were evaporated by the electric power input.

The backpressure is driven by the pressure drop of the warm gas in the recovery system.

## Outlook

- Procurement of a double-flow transfer line is ongoing, allowing to take measurements at low backpressures
- Optimization of the double-flow transfer lines will allow filling operation with minimal losses
- Emphasis is given on reducing the thermal mass of the transfer line
- Large cross-sections allow to redesign the pump for lower speeds

## Literature

[1] Berndt H, Doll and Wiedemann W: *Two Years' Experience in Liquid Helium Transfer with a Maintenance Free Centrifugal Pump Advances in Cryogenic Engineering Vol 35 1039-43*