Dynamic simulations of Phase-2 detector cooling systems

Context

Past, present and future of Silicon detector cooling

- Silicon detector cooling is hard
	- Low material budget
	- Low temperatures
	- Low thermal gradients
	- Many parallel lines
- CO2 as a working fluid
	- Large latent heat
	- Low pressure drop
	- (and more resistant to it)
	- Small tubes

Two-Phase Accumulator Controlled Loops (2PACL)

Present

• CMS and ATLAS working towards Phase-2 upgrades

- Phase 2 detector cooling:
	- More (**8x** plants for CMS, **6x** for ATLAS)
	- Larger (up to **70 kW** per plant)
	- Colder (**-45°C** on the Accumulator)
	- Longer (**15-**year lifetime)

• Design changes to 2PACL needed

- Impossible to keep all the refrigerant needed underground
	- Large amount of CO2 for detector heat loads (up to 1000 kg per system)
	- Stored Energy = Pressure × **Volume** → Large volumes = safety concern
	- Integration constraints
- Smaller accumulators \rightarrow change in system startup
- Store excess CO2 on surface → Surface storage
- Surface storage pressure limit → Back pressure regulator
- Many parallel plants \rightarrow Spare plant (always running)

Simulations: help understand new systems

2PACL system design

How 2PACL systems used to work, and how they will in the future

New design aspects

Simulation tool

The tool

- Component library in EcosimPro for modelling/simulating detector cooling systems
- Expands on Cryolib (by CERN Cryo)
- Validated against 3 sets of measured data (3 different systems)
- Startup, shutdown, step changes…

Heat Pump Cycles 2PACL Cycles 2PACL Cycles

The validations

V. Bhanot, R. Dhumane, P. Petagna, A. Cioncolini, H. Iacovides, J. Ling, V. Aute, **Development of a Numerical Tool for Dynamic Simulations of Two-Phase Cooling Systems**, Int. j. Simul. Model. 18 (2019) 302–313. https://doi.org/10.2507/IJSIMM18(2)476.

Bhanot, Viren; Petagna, Paolo; Cioncolini, Andrea; Ling, Jiazhen; and Aute, Vikrant, "**Modelling and Simulation of a Flash Tank Vapour Injection Heat Pump in Several Platforms**" (2021). International Refrigeration and Air Conditioning Conference, Purdue, Paper 2170

emper

(d) Pump Mass Flow Rate 1000 2000 3000 4000 5000 6000 $Time(s)$

Bhanot, P. Petagna, A. Cioncolini, H. Iacovides, **Development and validation of a simulation tool for next generation detector cooling systems**, Nuclear Instruments and Methods in Physics Research Section A: Accelerators, Spectrometers, Detectors and Associated Equipment. 955 (2020) 163264. https://doi.org/10.1016/j.nima.2019.163264. 14

New 2PACL simulations

Startup, set-point change, power-cycle

- The problem of startup:
	- Diaphragm pumps cannot pump vapour → liquefy refrigerant at pump inlet
	- Detectors hate thermal shocks \rightarrow change temperature gradually
- CO2 during off-period:
	- Two-phase state (undefined exactly)
	- Fluid pressure corresponds to ambient temperature
- Existing system startup:
	- Pressurise whole system by Accumulator
	- Liquefy detector and pump inlet together

Enthalpy

Thome, John R., ed. *Encyclopedia Of Two-phase Heat Transfer And Flow Iv: Modeling Methodologies, Boiling Of Co2, And Micro-two-phase Cooling (A 4-volume Set)*. World Scientific Publishing, 2018. 16

Accumulators are now not big enough to pressurise the whole system

- Stage 1: Liquefy pump inlet
	- Allow pump start
	- Plant acts as 'actuator' for Accumulator
- Stage 2: Liquefy detector
	- Prevent thermal shock
	- Accumulator controls pump flow to detector
	- Pressurisation via back pressure regulator
- Stage 3: Cooldown and power-on

• CMS TK1 modelled *(kind of)* Simulation Model

• DTL and MTL models: single long line with cumulative volume

- Poor detector mechanics model
	- Parallel lines not modelled
	- Single long line
	- Goal is to study CO2 side initially,

Plant Startup

(plant is just an 'actuator' for the Accumulator)

- Step 0: Safety position
- Keep surface storage disconnected
- Keep everything else open
	- avoid liquid traps
	- everything at the same pressure

• Step 1: Equalise pressure

- Open plant to surface storage
	- Start from a defined state
- Surface storage will act as Accumulator

• Step 2: Liquefy pump inlet

- Turn on coldbox cooling
	- Condenser
	- Pump inlet
- We obtain subcooled liquid at pump inlet
- Ready to start circulation

• Step 3: Turn on pump

- Not yet ready to send to detector!
- Circulate locally
- Get stable flow, subcool at pump inlet

• Step 4: Supply liquid

- Send liquid towards Accumulator
- Slowly steal from local bypass
- Surface storage valves ready for level control
- Pump module has done its job

Accumulator startup

(Goal is to liquefy detector and then cool it down)

- Step 1: Request flow
- Accumulator waits patiently for flow
- Empty the accumulator
	- Otherwise, two "accumulators" fighting for control
- Set up bypass flow

- Step 2: Pressurise detector
- Throttle flow using back pressure regulator
- Trickle-flow liquid towards detector
- Slowly subcool detector

- Step 3: Detector circulation
- Safe to start circulating through detector
- Close TL bypass valve
- Detector flow control valve now regulates (Valve c)

- Step 4: Accumulator control
- Time to fill up the Accumulator
- Surface storage valves fill up the vessel

- Step 5: Detector cooldown
- Detector is liquid
	- No danger of thermal shock
- Accumulator is regulating
- ∴ we are ready to cool down
- Pre -vapourisation heating may be turned on now
	- Level control brings back Accumulator level

- Step 6: Detector power allow
- All done from CO2 side
- Detectors can turn on power when they like

Initial:

Fully liquid transfer line

Power-on:

Vapour travels faster than liquid Pump is constant volumetric flow rate Liquid displaced into accumulator

Detector power-off

- Accumulator cannot take us all the way there
- Accumulator pressure must stay *below* surface storage pressure
	- Otherwise, how do we send refrigerant down?
- Back pressure regulator has to do the rest of the job
- Safety concern: If BPR fails, we fall immediately to Accumulator pressure
- Mitigation: Try to find a surface storage that can operate at high pressure

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- New systems \rightarrow significantly so
- System control is undergoing big changes
- Simulations can help provide answers on Phase-2 system behaviour
- Future work: better detector models, spare plant handover, quick restart mode, virtual commissioning setup, operator training, co-simulation with modelica chiller model…

Accumulator Simulations

Sizing and pre-vapourisation

Initial:

Fully liquid transfer line

At power-on:

Vapour travels faster than liquid Liquid displaced into accumulator

- Parametric simulation on Accumulator volume
	- 10 sizes studied
	- Ranging from 50% to 300% of TL volume
- 70 kW evaporator heat load
	- Turned on after 100 seconds
- 100 m long transfer line
	- Divided into 10 m segments
- 70 g/s of CO2 flow

Accumulator sizing simulation

- 110% of TL return volume
	- Accu just gets full
	- ~120% of TL volume likely sufficient
- Steady-state once vapour front arrives at the Condenser

- Péclet number, Pe = Re.Pr
- Ratio of advection to diffusion
- Convective systems usually have *huge* Peclet numbers
- Downstream parameters have negligible influence on upstream parameters
- Additionally, Diffusion coefficient decreases with lowering temperature and decreases with increasing pressure

